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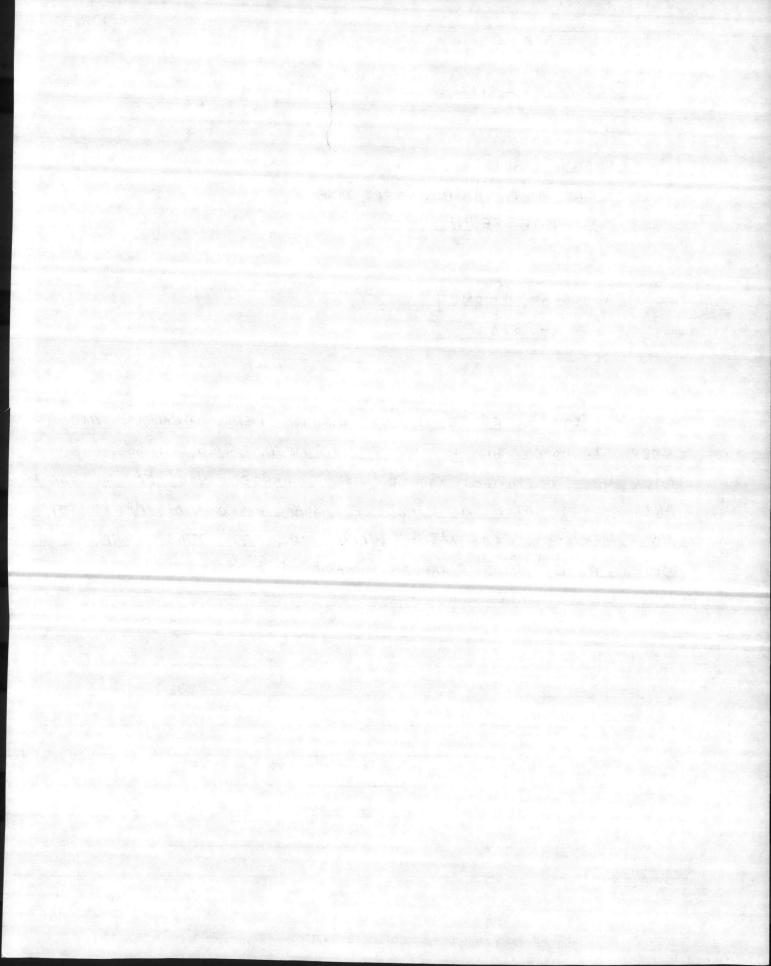
Date: OCTOBER 22, 1992

TO: <u>GARY DAVIS</u> Company: <u>ENV. MGT. MARINE CORPS BASE</u> City/State: <u>CAMP LEJEUNE</u>

From: DOUGLAS MOONEY Job/Project No: _____ R-3873

Comments: YOU MUST BE LIVING RIGHT. TERRY BRADHAM HAD A
COPY. I HOPE THIS IS WANT YOU NEED. CRS Sirrine (new
name for J.E. Sirrine) WOULD HAVE CHARGED YOU TO GO THRU
ARCHIVES TO FIND A COPY. WE HAVE A COMMON PAST BUT
NO WORKING RELATION SHIP WITH CRS AT THIS TIME. I
GUESSED WOULD HAVE YOUR CHANCES WERE 1 in 10.

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Feasibility Study

SOLID WASTE AND WOOD WASTE BURNING AND COGENERATION OPTIONS

MARINE CORPS BASE, CAMP LEJEUNE MARINE CORPS AIR STATION, CHERRY POINT, N.C.

Contract no. N62470-80-B-3801

L'EPARTMENT OF THE NAVY

ATLANTIC DIVISION

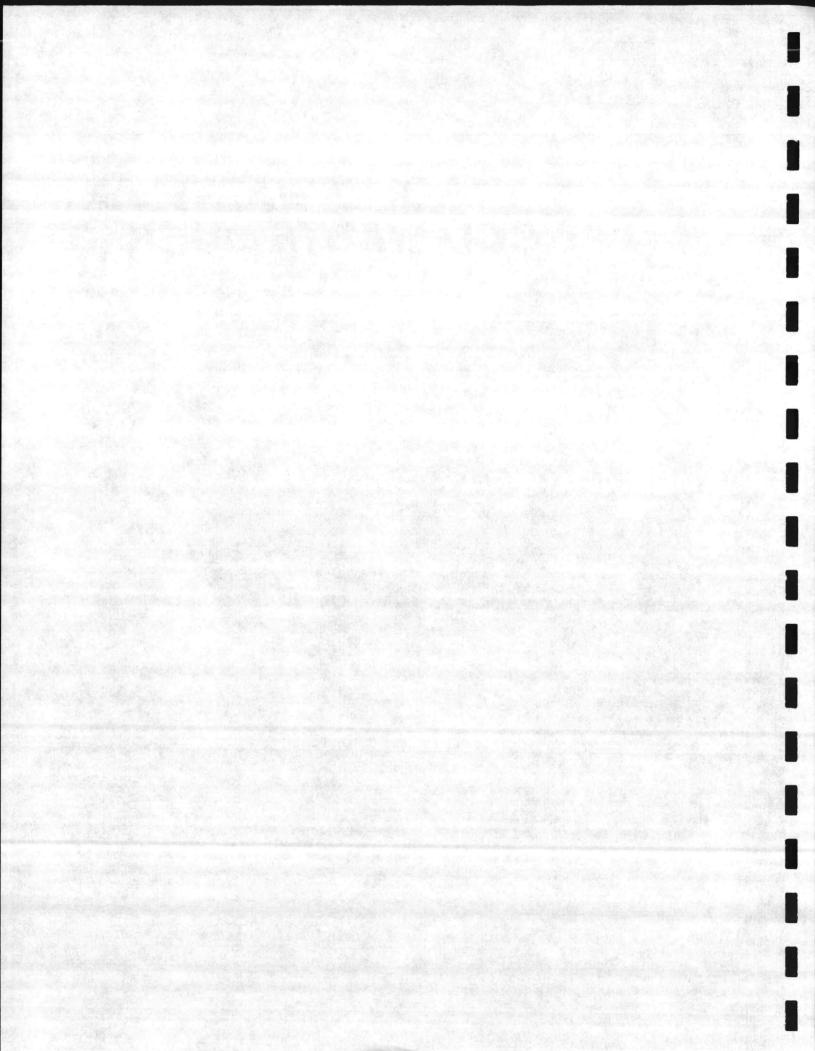
l aval Facilities Engineering Command Norfolk, Virginia

Phase II FINAL REPORT

J. E. SIRRINE COMPANY

A

North Carolina Division Sirrine Job No. R-1628



Environmental

ESTABLISHED 1902



POST OFFICE BOX 12748 RESEARCH TRIANGLE PARK, NORTH CAROLINA 27709 TELEPHONE (919) 541-2081

October 19, 1982

Department of the Navy Commander, Atlantic Division Naval Facilities Engineering Command Norfolk, Virginia 23511

Attention: Mr. J. D. Torma

Subject: Department of the Navy Feasibility Study for Solid Waste and Wastewood Burning and Cogeneration Options MARCORB Camp Lejeune and MCAS Cherry Point, N. C. Contract No. N-62470-80-B-3801 Sirrine Job No. R-1628

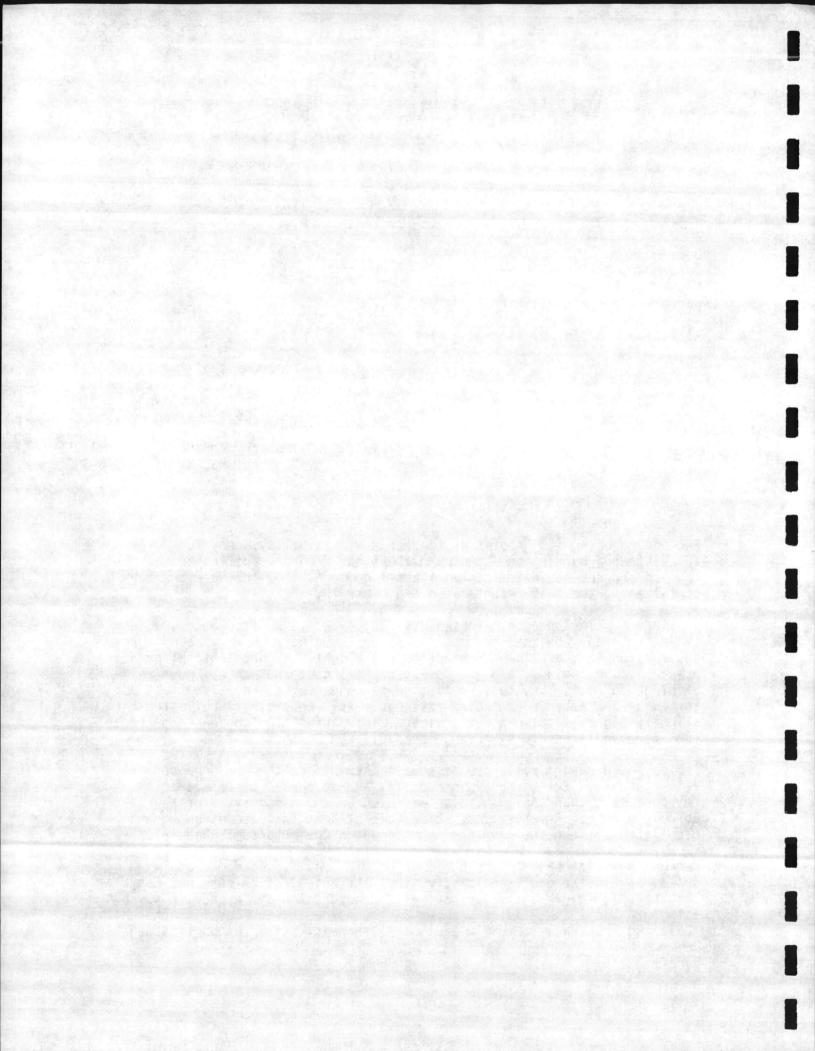
Gentlemen:

Enclosed are ten (10) copies of the revised Feasibility Study for Solid Waste and Wastewood Burning and Cogeneration Options Report. This report has been revised and re-issued to incorporate all comments from the Navy and Navy consultants, the most recent dated September 13, 1982.

In Sirrine's last response (dated July 26, 1982) to Navy comments, we continued to recommend the steam only case for burning refuse. Based on known assumptions at that time, this option was slightly higher in total project present value savings, had the lowest capital cost and had the most reliable maintenance cost. However, in this correspondence, a sensitivity was performed on increased electricity revenues. This sensitivity reflected a slightly higher total project present value savings for cogeneration under the increased electricity revenue scenario.

The enclosed report reflects, as a base assumption, the new proposed CP&L rate schedule, CSP-4, for avoided costs, and increases the electricity revenues more than the 20%, which was used in the sensitivity of the last correspondence. At this time, it appears evident that a contract could be negotiated between the Navy and CP&L based on the proposed Schedule CSP-4.

Because this base assumption has changed, the revised economic analysis shows, as did the past sensitivity, that the cogeneration case now has a slightly higher present value savings. However, the difference in savings between Cases 1 and 2 is only about 2%. Considering the level of the estimate, these two cases are virtually equal. All sensitivities run on this new base



J. E. SIRRINE COMPANY

Department of the Navy Sirrine Job No. R-1628 October 19, 1982 Page Two

assumption still do not make one case any more favorable than the other. A recommendation cannot be made based on these economic factors. Therefore, the Navy must make its decision based on intangible and other policy factors along with other economic factors which might be relevant to the Navy in this situation.

Regardless of which scenario for burning refuse is chosen, both show approximately a \$75 million savings over existing operations through the life of the project. Either case would be a beneficial investment to the Navy.

Yours very truly,

J. E. SIRRINE COMPANY

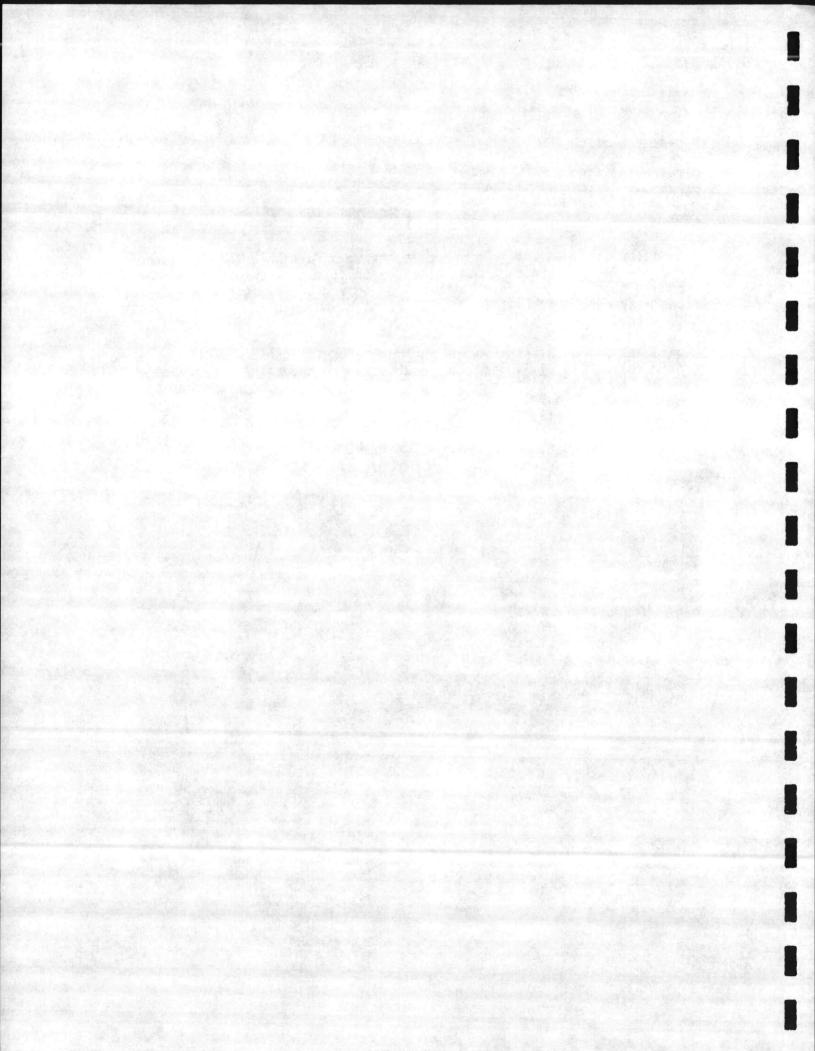
(7) Freeman

G. J. Freeman, P. E.

GJF/jos

Enclosures

cc: Vineta, Inc., w/(1) copy Att: Mr. Heinz A. Gorges Planning, w/(1) copy Environmental, w/(1) copy Power, w/(1) copy Project Manager, w/(1) copy



FEASIBILITY STUDY

SOLID WASTE AND WOOD WASTE BURNING AND COGENERATION OPTIONS

MARINE CORPS BASE, CAMP LEJEUNE MARINE CORPS AIR STATION CHERRY POINT, NORTH CAROLINA

DEPARTMENT OF THE NAVY ATLANTIC DIVISION NAVAL FACILITIES ENGINEERING COMMAND NORFOLK, VIRGINIA

SIRRINE JOB NO. R-1628

REVISED: OCTOBER 19, 1982

J. E. SIRRINE COMPANY P. O. BOX 12748 RESEARCH TRIANGLE PARK, NORTH CAROLINA 27709

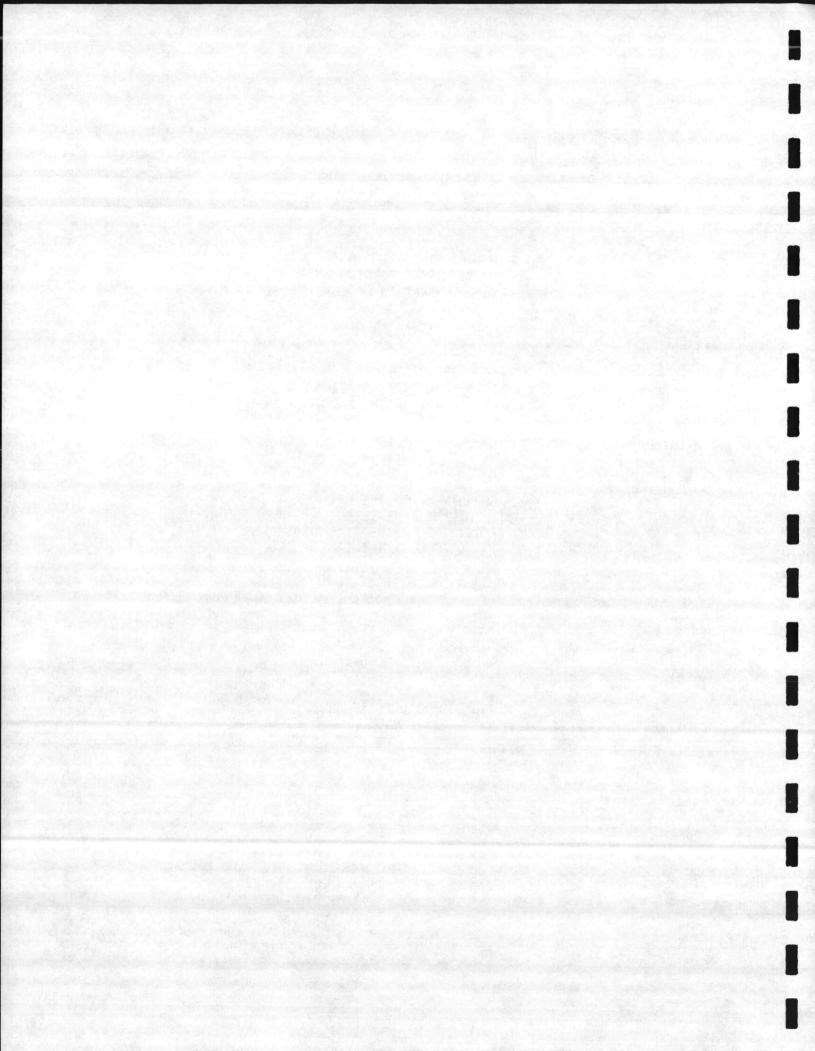


TABLE OF CONTENTS

- I. EXECUTIVE SUMMARY
- II. INTRODUCTION
- III. GENERAL PLANT DESCRIPTION
- IV. COST ESTIMATING & ANALYSIS METHODS

Life Cycle Cost Analysis Capital Costs Operating Costs Base Case Costs

V. CASE 1 - STEAM ONLY

Plant Description Cost Estimates LCC - Computations Analysis

VI. CASE 2 - ELECTRICITY WITH BACK PRESSURE TURBINE

Plant Description Cost Estimates LCC - Computations Analysis

VII. CASE 3 - ELECTRICITY WITH CONDENSING TURBINE

Plant Description Cost Estimates LCC - Computations Analysis

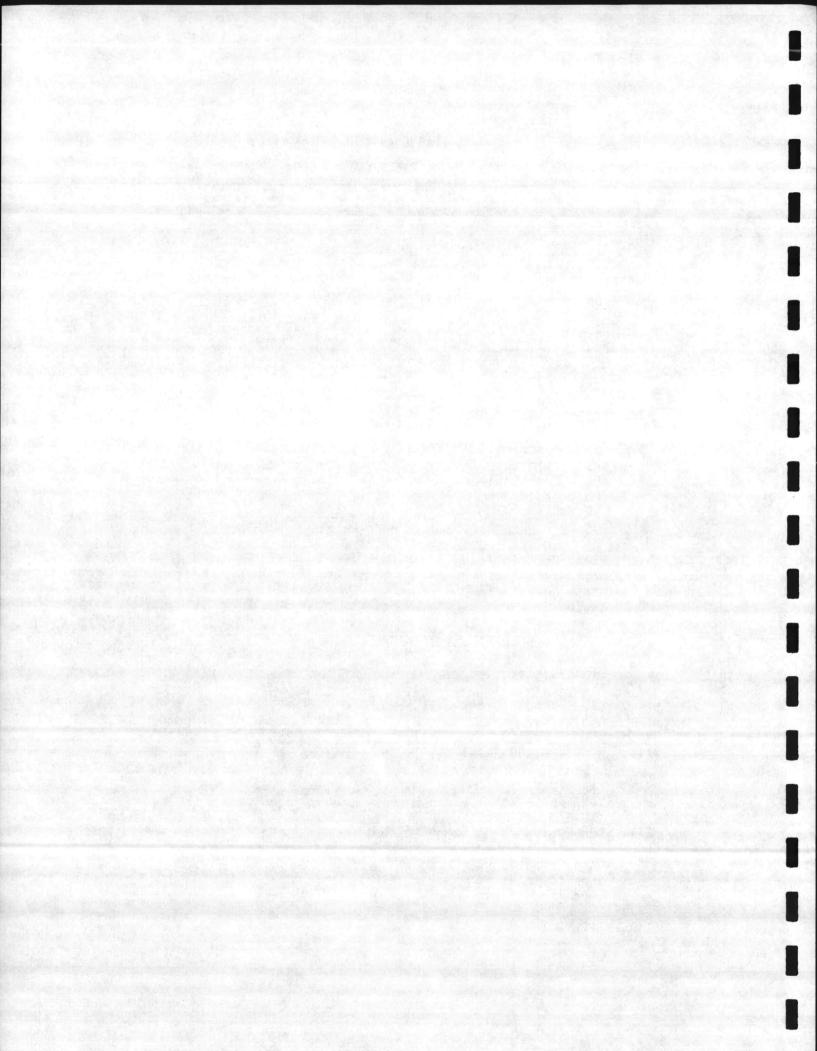
VIII. WOOD - FIRED PLANT

Plant Description Cost Estimate

IX. CONCLUSIONS & RECOMMENDATIONS

Case Comparisons Sensitivities Recommendations

X. APPENDIX



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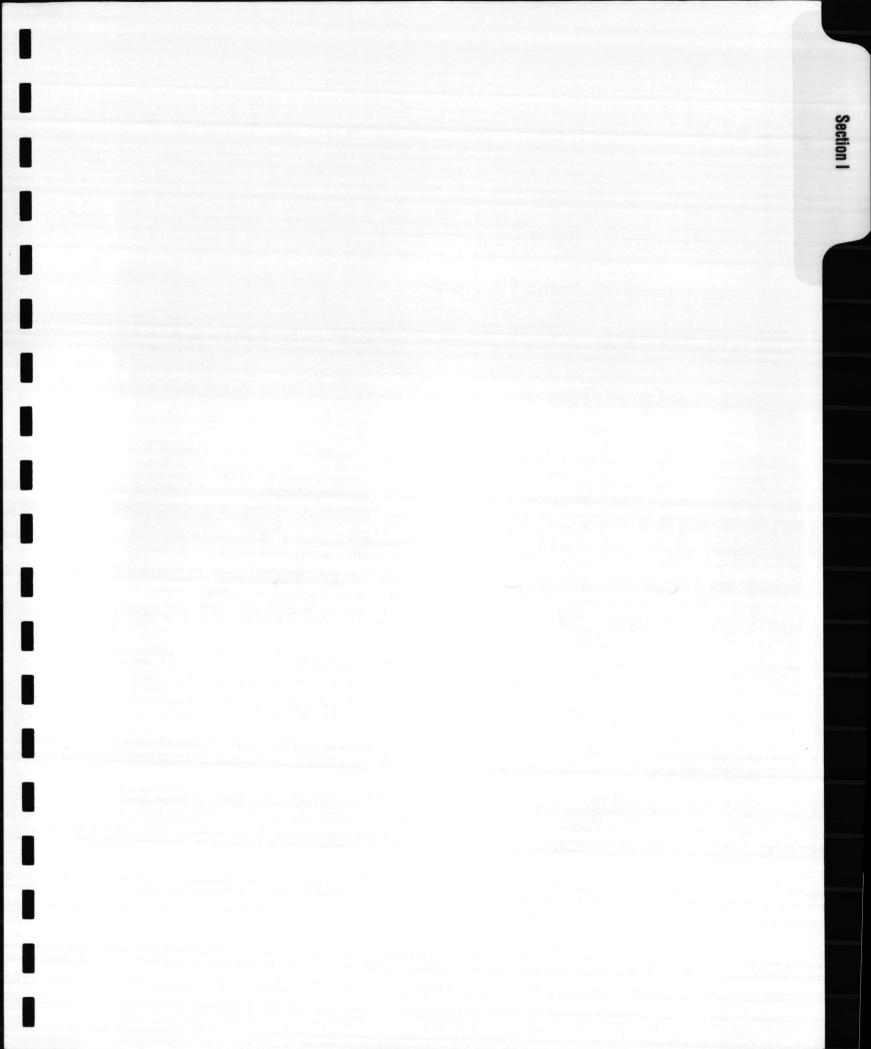
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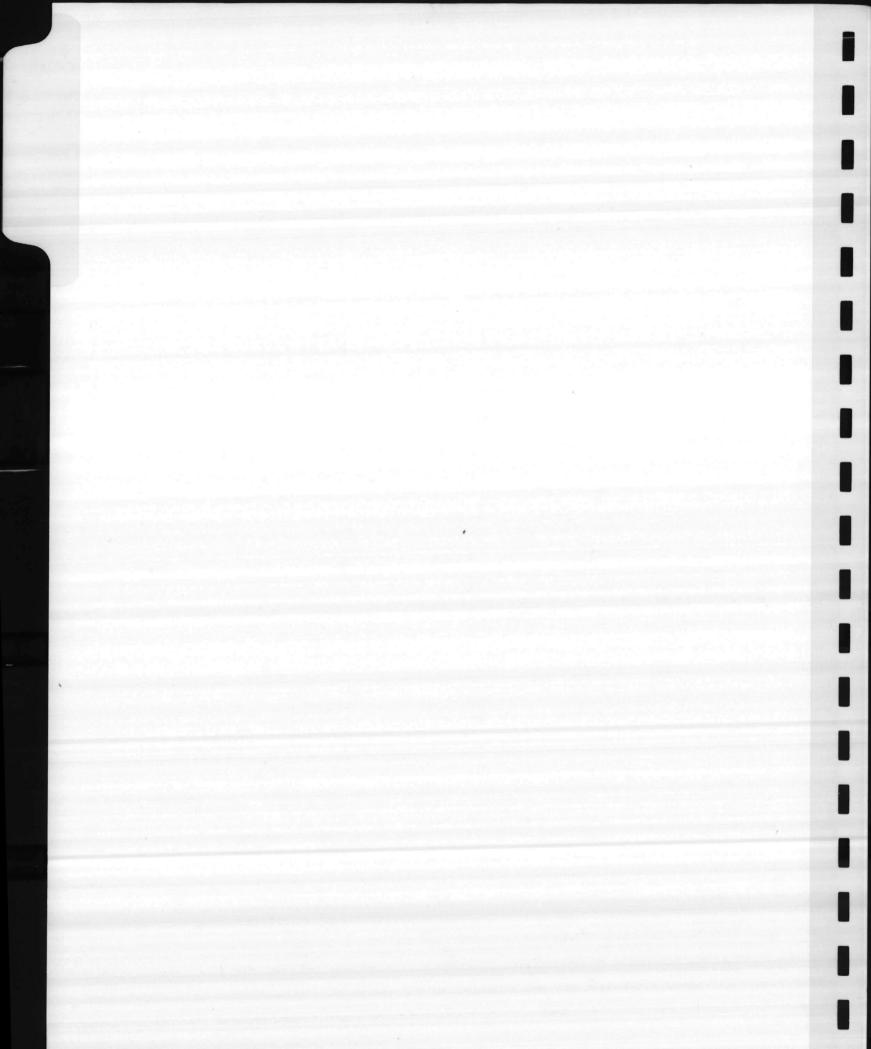
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Confidential Records Management, Inc. New Bern, NC 1-888-622-4425 9/08





I. EXECUTIVE SUMMARY

The purpose of Phase II of the solid waste, wood burning and cogeneration study was to prepare engineering cost estimates and economic evaluations of three systems for burning solid waste and one for burning wood. The two fuels were not considered in a unified system because of equipment compatibility problems. Since the primary purpose of the total project is to dispose of the solid waste, this fuel was given first priority and wood was studied as a "battery limits" system. Also, wood fuel has an associated harvesting cost, and solid waste is available at no incremental cost since the waste collection costs must be incurred whether it is burned or landfilled. Also, potential organizational policy and accounting problems exist if the Navy forests are the source of the wood fuel. Existing forest management practices do not lend themselves to economical wood fuel harvesting.

The three systems for burning solid waste are: <u>Case 1A</u> - Steam would be generated at a nominal 150-200 PSIG saturated pressure and would tie into the existing steam distribution systems of Camp Geiger and the Air Station.

<u>Case 2A</u> - Steam would be generated at 600 PSIG and 725°F. The steam would drive a turbine generator with exhaust at 150 PSIG. The exhaust steam would be tied into the existing Camp Geiger and Air Station systems. The power generated would be tied into the electrical distribution system and all sold to CP&L.

<u>Case 3A</u> - Steam would be generated at 600 PSIG and 725°F. All steam, except that required for feedwater heating, would be sent to a condenser. The electricity generated would be tied to the electrical distribution system and sold to CP&L.

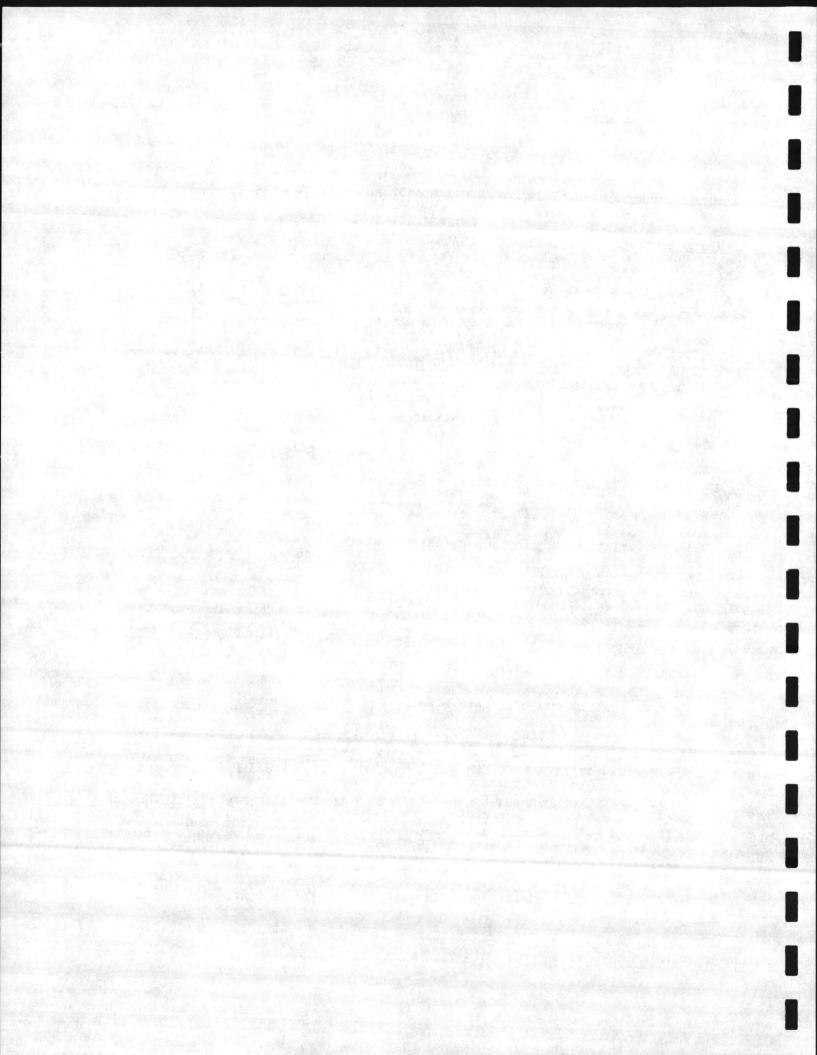
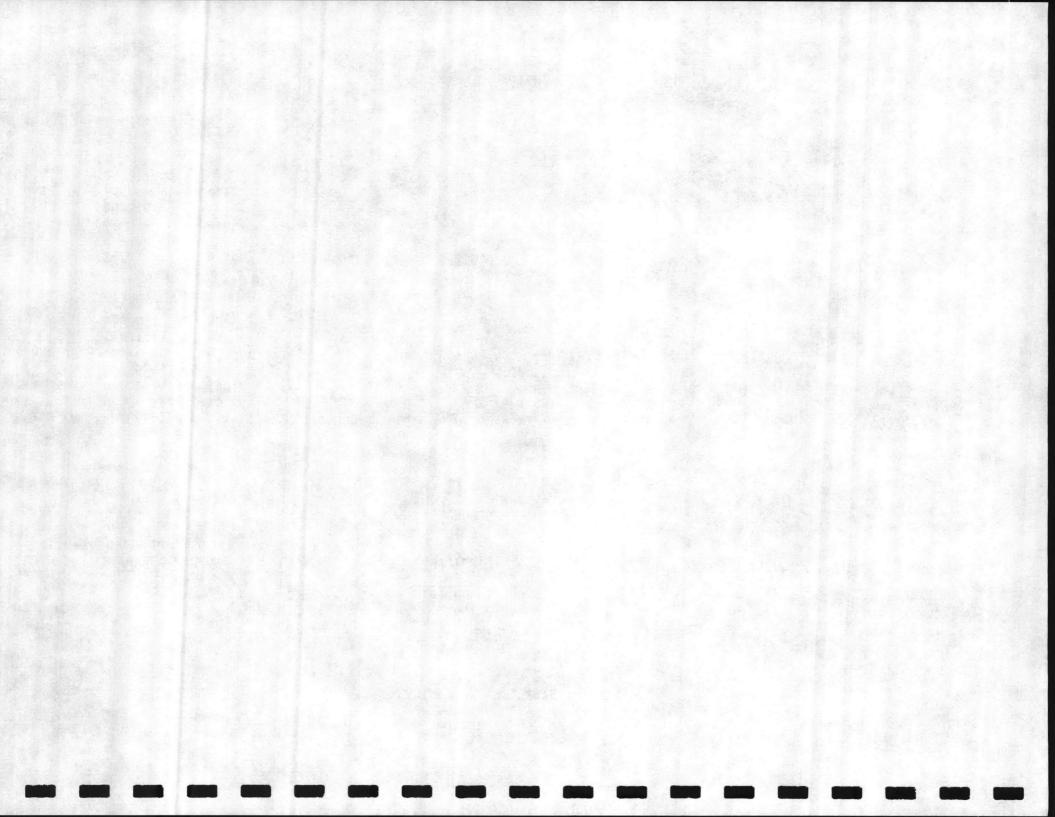


TABLE 1 COST SUMMARY DESIGN ANALYSIS (FY87)

	Construction Costs (1982 \$)	Total Project Cost Present Value	Total Refuse Plant Savings	Uniform Annual Cost	Annual Refuse Plant Savings
Case 1A - Refuse-fired plant producing steam only	15,468,300	37,728,374	74,241,165	3,961,400	7,795,166
Case 1B - Incremental cost of landfill for refuse and oil for steam		111,969,539		11,756,566	
Case 2A - Refuse-fired plant producing steam and electricity with a backpressure turbing	19,134,300	34,030,099	75,918,667	3,573,089	7,971,301
Case 2B - Incremental cost of landfill for refuse and oil for steam		109,948,766		11,544,390	
Case 3A - Refuse-fired plant producing electricit with a condensing turbine	18,178,800 ;y	8,216,527		862,718	-
Case 3B - Incremental cost of of a landfill		7,449,585	<766,942>	782,191	<80,527>

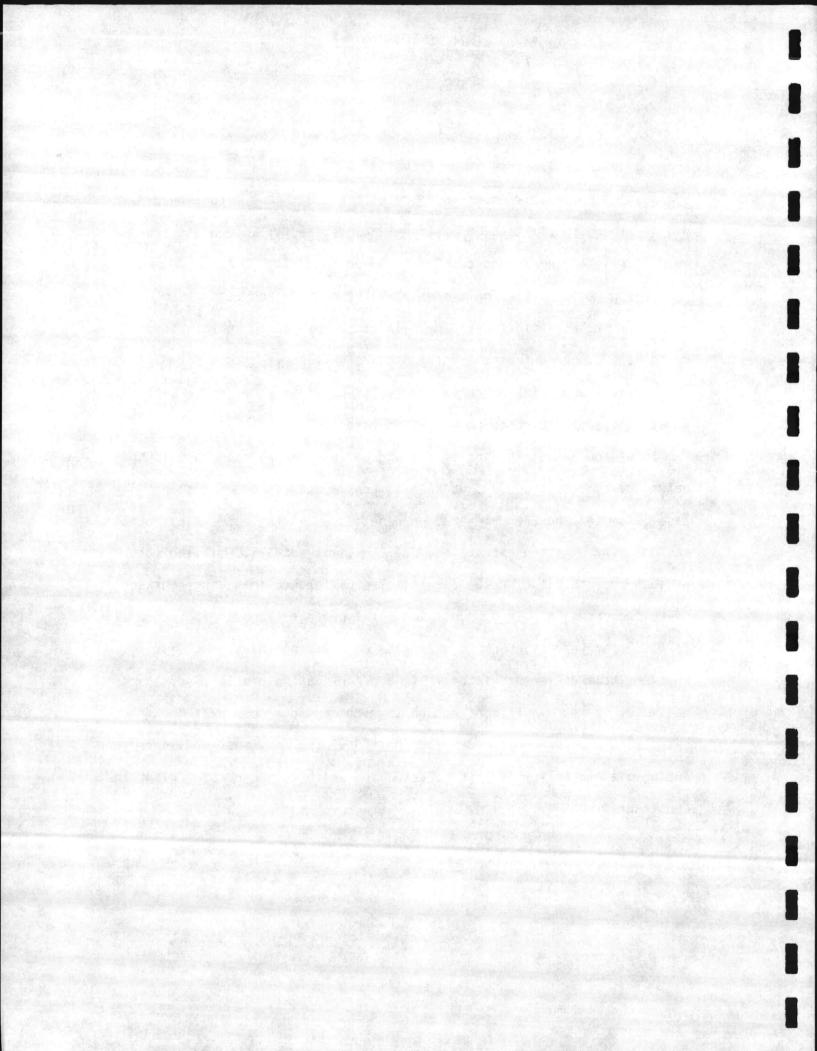
I-2



The capital and operating costs were estimated for each refuseburning system. The cost of each system was then compared to the cost of existing operations which could be eliminated if the refuse-burning plant was built. Existing operations include landfilling refuse and burning oil to generate steam (Cases 1B, 2B and 3B).

Costs were analyzed on a present value basis which considers the impact of the cash flows over the life of the project. Uniform annual costs were computed from the total project present values.

Table 1 summarizes the capital costs, present values and uniform annual costs of the three refuse plant cases. The table also breaks down the total and annual savings that could be realized in each case if the refuse plant described in that case is constructed. Both the steam only case (Case 1A) and the cogeneration case (Case 2A) reflect a substantial savings over existing operations, \$74.2 million and \$75.9 million total project present value, respectively. The difference in savings between these two cases is only \$1.7 million total present value or approximately \$176,000 per year with the cogeneration case having the highest savings. However, this difference is only 2%, and considering the level of the estimate, is not significant enough to recommend one case over the other based solely on economic factors. Therefore, the Navy must consider intangible and policy factors to determine which refuse burning plant to construct.



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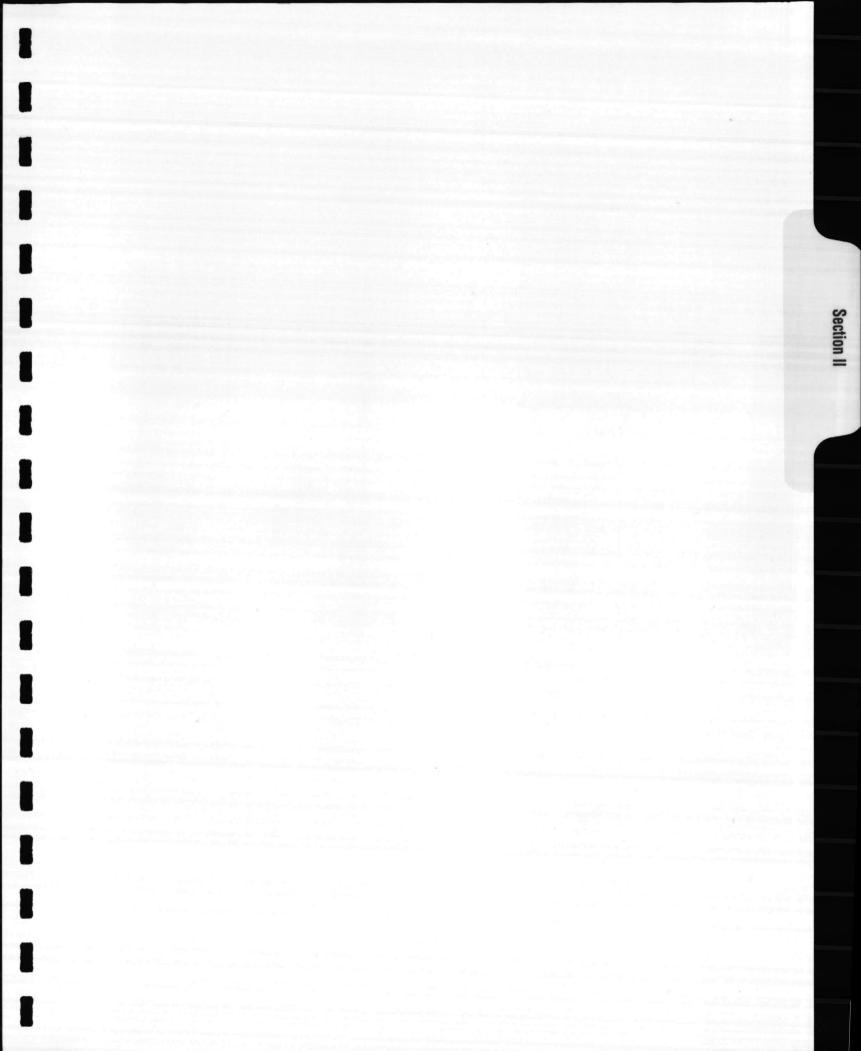
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II. INTRODUCTION

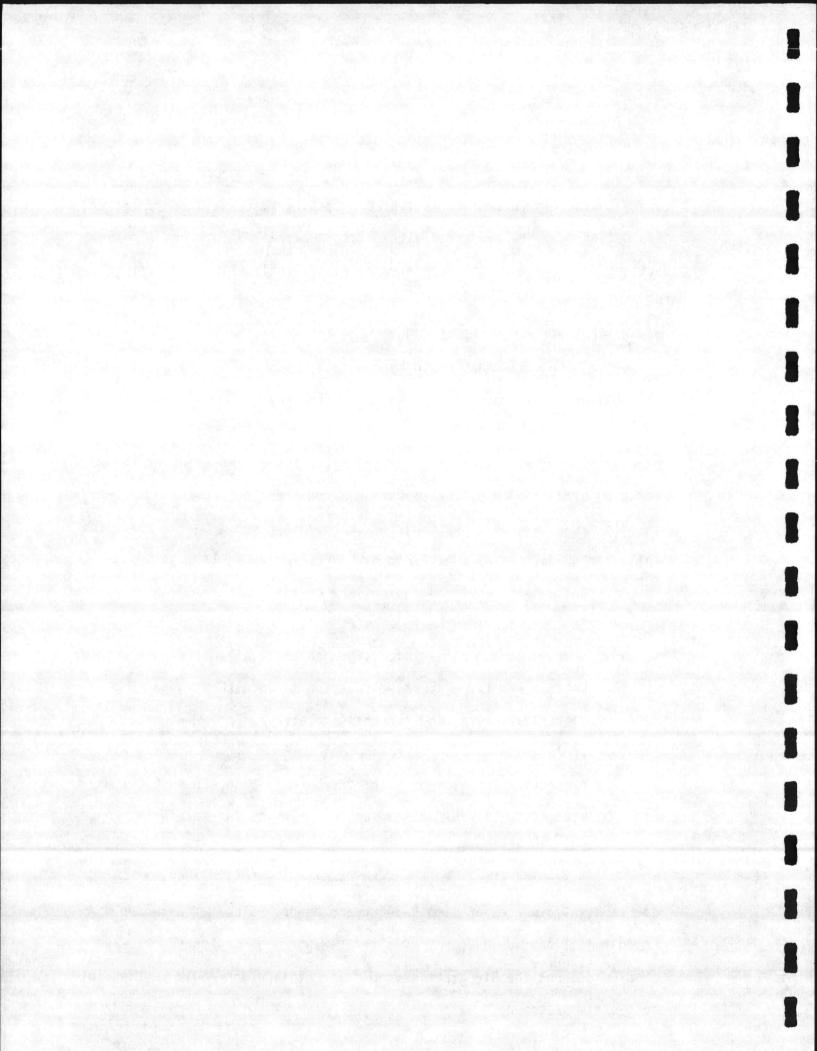
The purpose of Phase II of the solid waste, wood burning and cogeneration study is to perform engineering cost estimates and economic evaluations for the preferred alternatives determined in Phase I. The options studied in Phase I appeared to be of little advantage to the Navy because the proposed plant(s) would replace a 75% coal and 25% oil fuel mix at Central Heating Plant 1700.

Also, the steam that could be generated with the new fuel(s) would not match the steam demand for the specified area. The other reasons are that the use of wood with refuse would cause equipment compatability problems in boiler design; and the procurement and management of the wood would require a major policy adjustment from present systems.

To make the study investigations more advantageous to the Navy, the following guidelines were outlined by NAVFAC for Phase II:

- 1. Solid waste would be the primary boiler fuel.
- 2. The fuel replaced would be 100% oil.
- 3. A steam demand compatible with the fuel availability was needed.
- Options providing steam, extraction steam with by-product electrical power, and condensing electrical power were to be included.
- 5. A "battery limit" type plant for burning wood (30-40,000 lb/hr steam output) would be included as a guide for any further wood fuel investigations.

The first guideline, fuel supply, would be met by utilizing the combined solid wastes of Camp Lejeune and Cherry Point. The second and third guidelines would be met by a refuse energy plant located between Camp Geiger and the Air Station complexes. This plant would be tied into both steam systems.



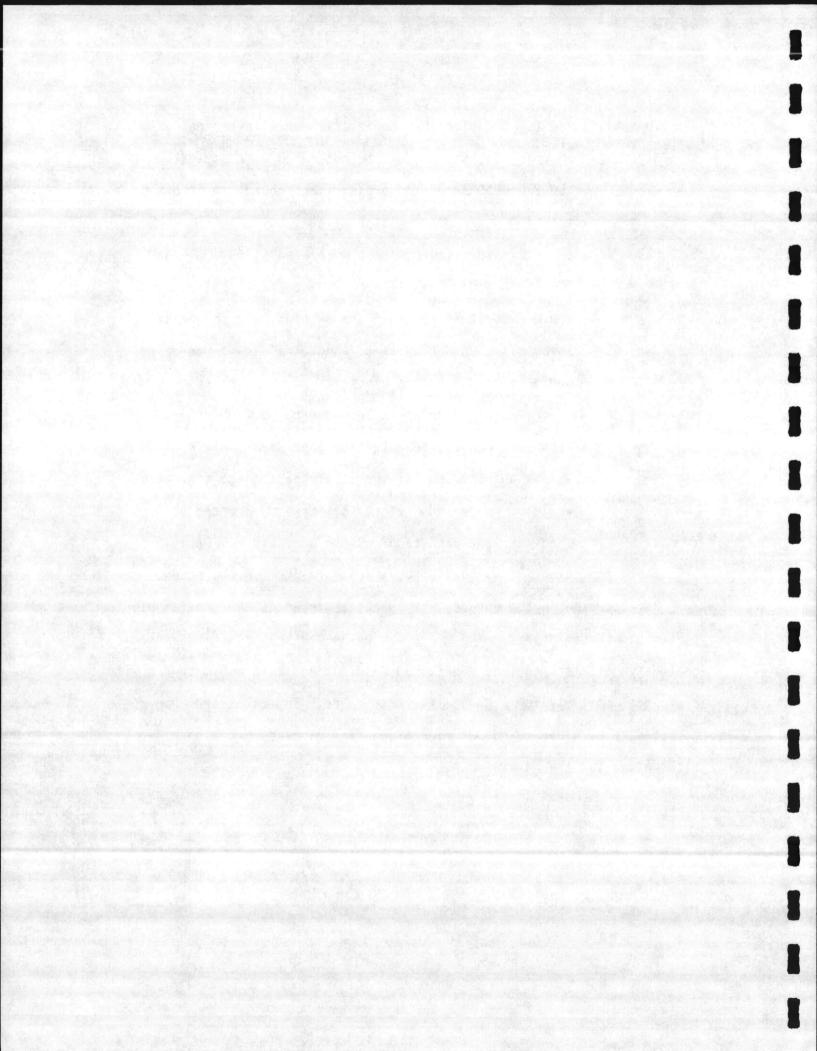
To satisfy the fourth guideline, three cases were investigated:

Case 1A - In this case steam would be generated at a nominal 150-200 PSIG saturated pressure and would tie into the existing steam distribution systems.

- Case 2A In this case steam would be generated at 600 PSIG and 725°F and would feed a turbine generator. The steam would exhaust at 150 PSIG and be tied into the existing steam distribution systems. Electrical power generated would be tied into the electrical system and sold to CP&L.
- Case 3A In this case steam would be generated at 600 PSIG and 725°F and would feed a turbine generator. All steam, except that needed for feedwater heating and deaeration, would be condensed. Electrical power generated would be tied into the electrical system and sold to CP&L.

The fifth guideline is handled as a separate item of the study.

As according to the purpose, this report discusses the general plant concept, methods for determining project costs and the basis for economic analysis. It also provides a detailed description, cost estimate and life cycle cost analysis for each of the three cases. The cases are then compared to each other and recommendations are made as to the best alternative for the Navy.



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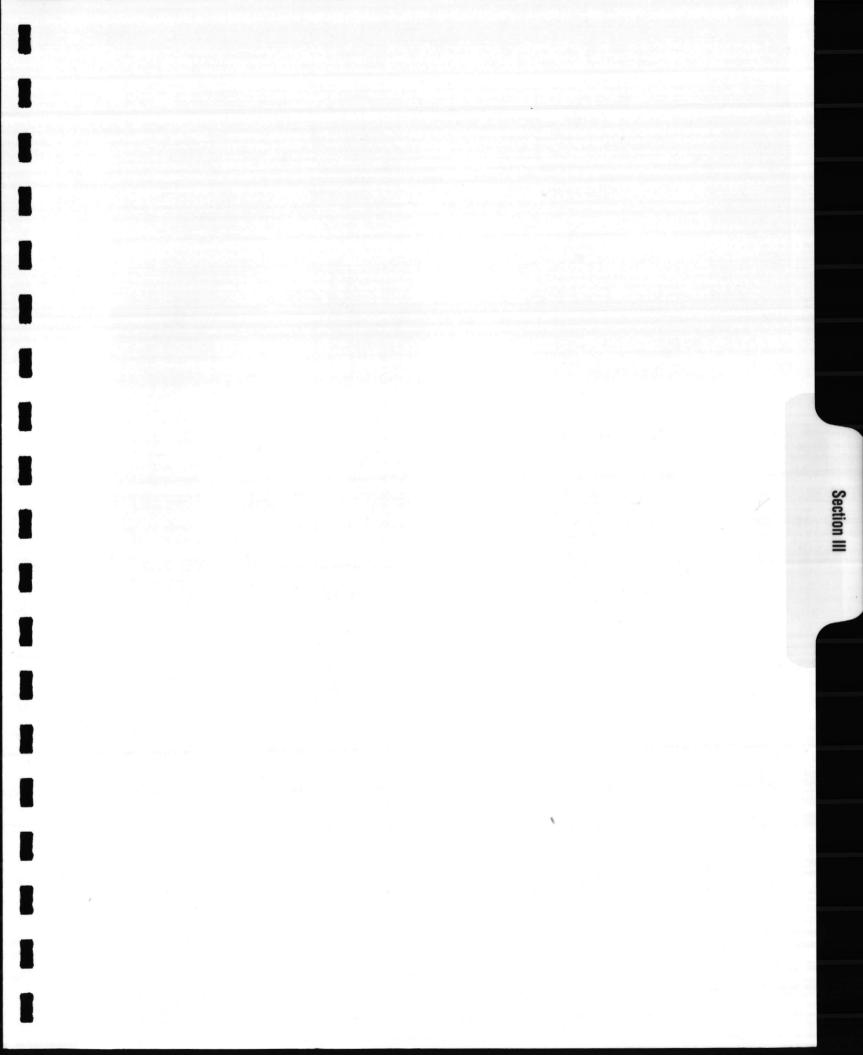
SECTION III

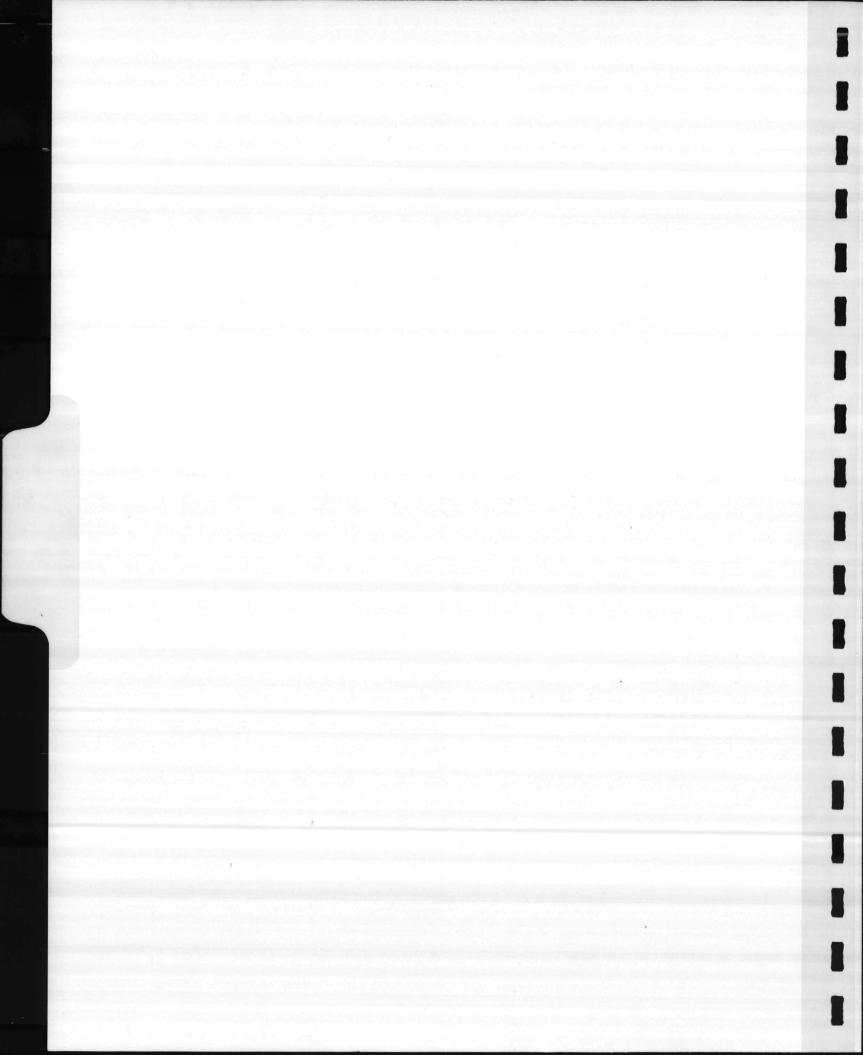
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III. GENERAL PLANT DESCRIPTION

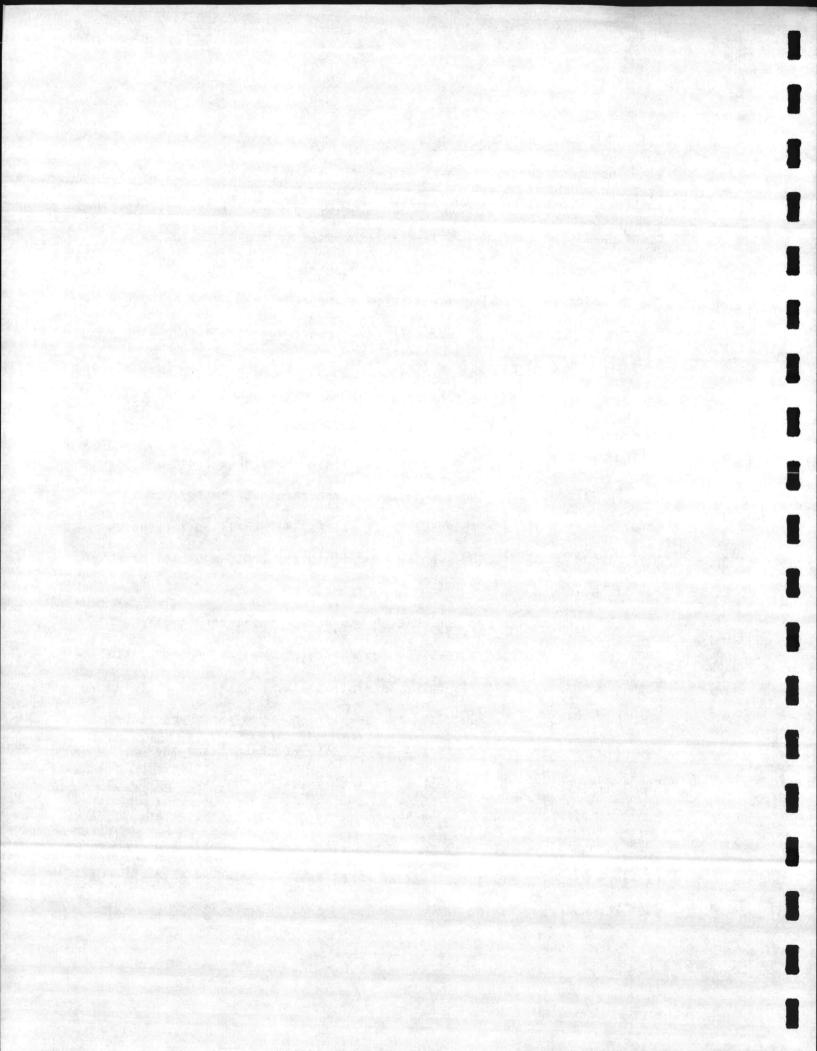
The plant concept emphasizes overall plant efficiency and availability. Two boilers and precipitators, along with a spare material feed crane, will provide the 80% availability used in the economic analysis.

The boiler sizes were based on the available tons of trash from Cherry Point and Camp Lejeune as determined from the SCS "Solid Waste Management Master Plan," 1977. In that report, available tons were projected to 1985 and 2000. These figures were extrapolated to 2011 for the purpose of this report. It was assumed that the percent composition of burnables and non-burnables would remain constant throughout the study period. See Table 2 for a yearly schedule of available trash.

The alternatives considered to convert refuse to energy were: modular incinerators with waste heat boilers, waterwall boilers using mass firing or suspension burning, and fluidized bed combustion or other new technology.

The modular incinerator concept was not pursued since a plant of this type has not been successful for the refuse volume of this installation (200 T/D), and it was felt the availability and thermal efficiency were not attractive. Fluidized bed combustion, pyrolysis, and other new technologies were not considered to be state of the art and the original scope document on this project specifically stated that systems which would require an advance in technology were not to be considered.

Waterwall boilers were considered since that type of system could be expanded upon for all three options to be investigated, simplifying the evaluation. Mass firing was chosen for overall availability, thermal



efficiency and cost for a facility of this size. Operating and maintenance costs for preparing the refuse for suspension firing would be excessive. Mass firing plants in this size range exist at Hampton, Virginia (200 T/D) and the Norfolk Naval Station (180 T/D).

The following is a general description of the Waterwall boiler system with mass firing.

Fuel Feed

The collection process for the refuse to be disposed of at the refuse energy facility will be selective. Large metal items (55-gallon drums, appliances, etc.), highly flammable or explosive items, and bulky items will have to be collected separately and disposed of at landfills.

The refuse collection trucks will enter an enclosed tipping area and dump the refuse into a storage pit. The pit is of sufficient size to store at least a 3-day supply of refuse.

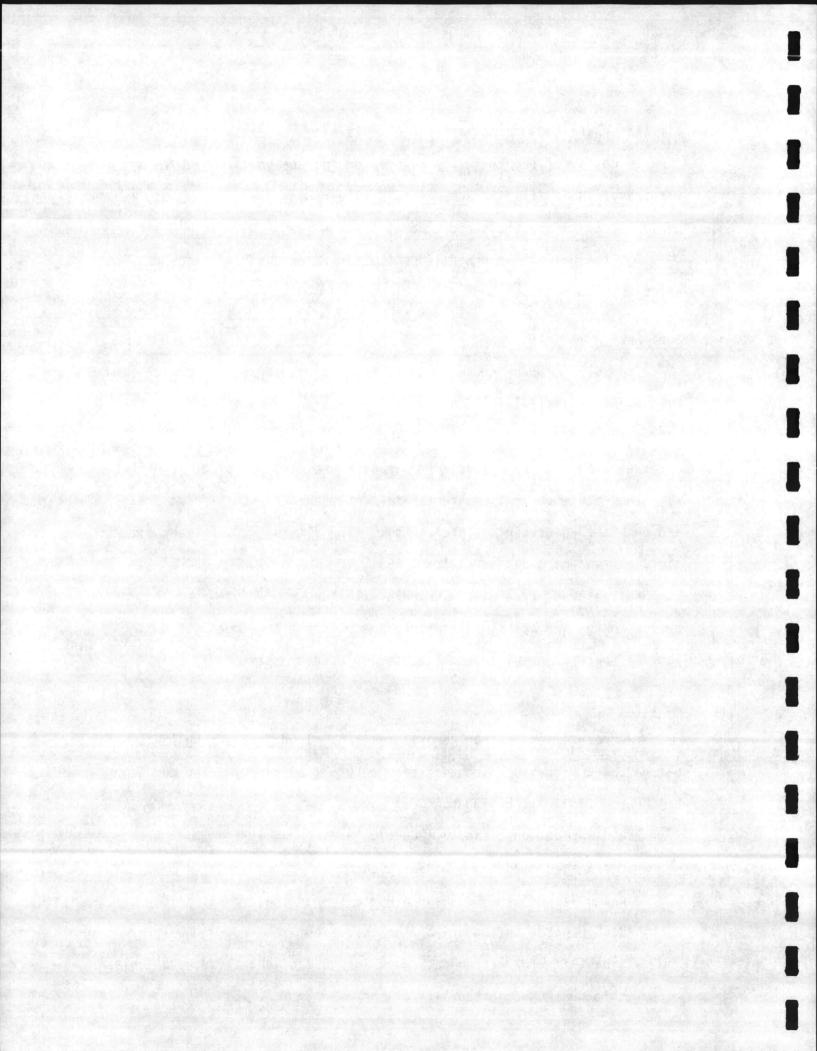
An overhead crane with a grapple will feed the refuse into the boiler charging hoppers. Since this crane is the only means of fuel feed, a spare crane will be available for standby service.

Boilers

Two refuse-fired steam generators, each sized for burning 100 tons per day, are proposed. The available refuse from Cherry Point and Camp Lejeune in 1985 will be 130 tons per day.

The plant design capacity (200 T/D) will provide:

- extra margin during a boiler outage;
- capability of the boilers to operate near their most efficient design point during a 2-boiler operation;
- capability for accommodating an increase of the refuse available through the projected life of the plant.



After the refuse is fed into the hopper it will be sent to the stoker by means of an hydraulic ram feeder. The stoker will be a reciprocating grate type which will provide mixing and break-up of the refuse. A forced draft fan will supply overfire air. The combustion air will be drawn from the tipping room area to reduce odor and provide a negative draft in that area.

Supplementary fuels will not normally be used; however, a provision for firing No. 2 fuel oil is included. This will be used for flame stabilization at low load and for start-up only. No. 2 oil is used to minimize storage and handling difficulties.

Feedwater System

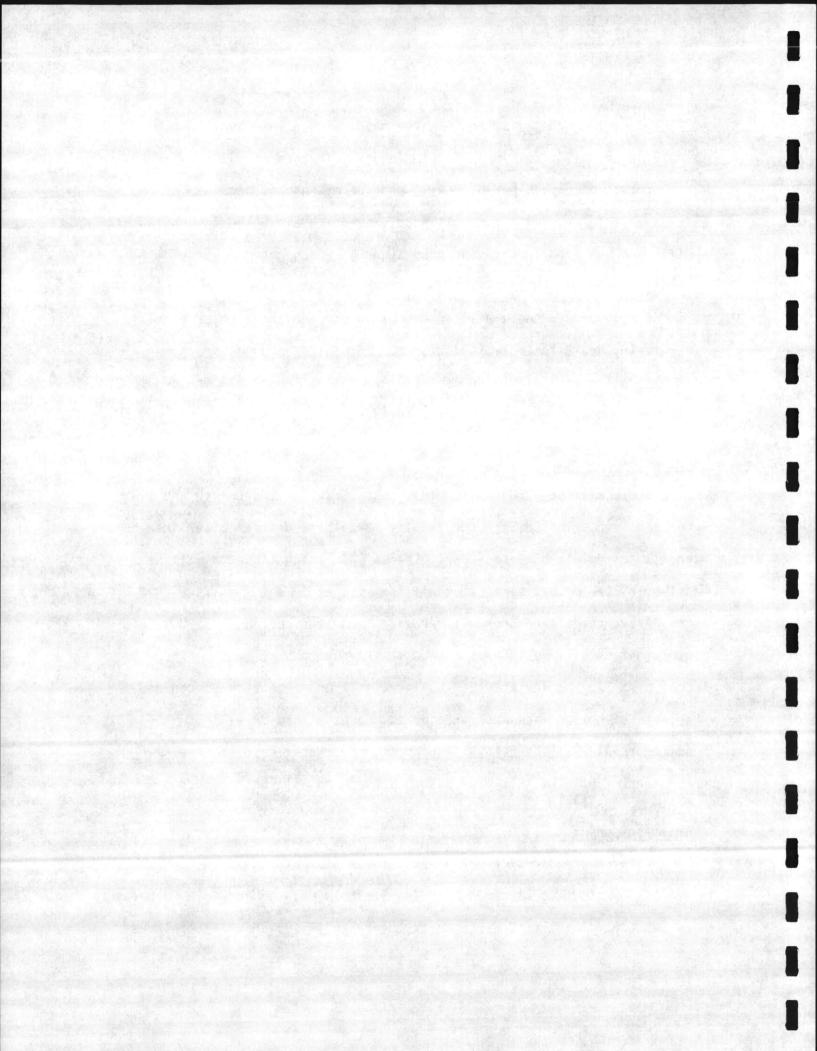
There will be three boiler feed pumps, one turbine driven and two motor driven. The Boiler code requires a turbine driven boiler feed pump on all solid fuel boilers. During normal operation the pump will be driven by the motors since this will be more efficient.

A tray type deaerator will provide feedwater heating. A 20-minute storage tank will be incorporated with the deaerator.

Case 1A, the low pressure boilers, will use a zeolite softening system for boiler feedwater treatment. Cases 2A and 3A will use the softeners plus silica removal equipment. Feedwater chemical treatment for control of alkalinity and oxygen scavenging will be provided.

Emission Control

Federal standards of performance for municipal refuse fired boilers address particulate matter only. The limit is 0.08 grains/SDCF corrected to 12% CO₂. This limit far exceeds the capabilities of mechanical dust



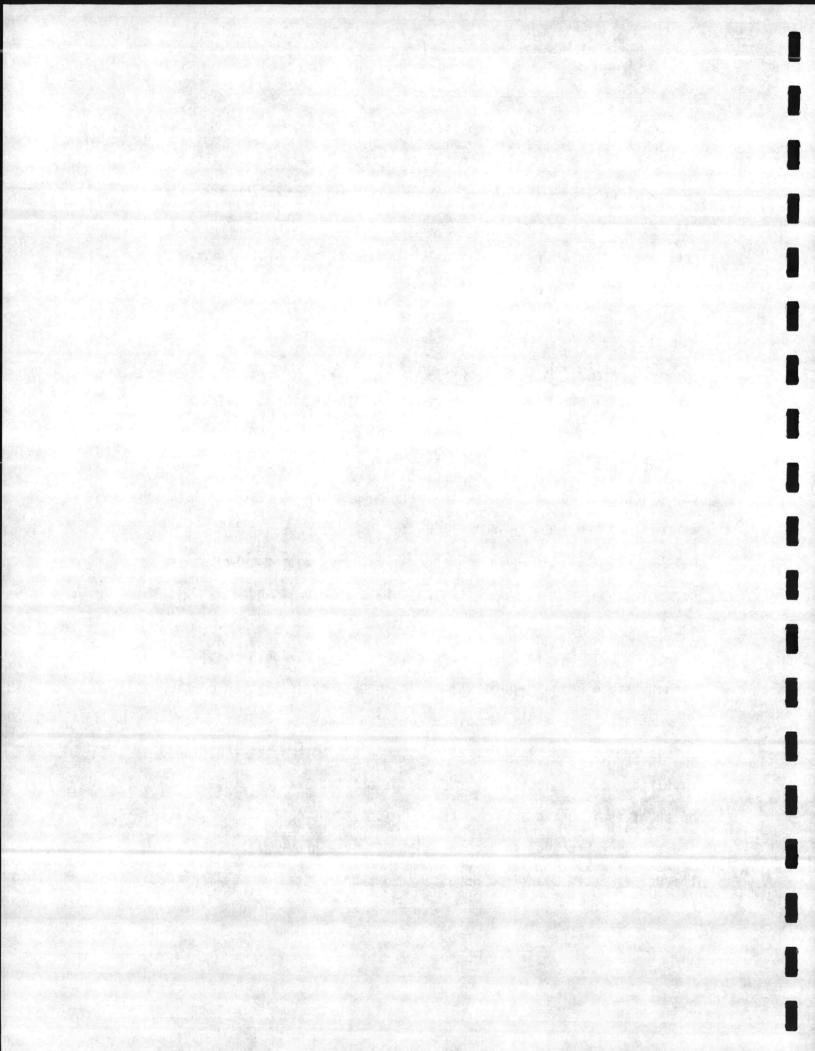
collector and low energy scrubbers. While high energy scrubbers and bag filterhouses may be applicable to mass fired boilers in the future, the most preferred system in use today is the dry type electrostatic precipitator. Compliance will be achieved through use of an electrostatic precipitator on each boiler. An I.D. fan will be installed after each precipitator and discharge will be through a stack for each unit.

Ash Handling

The bottom ash will be handled with water-filled submerged scraper conveyors. The bottom ash will contain all non-combustible materials which pass through the boiler. Since the possibility of fouling or pluggage is great, a flop gate valve will be located at the bottom of the ash discharge chute. Two troughs will be provided on each boiler. Fly ash will be handled dry and will be deposited at the upper end of the ash discharge chute. A sloped conveyor (to achieve some dewatering) will carry the ash to a dumpster station outside the building.

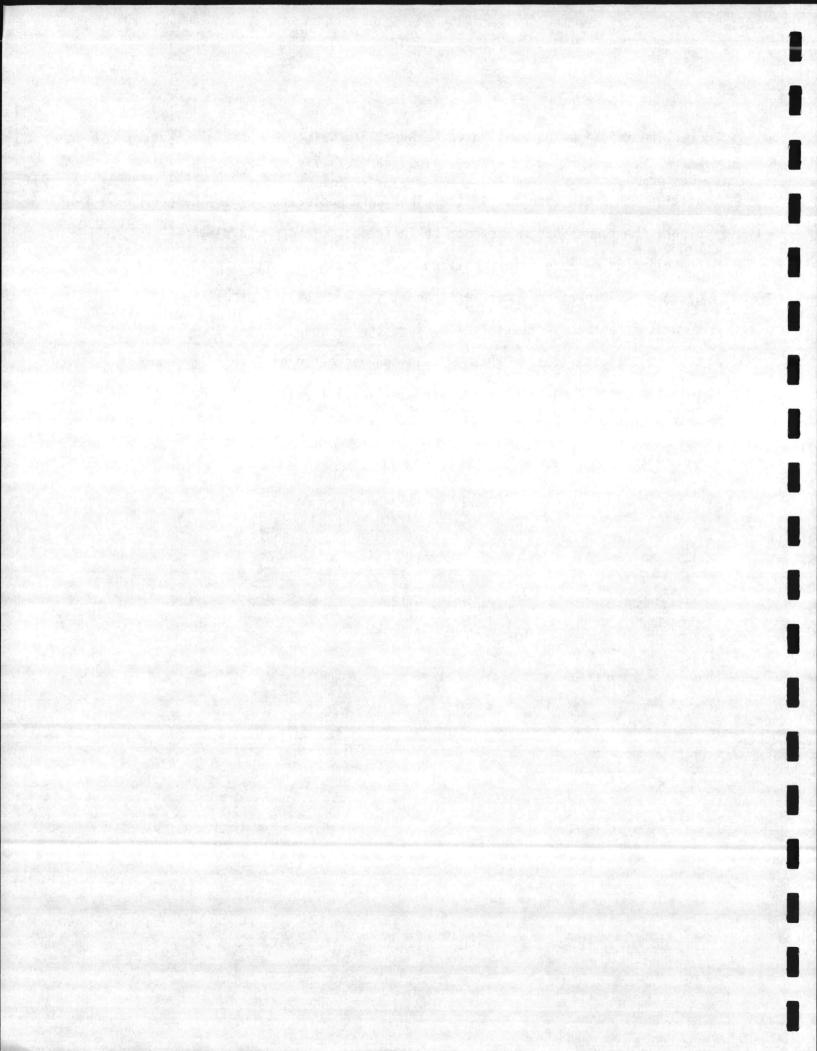
The following Tables 3 and 4 and Graphs 1, 2, and 3 portray the present steam usage figures for the Camp Geiger/Air Station complexes. As portrayed by Graph 3, Combined Location Usages, the best match for the refuse energy plant would be a location where both sites could be supplied. Such a location was found on the Air Station property to the north of the housing area and to the east of the Camp Geiger steam plant. The site is portrayed in Drawing MG1. It is approximately 2150 feet to the Geiger steam plant and 6500 feet to the Air Station steam plant.

III-4



The refuse plant is located between Camp Geiger and the Air Station because the summer steam load at either installation is not enough to utilize the steam output. If the plant were dedicated to Camp Geiger alone, the summer steam use must be increased. This would require installation of absorption chilling equipment. It is felt that the cost of this additional equipment will equal the cost of the steam line connected to the air station. The advantge of keeping the refuse plant tied to both stations is that in case the operation of either is reduced in later years a market for the steam will still exist.

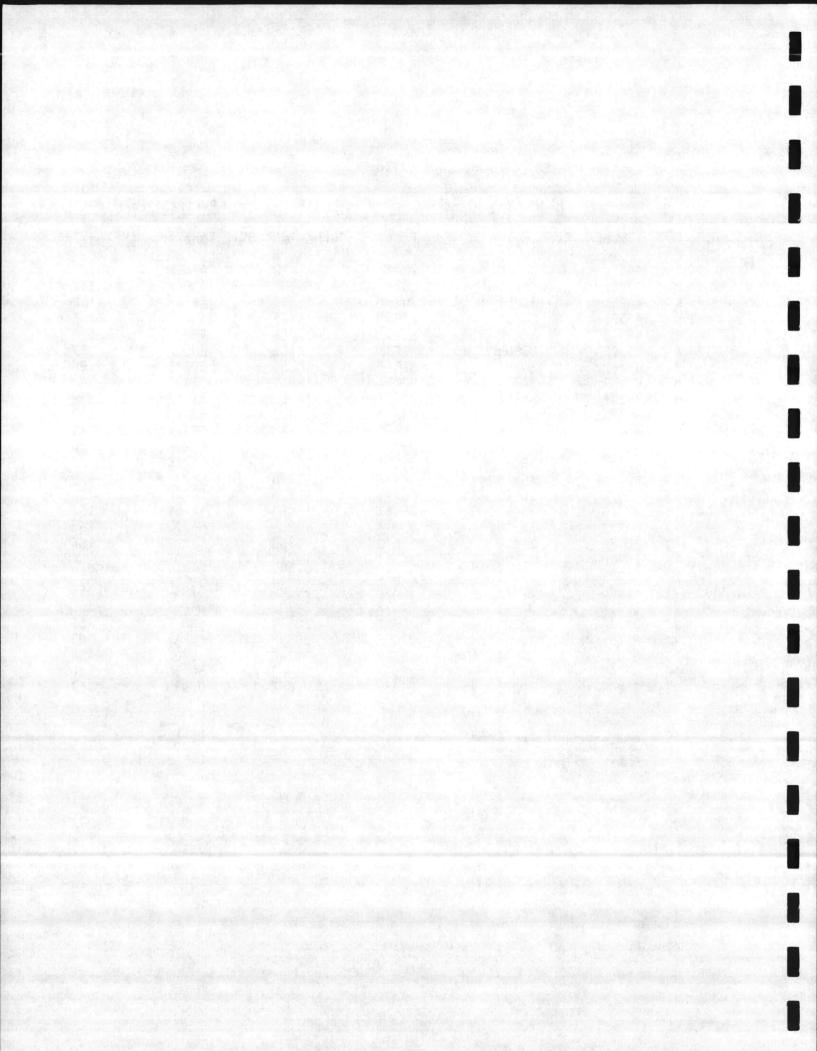
Drawings MG2 and MG3 show the conceptual arrangement of the proposed facility.



						TOTAL	TOTAL
		CAMP LEJEUNE		CHERRY POINT		BURNABLE	BURNABLE
Year		Total	Burnable (73%)	Total	Burnable (75%)	Tons/yr.	Tons/dy.
1985	1	44520	32500	20037	15028	47528	130
	2	44877	32760	20377	15282	48043	132
	3	45234	33021	20717	15538	48559	133
	4	45591	33281	21057	15793	49074	134
	5	45948	33542	21397	16048	49590	136
1990	6	46305	33803	21737	16303	50106	137
	7	46662	34063	22077	16558	50621	139
	8	47019	34324	22417	16813	51137	140
	9	47376	34584	22757	17068	51652	142
	10	47733	34845	23097	17323	52168	143
1995	11	48090	35106	23437	17578	52684	144
	12	48447	35366	23777	17833	53199	146
	13	48804	35627	24117	18088	53715	147
	14	49161	35888	24457	18343	54231	149
	15	49518	36148	24797	18598	54746	150
2000	16	49875	36409	25137	18853	55262	151
	17	50232	36669	25477	19108	55777	153
	18	50589	36930	25817	19363	56293	154
	19	50946	37190	26157	19618	56808	156
	20	51303	37451	26497	19873	57324	157
2005	21	51660	37712	26837	20128	57840	158
	22	52017	37972	27177	20383	58355	160
	23	52374	38233	27517	20638	58871	161
	24	52731	38494	27857	20893	59387	163
	25	53088	38754	28197	21148	59902	164
	26	53445	39015	28537	21403	60418	166
2011	27	53802	39275	28877	21658	60933	167

Source: Extrapolated from SCS Report

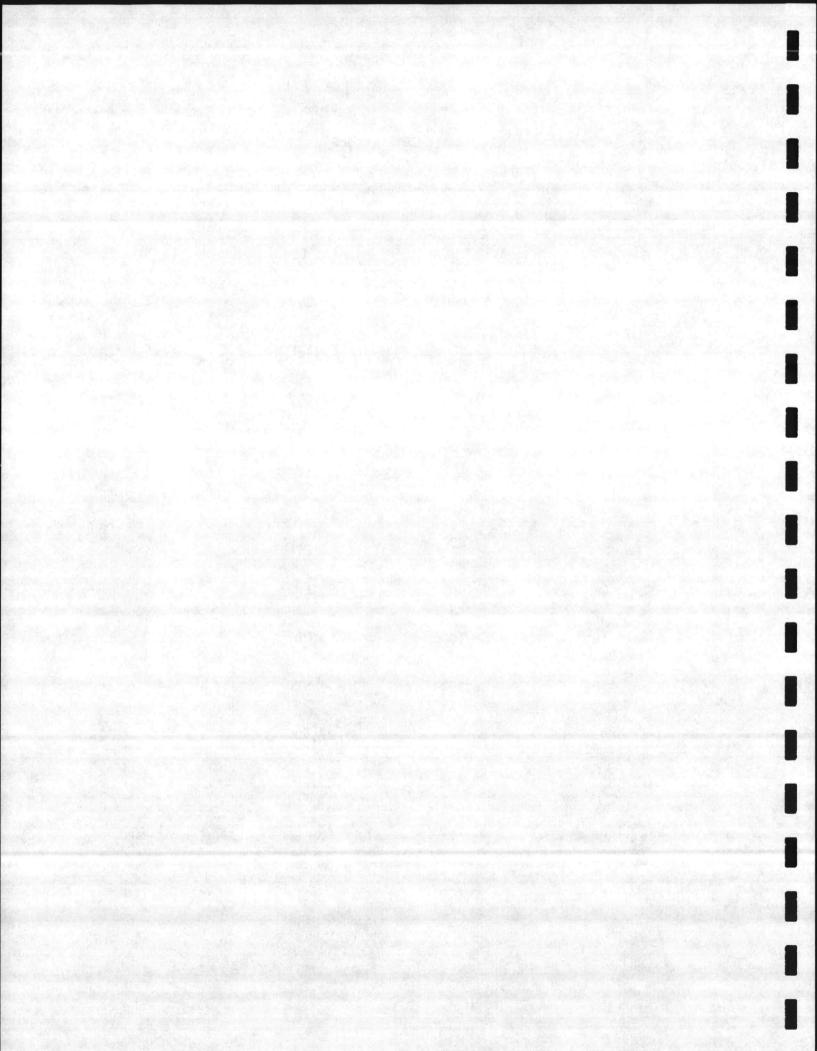
TOTAL



CAMP GEIGER STEAM DATA

TABLE 3

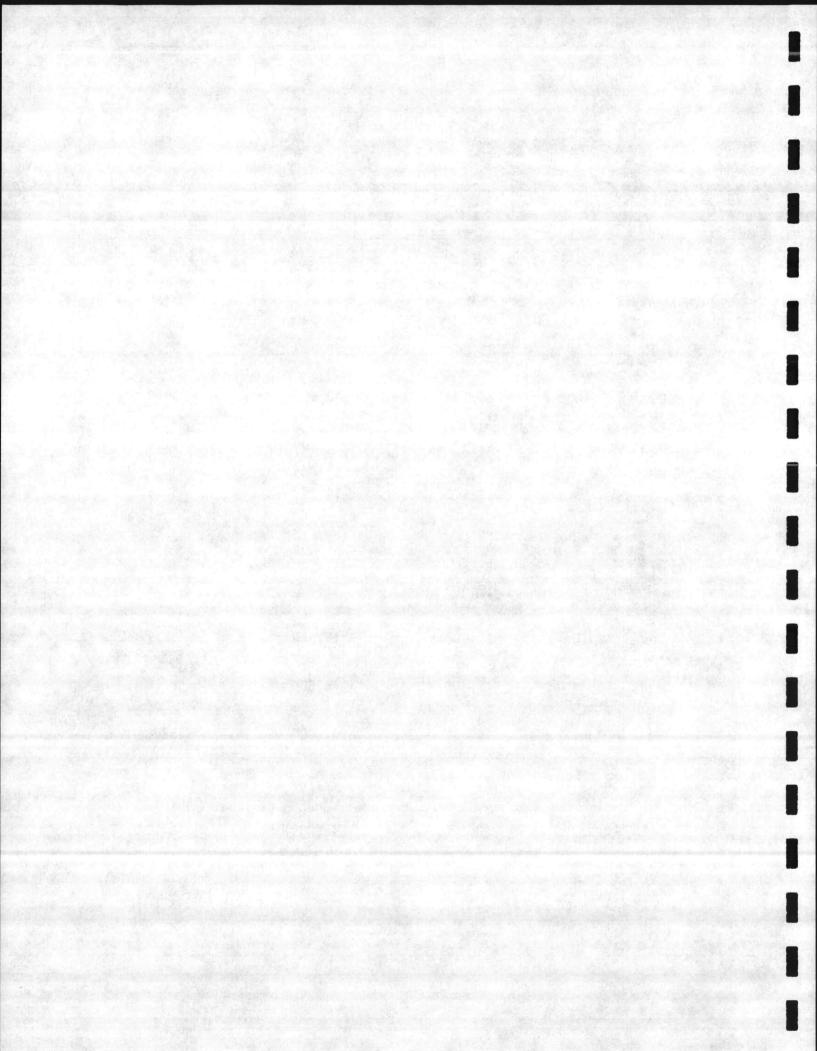
	Avg. Load	Highest Load	Avg. % Make-Up
Jan. '81	38,400	52,250	43.2
Feb. '81	33,400	51,300	41.6
March '81	33,600	43,800	43.2
April '81	21,400	35,500	75.1
May '81	19,300	34,000	85.5
June '81	14,000	26,500	62.8
July '80	17,000	23,500	60.2
August '80	16,100	24,000	43.7
Sept. '80	15,000	19,500	44.5
Oct. '80	20,800	27,500	50.1
Nov. '80	26,400	39,900	41.7
Dec. '80	31,700	44,700	41.0
Annual Average	23,950		52.7%

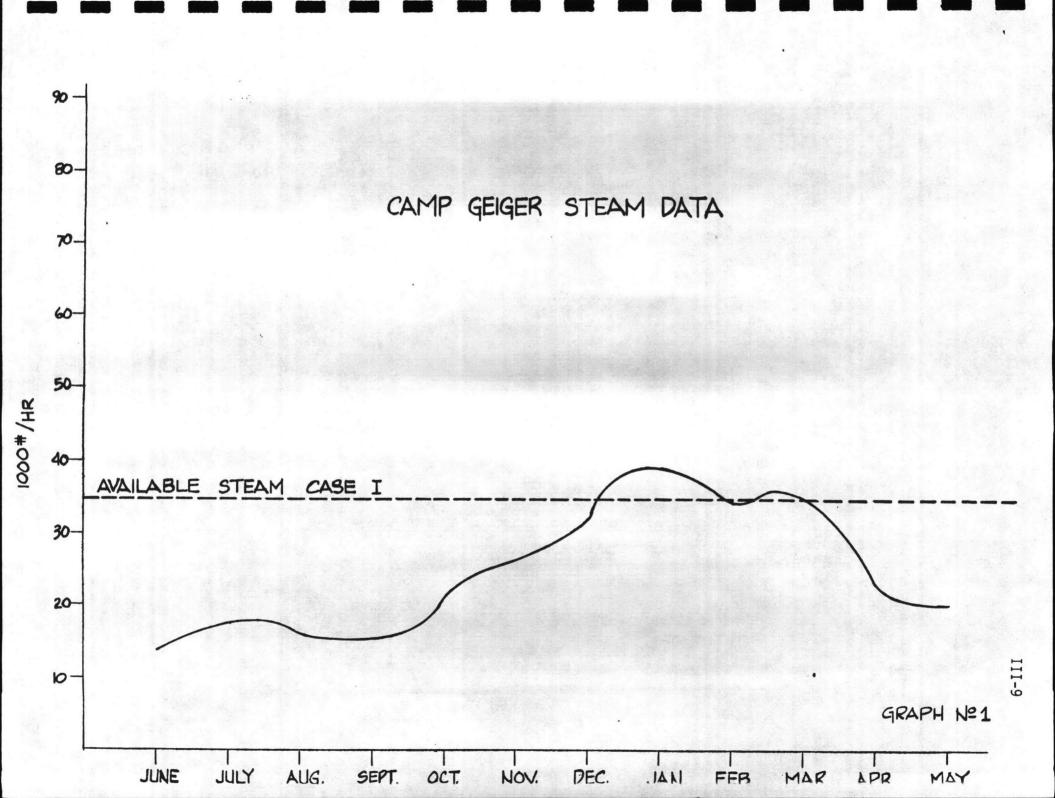


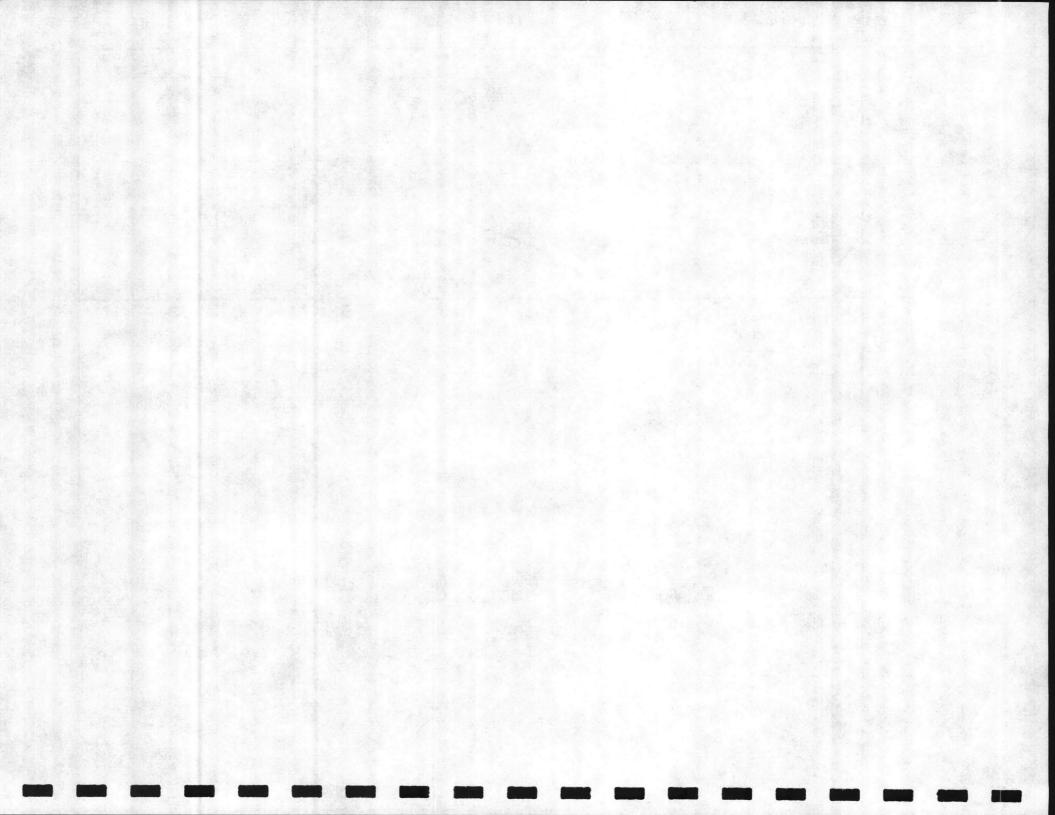
NEW RIVER STEAM DATA

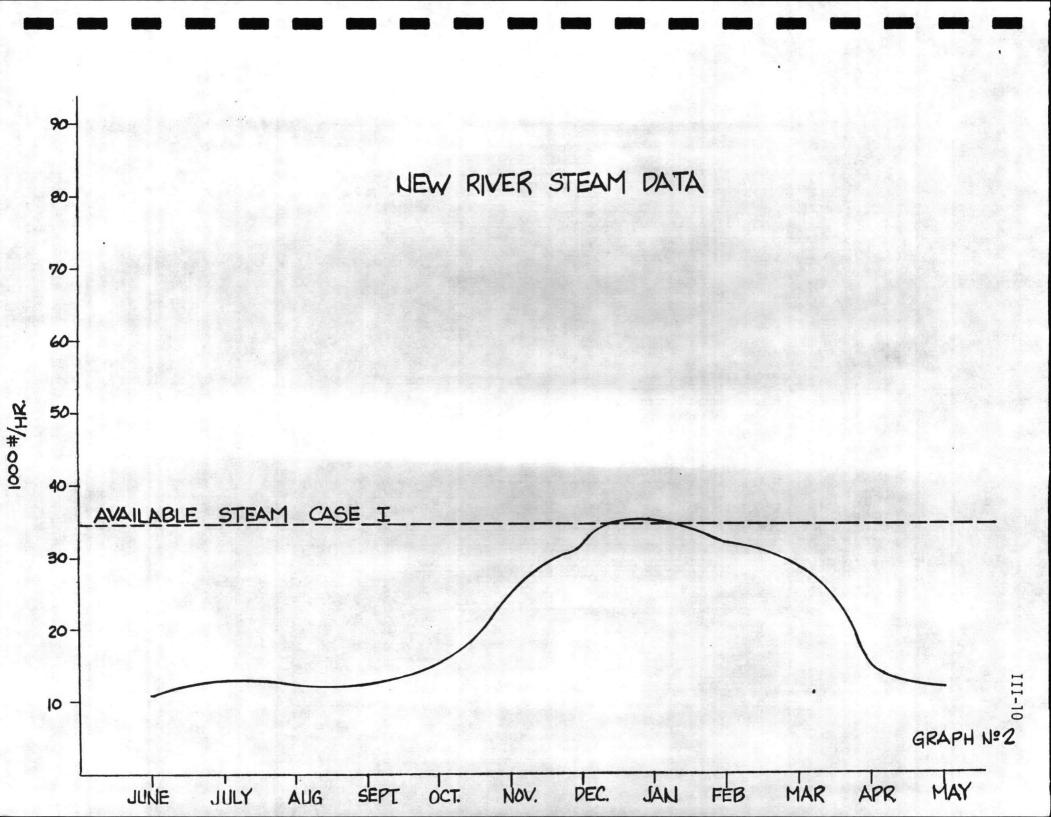
TABLE 4

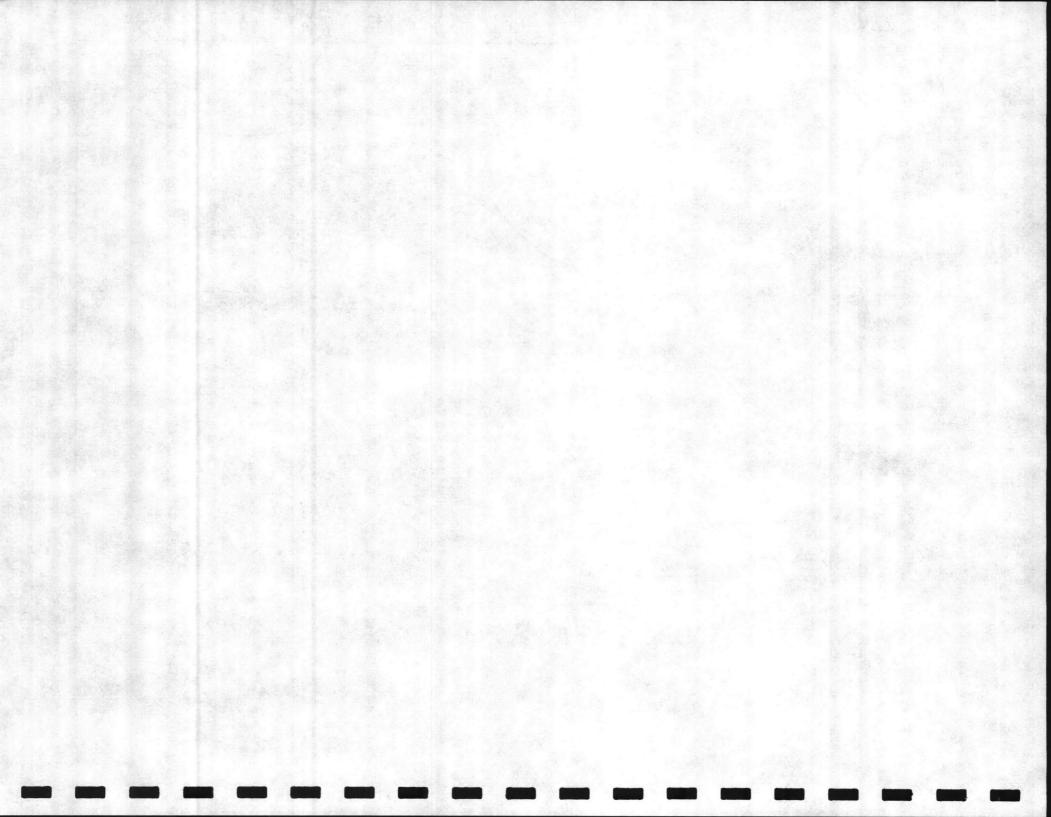
	Avg. Steam Load	Highest Load	Avg. % Make-Up
Jan. '81	35,500	48,600	27.1
Feb. '81	31,800	54,000	32.5
March '81	28,000	40,500	39.8
April '81	14,600	25,200	62.3
May '81	12,200	19,350	55.6
June '80	11,100	17,000	61.0
July '80	12,600	15,750	55.9
August '80	12,400	12,550	51.7
Sept. '80	12,400	46,800	54.8
Oct. '80	14,500	32,400	52.8
Nov. '80	25,000	40,200	29.5
Dec. '80	30,100	43,200	27.2
Annual Average	20,000		45.9%

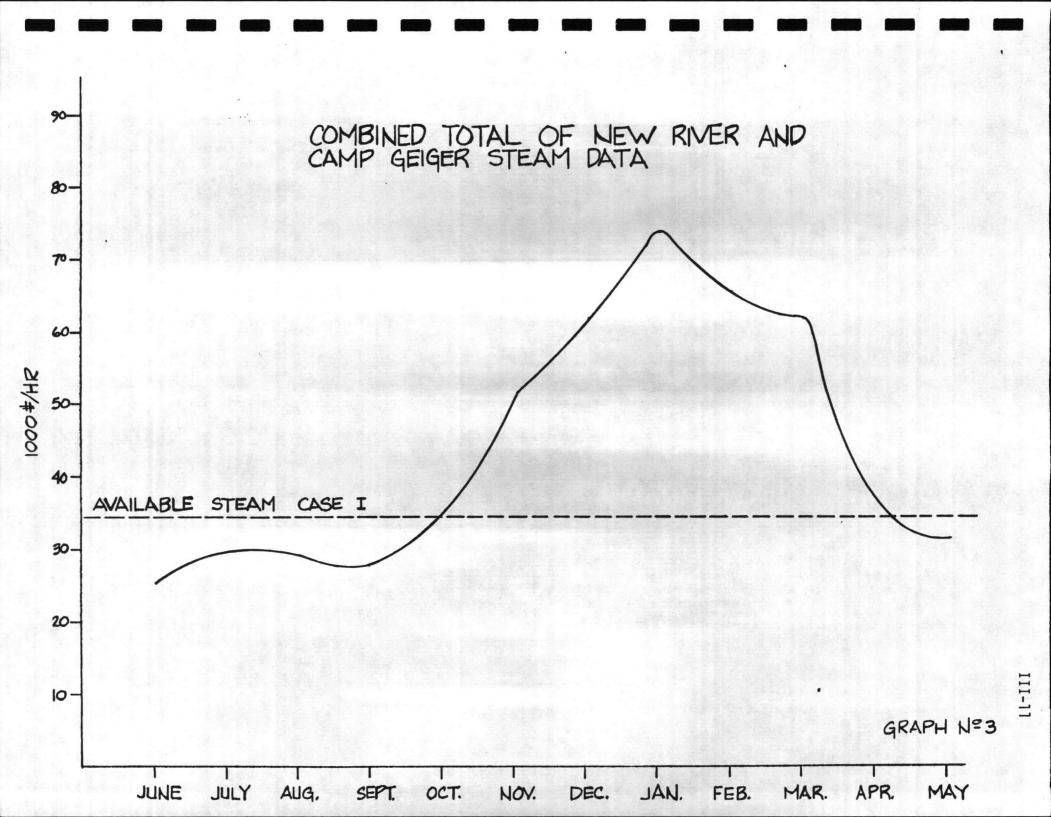


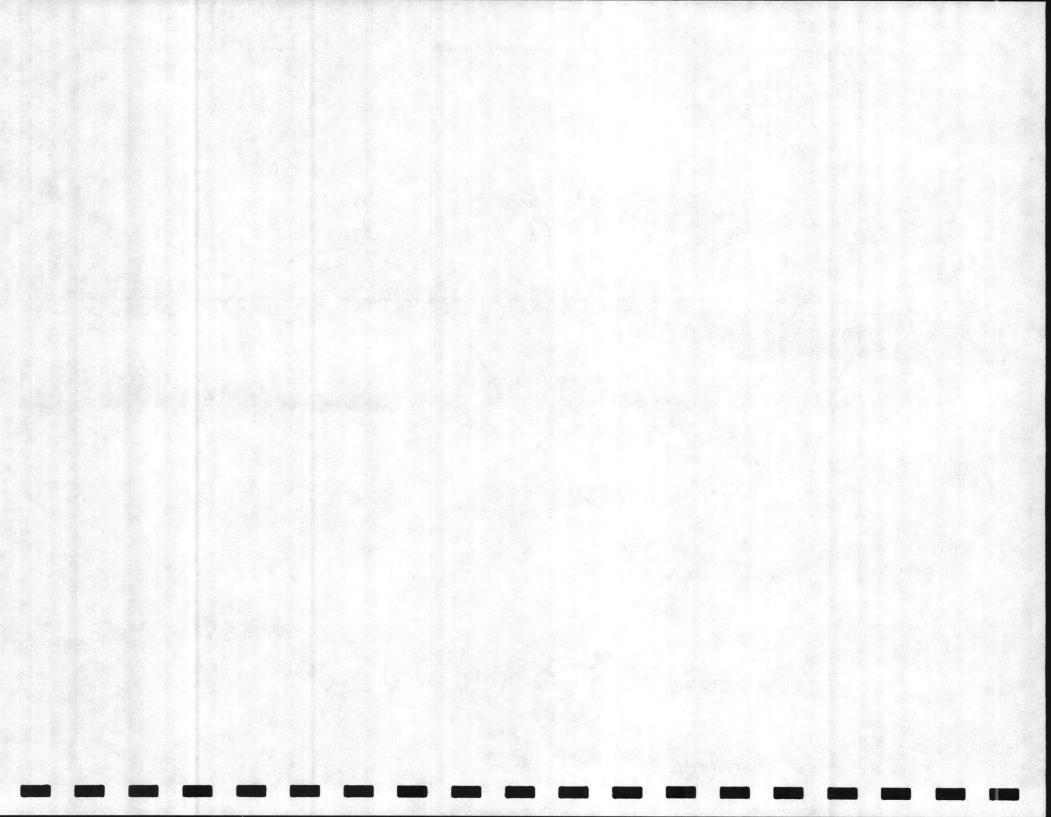


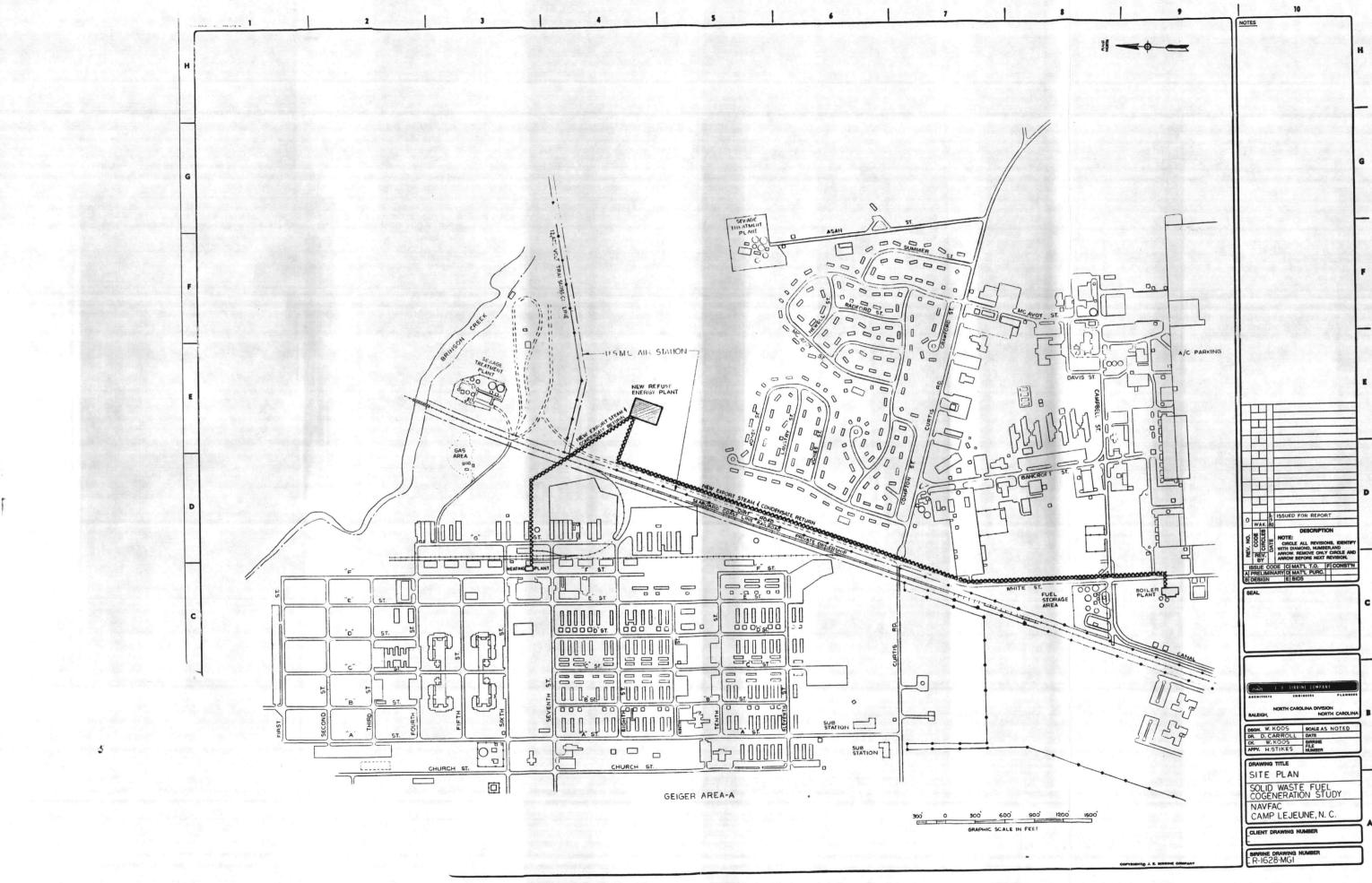


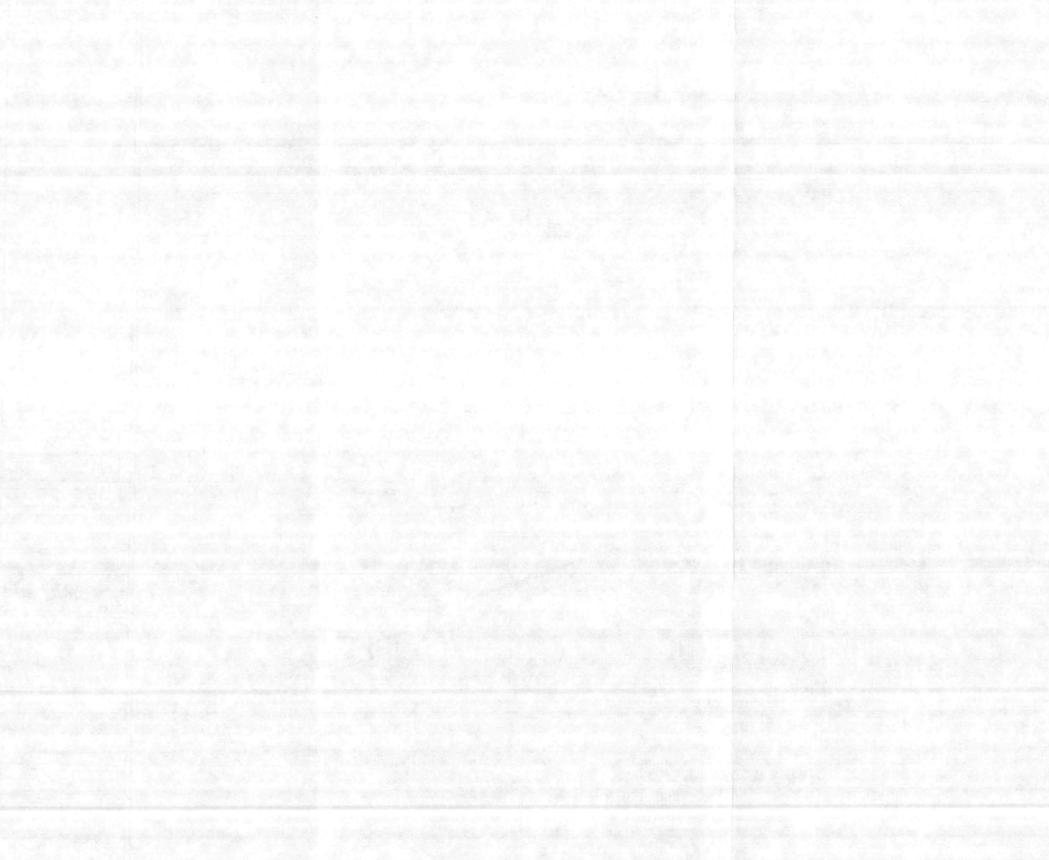


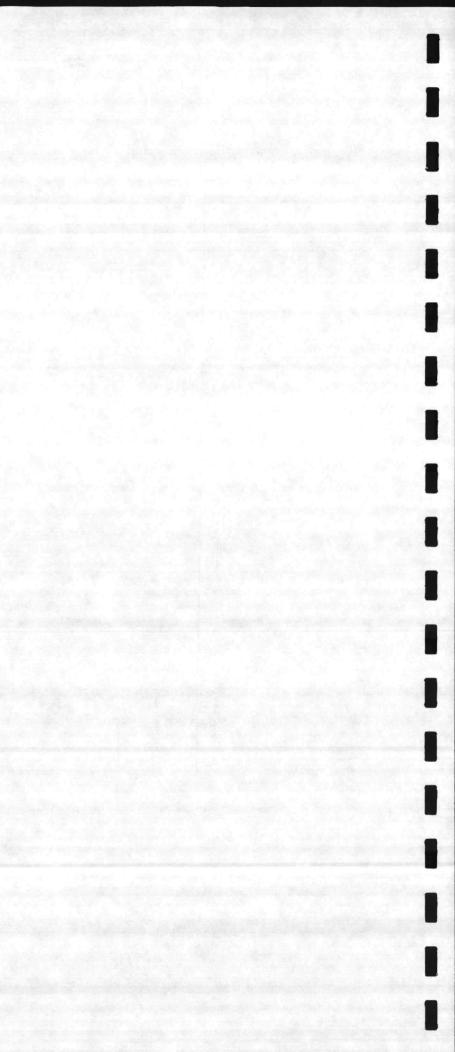


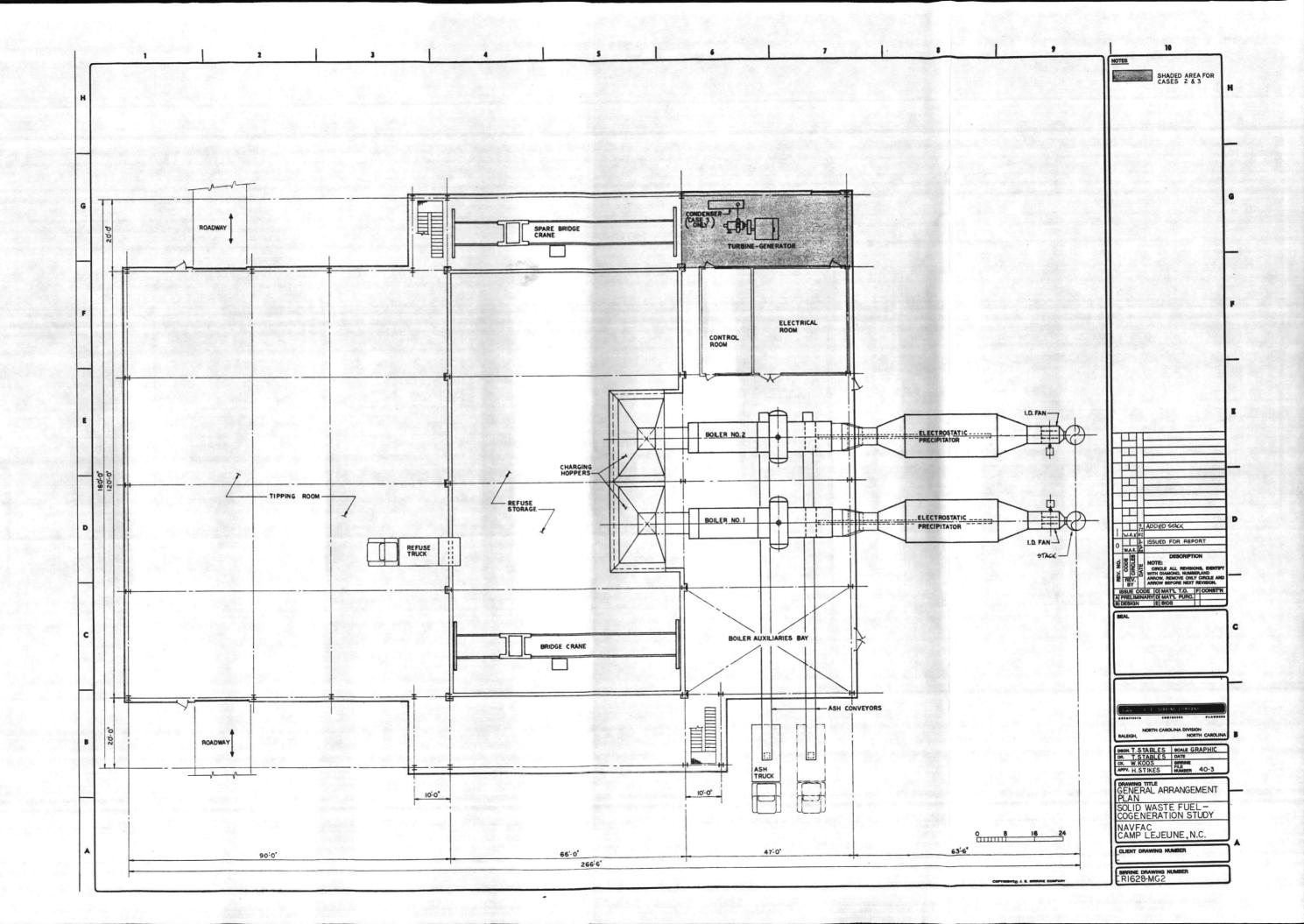












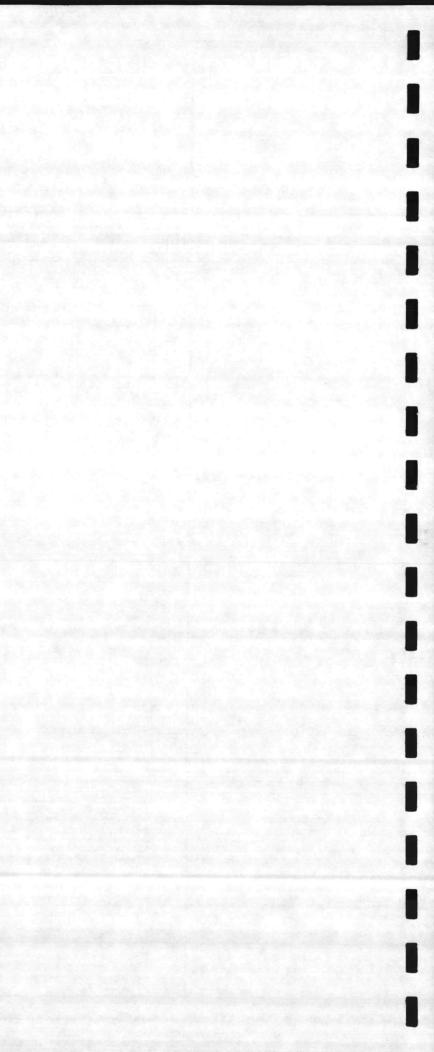
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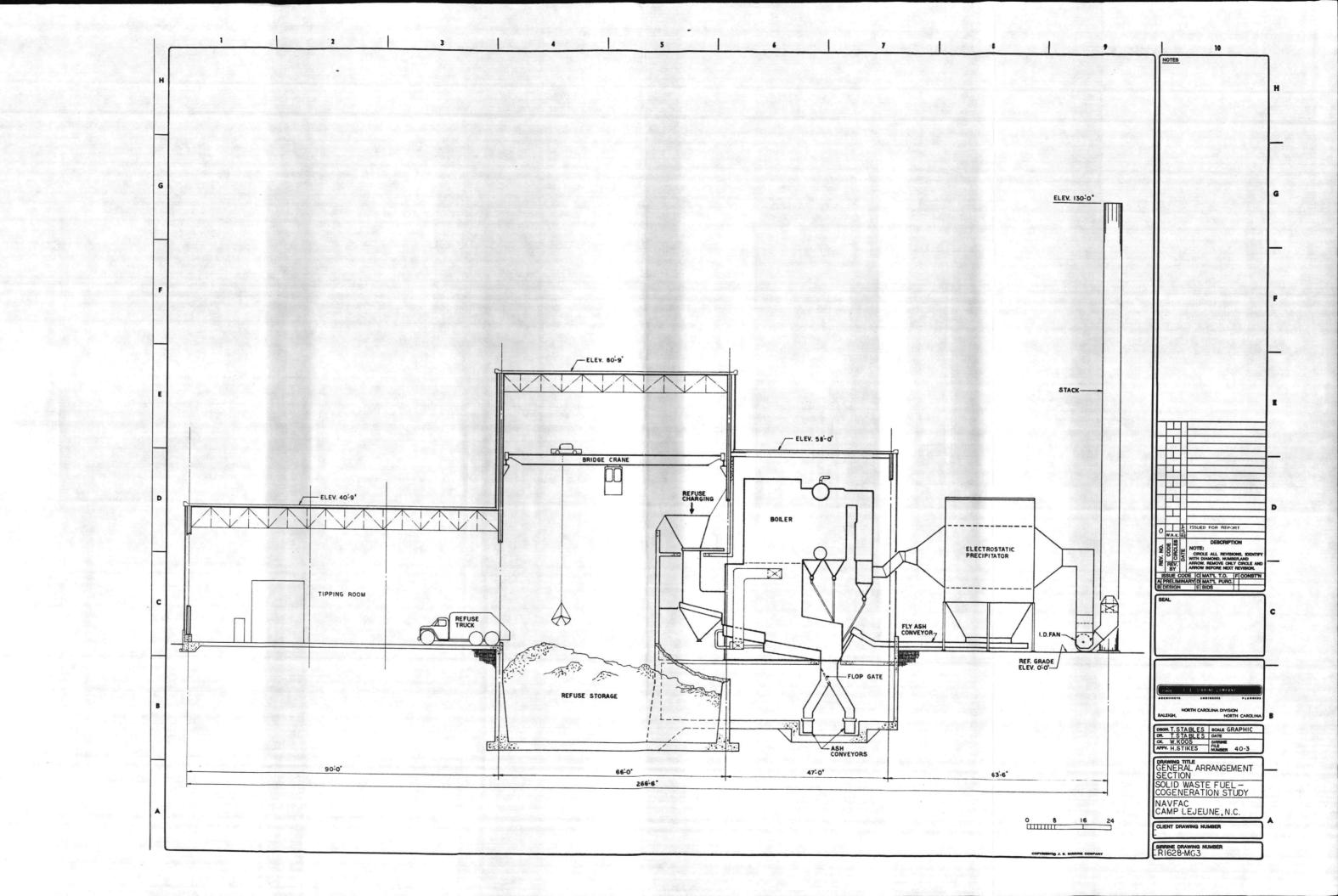
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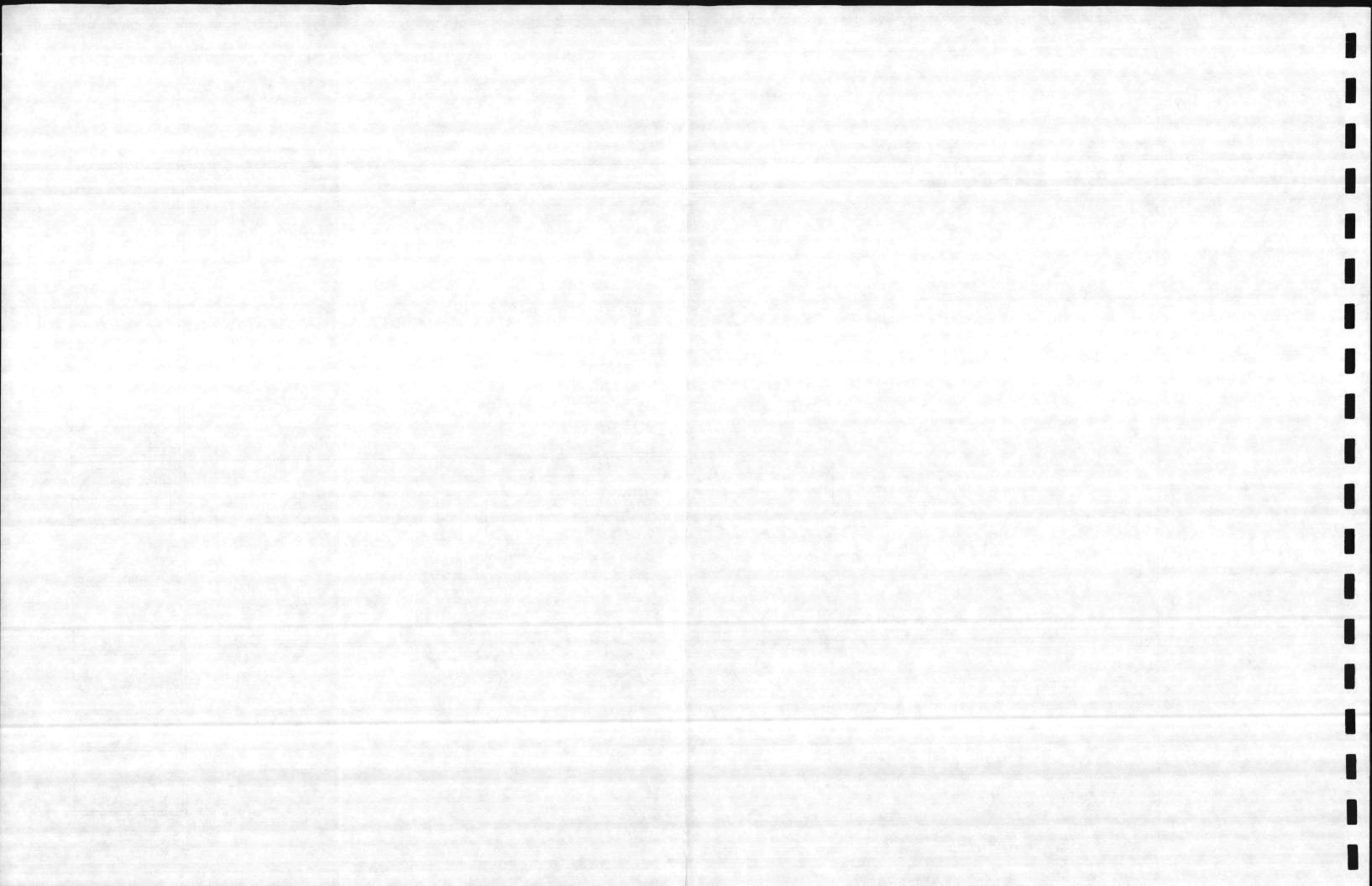
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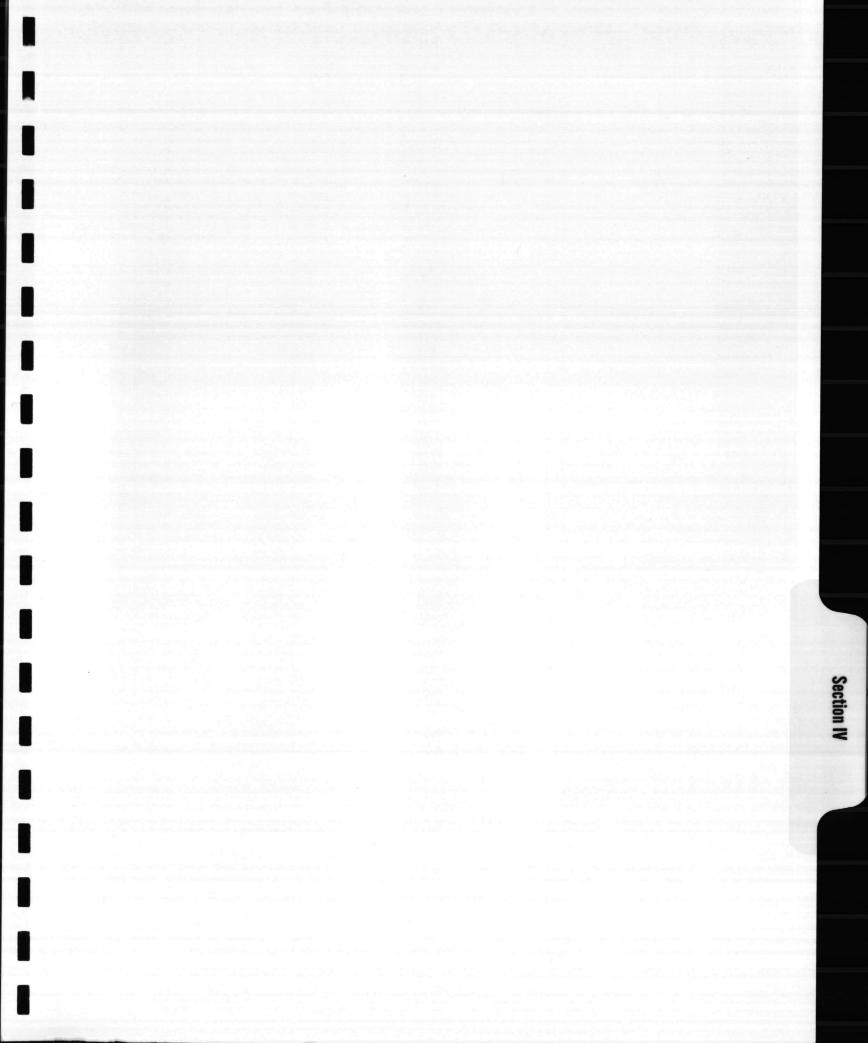


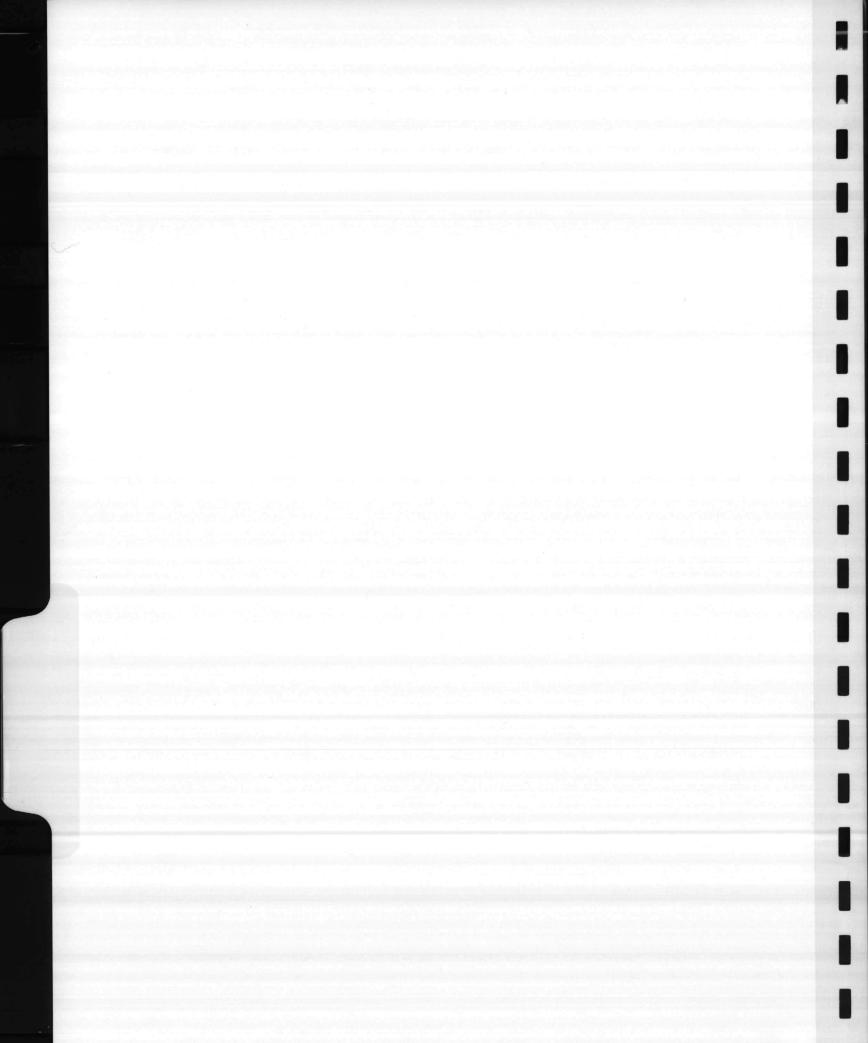


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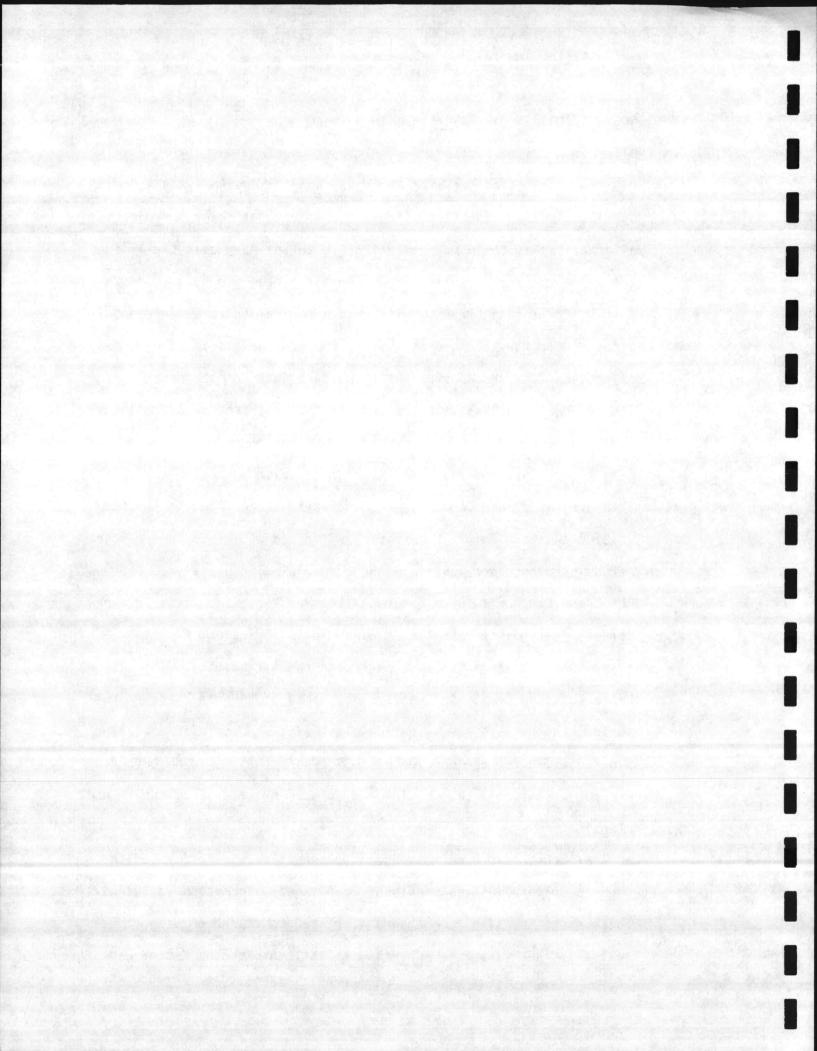
IV. COST ESTIMATING AND ANALYSIS METHODS

Life Cycle Cost Analysis

The purpose of the Life Cycle Cost and Design Analysis is to provide a method of determining which, if any, of several project alternatives is the most cost effective to the Navy over the life of the project. For these analyses, the first step was to compare the cost of the refuse plant and its design options to existing operations so the Navy can decide whether the project itself is costeffective. The second step was to compare which of the three project design options entails the least cost (highest savings) to the Navy.

At present, the Navy is disposing of solid waste in landfills at Cherry Point and Camp Lejeune, and steam is provided to the Air Station and Camp Geiger by existing oil-fired boilers. The proposed refuse plant project would use the burnable solid waste from Cherry Point and Camp Lejeune to generate steam and/or electricity in a new refuse-fired boiler, displacing a portion of the steam from the existing oil boilers at Camp Geiger and the Air Station. The Life Cycle Cost and Design Analysis, then, compares, over a 25-year period, the costs of a new refuse plant with the costs of operating two landfills for the portion of solid waste that could be burned and the cost of oil that could be displaced by steam from the refuse plant.

All costs and benefits of each alternative were estimated in today's dollars (unless previously published information was used). These costs (benefits) were then escalated to year 1 of the analysis. Year 1 of the analysis is 1987. A discount factor was then applied, with applicable differential factors, to compute the



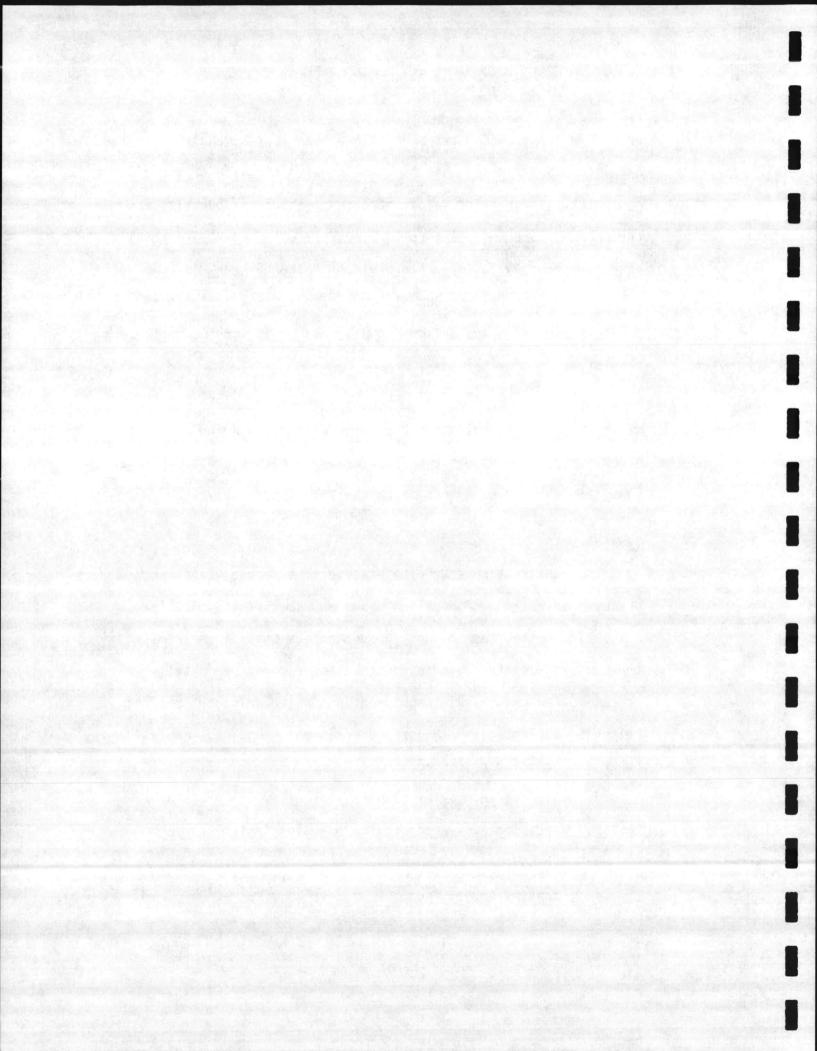
present value of each cost/benefit over the 25-year analysis period. A 25-year analysis was used to coincide with the life of the project equipment. The present values of each of the costs/benefits were then summed to provide a total project present value. The total project present value was then divided by the 25-year discount value to determine the Uniform Annual Cost. The alternative with the smallest present value uniform annual cost is the most advantageous plan of action for the Navy.

One note about the Design Analysis Computations of present value - due to the detail of the calculations, rounding was necessary for report presentation. Therefore, the products and/or sums of the numbers may not match the totals precisely.

Capital Costs

The construction cost estimates for the refuse plant were prepared in advance of detailed plans and specifications. The estimating method was to apply budget prices to an itemized list of the equipment that should be required for a complete installation. Prices for major pieces of equipment are based on quotations from reliable manufacturers. Major pieces of equipment and manufacturer's submitting prices were:

- 1. Boilers E. Keeler Company, and Riley Stoker Corp.
- 2. Precipitator Precipitair Pollution Control
- 3. Ash Handling Equipment Beaumont Birch Company
- 4. Cranes Krano, Inc.
- 5. Stack Warren Environment Co.



6. Water Treatment - Illinois Water Treatment Company

7. Turbine Generators - Trane, and Terry Turbine

Pricing of minor pieces of equipment was based on recent prices received for similar equipment on other projects.

Building and structural estimates were prepared based on preliminary arrangement drawings. Piping costs were prepared based on preliminary flow diagrams and arrangement drawings. Electrical and installation costs were derived from past projects of similar design and size.

Operating Costs

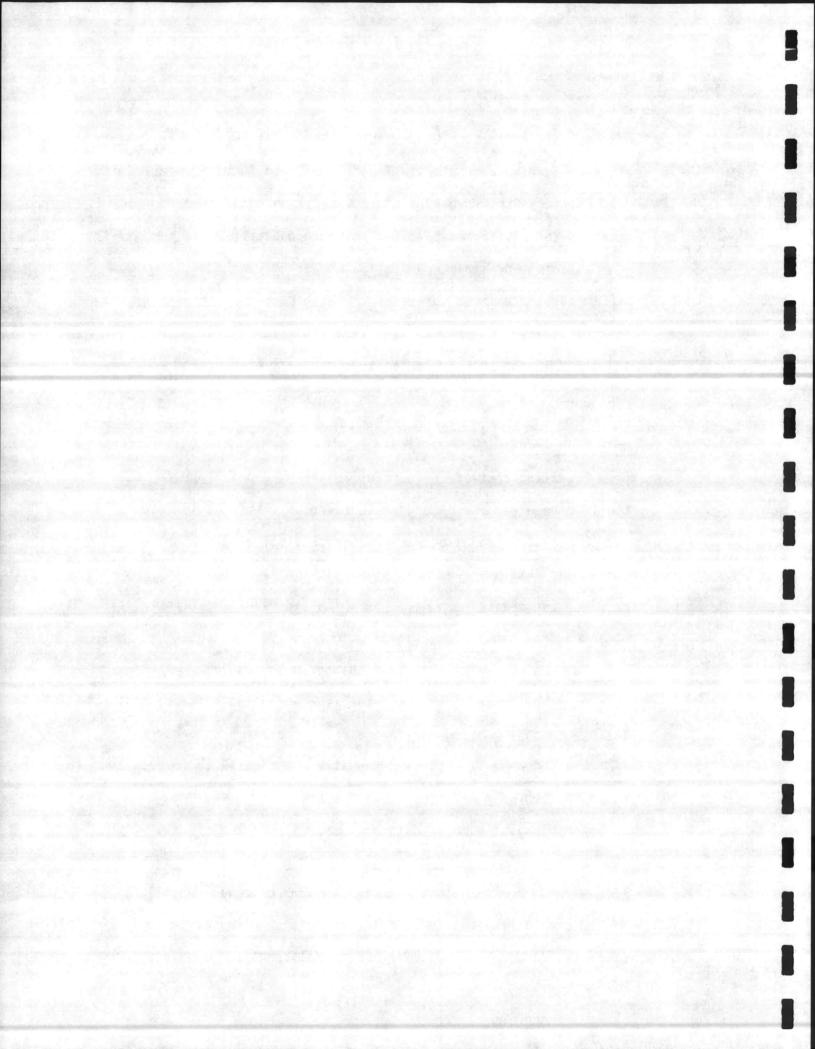
Operating costs for the refuse plant were developed for the specific requirements of each case based on the following items.

Labor -In each case a crane operator, boiler operator and boiler mechanic are required 24 hours per day. A supervisor is required two shifts each day. Salaries and classifications were obtained from Camp Lejeune, Base Maintenance Department.

Maintenance - The installed cost of major equipment items was multiplied by a use factor to obtain the annual maintenance cost. The use factor is based on Sirrine experience in the industry.

Plant Overhaul - Standard industry practice is to inspect and overhaul turbine generators every 5 years.

Ash Disposal - This cost includes \$.51 per ton of ash, which covers the operation and maintenance cost of a truck and dumpsters to haul ash from the plant site to the Camp Lejeune landfill, a distance of approximately 15 miles. The cost also includes \$8.84/hr. (source: Camp Lejeune Base Maintenance) for a part-time



employee to do the hauling. The assumptions to determine the amount of ash to be disposed of are:

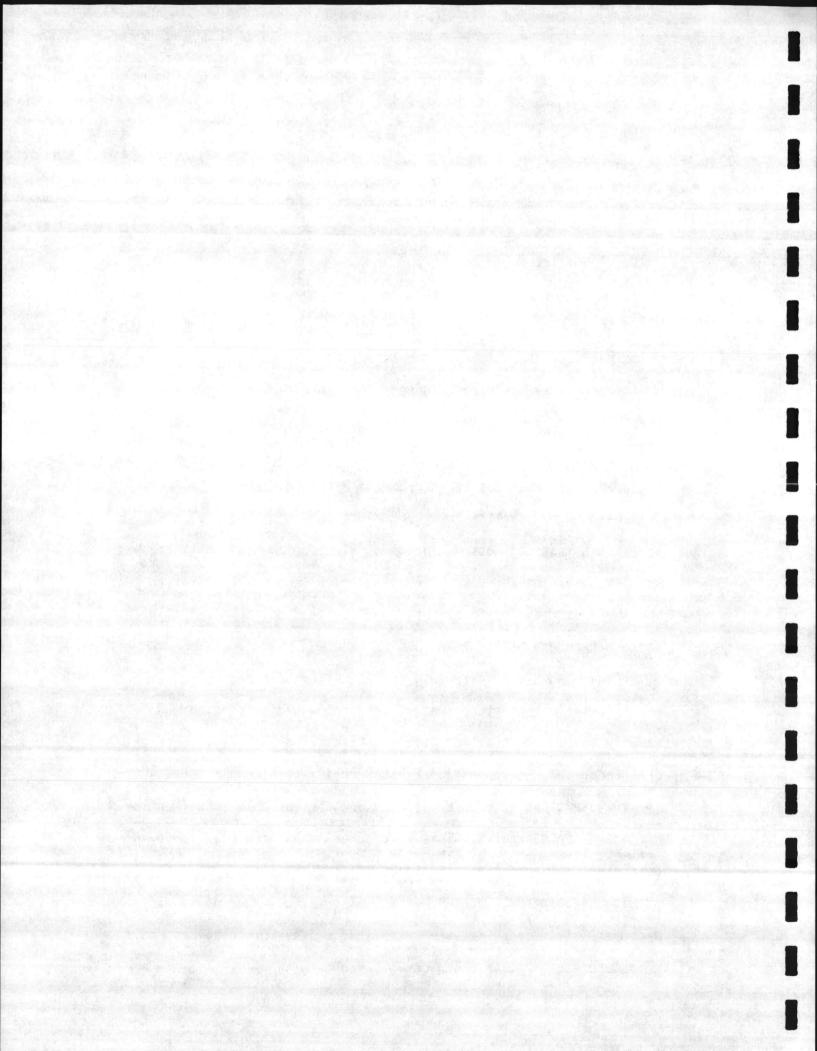
- 20% ash per ton of trash
- 80 lbs/cf
- 30% moisture
- disposal 5 days per week

Based on this data, it will take 9 trips per week until 1994 and 10 trips per week thereafter to dispose of the ash.

Incremental Electrical Costs - This cost includes the price of electricity to run equipment in the new refuse plant. Horsepower was converted to kilowatts. Both the demand and per kwh costs were included. The cost was taken from the actual rates new charged Camp Lejeune by Carolina Power and Light Co.

Trash Transfer Cost - A price of \$10 per ton (1977 dollars) was used to determine the cost of hauling trash from Cherry Point to Camp Lejeune. This price was taken directly from the SCS "Solid Waste Management Master Plan."

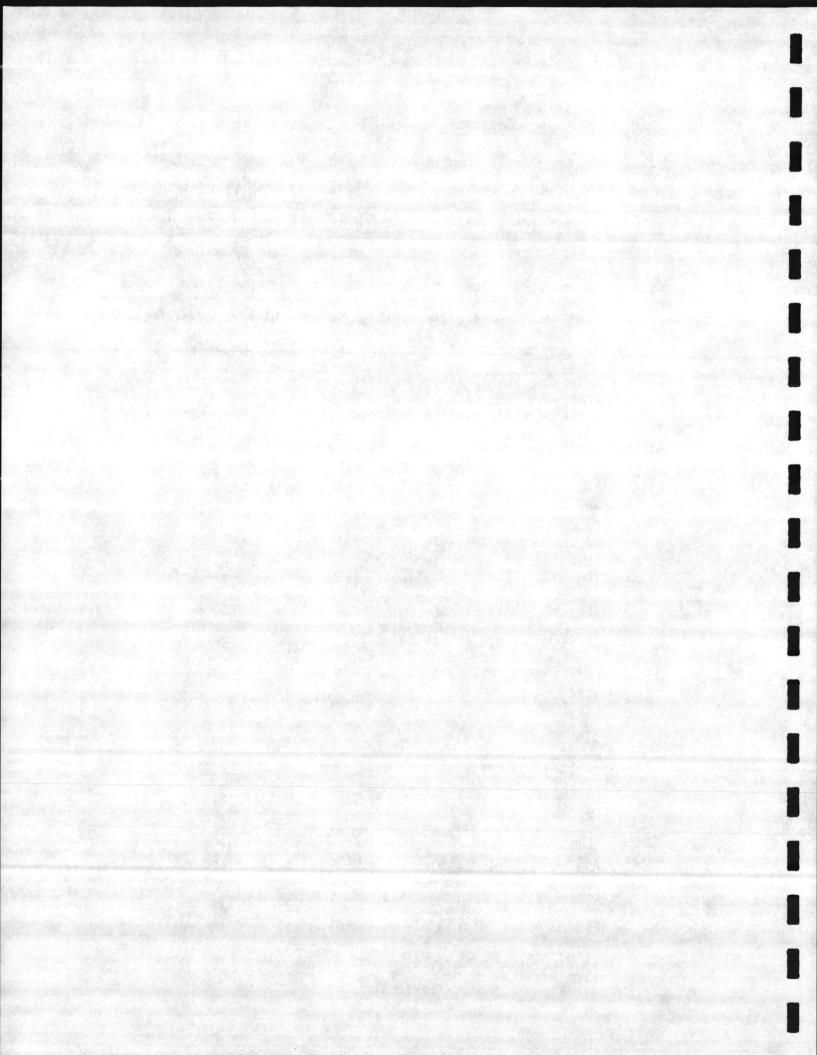
Generated Electricity Sold to CP&L - In the cases where electricity is generated, the refuse plant would be tied to the utility system and the generated electricity would be sold back to CP&L under their cogeneration avoided cost rate Schedule CSP-4. The 10-year capacity credit was used and the variable annual energy credit. (See Appendix). This rate schedule has not been approved by the NC Utilities Commission, but all indications are that it should be approved to go into effect after a full hearing in December 1982. These are the rates that CP&L is presently using to negotiate cogeneration contracts with customers.



Cost of Existing Operations

Landfills - Information from the SCS "Solid Waste Management Master Plan," 1977, was used as much as possible in determining the effects of burning trash on the landfills at Camp Lejeune and Cherry Point. The SCS report contains assumptions, recommendations, costs and schedules of development for the landfills. The principal logic used in the development of landfill costs for this design analysis is that volume reduction from burning trash has an associated cost reduction at the two landfills, taking into consideration that ash from the refuse plant would be disposed of at the Camp Lejeune landfill. Certain other factors were assumed in developing the landfill costs:

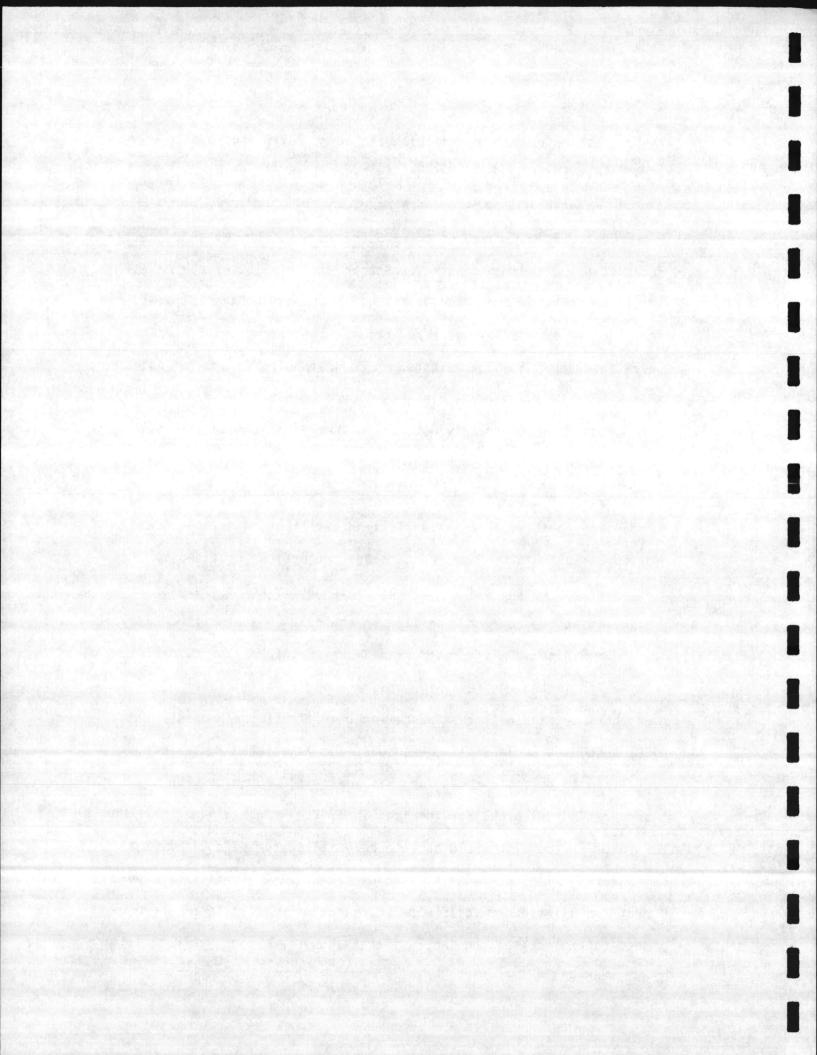
- The life of the current landfill at Cherry Point is approximately 10 years (1982-1992).
- The composition of waste at Cherry Point and Camp Lejeune remains constant over the 25-year analysis period.
- Inert waste has a density of 2000 pounds per cubic yard.
- Trash has a density of 800 pounds per cubic yard.
- Ash from burnable trash has a density of 80 pounds per cubic foot at 30% moisture.
- Inert and oversized waste will remain at Cherry Point and all burnable trash will be hauled to the refuse-burning plant throughout the life of the project.
- All costs in the SCS report are based on an average volume over the period of analysis.
- Estimated remaining life of the landfill at Cherry Point (1987-1992) would be sufficient to dispose of inerts and oversized waste for 1987-2011.



 Estimated volume reduction at Cherry Point and Camp Lejeune has a direct relationship to landfilling costs and maintenance costs at each base.

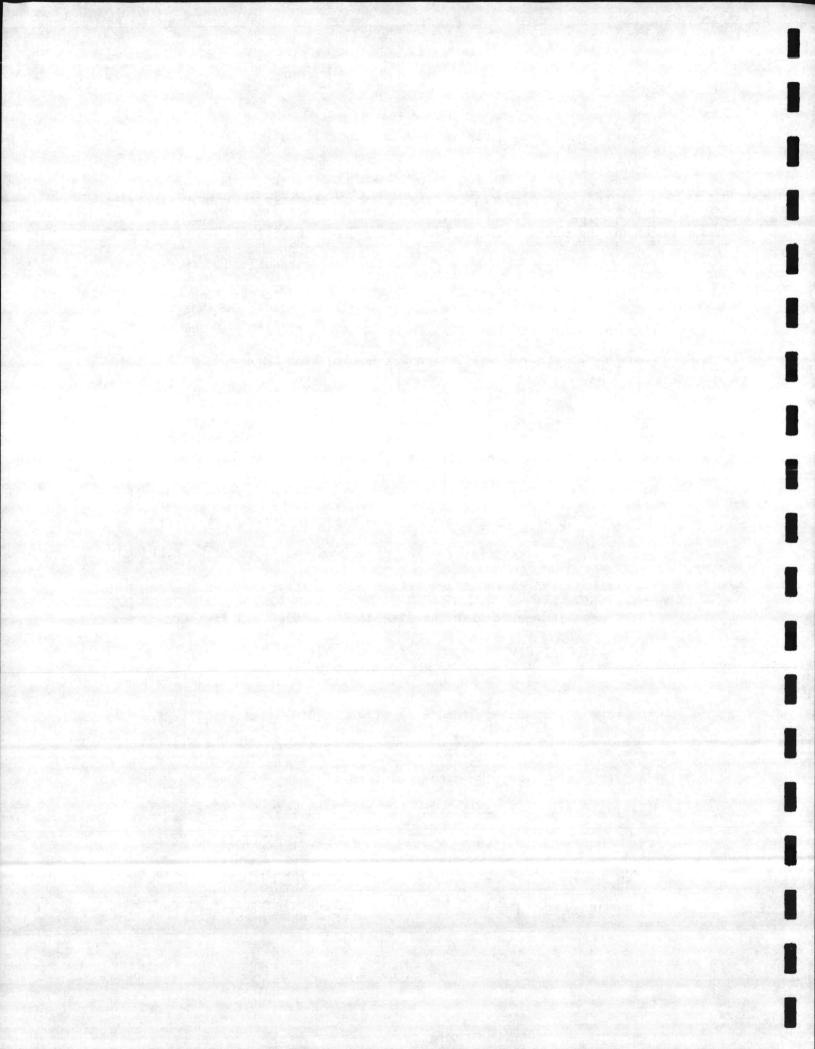
Cherry Point -Based on the SCS breakdown of the waste consistency, it was projected that approximately 15% of the waste would be inert or oversized, 75% would be burnable, and 10% would be recycled or removed by waste reduction. The percentage breakdowns were based on a tonnage weights. A corresponding volume for each projected tonnage was calculated and used to determine a volume reduction of approximately 90% at the Cherry Point landfill, based on removing the burnable trash.

Costs were estimated to be directly related to the volume reduction on items such as landfill preparation and maintenance of disposal equipment. Based on a recent projection, provided by McDowell and Jones, all of the wastes at Cherry Point could be disposed at the current landfill for the next 10 years (1982-1992). If burnable trash was removed from Cherry Point beginning in 1987, it was estimated the remaining volume would be sufficient to dispose of the inert and oversized waste for the life of the project. The SCS schedules of landfill development and associated costs were utilized to estimate costs for this analysis, beginning with the preparation of Forest Service land in 1992. It was assumed that the Forest Service site would have to be utilized beginning in 1992 if the refuse plant project is not undertaken. All landfill development and maintenance costs were increased over the life of the project to reflect the constantly increasing volume that would have to be disposed.



Camp Lejeune -Waste volumes and constituencies were estimated for Camp Lejeune using the same methodology that was applied at Cherry Point. Based on tonnage, it was estimated that approximately 72% of the waste would be burnable, 24% would be inert or oversized, and 3% would be recycled or removed by waste reduction. It was estimated that a total volume of approximately 2.6 million cubic vards would be required to dispose of waste at Camp Lejeune if the trash is not burned. If trash was burned from Cherry Point and Camp Lejeune, the estimated volume reduction would be approximately 95%. This volume reduction considered the disposal of ash in the Camp Lejeune landfill, and that some burnable trash (see Table 5) would be disposed in the landfill during plant outages of more than three days. The plant has a 3-day storage capacity for refuse. The estimated costs associated with the volume reduction at Camp Lejeune were calculated on the same basis as the costs at Cherry Point. All costs were increased over the life of the project to reflect a continual increase in volume that would have to be disposed.

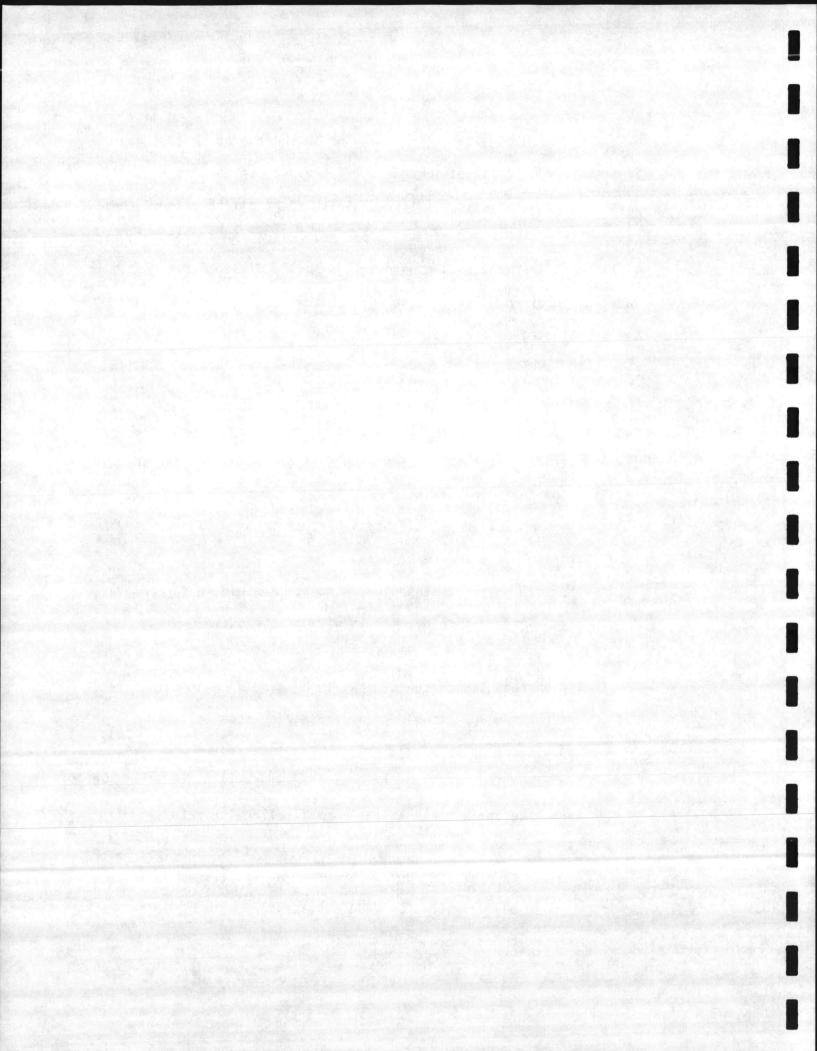
Incremental Cost of Fuel Oil -The amount of fuel oil that does not have to be burned because of steam generated by the refuse plant depends on the availability of the refuse plant. This availability, in turn, determines the number of tons of trash that can be burned. A total system availability of 80% has been assumed. The outage times used are 15% scheduled and 5% unscheduled. This works out to 7000 hours of total plant on line availability with 1320 hours of scheduled down time and 440 hours of unscheduled outage time.



The scheduled outage time would be in the summer months, May -September. The required scheduled maintenance was assumed to be 10 days per month per unit. This would give the facility a single unit capability of 100 T/D during this period. Since the storage pit was sized for only three days of storage, some landfilling of refuse would be required during a long unit outage. It was assumed that the unscheduled outages will be less than 3 days, so the pit would absorb the excess refuse. The combined unit capability of 200 T/D would give the ability to deplete the excess. There would be a use for the excess steam during these times.

To arrive at the total displaced fuel oil potential for the facility the following was assumed:

- The Camp Geiger and Air Station steam loads will increase at the same rate as the refuse.
- The 1320 hours of scheduled outage time would be spread over five months, since both units will not be out simultaneoulsy.
- The unscheduled outage time would be handled with pit storage and burning up to the design capacity of both units to deplete the excess.
- The scheduled outage would give 10-day operation at a 100 T/D burn rate and 20 days at the normal collection rate (133 T/D 1987).
 - 10 days at 100 T/D = 25,800 lb/hr of steam
 - 20 days at 133 T/D = 34,500 lb/hr of steam
 - Weighted average = 31,600 lb/hr of steam



- 31,600 lb/hr equates to 122 T/D for five months with no venting of steam. The seven winter months were assumed to be at 133 T/D. (122 x 5) + (133 x 7)/12 = 128 T/D annual burn rate. This is 96% of potential. (See Table 5).
- The design analysis will use the maximum potential hours for equivalent oil plant operation, 8760. However, the availability penalty (4%) will be taken in the tons/day actually burned. Graph 4 depicts the expected steam production plotted with historial record of the combined Camp Geiger and Air Station plants.
- The cost of the displaced No. 6 Fuel Oil is \$5.92 per MMBTU (1982 dollars).

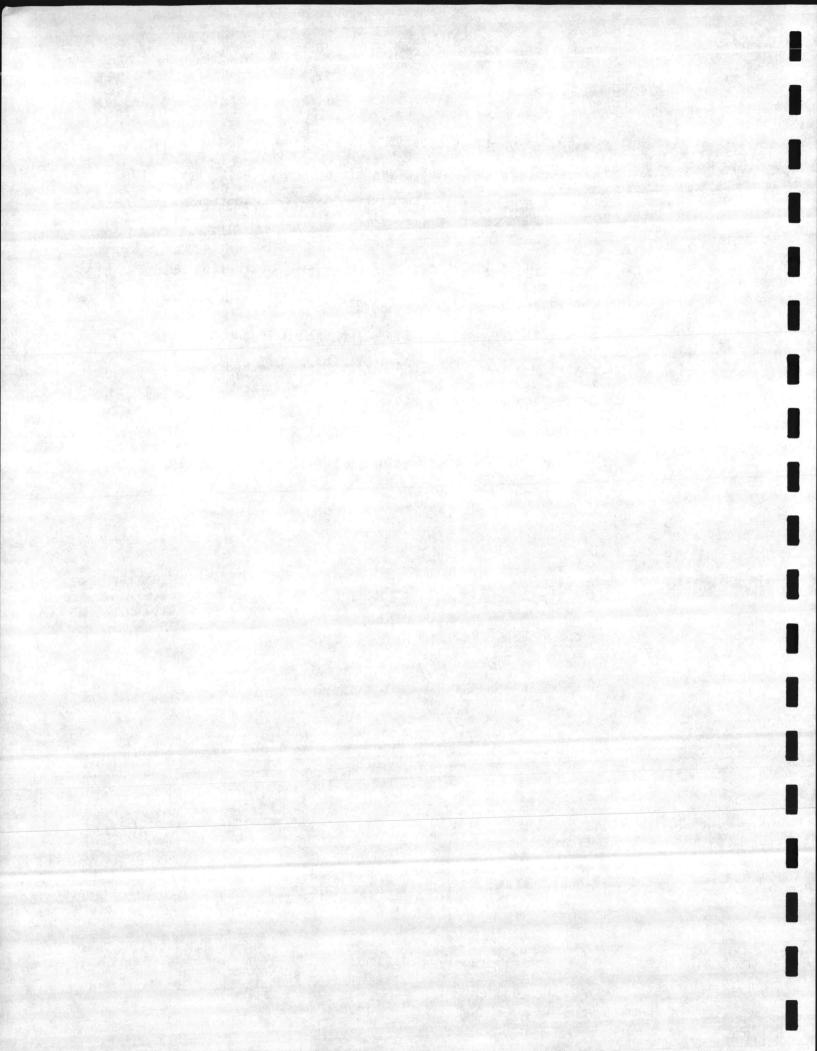
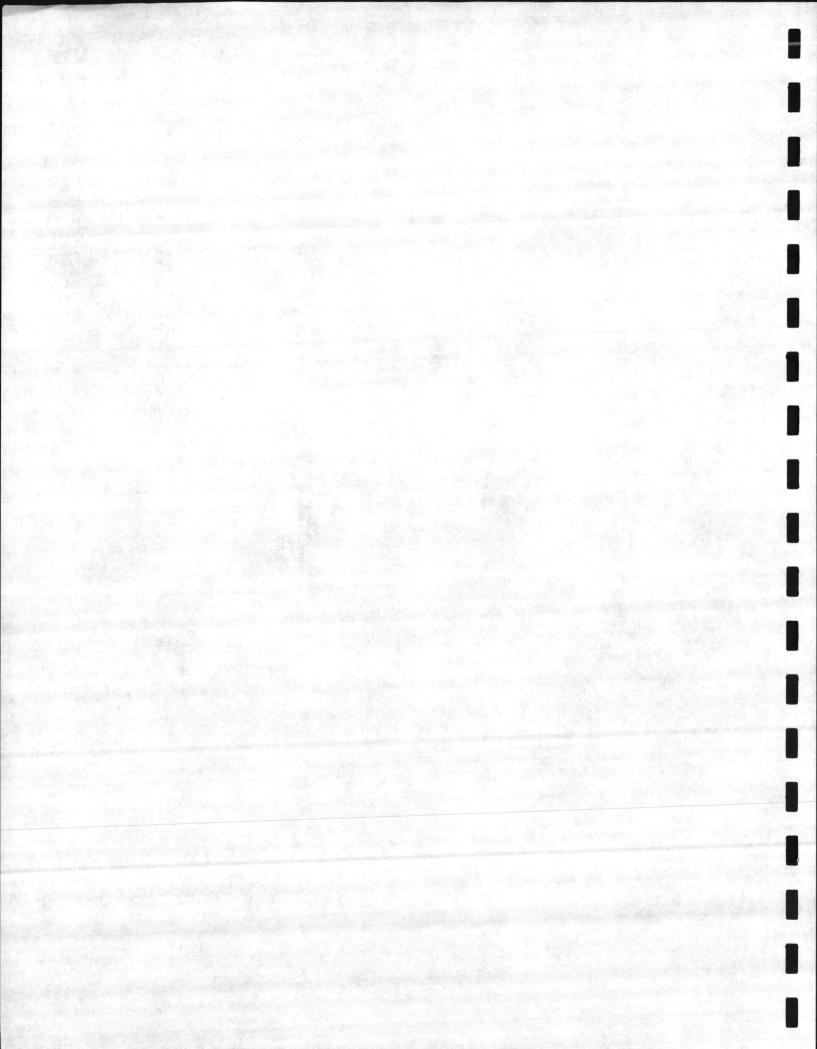
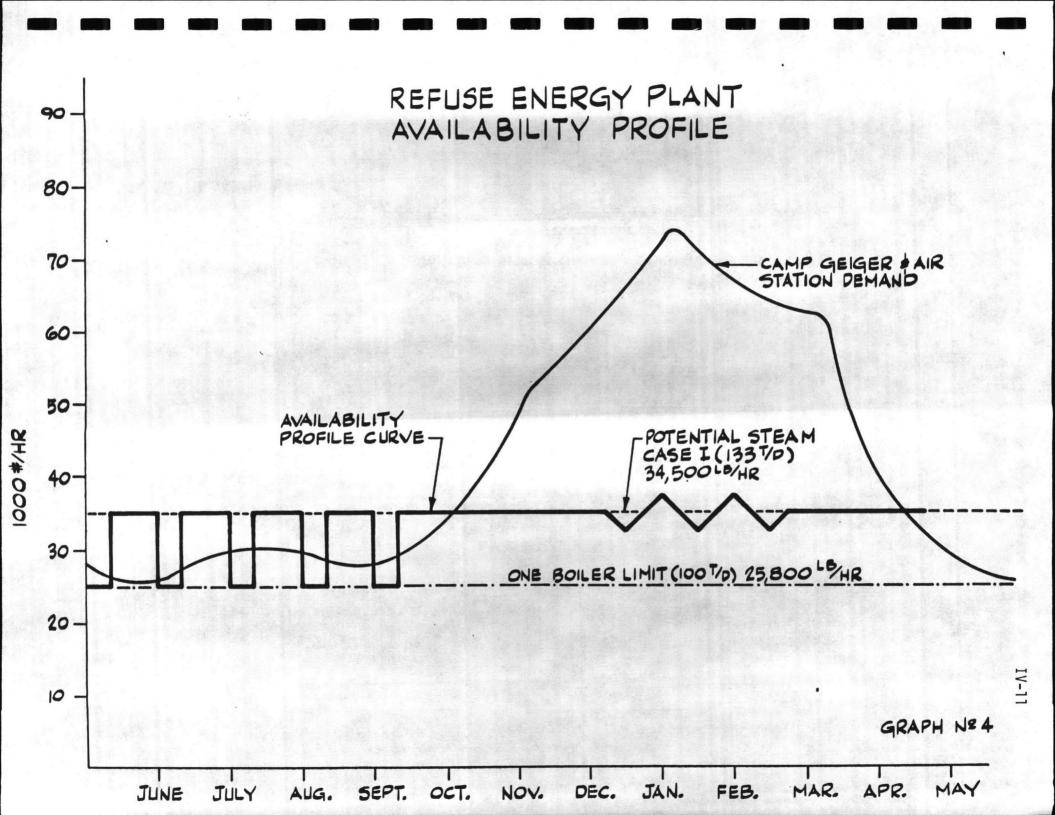


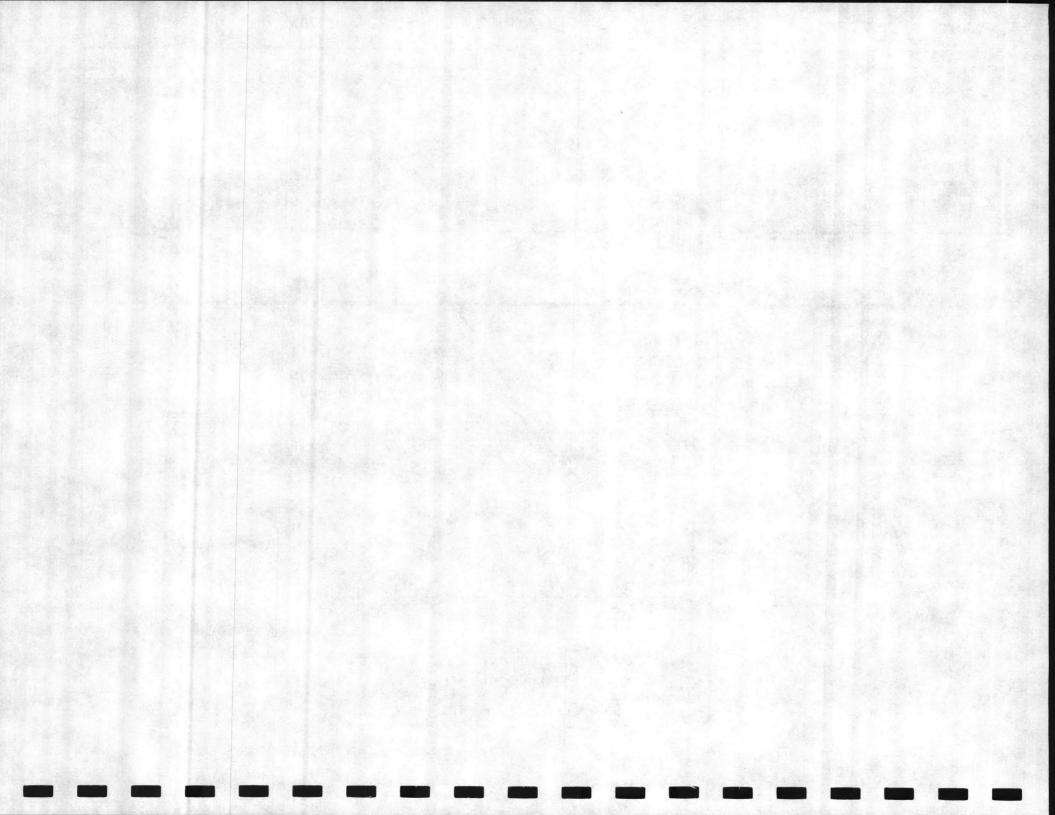
TABLE 5 TONS BURNED PER DAY

	Maximum available tons	5 month summer average *	Annual average daily capacity **	Unburned tons to landfill
1987	133	122	128	5
	134	123	129	5
	136	124	131	5
1990		125	132	5 5
1330	139	126	134	5
	140	127	135	5
	142	128	136	6
	143	129	137	6
1995		130	138	6
1330	146	131	140	6
	147	132	141	6
	149	133	142	7
	150	133	143	7
2000		134	144	7
2000	153	135	145	8
	154	136	146	8
	156	137	148	8
	157	138	149	8
2005		139	150	8 8
2000	160	140	152	8 8
	161	141	153	8
	163	142	154	9
	164	143	155	9
	166	144	157	9 9
2011		145	158	9

* 10 days at 100 tons/day 20 days at maximum availability ** (summer av. x 5) + (max. x 7) 12







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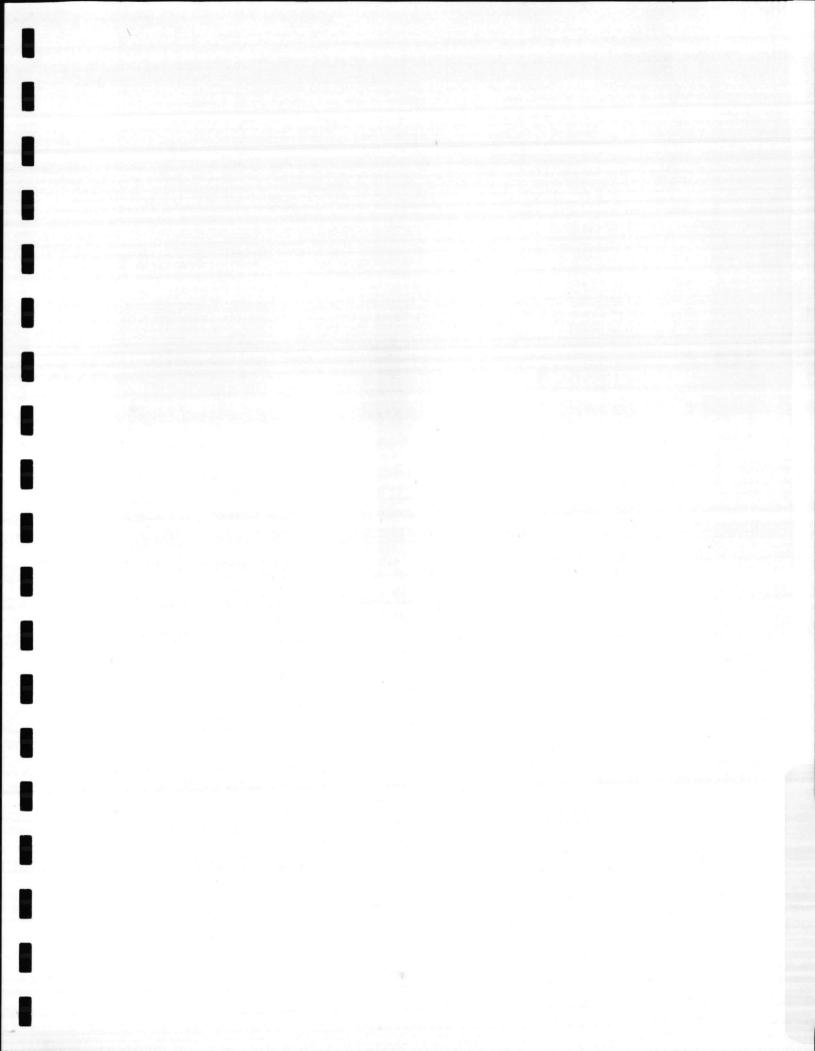
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V. CASE I - REFUSE PLANT FOR STEAM

Plant Description

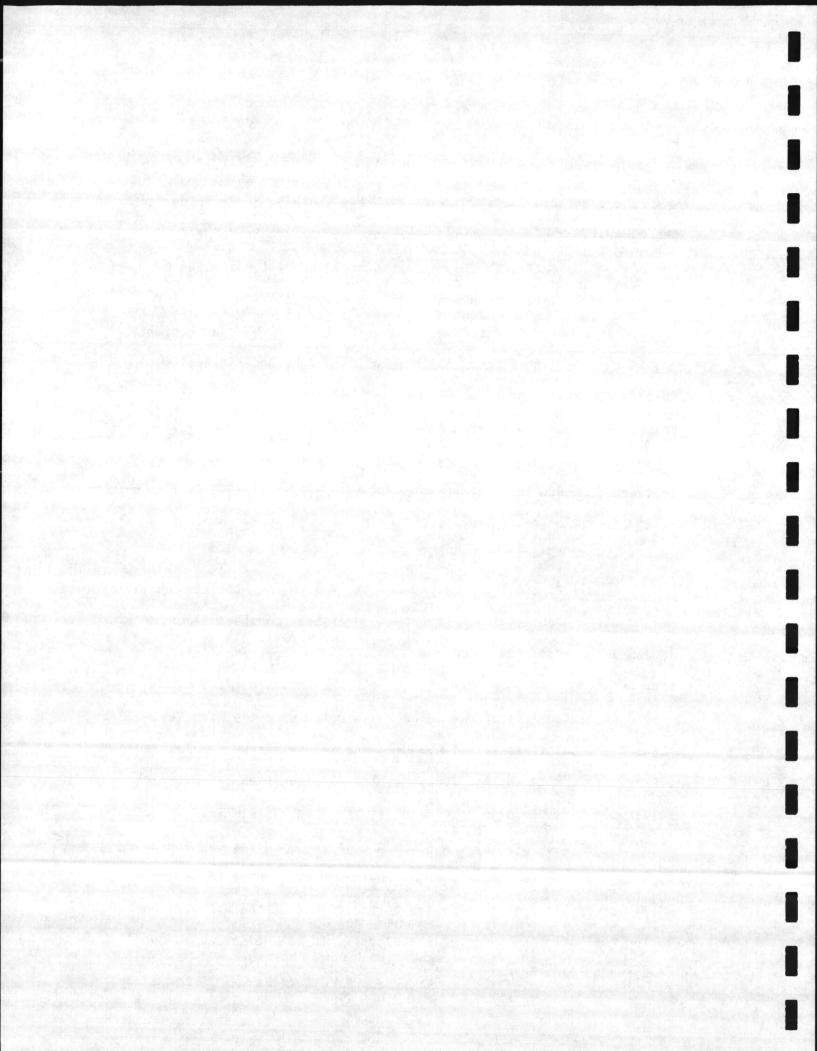
The plant configuration for this case would be as described in the general plant description. The boilers would operate at a nominal pressure of 200 PSIG saturated steam conditions. Each boiler would have an approximate maximum steam capacity of 25,800 1b/hr. This maximum output would be a function of the heat content of the refuse being fired. All numbers used for economic analysis in this report are based on 4500 Btu/lb. Ranges of higher heat values of refuse can be from 4000-6000 Btu/lb.

During initial operation of 133 tons per day of refuse delivered, 34,500 lb/hr of steam could be generated. This is based on a 70% boiler efficiency. The details of this cycle are shown on Drawings MX1 and MF1.

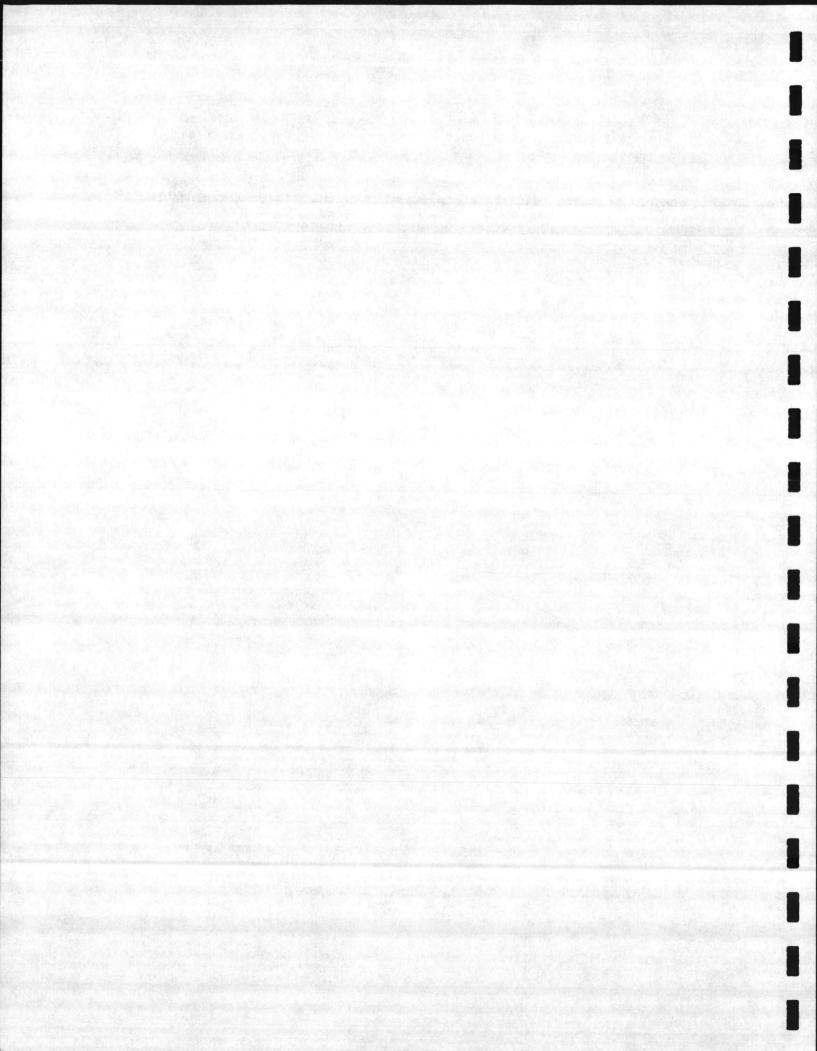
Steam lines would be run approximately 2100 feet to the Camp Geiger steam plant and 6500 feet to the Air Station steam plant. Pressure control valves would be used at each respective location to provide steam conditions compatible with the existing systems.

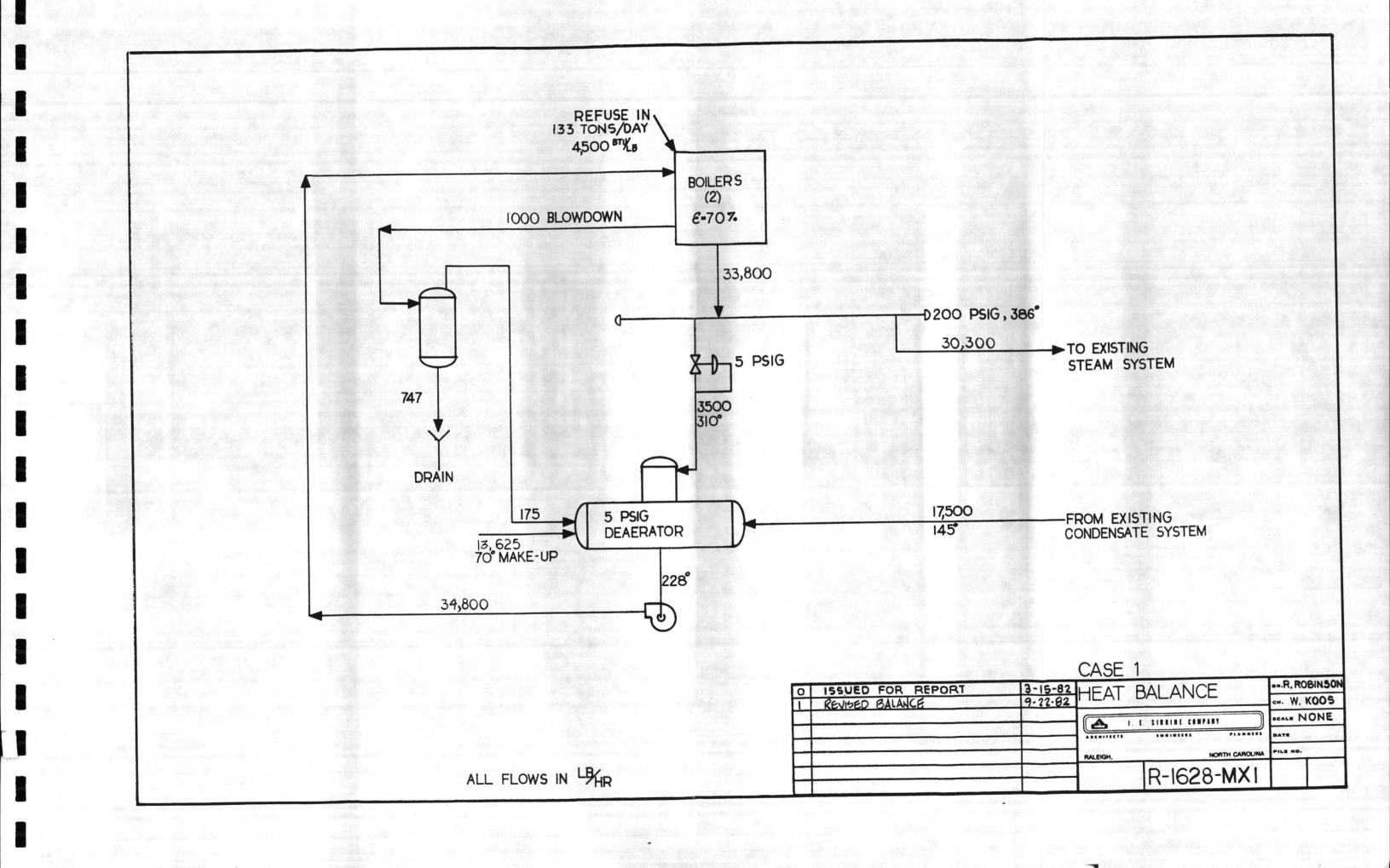
A suggested mode of operation would be to have the Camp Geiger steam needs satisfied at all times by the refuse energy complex and the excess sent to the Air Station. This is suggested since the Geiger plant is the older site and has the larger steam load.

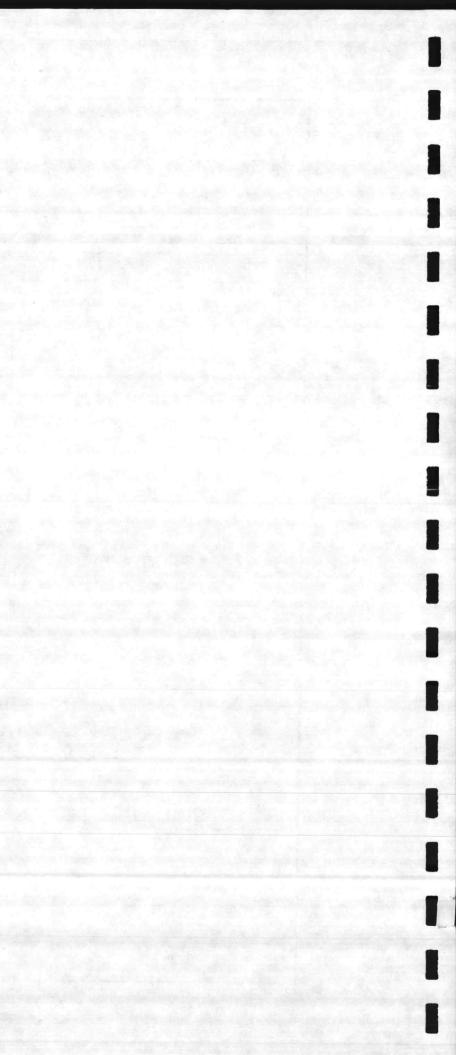
The average steam usages are shown in Tables 3 and 4 and Graphs 1, 2, and 3. As can be seen from Graph 3, during September through April, the oil boilers would have to be on line at the Air Station. During the months of December and January, an oil boiler would be required at Camp Geiger.

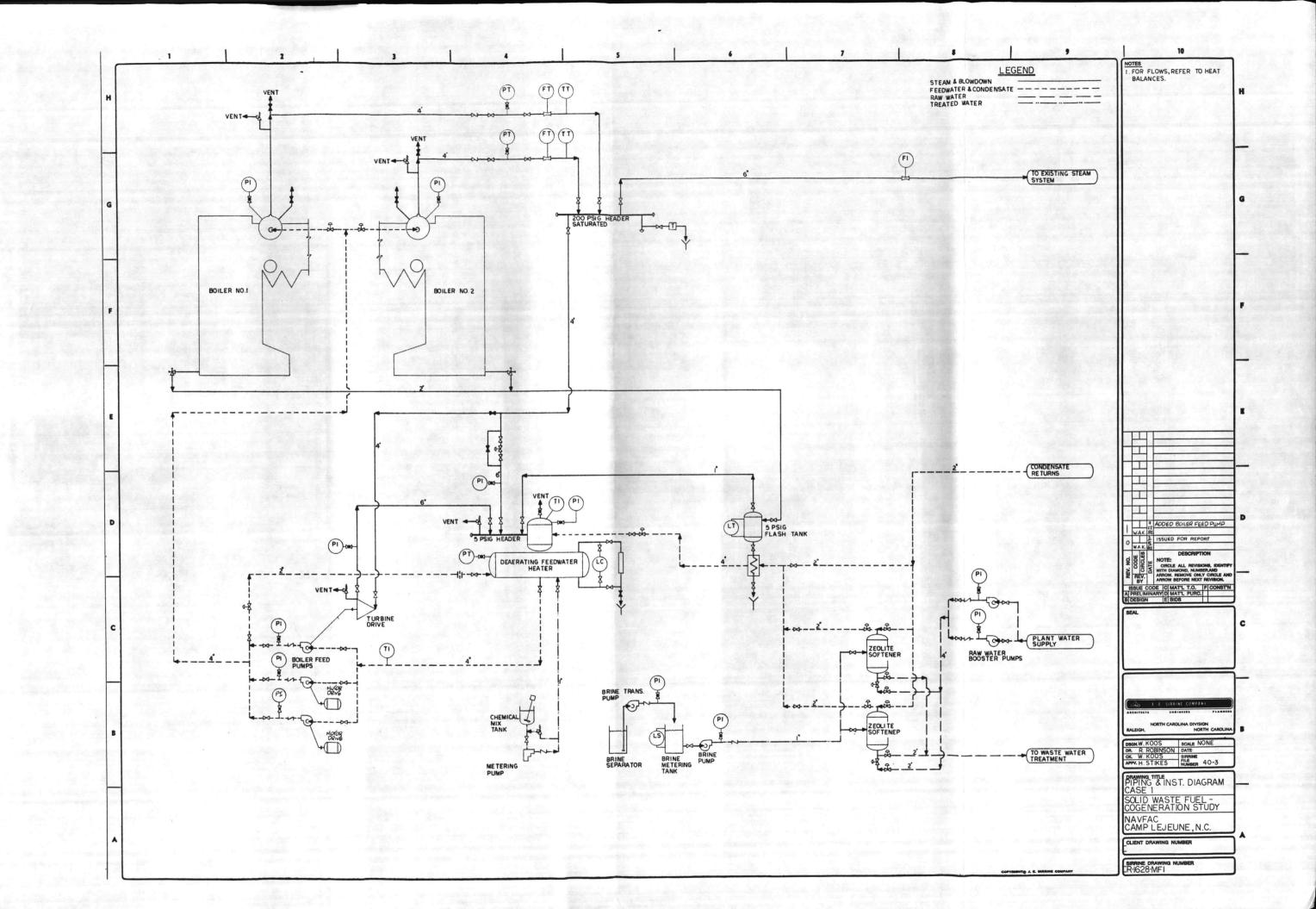


Condensate returns would be as they are at the present time. A new pump would be installed at each site and condensate lines would be run from the respective steam plants to a collecting tank in the refuse energy plant.

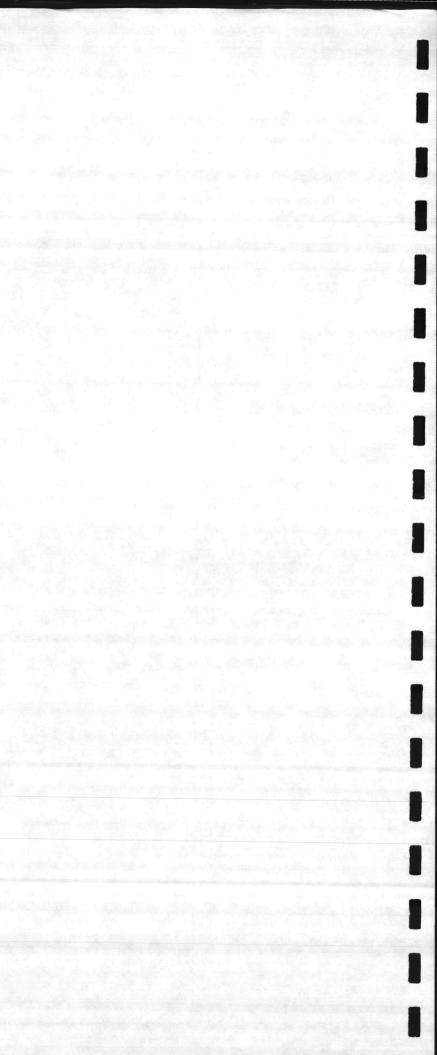








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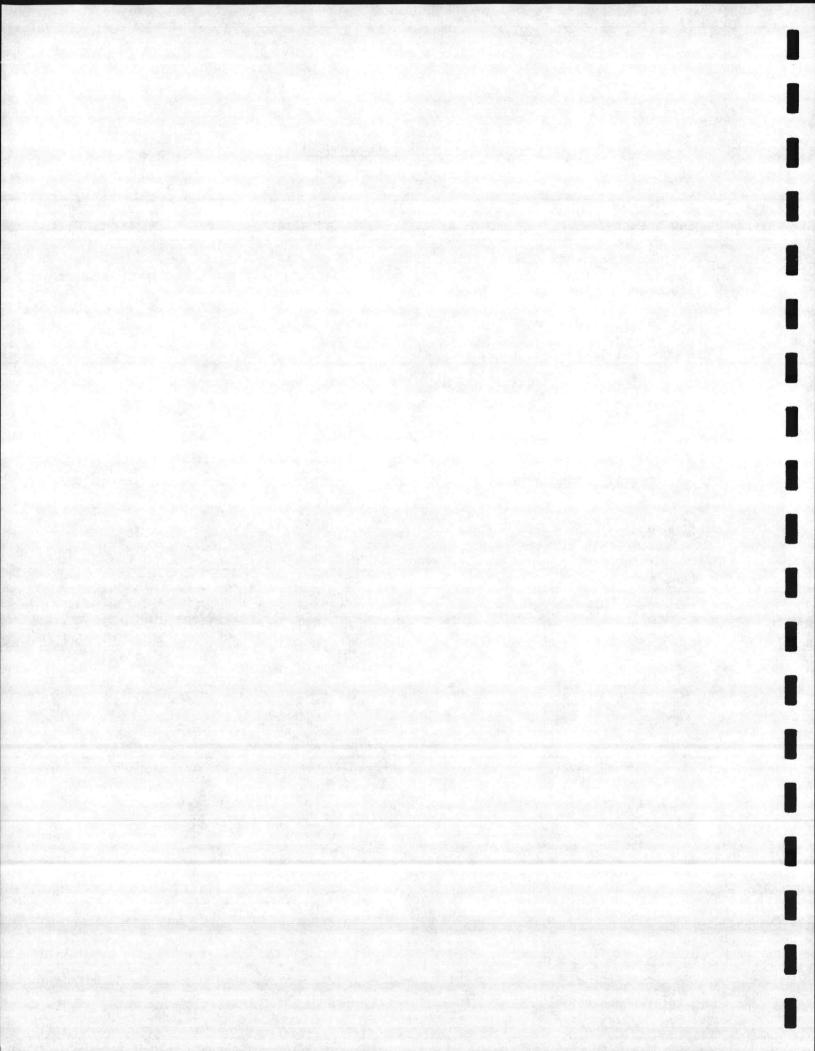
Cost Estimate

DEPARTMENT DIRECT COST SUMMARY

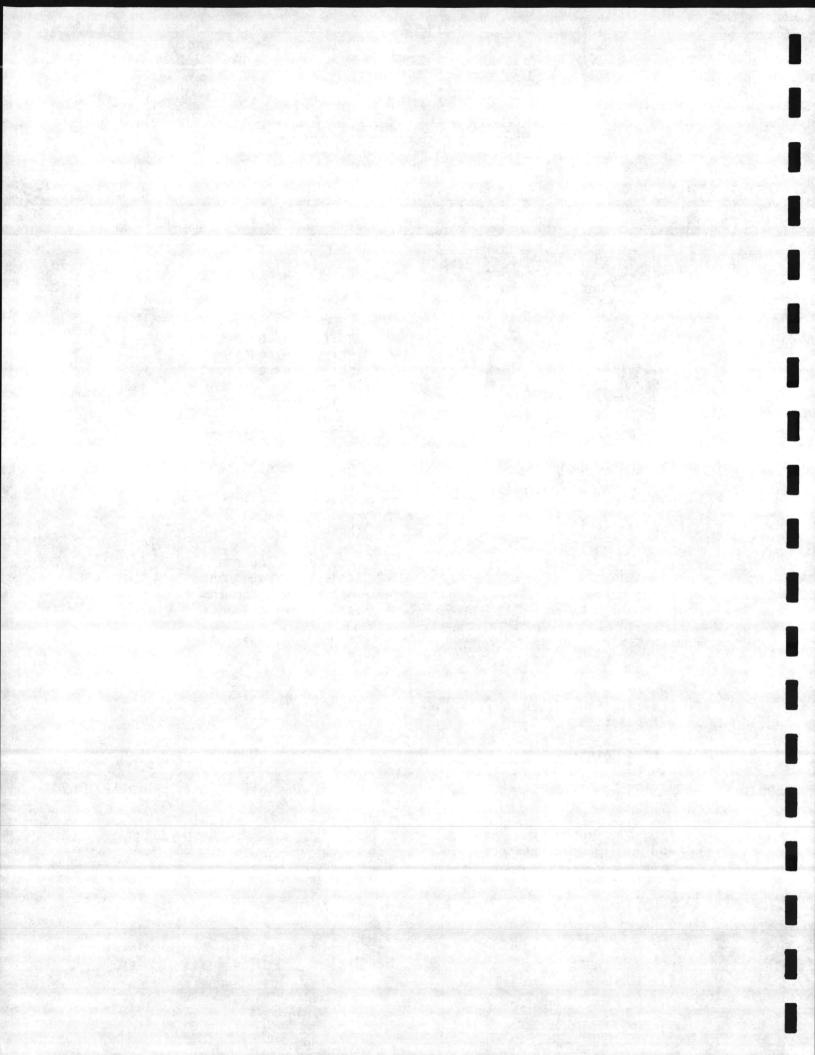
CASE I - STEAM ONLY

Equipment	\$ 6,481,000	
Equipment Erection	124,600	
Equipment Foundations and Other Costs	289,400	
Buidings & Structures	3,400,000	
Electrical Installation Cost	338,000	
Instrumentation Installation Cost	200,000	
Piping Cost	2,116,000	
Area Cost	380,000	
SUBTOTAL CONSTRUCTION COST		\$ 13,329,000
SIOH @ 5.5% (Supervision, inspection & overhead)		733,000
Contingency @ 10%		1,406,200
TOTAL CONSTRUCTION COST		\$ 15,468,300

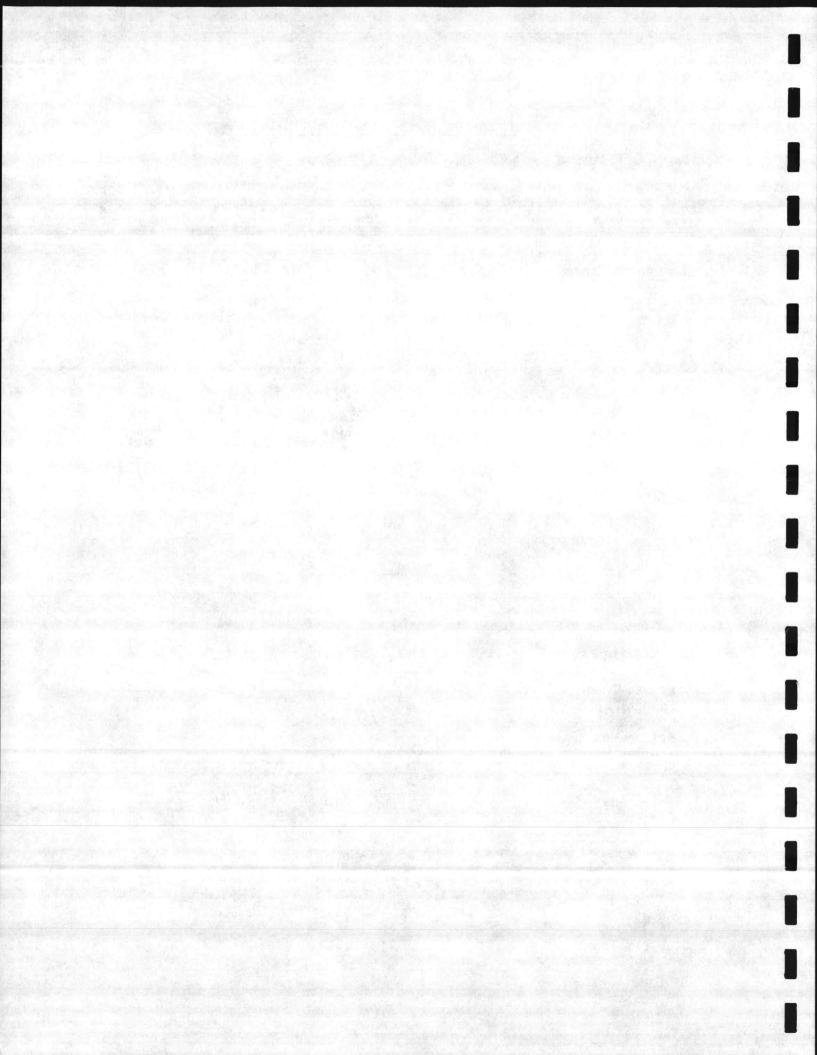
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ASI	<u>I</u>	Motor		Equipment	Equip. Supports Platforms and
	Item Description	HP-RPM	Equipment	Erection	Other Costs
			\$	\$	\$
1.	Boiler, 100 T/D Maximum Input 250 PSIG Design Pressure Unit No. 1		1,625,500	w/Equipment	w/Bldg. Cost
2.	F.D. Fan		Incl.	w/Equipment	
	Coupling		Incl.	w/Equipment	
	Controls		Incl.	w/Equipment	
	Motor	50	Incl.	w/Equipment	
	Intake Silencer		Incl.	w/Equipment	
3.	Combustion Controls		Incl.	w/Equipment	
4.	Boiler Breeching		Incl.	w/Equipment	w/Bldg.
5.	Economizer		Incl.	w/Equipment	w/Bldg.
6.	Stoker	10	Incl.	w/Equipment	w/Boiler
7.	I.D. Fan		Incl.	w/Equipment	7,000
	Coupling		Incl.	w/Equipment	
	Fluid Drive		Incl.	w/Equipment	
	Motor	75	Incl.	w/Equipment	
8.	Precipitator No. 1		600,000	w/Equip. Co	st 20,000
9.	Ductwork -				
	To Precip., Fan, Stack w/Insulation		45,000	D&E	65,000
0.	Expansion Joints		12,000	2,000	N/A
1.	Isolation Damper	5	28,000	2,000	Incl.
2.	Boiler, 100 T/D Maximum Input 250 PSIG Design Pressure Unit No. 2		1,625,500	w/Equip. Co	st w/Bldg.
3.	F.D. Fan		Incl.	Incl.	4,000
	Coupling		Incl.	Incl.	Incl.
	Controls		Incl.	Incl.	Incl.
	Motor .	50	Incl.	Incl.	Incl.
	Intake Silencer		Incl.	Incl.	Incl.

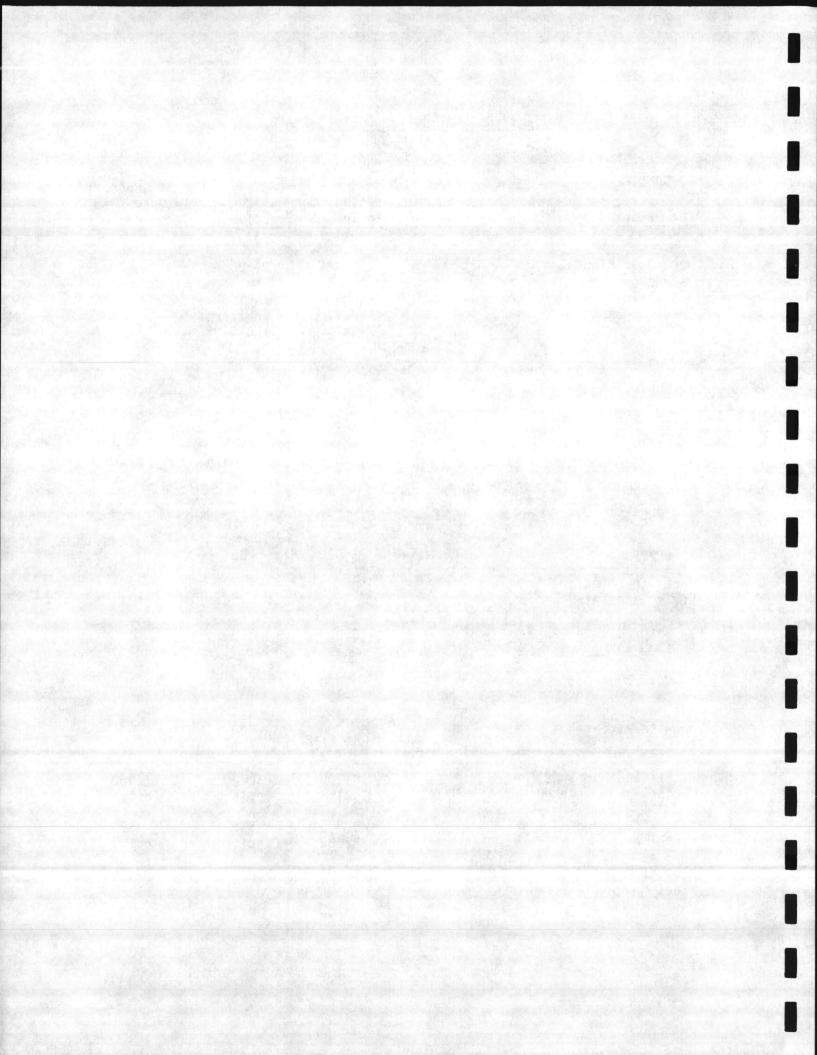


	<u>JIPMENT LIST</u> <u>SE I</u> <u>Item Description</u>	Motor HP-RPM	Equipment \$	Equipment Erection \$	Equip. Supports Platforms and Other Costs \$
14.	Combustion Controls		Incl.	Incl.	
15.	Boiler Breeching		Incl.	Incl.	w/Bldg.
16.	. Economizer		Incl.	Incl.	w/Bldg.
17.	. Stoker	10	Incl.	Incl.	w/Boiler
18.	. I.D. Fan Coupling Fluid Drive Motor	75	Incl. Incl. Incl. Incl.	Incl. Incl. Incl. Incl.	7,000
19.	. Precipitator No. 2		600,000	Incl.	20,000
20.	 Ductwork - To Precip., Fan, Stack w/Insulation 		45,000	D&E	65,000
21.	. Expansion Joints		12,000	2,000	N/A
22	. Isolation Damper	5	28,000	2,000	N/A
23	. Ash Handling System	80 (Total)	575,000	Incl.	w/Bldg.
24	 Overhead Crane - 5 Ton Control Cab Grapple Bridge Motor Trolley Motor Hoist Motors (2) 	15 10 10 (Ea)	375,000 Incl. Incl. Incl. Incl. Incl.	50,000	w/Bldg.
25	 Spare Crane Control Cab Grapple Bridge Motor Trolley Motor Hoist Motors (2) 	15 10 10 (Ea)	375,000 Incl. Incl. Incl. Incl. Incl.	50,000	w/Bldg.
26	. Deaerator		30,000	2,000	1,300
27	. Blow-Off Tank		5,000	1,000	100

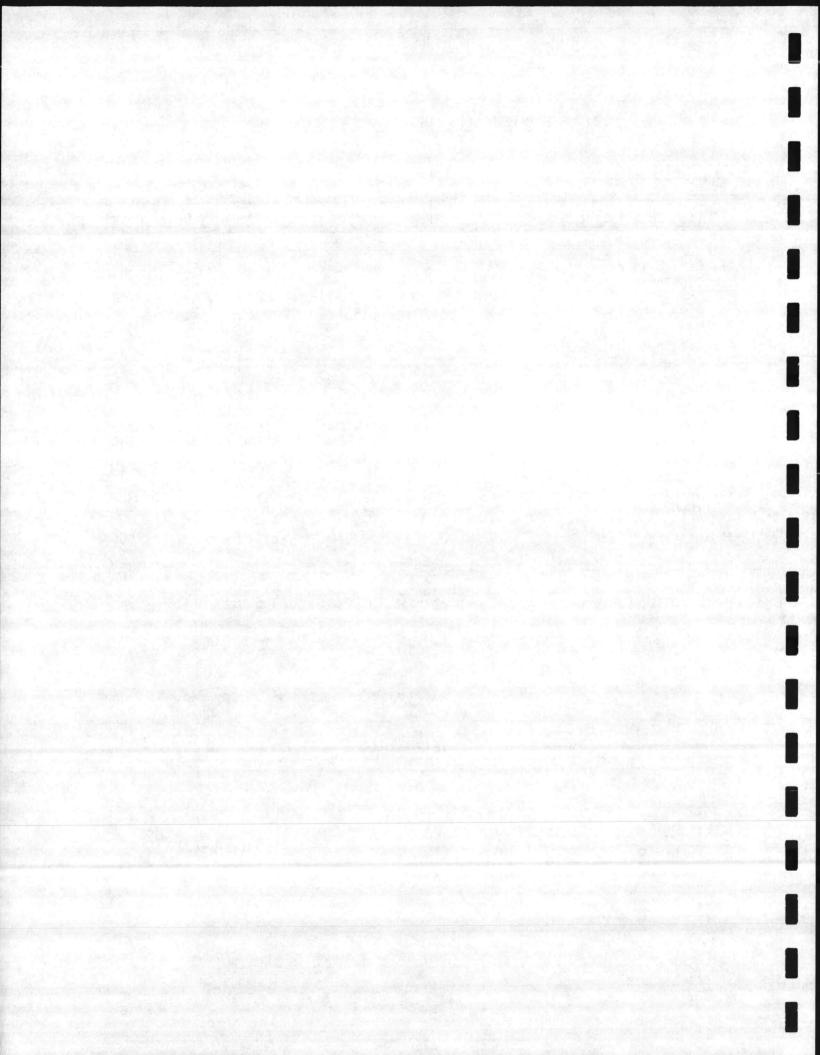


EQUIPMENT LIST CASE I

CAS	<u>Item Description</u>	Motor HP-RPM	Equipment \$	Equipment Erection \$	Equip. Supports Platforms and Other Costs
28.	Continuous Blowdown System		16,500	2,500	500
	Flash Tank Heat Exchanger Valves		Incl. Incl. Incl.	Incl. Incl. Incl.	
29.	Condensate Tank		15,000	1,000	100
30.	Condensate Transfer Pump Motor	10	3,000 Incl.	500 500	200 200
31.	Air Compressor Air Receiver	25	6,000 Incl.	500	200
32.	Air Compressor Air Receiver	25	6,000 Incl.	500	200
33.	Air Dryer		3,000	200	100
34.	Stack - Dual Wall (2) 150' x 9'-0" Dia.		310,000	Incl.	90,000
35.	Raw Water Booster Pump Motor	20	3,000 Incl.	500 Incl.	100 Incl.
36.	Raw Water Booster Pump Motor	20	3,000 Incl.	500	100
37.	Feedwater Treatment Equipment	30 Total	35,000	2,000	1,000
38.	Boiler Feed Pumps (2) Motor	2 @ 50	10,000 Incl.	10,000 Incl.	1,000 Incl.
39.	Boiler Feed Pump Turbine		5,000 8,000	500 Incl.	500 Incl.
40.	Chemical Feed Equipment	2 @ 5	5,000	800	300

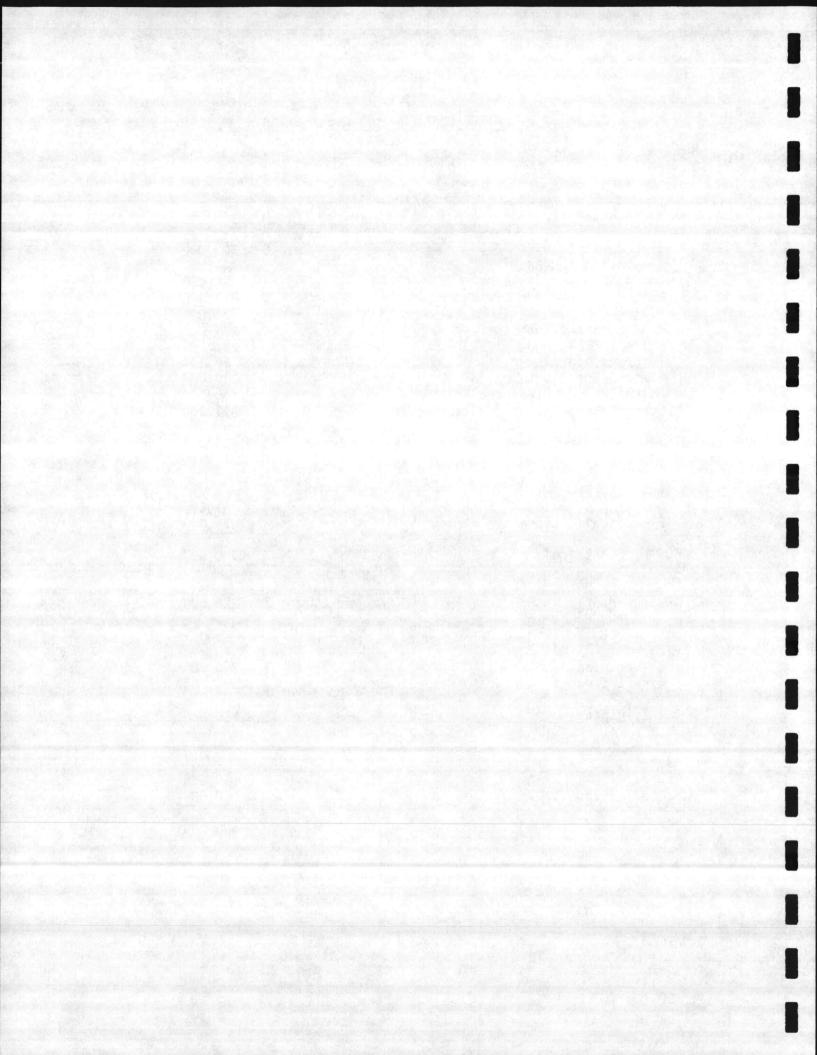


EQU CAS	IPMENT LIST E I	Motor		Equipment	Equip. Suppor Platforms ar	
	Item Description	HP-RPM	Equipment \$	Erection \$	Other Costs	
41.	Camp Geiger Condensate Transfer Pump Motor	30	7,000 Incl.	500 200	100 Incl.	
42.	Air Station Condensate Transfer Pump Motor	50	7,000 Incl.	500 200	100 Incl.	
43.	Condensate Collection Tank Pump Motor	10	15,000 3,000 Incl.	500 200 Incl.	200 100 Incl.	
44.	No. 2 Oil Storage Tank 10,000 Gallon		25,000	500	500	
45.	HVAC Equipment	20	15,000	Incl.	500	
	TOTAL, Equipment		\$6,481,000	\$124,600	\$289,400	



CASE I

46. Buildings and Structures Structural Steel \$ 800,000 Excavation and Backfill 445,000 Refuse Pit and Basement 690,000 Mat 313,000 Piling 66,000 Roof Deck and Roofing 179,000 Walls and Siding 242,500 Intermediate Floors 68,500 Stairs, Doors and Drains 110,000 Miscellaneous Steel and Grating 115,000 Support Steel and Miscellaneous 371,000 TOTAL, Building and Structures \$ 3,400,000 47. Electrical Building Lighting \$ 63,000 Electrical Equipment & Wiring 275,000 TOTAL, Electrical \$ 338,000 48. Instrumentation \$ 200,000 49. Piping Boiler Plant 740,000 \$ Export Steam & Condensate Return Lines 1,376,000 TOTAL, Piping \$ 2,116,000 50. Area Area \$ 130,000 Road Paving 250,000 TOTAL, Area \$ 380,000



CASE 1

DESIGN ANALYSIS COMPUTATIONS

JANUARY 1982

(Present Value = 1987 Dollars)

ALTERNATIVE A - Refuse-Burning Plant

- 1. Investment Cost
 - a. Refuse-Burning Plant Capital Costs (from equipment list)

Construction	\$ 13,329,000
SIOH @ 5.5%	733,000
Contingency @ 10%	1,406,200

Total Unescalated Construction \$ 15,468,300

Total Construction escalated to April 1985 \$ 15,468,300 x 2384 = \$ 19,186,500 1922

> 10% Discount (2% differential) 1.1 Present Value Construction Cost

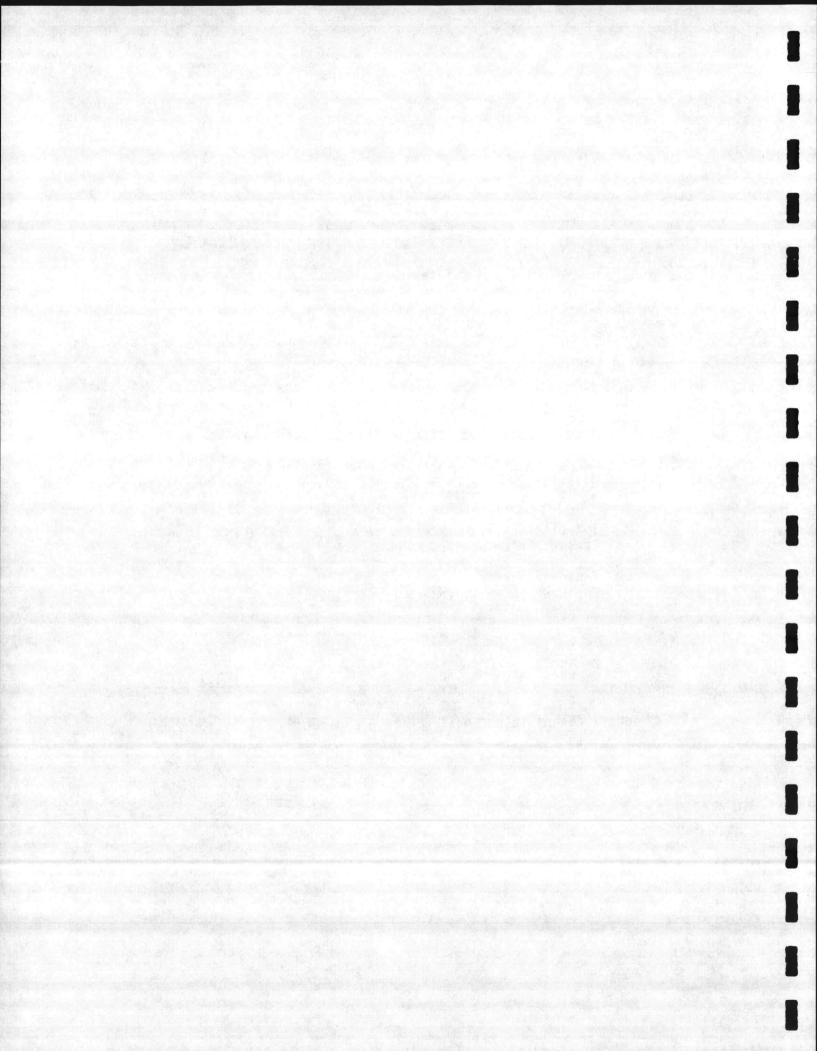
1.1198 \$ 21,485,042

Engineering @ 6% = \$ 928,100 Engineering escalated to April 1984 \$ 928,100 x 2253 = \$ 1,087,900 1922

10% Discount (2% differential) Present Value Engineering

1.2071 \$ 1,313,204

Total Present Value Construction & Engineering \$ 22,798,246



Investment for truck (\$70,000) and 5 disposal containers (\$26,000) \$96,000 in years 1, 9, 17

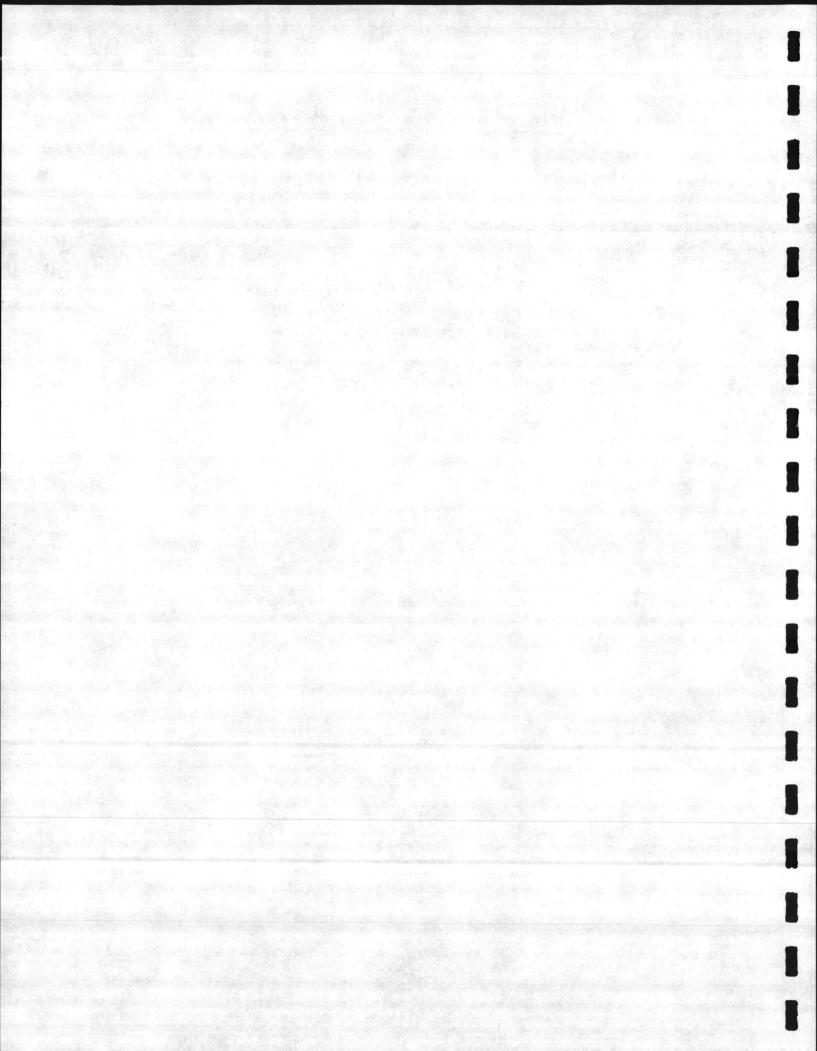
Escalated to Oct. 1987 \$96,000 x $\frac{2684}{1922}$ = \$134,060

Present Value

10% Discount (2% differential) year 1.963Present Value\$129,10010% Discount (2% differential) year 9.526Present Value\$ 70,51610% Discount (2% differential) year 17.288

Total Present Value Ash Disposal Investment \$238,225

\$ 38,609



2. Recurring Costs

a. Annual Boiler Plant Labor Costs

4 Crane Operators (WG-8) @ \$9.98/hr. (incl. benefits) 4 Boiler Operators (WG-7) @ \$9.43/hr. (incl. benefits) 4 Boiler Mechanics (WG-10) @ \$11.09/hr. (incl. benefits) 3 Supervisors (WS-7) @ \$12.78/hr. (incl. benefits)

Unescalated Labor Cost

 $(4 \times 9.98 \times 2080) + (4 \times 9.43 \times 2080) + (4 \times 11.09 \times 2080)$ + $(3 \times 12.78 \times 2080) = $333,508$

Labor escalated to Oct. 1987

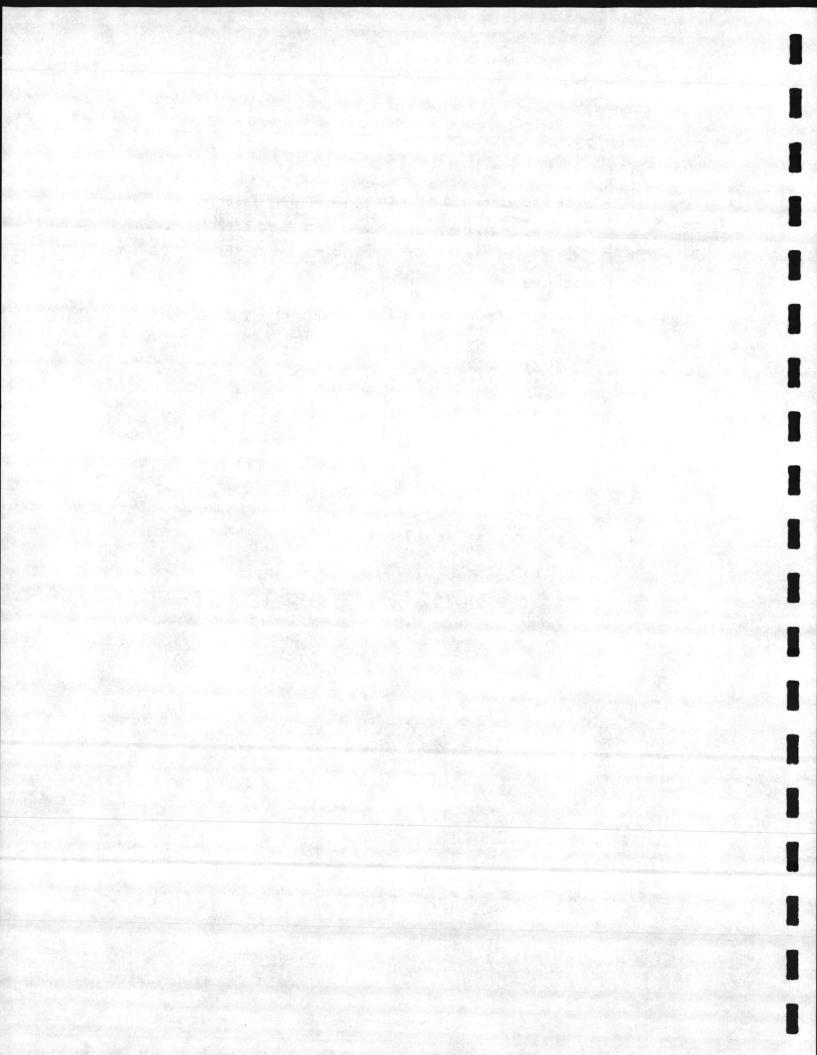
Fy 82 Fy 83 Fy 84 Fy 85 Fy 86 Fy 87 \$333,508 x 1.056 x 1.056 x 1.056 x 1.056 x 1.056 x 1.056 = \$462,476

10% Discount (0% differential)

Present Value Labor Cost

\$4,404,621

9.524



b. Annual Boiler Maintenance Cost

ITEM	INSTALLED COST (\$ X 10 ³)	MAINT. FACTOR	COST (\$ X 10 ³)
Boilers & Fans	3,250	0.025	81.25
Precipitators	1,200	0.015	18.00
Ducts & Stack	245	0.010	2.45
Ash Handling	575	0.025	14.38
Pumps	33	0.015	0.50
Water Treatment	37	0.020	.74
Building	3,400	0.005	17.00
Internal Piping	740	0.005	3.70
Export Piping	1,376	0.010	13.76
Cranes	850	0.020	17.00
Electrical Instrumentation	538	0.020	10.76

Total Unescalated Maintenance

179.54

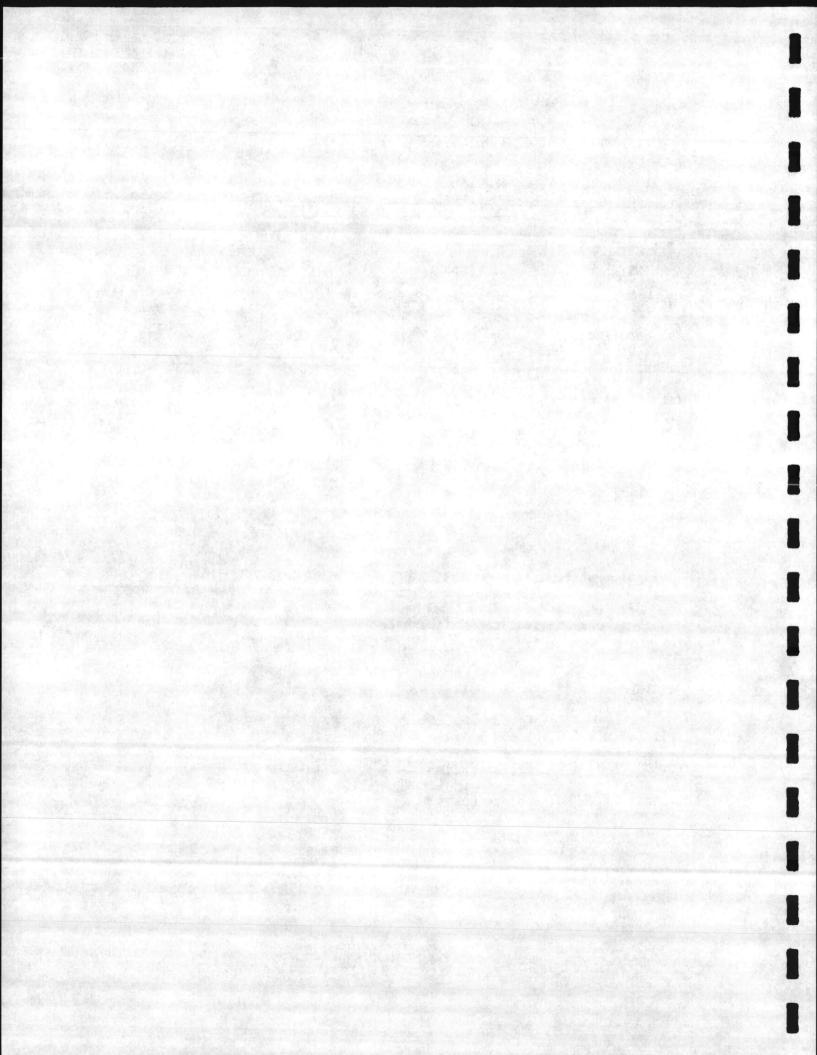
Maintenance escalated to Oct. 1987

 Fy 82
 Fy 83
 Fy 84
 Fy 85
 Fy 86
 Fy 87

 \$179,540 x 1.056 = \$248,969

 10% Discount (0% differential)
 9.524

 Present Value Maintenance Costs
 \$2,371,178



c. Annual Incremental Electrical Costs

SERVICE	POWER (KW)	USE FACTOR	EFFECTIVE POWER
Pumping Power*	60	0.8	48
Crane Operation	30	1.0	30
Precipitators	400	0.8	320
Ash Handling	60	0.8	48
		TOTAL	446 KW

* NOTE: Feedwater pumping is not included since a reduction in existing feedwater pumping will be realized.

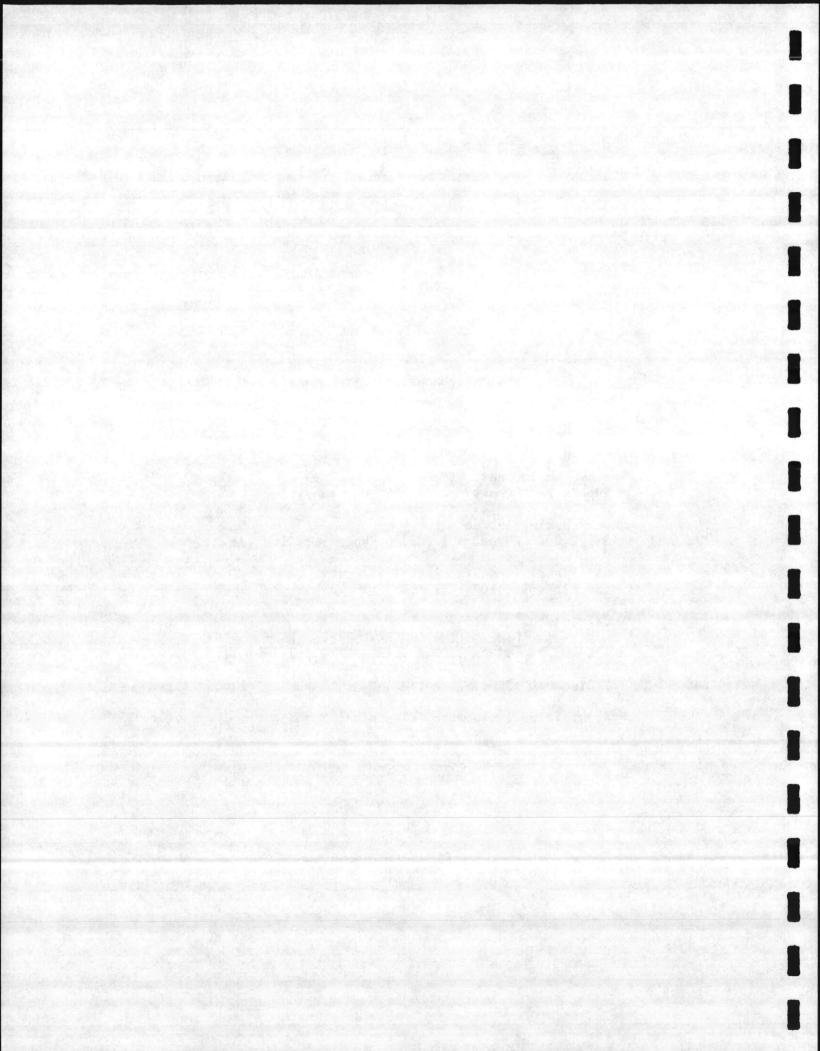
Annual Demand Cost Increase 446 KW x \$73.598/KW = \$32,825/yr.

Annual KWH Increase 446 KW X 7000 hrs/yr. = 3,122,000 KWh/yr.

Annual Dollar Increase per Kwh
3,122,000 KWH/hr. X \$.02726/KWh = \$ 85,106/yr.

Total Annual Increase Electrical Cost \$32,825 + \$85,106 = \$117,931

Escalated to Oct. 1987 FY82 FY83 FY84 FY85 FY86 FY87 \$117,931 X 1.13 X 1.13 X 1.13 X 1.13 X 1.13 X 1.13 = \$245,527 10% Discount (7% differential) 18.049 Present Value Incremental Electrical Cost \$4,431,517



d. Annual Trash Transfer Cost from Cherry Point to Lejeune

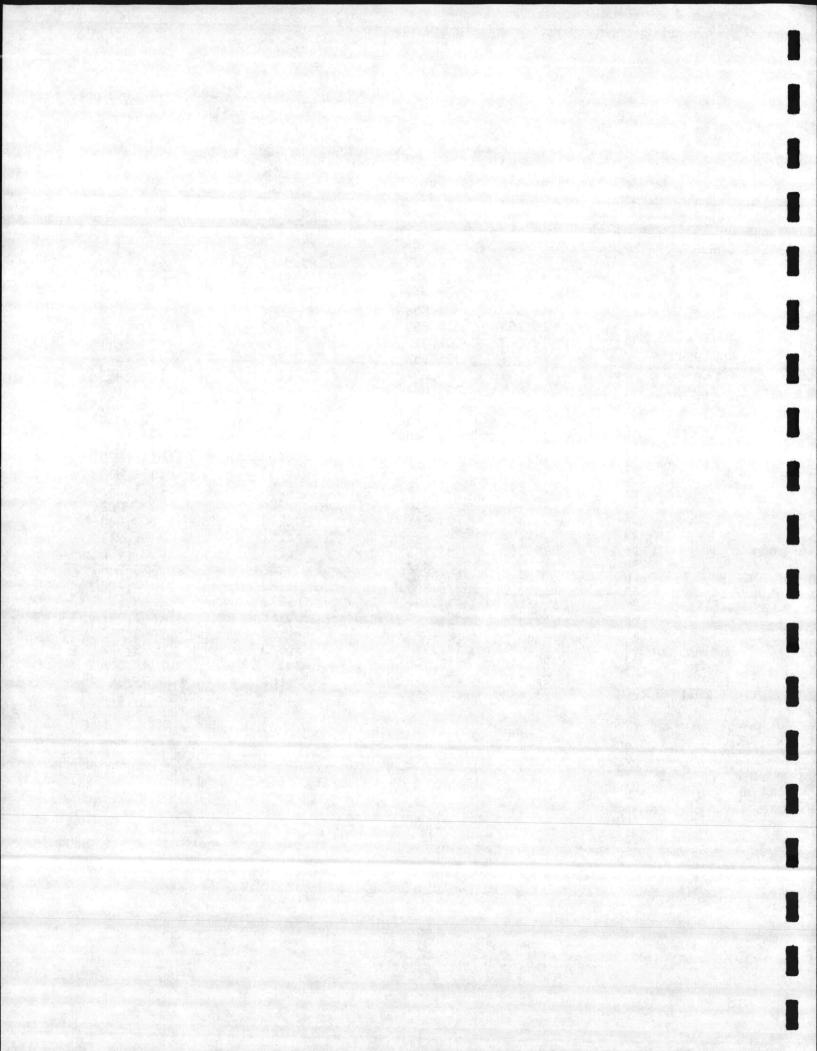
\$10/ton (1977) escalated to Oct. 1987

 $10 \times \frac{2684}{1355} = 19.81$

	Yr. of Op.	Tons/yr.	\$/yr.	10% Discount (0% differential)	Present Value
1987	1	15,538	\$ 307,808	.954	\$ 293,649
	1 2 3	15,793	312,859	.867	271,249
		16,048	317,911	.788	250,514
1990	4	16,303	322,962	.717	231,564
	4 5	16,558	328,014	.652	213,865
	6	16,813	333,066	.592	197,175
	6 7	17,068	338,117	.538	181,907
	8 9	17,323	343,169	.489	167,809
	9	17,578	348,220	.445	154,958
	10	17,833	353,272	.405	143,075
	11	18,088	358,323	.368	131,863
	12	18,343	363,375	.334	121,367
	13	18,598	368,426	.304	112,002
2000	14	18,853	373,478	.276	103,080
	15	19,108	378,529	.251	95,011
	16	19,363	383,581	.228	87,456
	17	19,618	388,632	.208	80,836
	18	19,873	393,684	.189	74,406
	19	20,128	398,763	.172	68,582
	20	20,383	403,787	.156	62,991
	21	20,638	408,839	.142	58,055
	22	20,893	413,890	.129	53,392
	23	21,148	418,942	.117	49,016
	24	21,403	423,993	.107	45,367
2011	25	21,658	429,045	.097	41,617

Total Present Value Transfer Cost

\$3,290,806



e. Annual Ash Disposal Cost

	Yr. of Op.	<u>1982 \$*</u>	<u>1987 \$*</u>	10% Discount (0% differential)	Present Value
1987	1 2	\$ 13,702	\$ 19,134	.954	\$ 18,254
	2	13,756	19,210	.867	16,655
	3	13,862	19,358	.788	15,254
1990		13,916	19,433	.717	13,933
	5	14,022	19,581	.652	12,767
	6	14,075	19,655	.592	11,636
	7	14,128	19,729	.538	10,614
	8	14,950	20,877	.489	10,209
	9	15,003	20,951	.445	9,323
	10	15,110	21,101	.405	8,586
	11	15,163	21,175	.368	7,792
	12	15,216	21,249	.334	7,097
	13	15,269	21,323	.304	6,482
2000	14	15,323	21,398	.276	5,906
	15	15,376	21,472	.251	5,389
	16	15,429	21,546	.228	4,912
	17	15,535	21,694	.208	4,512
	18	15,588	21,768	.189	4,114
	19	15,642	21,843	.172	3,757
	20	15,748	21,991	.156	3,431
	21	15,802	22,067	.142	3,134
	22	15,855	22,141	.129	2,856
	23	15,908	22,215	.117	2,599
	24	16,014	22,363	.107	2,393
2011	25	16,067	22,437	.097	2,176

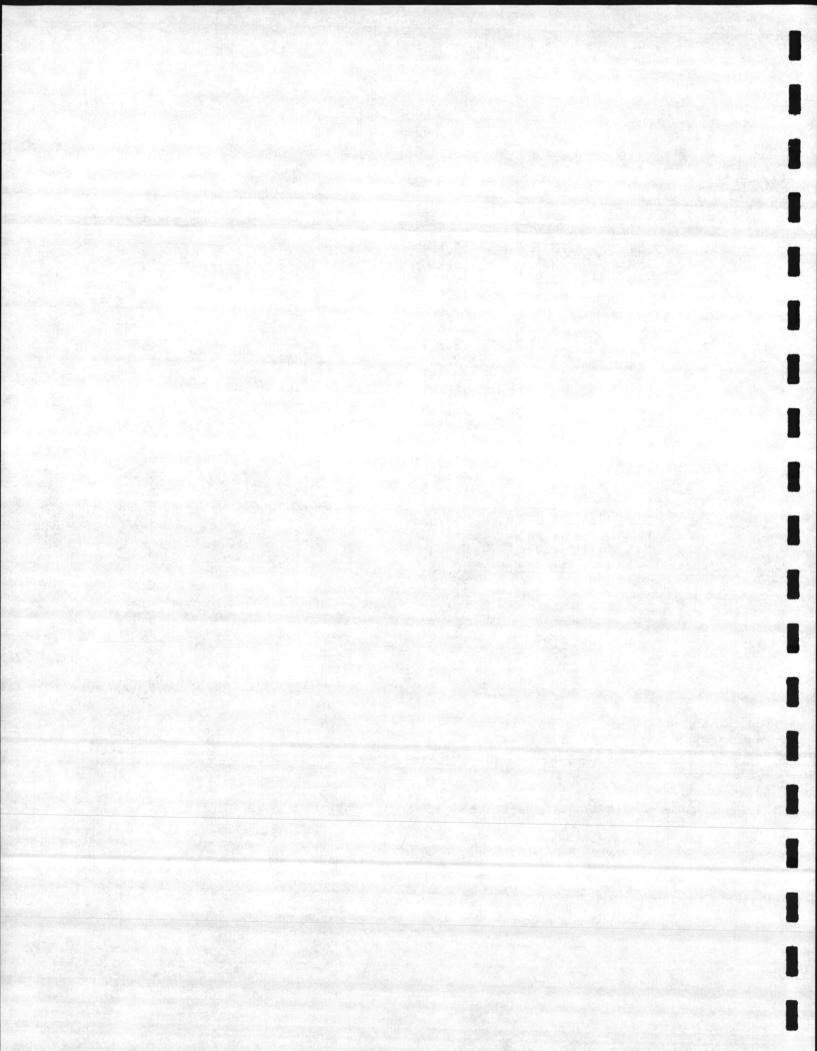
Total Present Value Ash Disposal Cost

\$ 193,781

* Escalation from 1982 to 1987 = $\frac{2684}{1922}$ = 1.3965

Ash - 80 lbs/cf, 30% moisture

Ash Disposal - 5 days per week



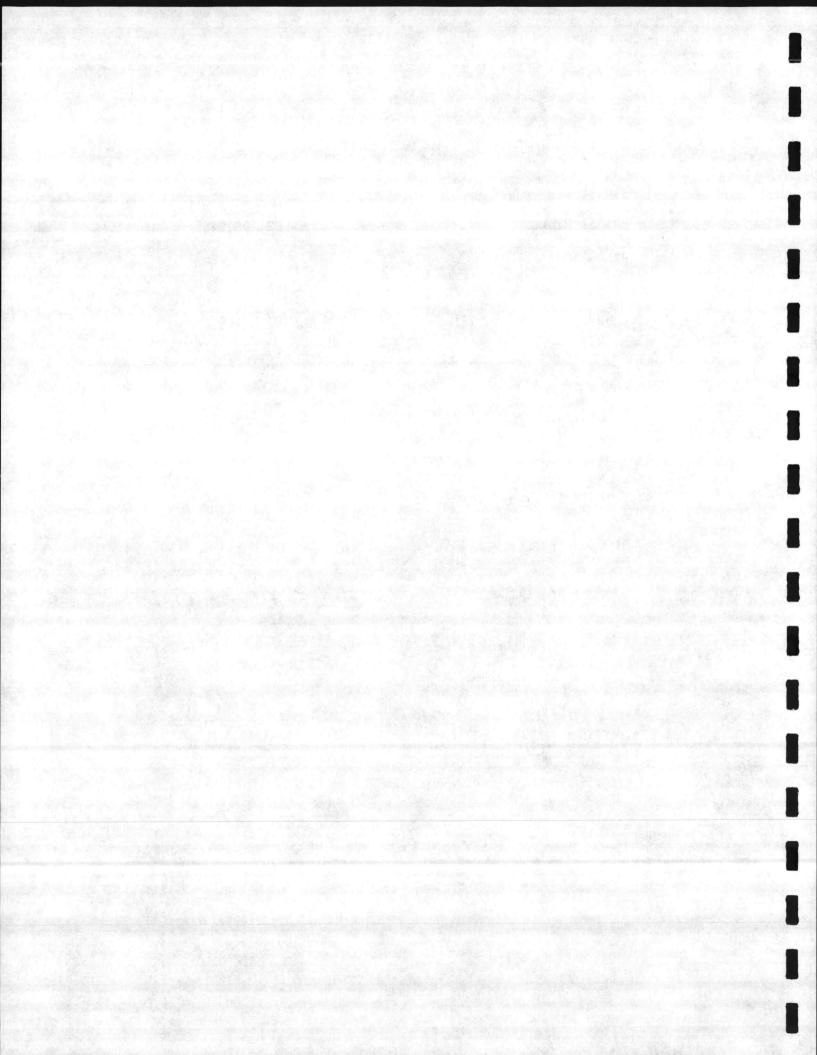
Summary Sheet Alternative 1A - Total Present Value

Investment Cost	
Boiler Plant	\$ 22,798,246
Ash Disposal	238,225
Recurring Costs	
Labor	4,404,621
Maintenance	2,371,178
Incremental Electrical	4,431,517
Trash Transfer	3,290,806
Ash Disposal	193,781
Total Present Value Alternative 1A	\$ 37,728,374

Discount Factor 9.524

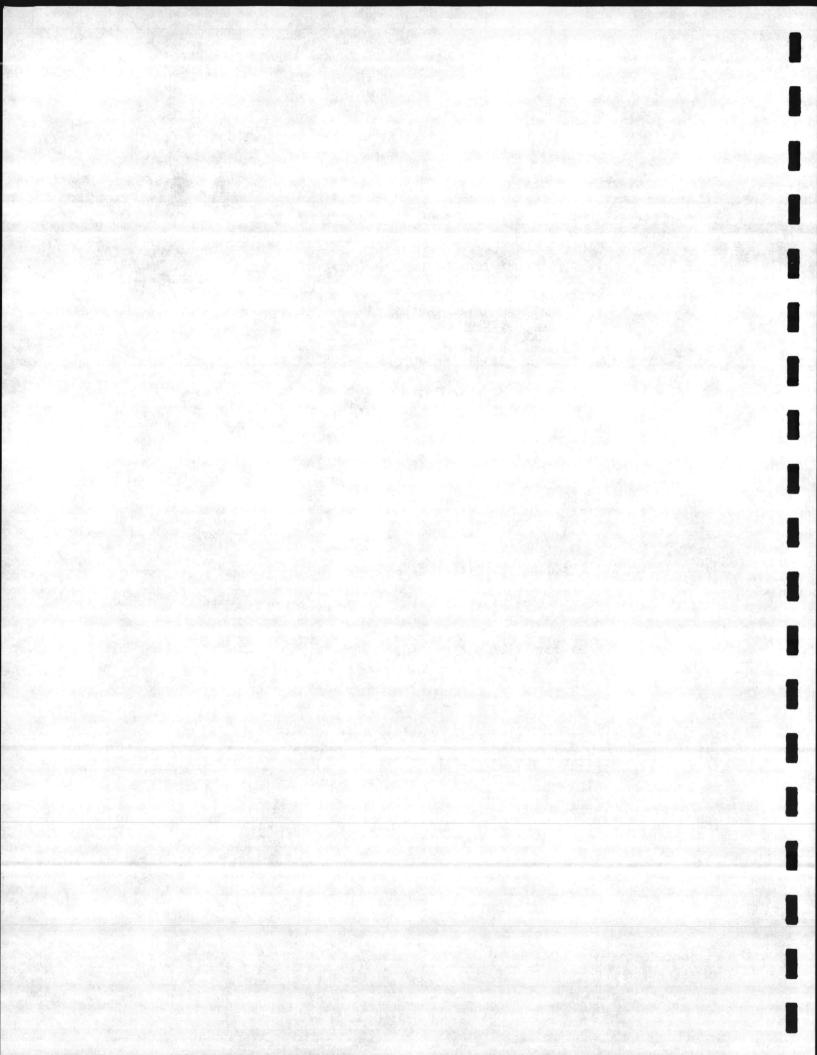
Uniform Annual Cost

\$ 3,961,400



ALTERNATIVE B - Incremental Cost of Refuse Landfills at Cherry Point and Camp Lejeune 1. Investment Costs a. Incremental Cost of Landfill - Cherry Point Capital Cost \$298,704 (1977) in year 5 Escalated to Oct. 1987 $298,704 \times 2684 = 591,676$ 1355 10% Discount (2% differential) year 5 .712 Present Value Capital Cost \$421,274 Capital Cost \$36,000 (1977) in years 8, 16, 23 Escalated to Oct. 1987 $36,000 \times 2684 = $71,309$ 1355 10% Discount (2% differential) year 8 .568 \$ 40,504 Present Value Capital Cost 10% Discount (2% differential) year 16 .310 \$ 22,106 Present Value Capital Cost 10% Discount (2% differential) year 23 .183 Present Value Capital Cost \$ 13,050

Total Present Value Capital Costs - Cherry Point \$496,934



b. Existing Boiler Plant Replacement/Upgrading Cost

Camp Geiger Capital Cost \$2,000,000 (1982\$) in 1989

Escalated to Oct. 1987 $\$2,000,000 \times \frac{2684}{1922} = \$2,792,924$

10% Discount (2% differential) year 2 .893

Present Value Capital Cost

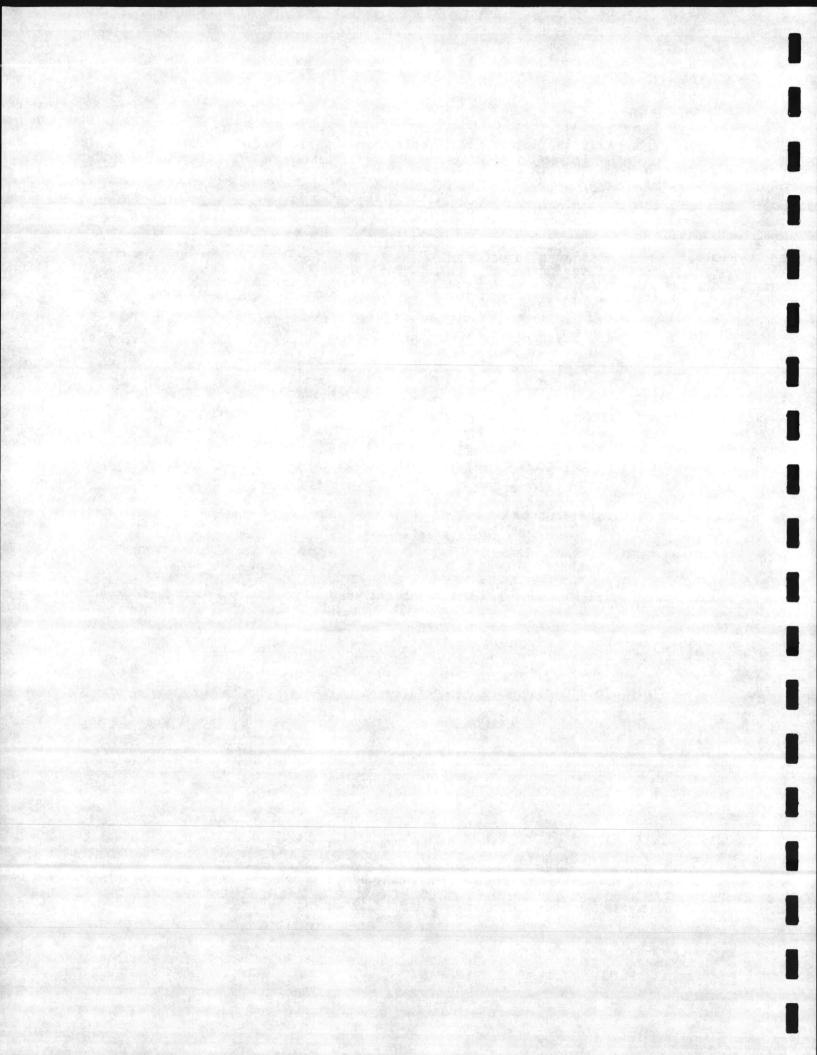
\$2,494,081

Air Station Capital Cost \$2,000,000 (1982) in 1996

Escalated to Oct. 1987 $\$2,000,000 \times \frac{2684}{1922} = \$2,792,924$

10% Discount (2% differential) year 10.488Present Value Capital Cost\$1,362,947

Total Present Value Replacement Costs \$3,857,028



2. Recurring Costs

a. Annual Incremental Landfill Development Cost - Cherry Point

Year Y	r. of Op.	<u>1977\$*</u>	<u>1987\$*</u>	10% Discount (2% differential)	Present Value
1987	1	53,312	105,600	0.963	\$ 101,693
	23	54,208	107,375	0.893	95,886
	3	55,104	109,150	0.828	90,376
1990	4	56,000	110,925	0.768	85,190
	5 6 7	56,896	112,700	0.712	80,242
	6	57,792	114,474	0.660	75,553
		60,438	119,716	0.612	73,266
	8	61,334	121,490	0.568	69,006
	9	62,230	123,265	0.526	64,837
	10	63,126	125,040	0.488	61,020
	11	64,022	126,815	0.453	57,447
	12	64,918	128,590	0.420	54,008
	13	65,814	130,364	0.389	50,712
2000	14	66,710	132,139	0.361	47,702
	15	67,606	133,914	0.335	44,861
	16	68,502	135,689	0.310	42,064
	17	69,398	137,464	0.288	39,590
	18	70,294	139,238	0.267	37,177
	19	71,190	141,013	0.247	34,830
	20	72,086	142,788	0.229	32,698
	21	72,982	144,563	0.213	30,744
	22	73,878	146,338	0.197	28,829
	23	74,774.	148,112	0.183	27,105
	24	75,670	149,887	0.170	25,481
2011	25	76,566	151,662	0.157	23,811

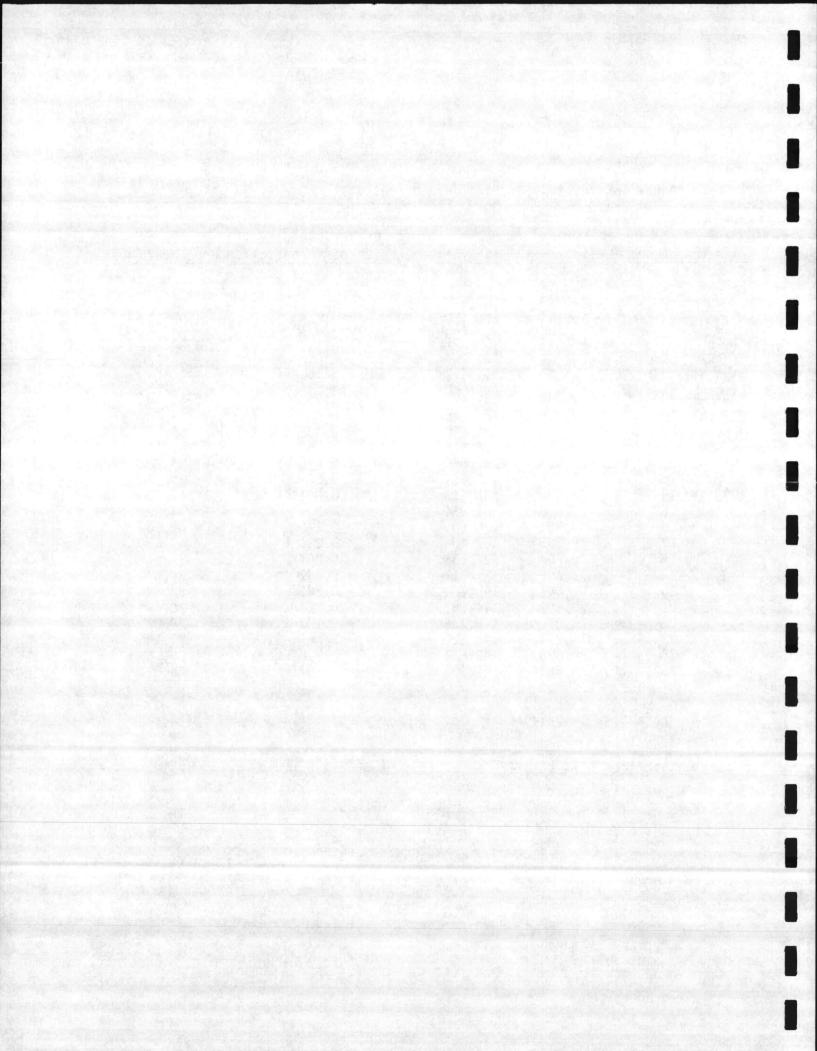
Total Present Value Development Cost - Cherry Point

\$ 1,374,128

* Escalation from 1977 to 1987

 $\frac{2684}{1355}$ =

1.9808



				10% Discount	
	Yr. of Op.	1977\$*	1987\$*	(2% differential)	Present Value
1987	1	\$ 215,809	\$ 427,477	.963	\$ 411,660
	2	217,609	431,042	.893	384,921
	2 3	219,157	434,109	.828	359,442
1990	4	220,956	437,672	.768	336,132
	4 5	222,505	440,741	.712	313,808
	6 7	224,304	444,304	.660	293,241
	7	223,732	443,171	.612	271,221
	8	225,532	446,736	.568	253,746
	9	227,331	450,300	.526	236,858
	10	228,879	453,366	.488	221,243
	11	230,679	456,932	.453	206,990
	12	230,107	455,799	.420	191,436
	13	231,906	459,362	.389	178,692
2000	14	233,706	462,928	.361	167,117
	15	233,134	461,795	.335	154,701
	16	234,933	465,358	.310	144,261
	17	236,481	468,424	.288	134,906
	18	238,281	471,990	.267	126,021
	19	240,080	475,553	.247	117,462
	20	241,629	478,622	.229	109,604
	21	243,428	482,185	.213	102,705
	22	242,856	481,052	.197	94,767
	23				
	24	246,204	487,684	.170	82,906
2011	25	248,003	491,247	.157	71,126
2011	23 24	244,655 246,204	484,616 487,684	.183 .170	88,685 82,906

b. Annual Incremental Landfill Development Cost - Camp Lejeune

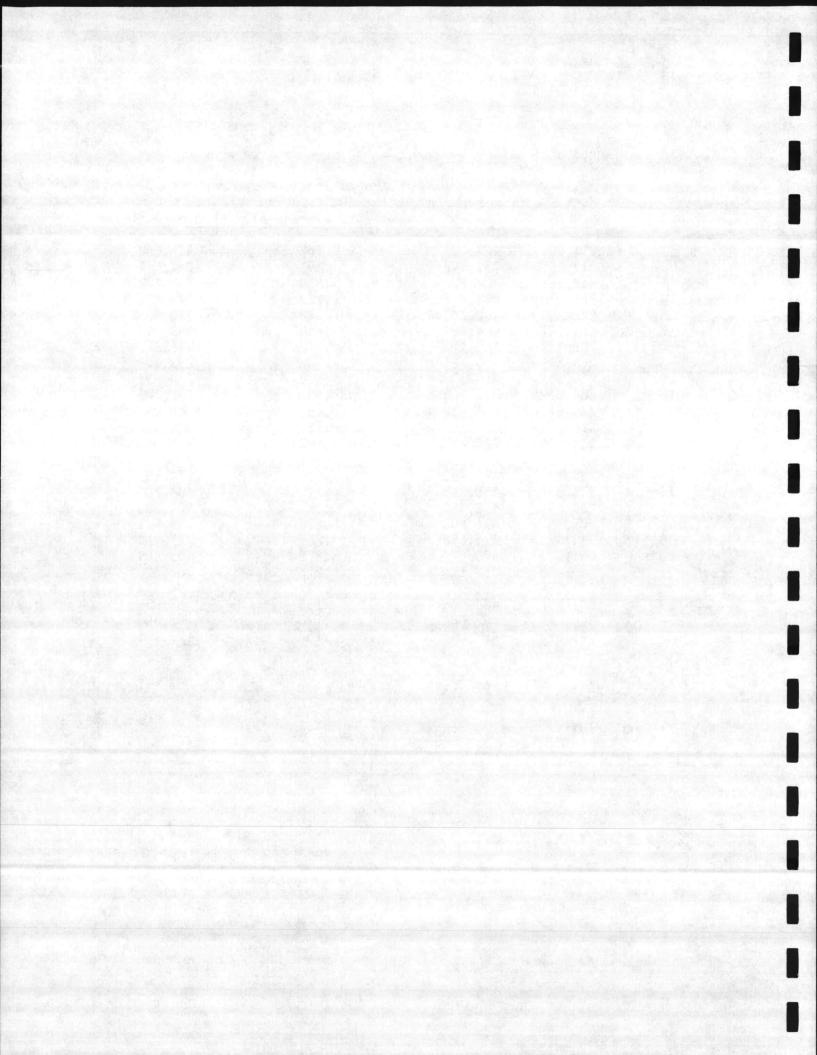
Total Present Value Development Costs - Camp Lejeune

=

\$ 5,053,651

* Escalation from 1977 to 1987

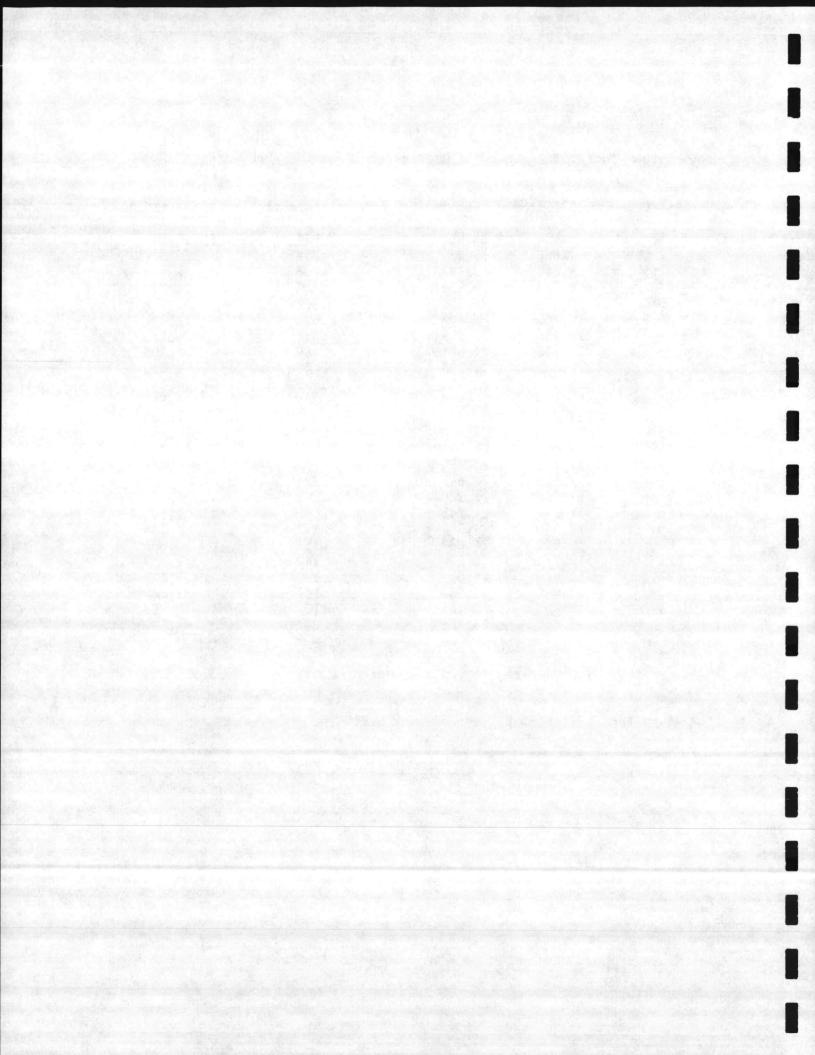
 $\frac{2684}{1355}$ = 1.9808



Year	Yr. of Op.	<u>1977\$*</u>	1987\$*	10% Discount (0% differential)	Present Value
1987	1	\$ 9,520	\$ 18,857	.954	\$ 17,990
	2	9,680	19,174	.867	16,624
	3	9,840	19,491	.788	15,359
1990	4	10,000	19,808	.717	14,202
	5	10,160	20,125	.652	13,122
	6	10,230	20,442	.592	11.914
	7	10,480	20,759	.538	11,168
	8	10,640	21,076	.489	10,306
	9	10,800	21,393	.445	9,520
	10	10,960	21,710	.405	8,793
	11	11,120	22,027	.368	8,106
	12	11,280	22,343	.334	7,463
	13	11,440	22,660	.304	6,889
2000	14	11,600	22,977	.276	6,342
	15	11,760	23,294	.251	5,847
	16	11,920	23,611	.228	5,383
	17	12,080	23,928	.208	4,977
	18	12,240	24,245	.189	4,583
	19	12,400	24,562	.172	4,225
	20	12,560	24,879	.156	3,881
	21	12,720	25,196	.142	3,579
	22	12,880	25,513	.129	3,292
	23	13,040	25,830	.117	3,022
	24	13,200	26,147	.107	1,412
2011	25	13,360	26,463	.097	1,296

c. Annual Incremental Landfill Maintenance Cost - Cherry Point

* Escalation from 1977 to 1987 = $\frac{2684}{1355}$ = 1.9808



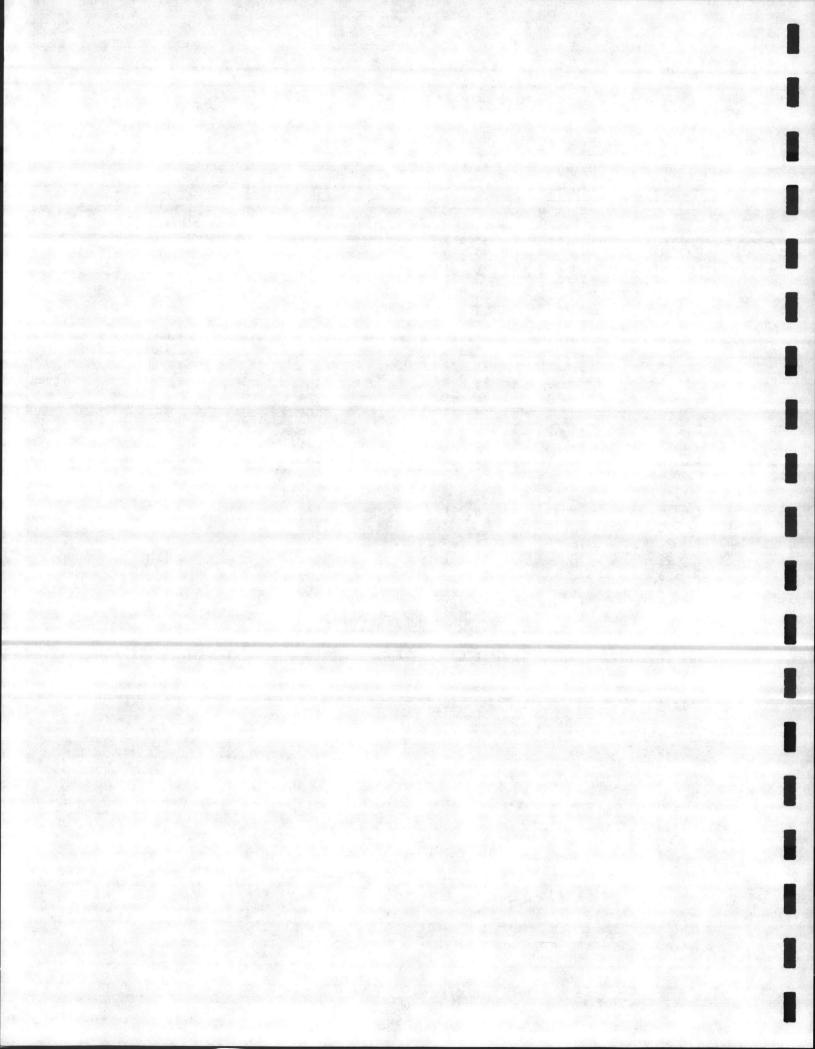
	Yr. of Op.	<u>1977\$*</u>	<u>1987\$*</u>	10% Discount (0% differential)	Present Value
1987	1	\$ 16,460	\$ 32,604	.954	\$ 31,104
	2	16,597	32,876	.867	28,503
	3	16,715	33,109	.788	26,090
1990	4	16,853	33,383	.717	23,936
	5	16,971	33,616	.652	21,918
	5 6	17,108	33,888	.592	20,062
	7	17,064	33,801	.538	18,185
	8	17,202	34,074	.489	16,662
	9	17,339	34,345	.445	15,284
	10	17,457	34,579	.405	14,004
	11	17,594	34,850	.368	12,825
	12	17,551	34,765	.334	11,612
	13	17,688	35,037	.304	10,651
2000	14	17,825	35,308	.276	9,745
	15	17,781	35,221	.251	8,840
	16	17,919	35,494	.228	8,093
	17	18,037	35,728	.208	7,431
	18	18,174	35,999	.189	6,804
	19	18,311	36,271	.172	6,239
	20	18,429	36,504	.156	5,695
	21	18,567	36,778	.142	5,222
	22	18,523	36,691	.129	4,733
	23	18,660	36,962	.117	4,325
	24	18,778	37,196	.107	3,980
2011	25	18,915	37,467	.097	3,634

d. Annual Incremental Landfill Maintenance Cost - Camp Lejeune

Total Present Value Maintenance Costs - Camp Lejeune

\$ 325,577

* Escalation from 1977 to 1987 = $\frac{2684}{1355}$ = 1.9808



	tons 1bs	tons/day tı /hr trash steam/hr u/hr	ash burned	- 24 hours/day X 6227 lbs stea X 1254 Btu/lb** X \$12.99/MMBtu*	k	= tons/h = equiva = MMBtu/ = \$/hr	lent lbs steam,	/hr*	
	\$/hr			X 8760 hrs/yr		= \$/yr			
	\$/yr			X discount fact	or	= presen	t value		
	4/31				Displaced			10% Discount	
					oil input		**	10% Discount	Dessart Value
	Year	tons/day	tons/hr.	lbs steam/hr.	MMBtu/hr.	\$/hr.	\$/yr.	(8% differential)	Present Value
987	1	· 128	5.33	33,211	41.65	\$ 540.98	\$ 4,739,018	.991	\$ 4,696,367
	2	129	5.38	33,470	41.97	545.21	4,776,042	.973	4,647,088
	3	131	5.46	33,989	42.62	553.66	4,850,089	.955	4,631,835
990	4	132	5.50	34,248	42.95	557.89	4,887,113	.938	4,584,112
	5	134	5.58	34,767	43.60	566.34	4,961,160	.921	4,569,228
	6	135	5.62	35,027	43.92	570.57	4,998.183	.904	4,518,358
	7	136	5.67	35,286	44.25	574.80	5,035,207	.888	4,471,263
	8	137	5.71	35,546	44.57	579.02	5,072,230	.871	4,417,912
	9	138	5.75	35,805	44.90	583.25	5,109.254	.856	4,373,521
	10	140	5.83	36,324	45.55	591.70	5,183,301	.840	4,353,973
	11	141	5.88	36,584	45.88	595.93	5,220,325	.825	4,306,768
	12	142	5.92	36,843	46.20	600.15	5,257,348	.810	4,258,452
	13	143	5.96	37,102	46.53	604.38	5,294,372	.795	4,209,026
000		144	6.00	37,362	46.85	608.61	5,331,396	.781	4,163,820
000	15	145	6.04	37,621	47.18	612.83	5,368,419	.766	4,112,209
	16	146	6.08	37,881	47.50	617.06	5,405,442		4,064,893
	17	148	6.17	38,400	48.15	625.51	5,479,490	.739	4,049,343
	18	149	6.21	38,659	48.48	629.74	5,516,513	.725	3,999,472
	19	150	6.25	38,919	48.80	633.96	5,553,537	.712	3,954,118
	20	152	6.33	39,438	49.45	642.42	5,627,584	.699	3,933,681
	21	153	6.38	39,697	49.78	646.64	5,664,608	.687	3,891,585
	22	154	6.42	39,956	50.10	650.87	5,701,631	.674	3,842,899
	23	155	6.46	40,216	50.43	655.10	5,738,655		3,798,989
	24	155	6.54	40,735	51.08	663.55	5,812,702		3,778,256
011		157	6.58	40,994	51.41	667.78	5,849,726		3,732,125

Total Present Value Fuel Oil Cost

\$ 100,662,926

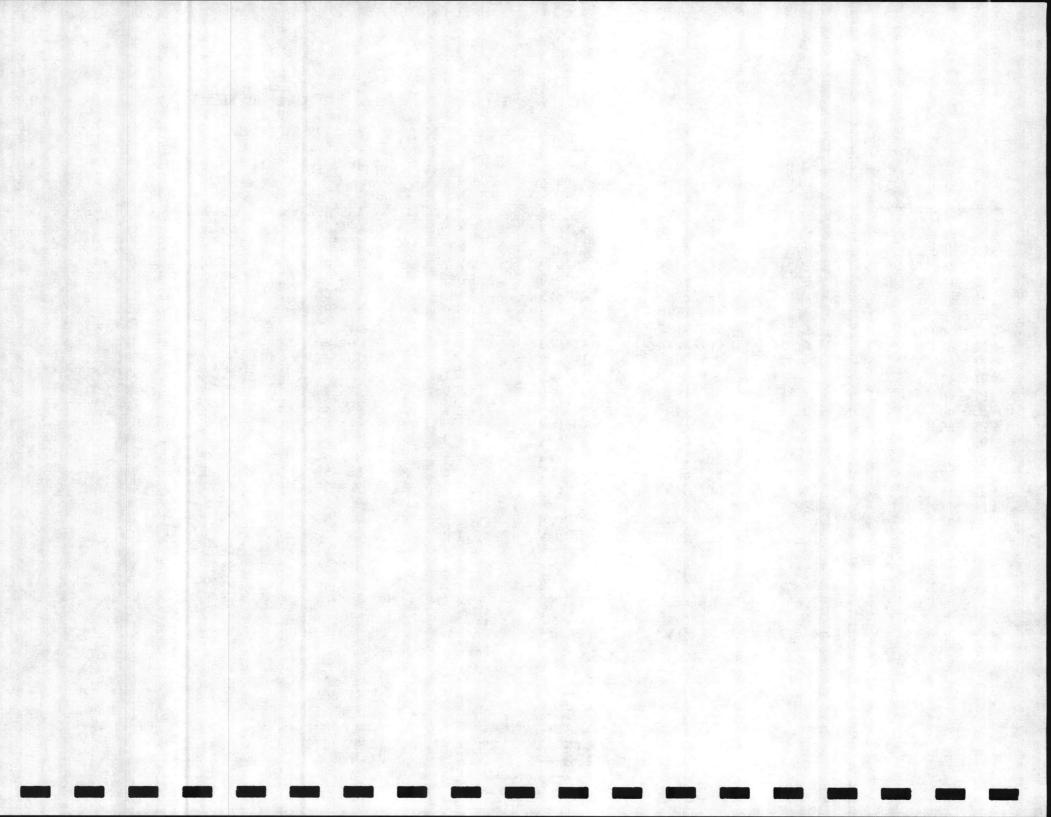
Includes blowdown and feedwater hearing *

Includes Camp Geiger Plant Efficiency **

*** \$5.92 (Jan. 82) escalated to Oct. 87

Fy82 Fy83 Fy84 Fy85 Fy86 Fy87 \$5.92 X 1.14 X 1.14 X 1.14 X 1.14 X 1.14 X 1.14 = \$12.99

V-23



Summary Sheet Alternative 1B - Total Present Value

Investment Costs

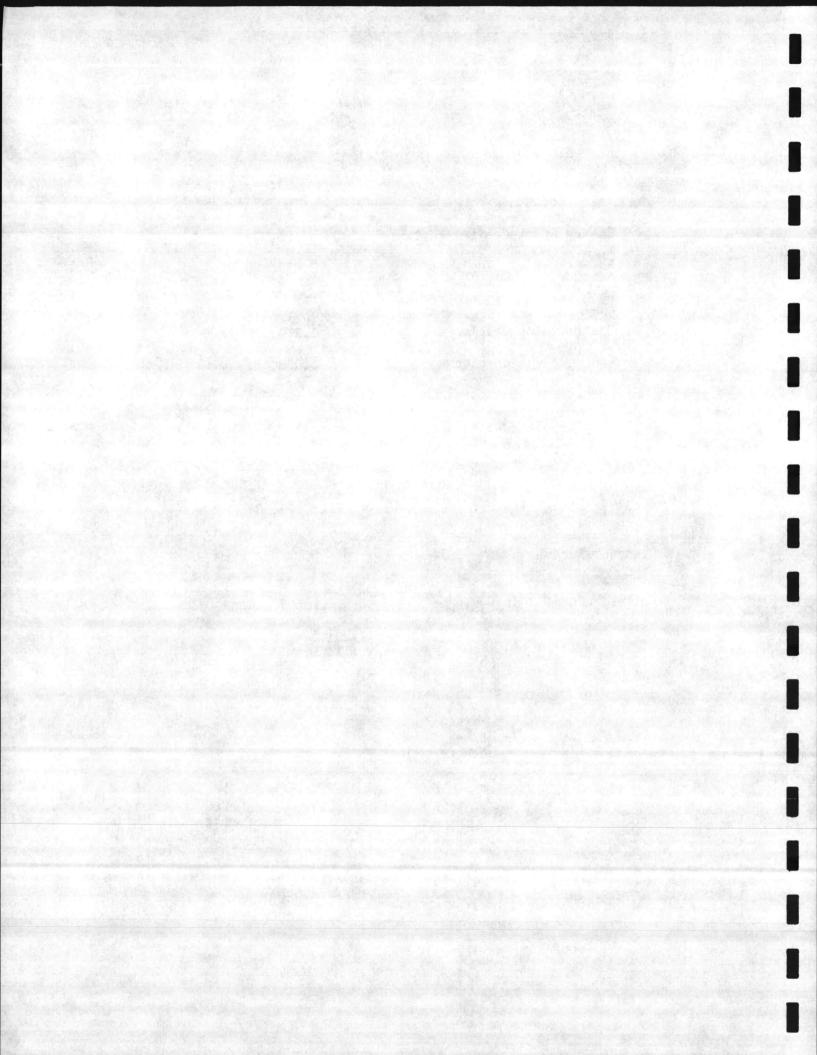
Cherry Point Capital Costs	\$	496,934
Boiler Plant - Replacement Costs		3,857,028
Recurring Costs		
Cherry Point Development		1,374,128
Camp Lejeune Development		5,053,651
Cherry Point Maintenance		199,295
Camp Lejeune Maintenance		325,577
Fuel Oil	_10	00,662,926

Total Present Value Alternative 1B \$111,969,539

Discount Factor 9.524

Uniform Annual Cost

\$ 11,756,566

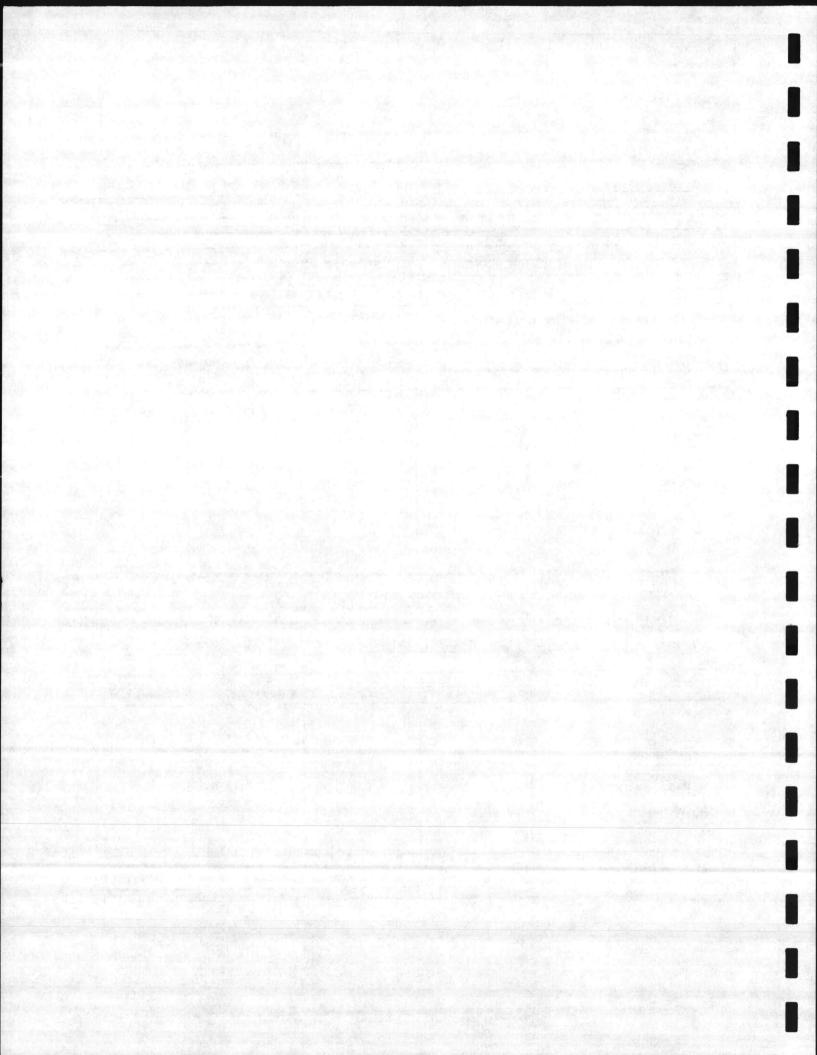


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				March 1982
Refuse Plant, Camp Le PROJECT TITLE			- A State of the second se	NQ.
Design Analysis (Fy 87) DESCRIPTION OF ALTERNATIVES				
Case I				
A. Refuse Plant - St	eam Only			and the second
B. Landfill and Oil-	fired Boilers			
PROJECT COST PROJECTIONS BY	ALTERNATIVES			
ALTERNATIVE A Refus	e Plant		ECONO LIFE	NIC 25 TR
DESCRIPTION AND YEAR	COS ONE TIME	RECURNING	DISCOUNT	PRESENT VALUE (S)
INVESTMENT				
OPERATIONS				And the second second
NA INTERANCE		The second	THE REAL PROPERTY.	
PERSONNEL		and the second		Prove states in
		A state of the second state		
TERMINAL VALUE				· · · ·
TERMINAL VALUE Other:				
	The A - S37,72	8,374 ÷	SCOUNT FACTOR 9.524 =	UNIFORM ANNUAL CO 3,961,400
OTHER: TOTAL PRESENT VALUE ALTERNAT		<u>8,374</u> ÷		3,961,400
OTHER: TOTAL PRESENT VALUE ALTERNAT	ill and Oil-fir	<u>8,374</u> ÷	9.524 =	3,961,400
STHER: TOTAL PRESENT VALUE ALTERNAT ALTERNATIVE B Landf DESCRIPTION AND YEAR	ill and Oil-fir	8,374 ÷	9.524 =	3,961,400
OTHER: TOTAL PRESENT VALUE ALTERNAT ALTERNATIVE B Landf DESCRIPTION AND YEAR INVESTMENT	ill and Oil-fir	8,374 ÷	9.524 =	3,961,400
OTHER: TOTAL PRESENT VALUE ALTERNAT ALTERNATIVE BLandf DESCRIPTION AND YEAR INVESTMENT	ill and Oil-fir	8,374 ÷	9.524 =	3,961,400
OTHER: TOTAL PRESENT VALUE ALTERNAT ALTERNATIVE BLandf	ill and Oil-fir	8,374 ÷	9.524 =	3,961,400
STHER: TOTAL PRESENT VALUE ALTERNAT ALTERNATIVE BLandf DESCRIPTION AND YEAR INVESTMENT OPERATIONS	ill and Oil-fir	8,374 ÷	9.524 =	3,961,400
STHER: TOTAL PRESENT VALUE ALTERNAT ALTERNATIVE BLandf DESCRIPTION AND YEAR INVESTMENT GPERATIONS MAINTENANCE	ill and Oil-fir	8,374 ÷	9.524 =	3,961,400
OTHER: TOTAL PRESENT VALUE ALTERNAT ALTERNATIVE B Landf DESCRIPTION AND YEAR INVESTMENT OPERATIONS MAINTENANCE PERSONNEL	ill and Oil-fir	8,374 ÷	9.524 =	3,961,400

V-25

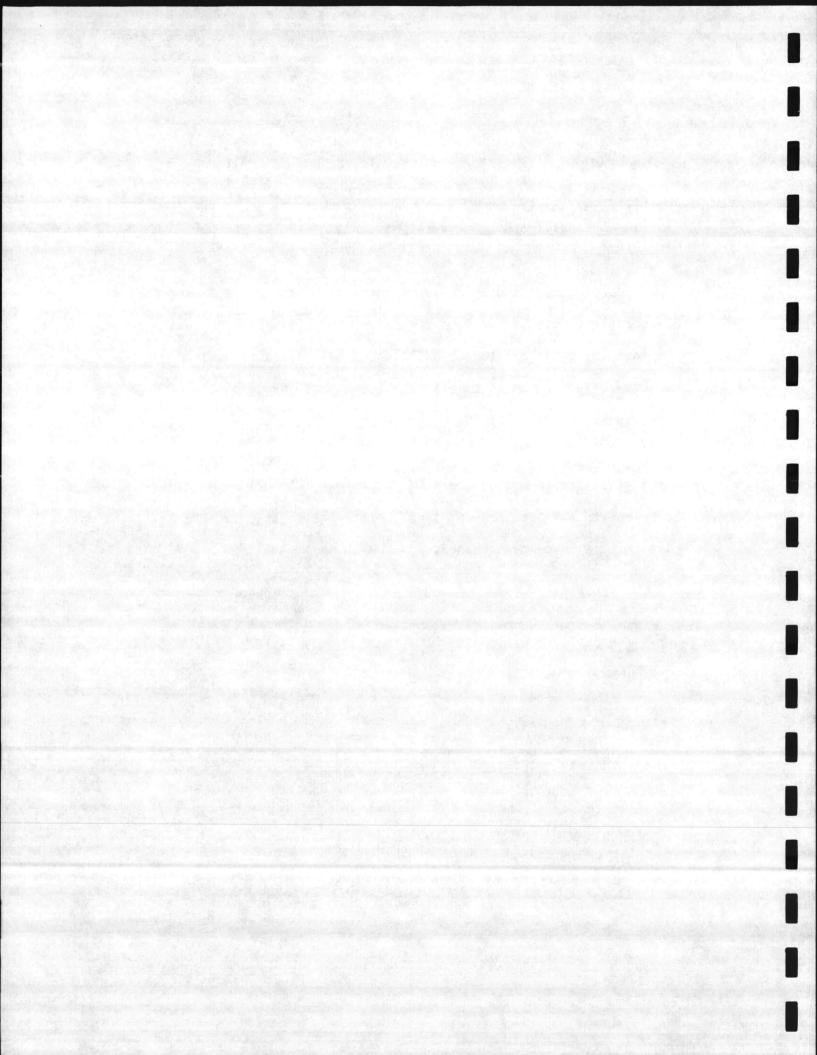
(Attach separate suget showing derivation of cost entries)



Analysis

	Total Present Value Cost	Uniform Annual Cost
Case 1A - Refuse Plant Case 1B - Landfill & Oil	\$ 37,728,374 111,969,539	\$ 3,961,400 11,756,566
Difference	74,241,165	7,795,166

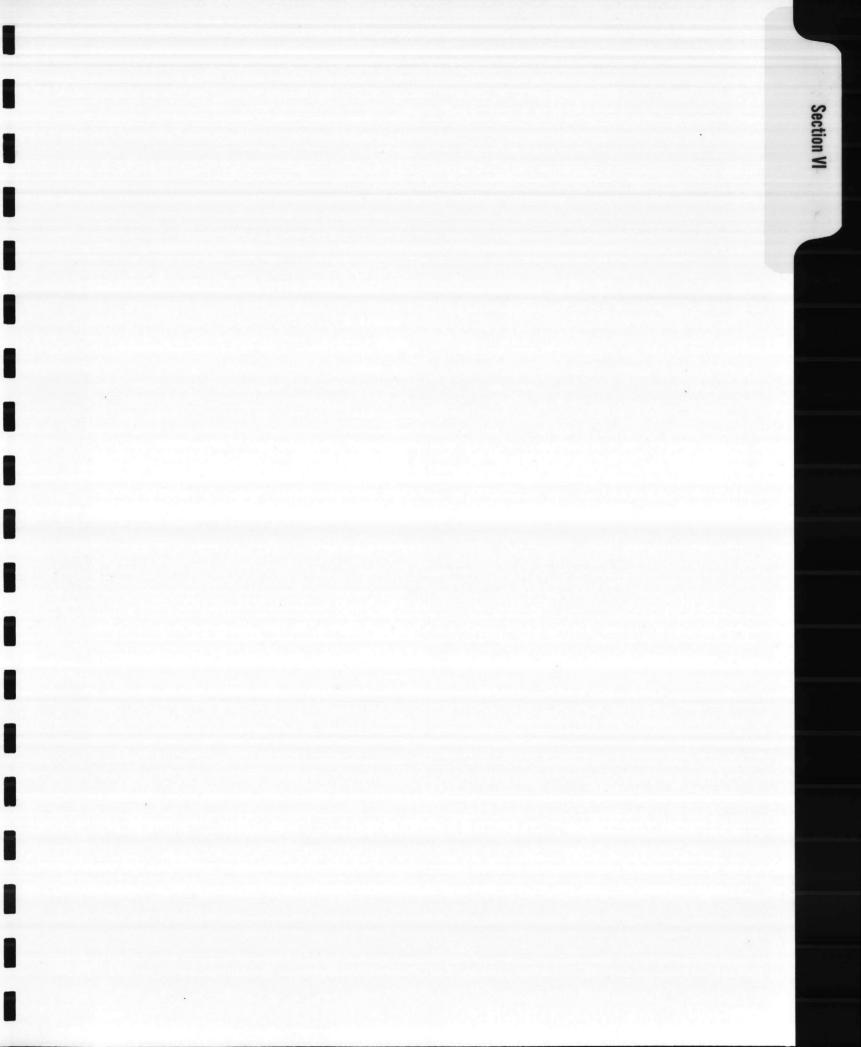
According to the present value analysis of the project over the 25-year plant life, the refuse plant would cost \$74,241,165 less than operating the existing landfills and oil plants at maximum capacity. This converts to a \$7,795,166 annual savings. The oil represents approximately 90% of the cost of Case 1B. The effect of the landfill costs on this alternative is small. Even though, the price of oil is generally dropping at present, the price would have to be cut to half its present level before the least cost alternative in this case would change.



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VI. CASE 2 - ELECTRICITY WITH BACK PRESSURE TURBINE

Plant Description

Boilers

The plant would be as in the general description except the steam would be generated at 600 PSIG, 725°F. These steam conditions are the highest desirable to limit chloride corrosion in the boiler tubes. The boilers would be the same as Case 1A except for the inclusion of a superheater.

Turbine

All of the steam generated by the boilers (30,200 lb/hr) would be expanded through a turbine. The exhaust pressure would be 150 PSIG. A small amount of steam would be reduced for use in a deaerating feedwater heater. The rest would be desuperheated and sent to the respective steam distribution systems.

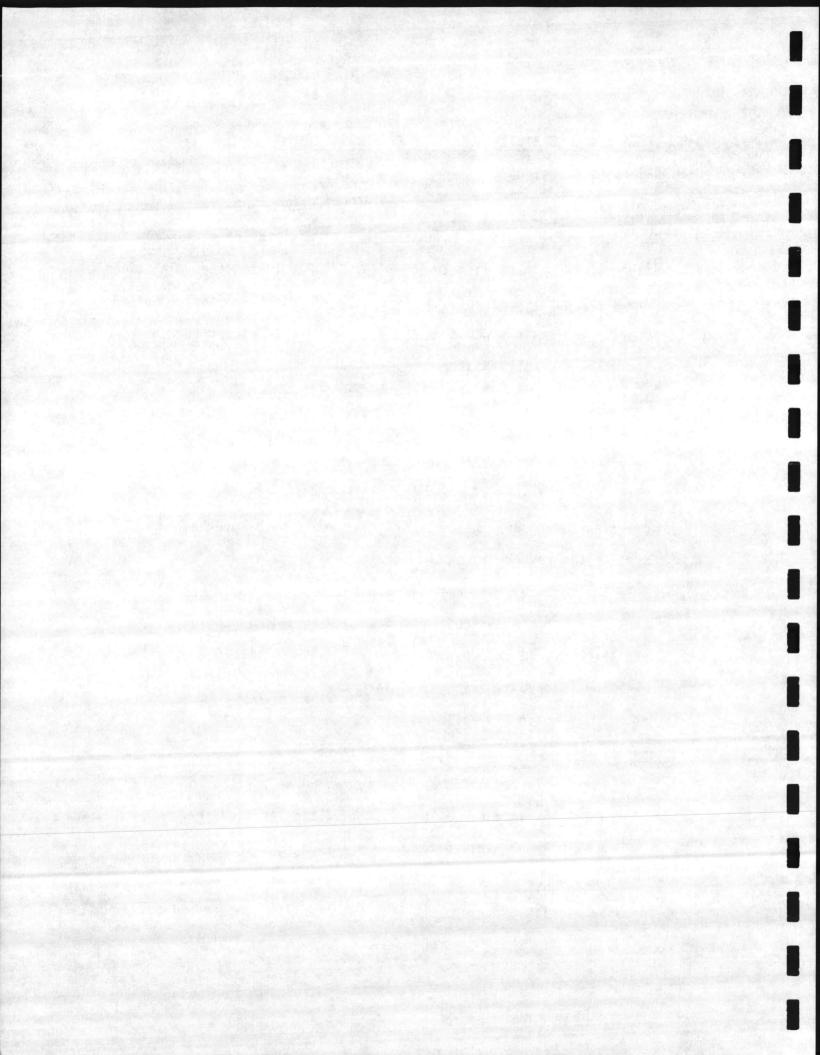
The turbine would operate at high speed and would drive a generator through a reduction gear. During initial operation approximately 725 KW would be produced.

The turbine-generator and electrical switchgear would be in a room adjacent to the boilers.

Electrical

The generator would be sized to match the turbine and would generate 1175 KVA power at the system voltage of 12.47 KV.

A switchgear line-up would be provided containing a 125 VDC air-operated or vacuum circuit breaker and auxiliary compartment, necessary relaying to protect the generator, switchgear and outgoing

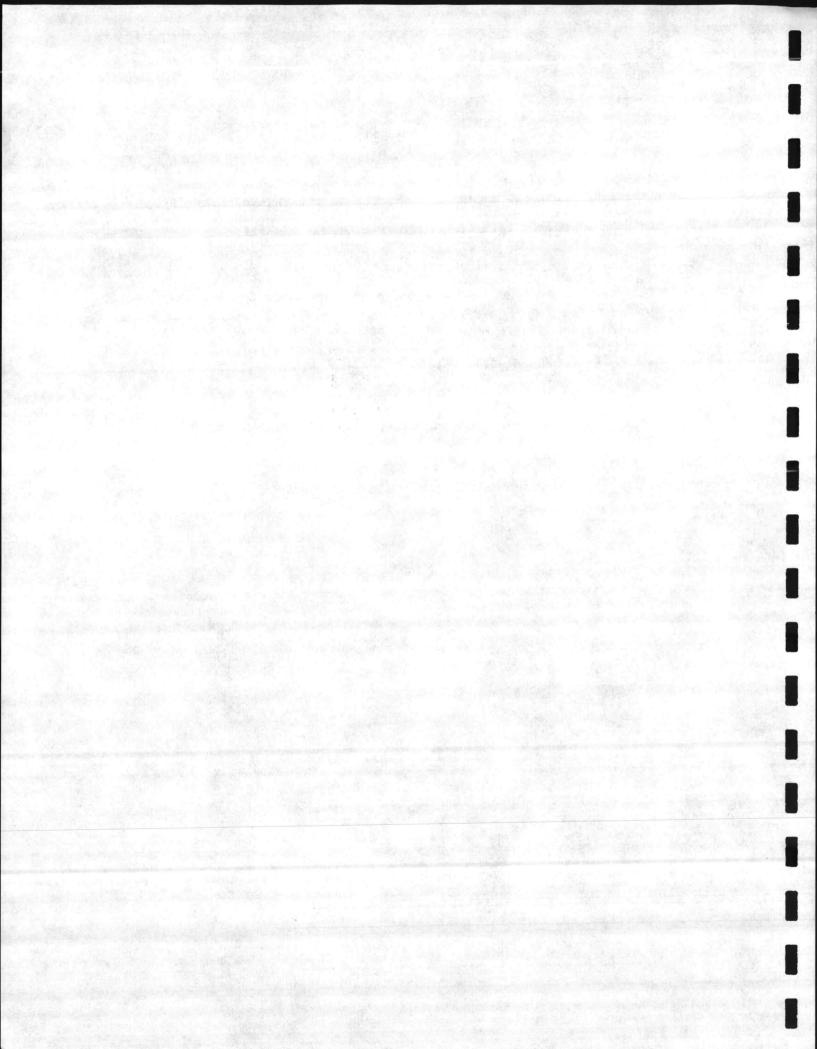


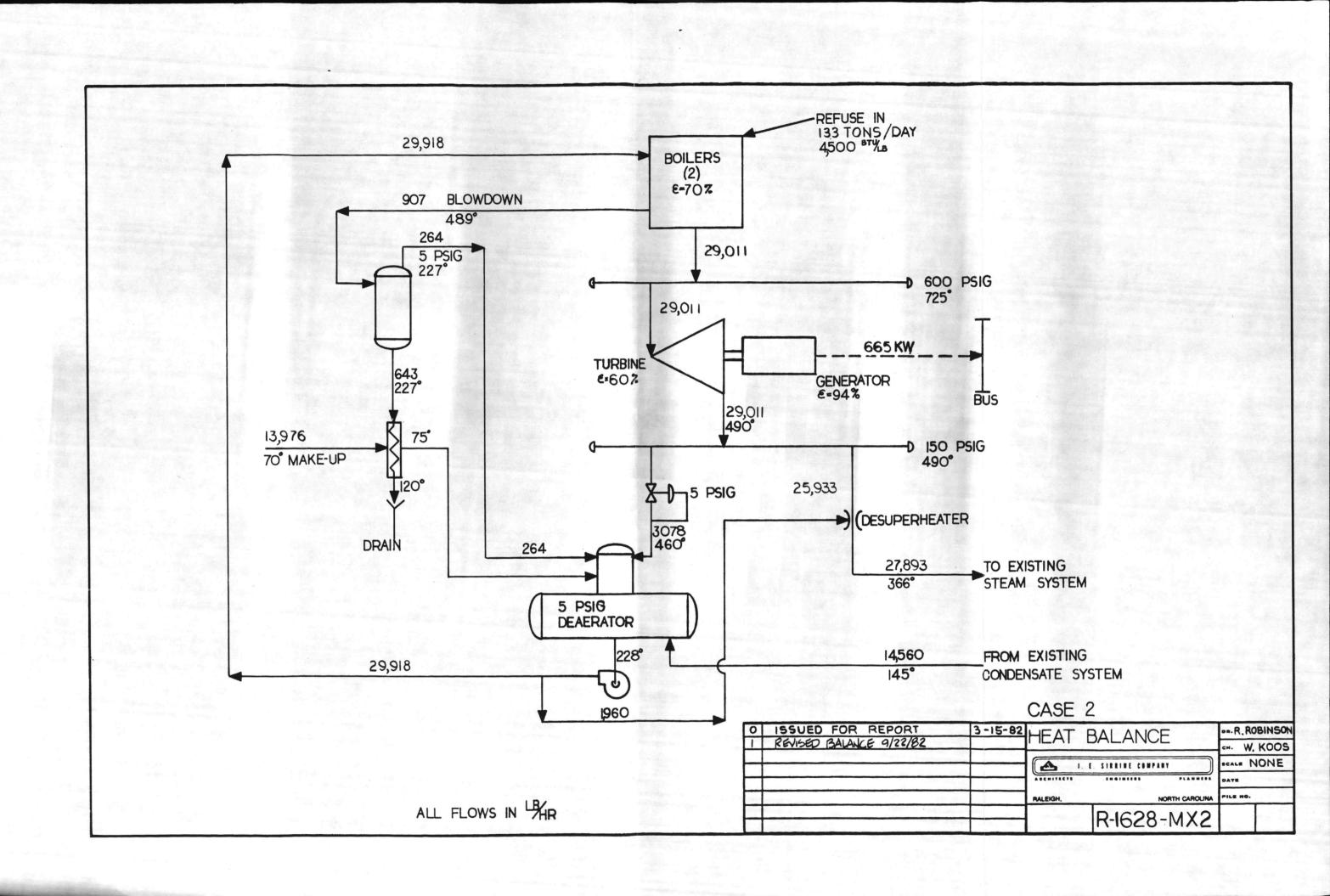
line. The necessary controls to allow for synchronizing to the present electrical system would be provided.

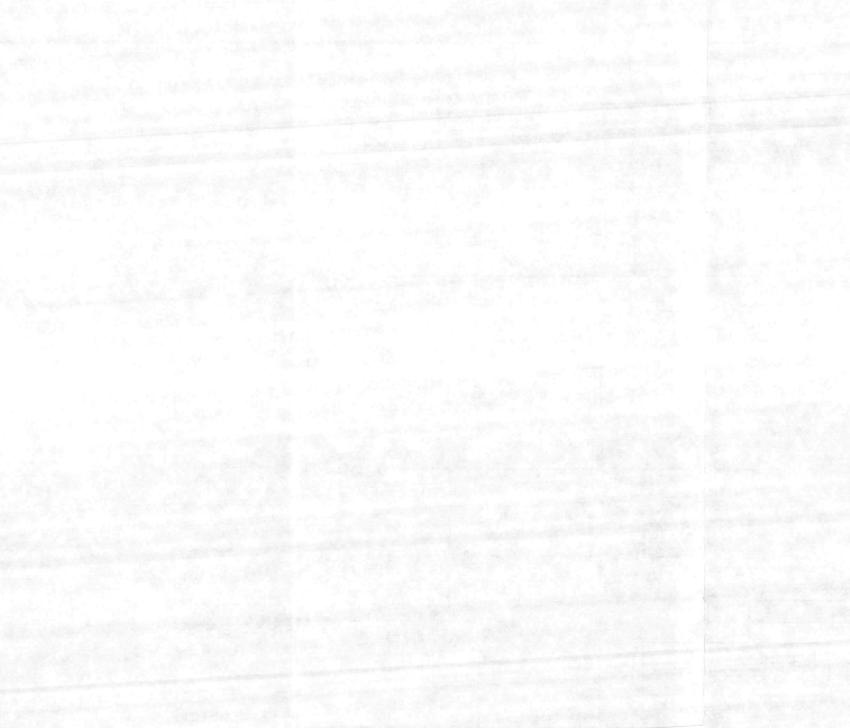
The generator would be connected to the switchgear using 15 KV shielded cable. The outgoing line would be connected to the switch-gear using 15 KV shielded cable.

Tie-in to the electrical system would be on the nearby 12.47 KV transmission line. Metering and recorders to account for the amount of power produced would be included.

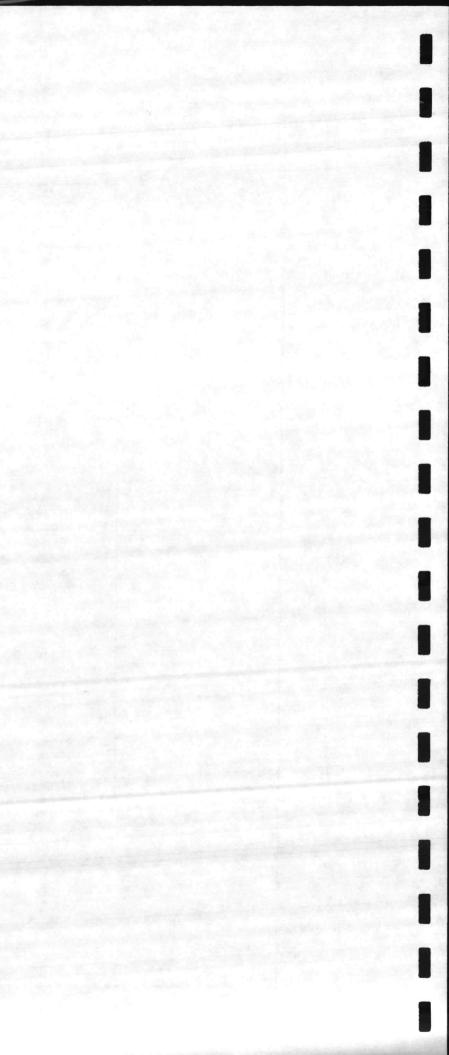
The conceptual heat balance is shown on Drawing MX2. The flow sheet for the steam and water systems are on Drawing MF2.

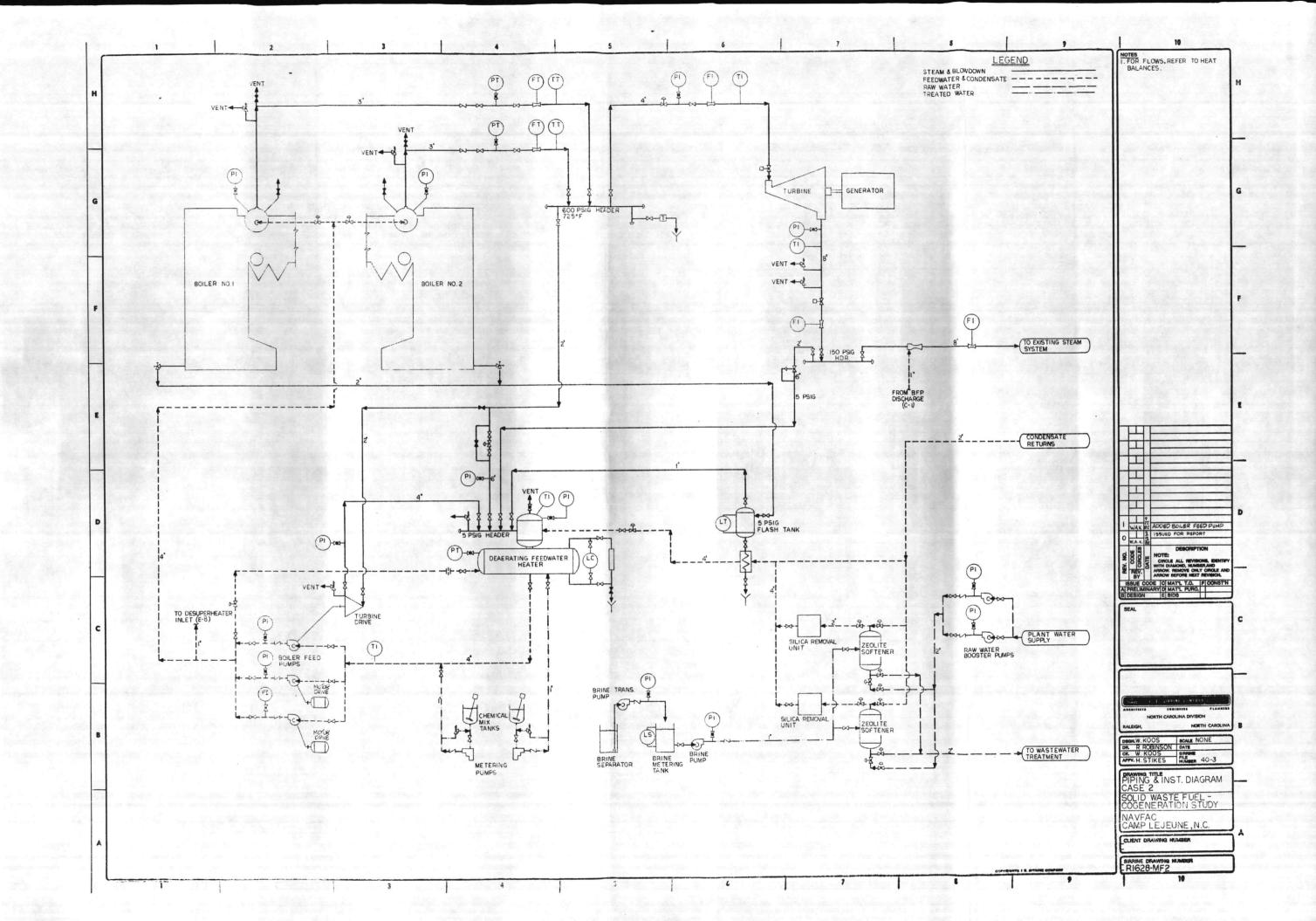


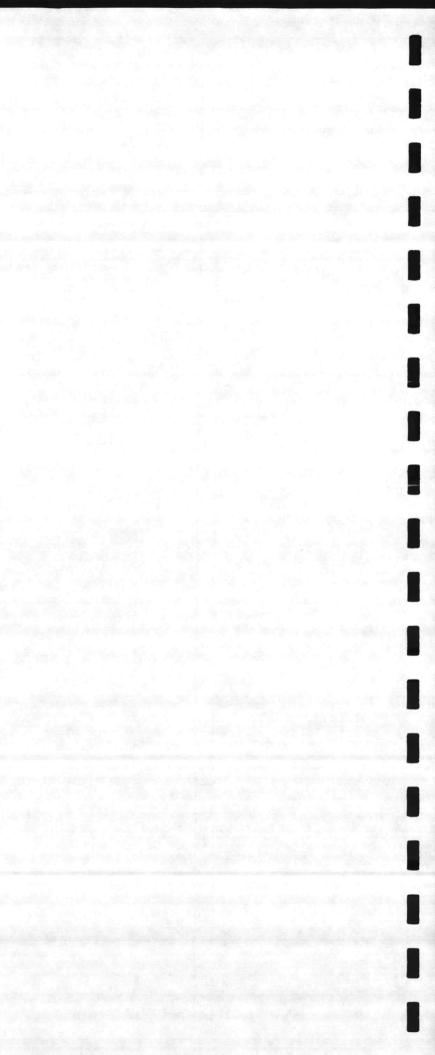




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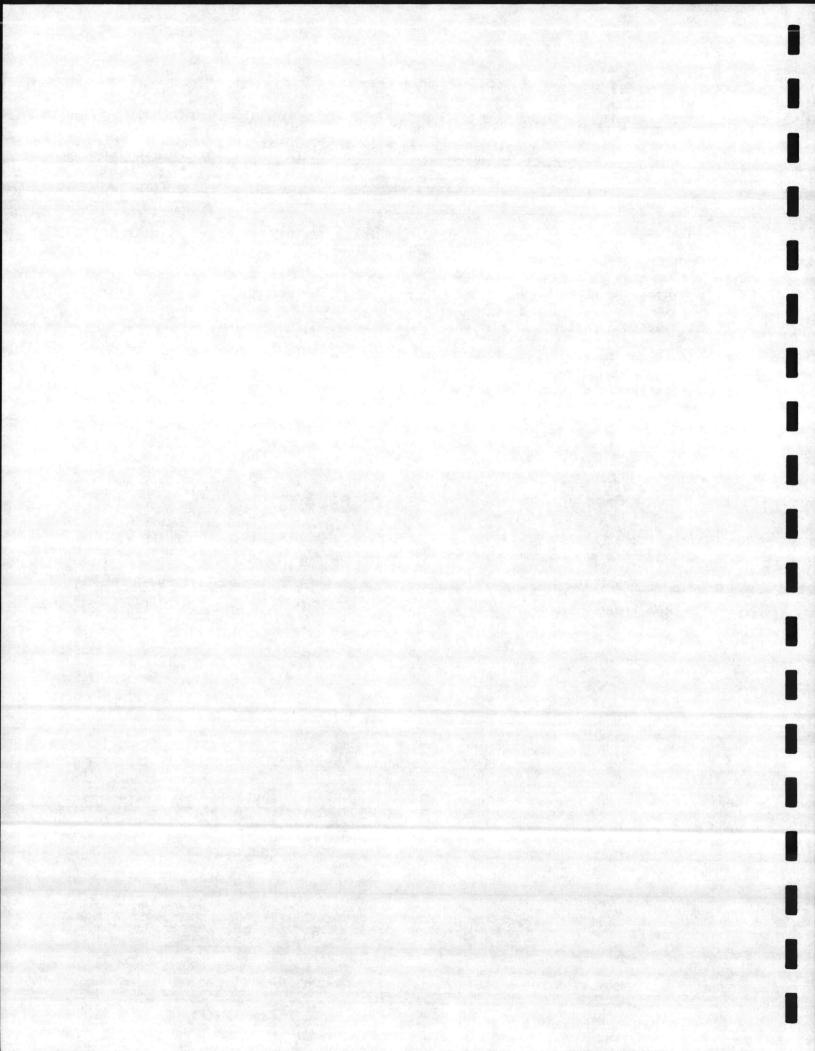


Cost Estimate

DEPARTMENT DIRECT COST SUMMARY

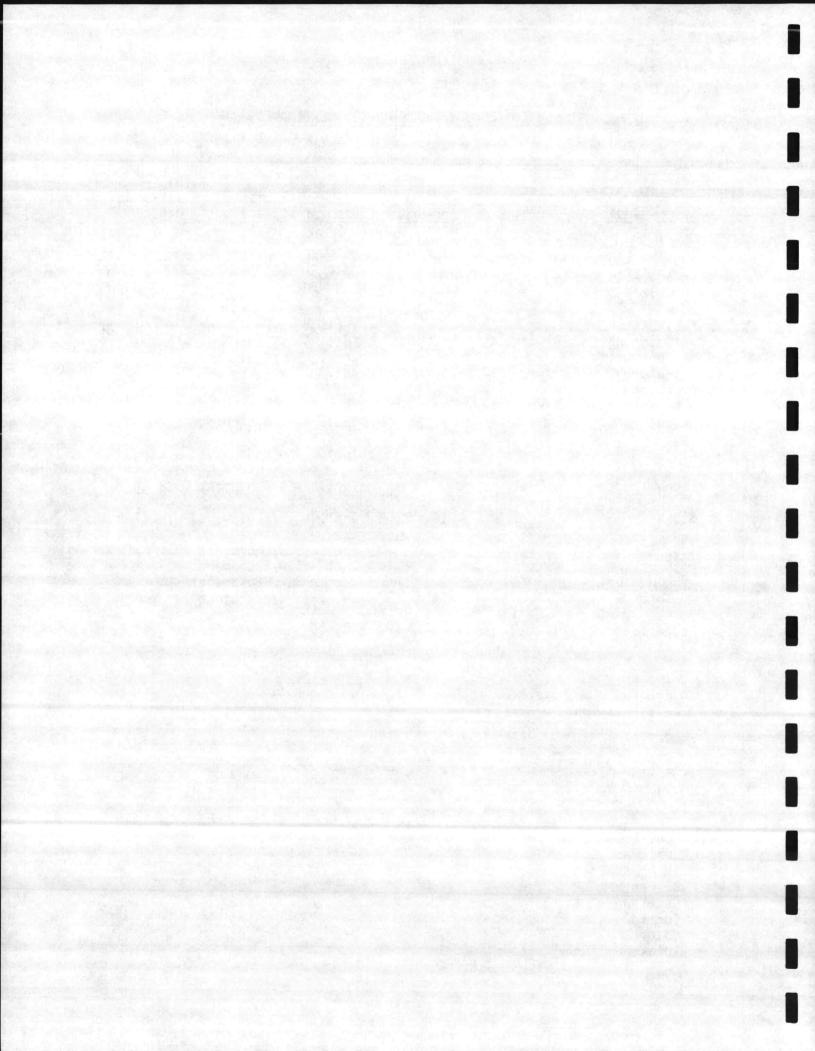
CASE 2 - BACK PRESSURE TURBINE

Equipment	\$	8,984,000	
Equipment Erection		170,600	
Equipment Foundations and Other Costs		294,400	
Buidings & Structures		3,700,000	
Electrical Installation Cost		463,000	
Instrumentation Installation Cost		250,000	
Piping Cost		2,246,000	
Area Cost	-	380,000	-
SUBTOTAL CONSTRUCTION COST			\$ 16,488,000
SIOH @ 5.5% (Supervision, inspection & overhead)			906,800
Contingency @ 10%			1,739,500
TOTAL CONSTRUCTION COST			\$ 19,134,300



EQUIPMENT LIST

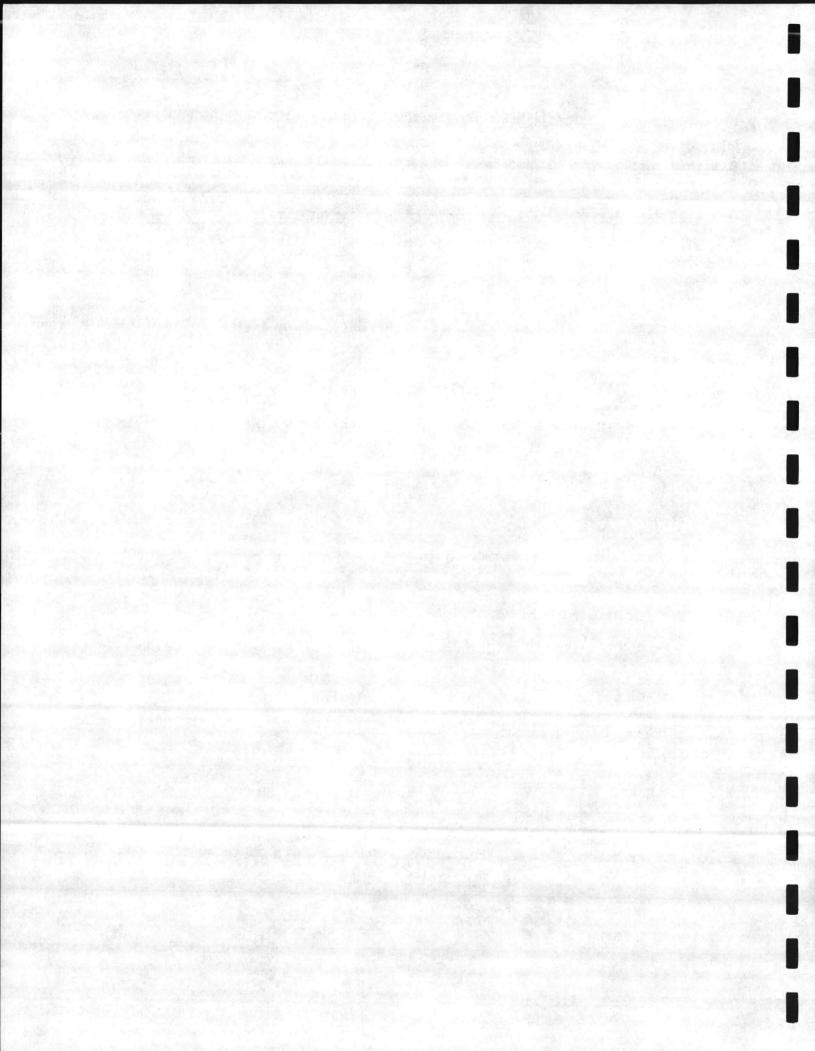
CAS		Motor	-	Equipment	quip. Supports Platforms and
	Item Description	HP-RPM	Equipment \$	Erection \$	Other Costs \$
1.	Boiler, 100 T/D Maximum Input 600 PSIG 725°F Unit No. 1		2,750,000	w/Equipment	w/Bldg. Cost
2.	F.D. Fan Coupling Controls Motor Intake Silencer	50	Incl. Incl. Incl. Incl. Incl.	w/Equipment w/Equipment w/Equipment w/Equipment w/Equipment	4,000
3.	Combustion Controls		Incl.	w/Equipment	
4.	Boiler Breeching		Incl.	w/Equipment	w/Bldg.
5.	Economizer		Incl.	w/Equipment	w/Bldg.
6.	Stoker	10	Incl.	w/Equipment	w/Boiler
7.	I.D. Fan Coupling Fluid Drive Motor	75	Incl. Incl. Incl. Incl.	w/Equipment w/Equipment w/Equipment w/Equipment	7,000
8.	Precipitator No. 1		600,000	w/Equip. Cos	st 20,000
9.	Ductwork - To Precip., Fan, Stack w/Insulation		45,000	D&E	65,000
10.	Expansion Joints		12,000	2,000	N/A
11.	Isolation Damper	5	28,000	2,000	Incl.
12.	Boiler, 100 T/D Maximum Input 600 PSIG 725°F Unit No. 2		2,750,000	w/Equip. Cos	st w/Bldg.
13.	F.D. Fan Coupling Controls Motor Intake Silencer	50	Incl. Incl. Incl. Incl. Incl.	Incl. Incl. Incl. Incl. Incl.	4,000 Incl. Incl. Incl. Incl.



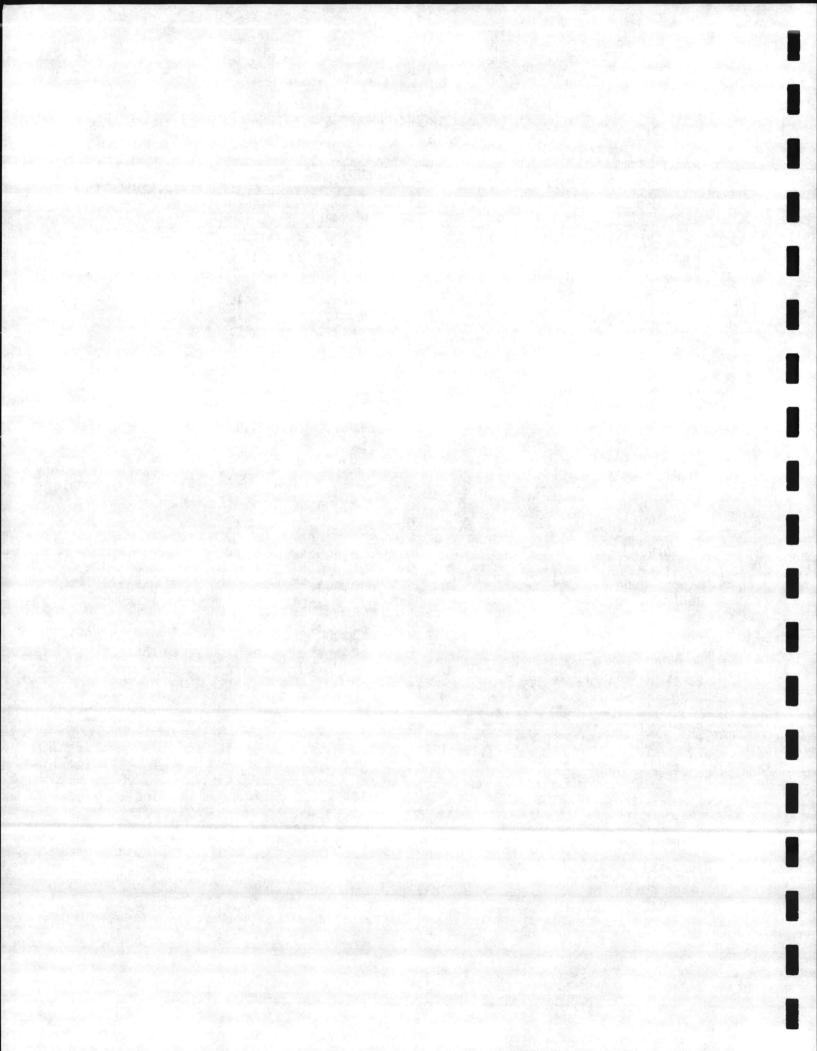
EQUIPMENT LIST

CAS	<u>E 2</u> <u>Item Description</u>	Motor HP-RPM	Equipment \$	Equipment Erection \$	Equip. Supports Platforms and Other Costs \$
14.	Combustion Controls		Incl.	Incl.	
15.	Boiler Breeching		Incl.	Incl.	w/Bldg.
16.	Economizer		Incl.	Incl.	w/Bldg.
17.	Stoker	10	Incl.	Incl.	w/Boiler
18.	I.D. Fan Coupling Fluid Drive Motor	75	Incl. Incl. Incl. Incl.	Incl. Incl. Incl. Incl.	7,000
19.	Precipitator No. 2		600,000	Incl.	20,000
20.	Ductwork - To Precip., Fan, Stack w/Insulation		45,000	D&E	65,000
21.	Expansion Joints		12,000	2,000	N/A
22.	Isolation Damper	5	28,000	2,000	N/A
23.	Ash Handling System	80 (Total)	575,000	Incl.	w/Bldg.
24.	Overhead Crane - 5 Ton Control Cab Grapple Bridge Motor Trolley Motor Hoist Motors (2)	15 10 10 (Ea)	375,000 Incl. Incl. Incl. Incl. Incl. Incl.	50,000	w/Bldg.
25.	Spare Crane Control Cab		375,000 Incl.	50,000	w/Bldg.
	Grapple Bridge Motor Trolley Motor Hoist Motors (2)	15 10 10 (Ea)	Incl. Incl. Incl. Incl.		
26.	Deaerator		30,000	2,000	1,500
27.	Blow-Off Tank		5,000	1,000	100

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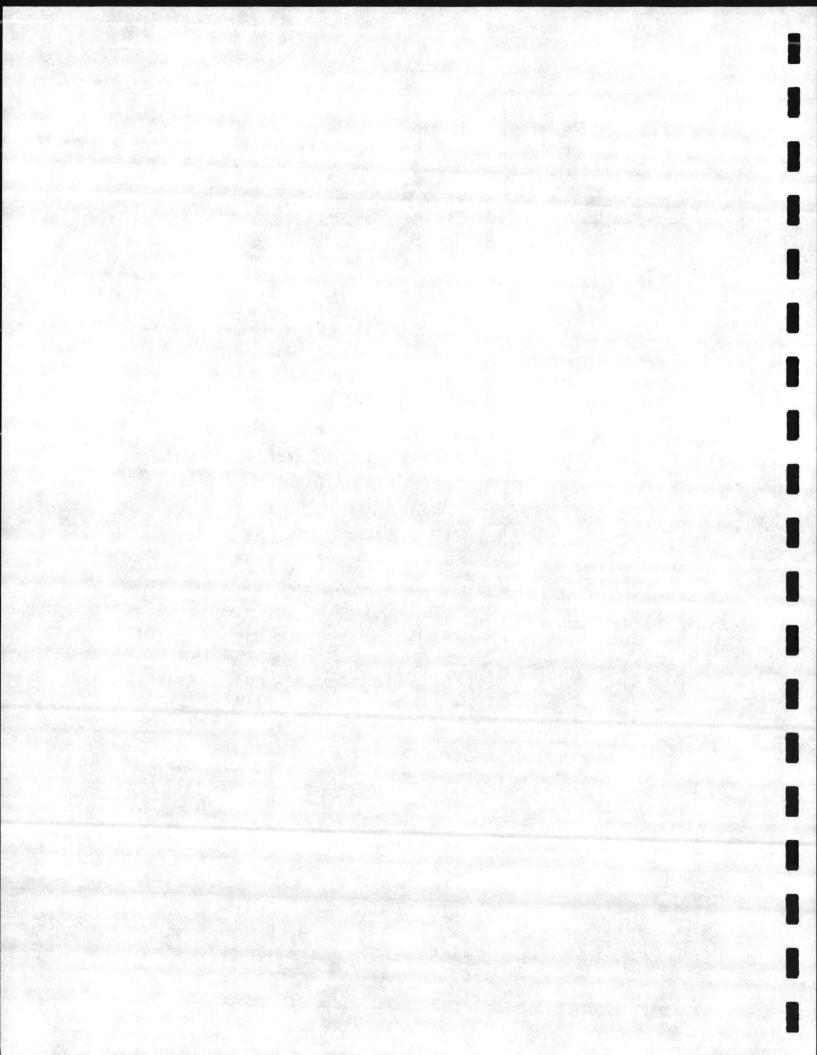


CAS	<u>E 2</u> Item Description	Motor HP-RPM	Equipment \$	Equipment Erection \$	Equip. Supports Platforms and Other Costs \$
28.	Continuous Blowdown System		17,000	2,500	500
	Flash Tank Heat Exchanger Valves		Incl. Incl. Incl.	Incl. Incl. Incl.	
29.	Condensate Tank		15,000	1,000	100
30.	Condensate Transfer Pump Motor	10	3,000 Incl.	500 500	200 200
31.	Air Compressor Air Receiver	25	6,000 Incl.	500	200
32.	Air Compressor Air Receiver	25	6,000 Incl.	500	200
33.	Air Dryer		3,000	200	100
34.	Stack - Dual Wall (2) 150' x 9'-0" Dia.		310,000	Incl.	90,000
35.	Raw Water Booster Pump Motor	20	3,000 Incl.	500 Incl.	100 Incl.
36.	Raw Water Booster Pump Motor	20	3,000 Incl.	500	100
37.	Feedwater Treatment Equipment	30 Total	70,000	8,000	1,000
38.	Boiler Feed Pumps (2) Motor	2 @ 75	16,000 Incl.	1,000 Incl.	1,000 Incl.
39.	Boiler Feed Pump Turbine		8,000 12,000	500 Incl.	500 Incl.
40.	Chemical Feed Equipment	2 @ 5	10,000	800	300



EQUIPMENT LIST

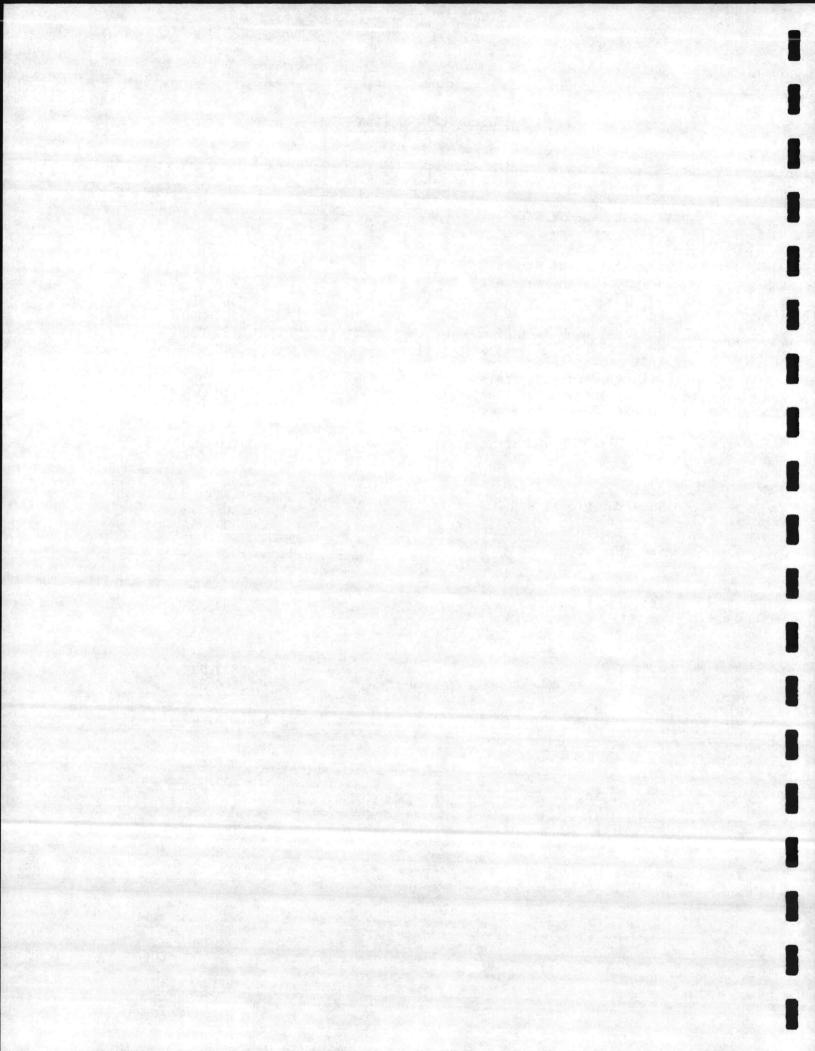
CAS	<u>E 2</u> Item Description	Motor HP-RPM	Equipment	Equipment Erection	Equip. Supports Platforms and Other Costs
			\$	ې ۲	\$
41.	Camp Geiger Condensate Transfer Pump Motor	30	7,000 Incl.	500 200	100 Incl.
42.	Air Station Condensate Transfer Pump Motor	50	7,000 Incl.	500 200	100 Incl.
43.	Condensate Collection Tank Pump Motor	10	15,000 3,000 Incl.	500 200 Incl.	200 100 Incl.
44.	No. 2 Oil Storage Tank & Pump 10,000 Gallon	5	25,000	500	500
45.	HVAC Equipment	20	15,000	Incl.	500
46.	Turbine Generator 900 KW Nominal Output 12,470 Volt Generator 1175 KVA Rating		200,000	40,000	4,800
	TOTAL, Equipment	5	\$8,984,000	\$170,600	\$294,400



CASE 2

47. Buildings and Structures Structural Steel \$ 880,000 Excavation and Backfill 445,000 Refuse Pit and Basement 690,000 Mat 365,000 Piling 86,000 Roof Deck and Roofing 190,000 Walls and Siding 270,000 Intermediate Floors 89,000 Stairs, Doors and Drains 160,000 Miscellaneous Steel and Grating 135,000 Support Steel and Miscellaneous 390,000 TOTAL, Building and Structures \$ 3,700,000 48. Electrical Building Lighting 63,000 Electrical Equipment & Wiring 400,000 TOTAL, Electrical \$ 463,000 49. Instrumentation \$ 250,000 50. Piping Boiler Plant 870,000 Export Steam & Condensate Return Lines 1,376,000 TOTAL, Piping \$ 2,246,000 51. Area Area \$ 130,000 Road Paving 250,000 TOTAL, Area \$ 380,000

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CASE 2

DESIGN ANALYSIS COMPUTATIONS

JANUARY 1982

(Present Value = 1987 Dollars)

ALTERNATIVE A - Refuse-Burning Plant

- 1. Investment Cost
 - a. Refuse-Burning Plant Capital Costs (from equipment list)

Construction	\$ 16,488,000
SIOH @ 5.5%	906,800
Contingency @ 10%	1,739,500

Total Unescalated Construction \$ 19,134,300

Total Construction escalated to April 1985 \$ 19,134,300 x 2384 = \$ 23,733,700 1922

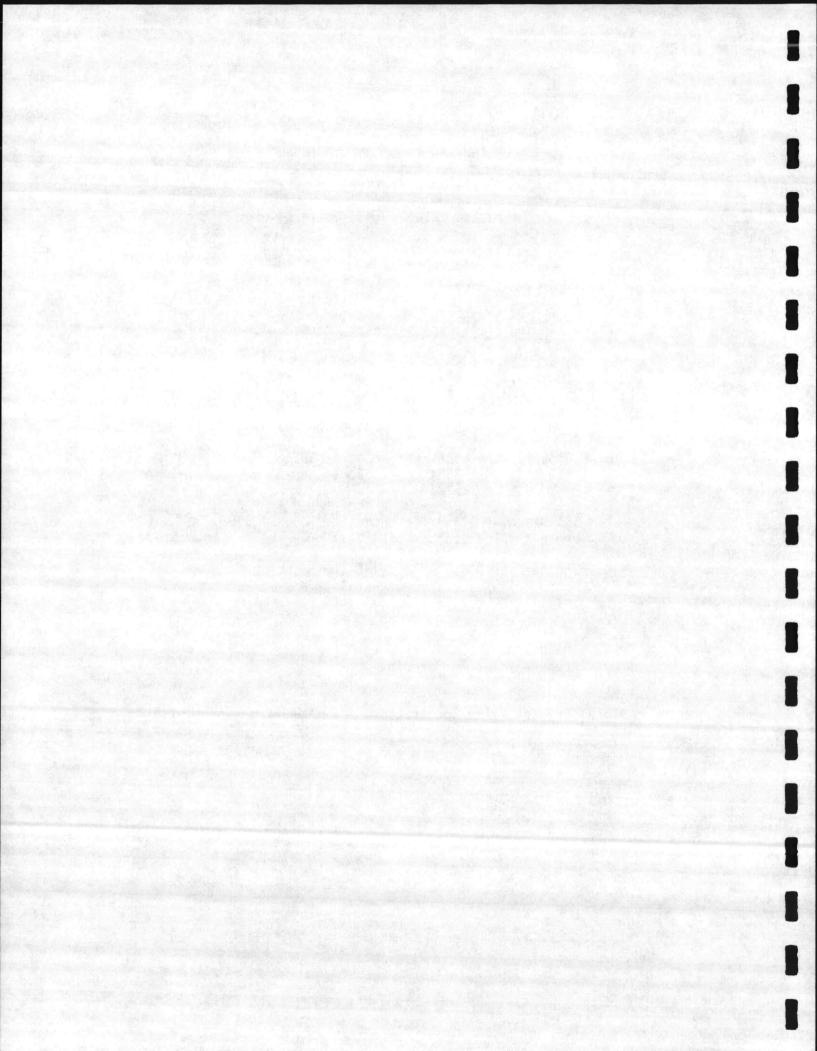
10% Discount (2% differential)1.1198Present Value Construction Cost\$ 26,

\$ 26,576,997

Engineering @ 6% = \$ 1,148,100 Engineering escalated to April 1984 \$ 1,148,100 x 2253 = \$ 1,345,800 1922

10% Discount (2% differential)1.2071Present Value Engineering\$ 1,624,515

Total Present Value Construction & Engineering \$ 28,201,512



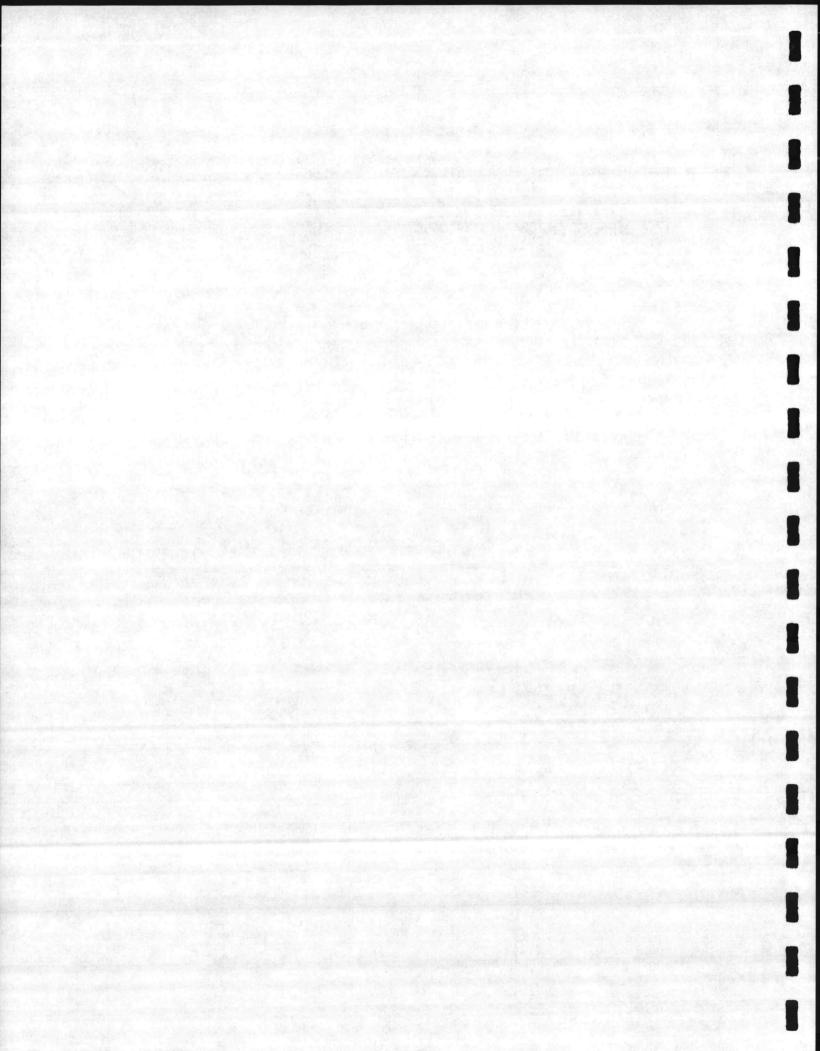
b. Capital Costs for Ash Disposal

Investment for truck (\$70,000) and disposal containers (\$26,000) \$96,000 in years 1, 9, 17

Escalated to Oct. 1987 \$96,000 x $\frac{2684}{1922}$ = \$134,060

10% Discount (2% differential) year 1.963Present Value\$129,10010% Discount (2% differential) year 9.526Present Value\$70,51610% Discount (2% differential) year 17.288Present Value\$38,609

Total Present Value Ash Disposal Investment \$238,225



2. Recurring Costs

a. Annual Boiler Plant Labor Costs

4 Crane Operators (WG-8) @ \$9.98/hr. (incl. benefits) 4 Boiler Operators (WG-7) @ \$9.43/hr. (incl. benefits) 4 Boiler Mechanics (WG-10) @ \$11.09/hr. (incl. benefits) 3 Supervisors (WS-7) @ \$12.78/hr. (incl. benefits)

Unescalated Labor Cost

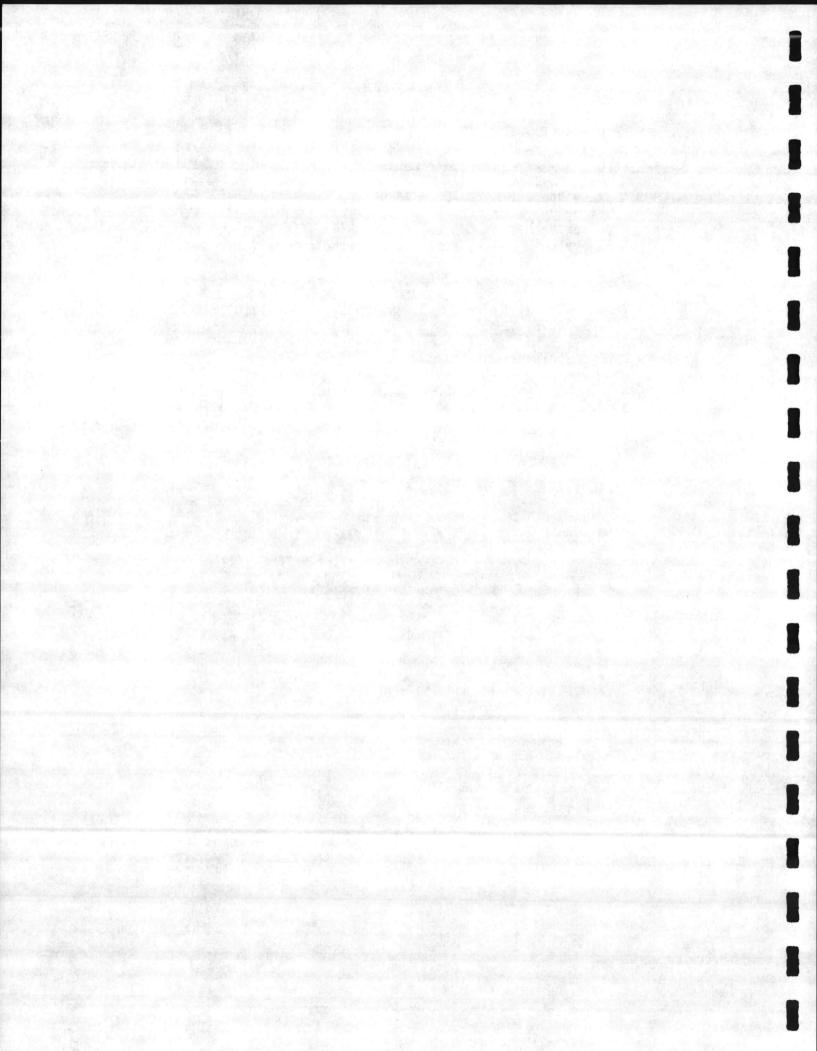
 $(4 \times 9.98 \times 2080) + (4 \times 9.43 \times 2080) + (4 \times 11.09 \times 2080)$ + $(3 \times 12.78 \times 2080) = $333,508$

Labor escalated to Oct. 1987

Fy 82 Fy 83 Fy 84 Fy 85 Fy 86 Fy 87 \$333,508 x 1.056 x 1.056 x 1.056 x 1.056 x 1.056 x 1.056 = \$462,476

10% Discount (0% differential)9.524Present Value Labor Cost\$4,404,621

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b. Annual Boiler Maintenance Cost

ITEM	INSTALLED COST (\$ X 10 ³)	MAINT. FACTOR	COST <u>(\$ X 10³)</u>
Boilers & Fans	3,250	0.025	81.25
Precipitators	1,200	0.015	18.00
Ducts & Stack	245	0.010	2.45
Ash Handling	575	0.025	14.38
Pumps	33	0.015	0.50
Water Treatment	37	0.020	.74
Building	3,400	0.005	17.00
Internal Piping	740	0.005	3.70
Export Piping	1,376	0.010	13.76
Cranes	850	0.020	17.00
Electrical Instrumentation	538	0.020	10.76
Turbine Generator	200	0.020	4.00

Total Unescalated Maintenance

183.54

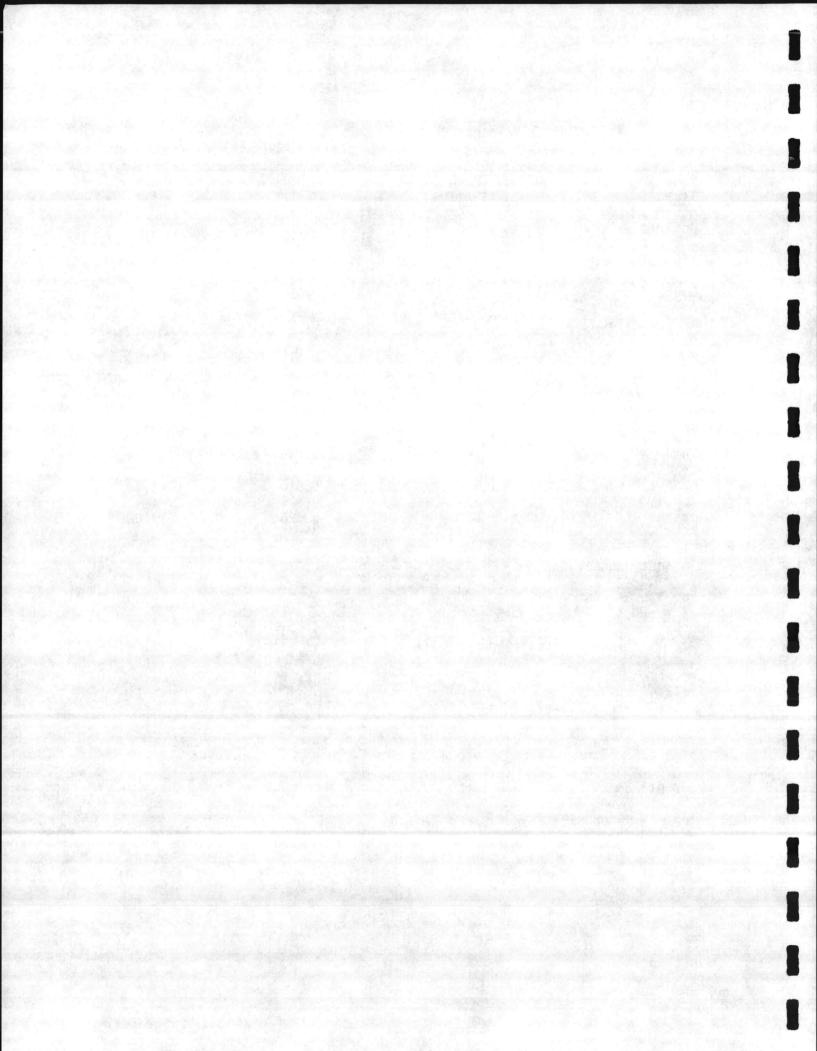
Maintenance escalated to Oct. 1987

 Fy 82
 Fy 83
 Fy 84
 Fy 85
 Fy 86
 Fy 87

 \$183,540 x 1.056 x 1.056
 \$1.056 x 1.056 x 1.056 = \$254,515

 10% Discount (0% differential)
 9.524

 Present Value Maintenance Costs
 \$2,424,005

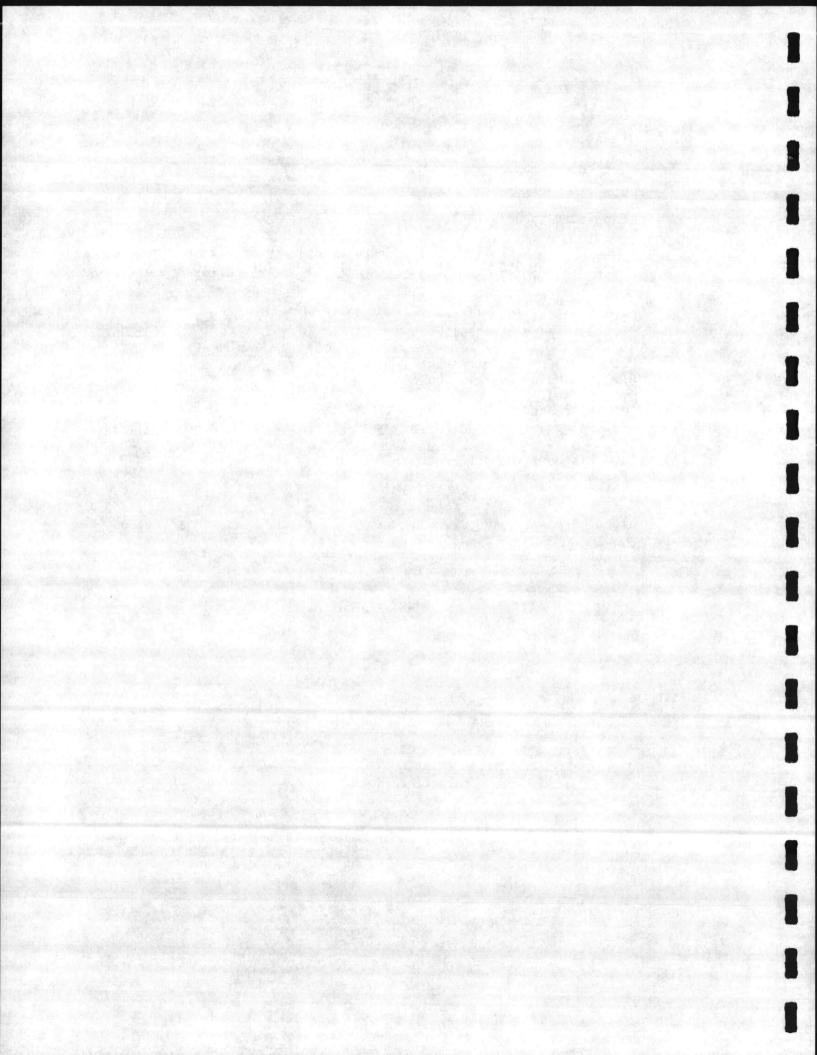


c. Plant Overhaul

\$ 50,000 every 5 years

Escalated to Oct. 1987

Fy 82 Fy 83 Fy 84 Fy 85 Fy 86 Fy 87 \$ 50,000 x 1.056 x 1.056 x 1.056 x 1.056 x 1.056 x 1.056 = \$ 69,335 10% Discount (0% differential) year 5 Present Value Overhaul Cost .652 \$ 45,206 10% Discount (0% differential) year 10 .405 Present Value Overhaul Cost \$ 28,081 10% Discount (0% differential) year 15 Present Value Overhaul Cost .251 17,403 \$ 10% Discount (0% differential) year 20 .156 Present Value Overhaul Cost \$ 10,816 Total Present Value Overhaul Costs \$ 101,506



d. Annual Incremental Electrical Costs

SERVICE	POWER (KW)	USE FACTOR	EFFECTIVE POWER
Pumping Power*	110	0.8	88
Crane Operation	30	1.0	30
Precipitators	400	0.8	320
Ash Handling	60	0.8	48
		TOTAL	486 KW

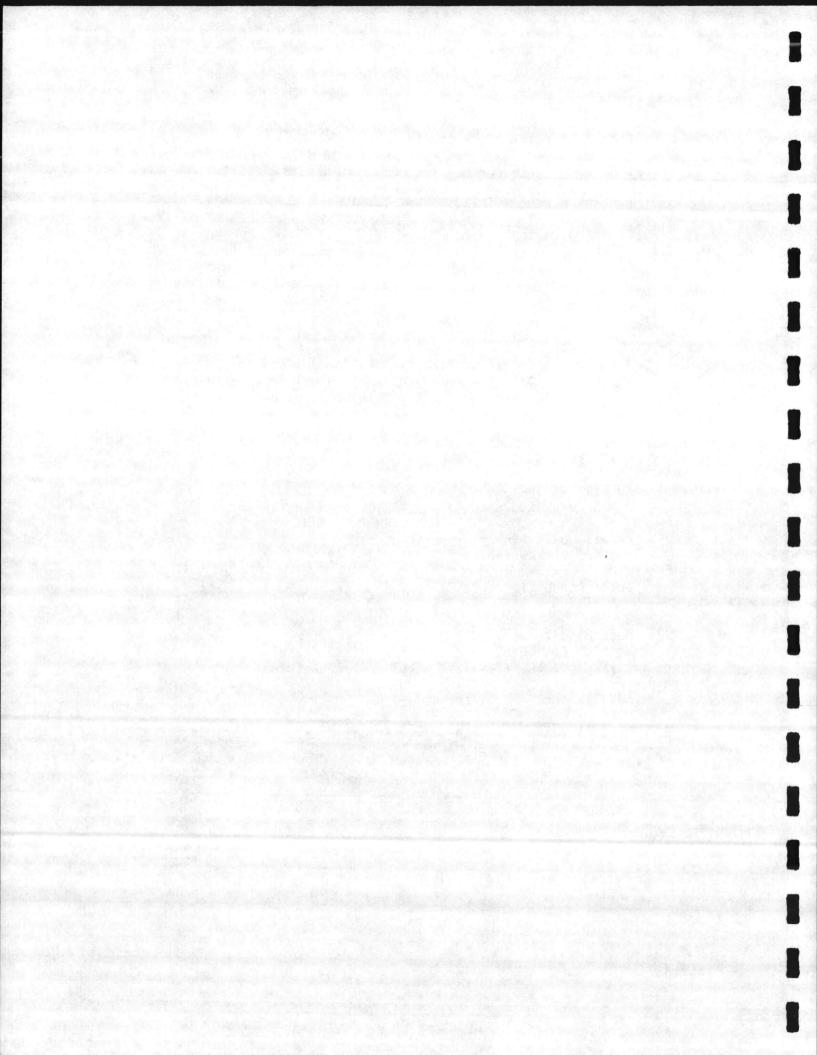
* NOTE: Feedwater pumping is not included since a reduction in existing feedwater pumping will be realized. Adjustment is made for higher pressure feedwater.

Annual Demand Cost Increase 486 KW X \$ 73.598/KW = \$ 35,769/yr.

- Annual KWH Increase 486 KW X 7000 hrs/yr. = 3,402,000 KWh/yr.
- Annual Dollar Increase per KWH
 3,402,000 KWh/hr. X \$.02726/KWh = \$ 92,738/yr.

Total Annual Increase Electrical Cost \$ 35,769 + \$ 92,738 = \$ 128,507

Escalated to Oct. 1987 FY82 FY83 FY84 FY85 FY86 FY87 \$128,507 X 1.13 X 1.13 X 1.13 X 1.13 X 1.13 X 1.13 = \$267,545 10% Discount (7% differential) 18.049 Present Value Incremental Electrical Cost \$4,828,920



e. Annual Trash Transfer Cost from Cherry Point to Lejeune

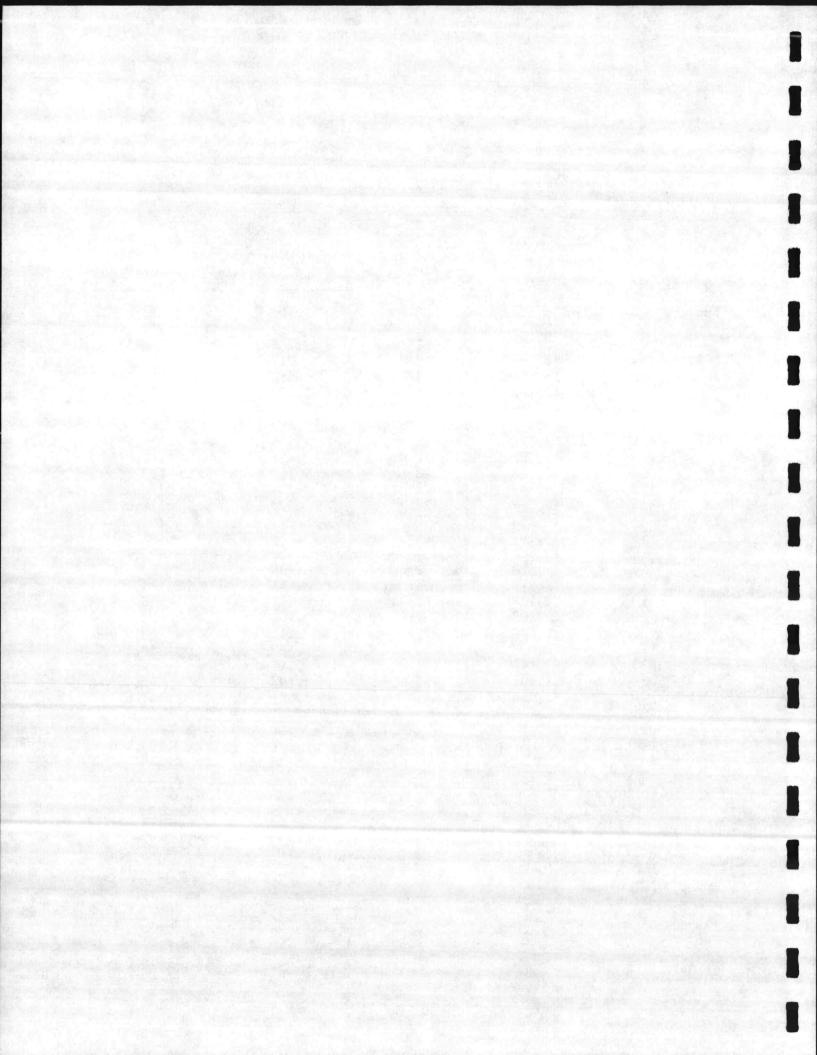
\$10/ton (1977) escalated to Oct. 1987

 $10 \times \frac{2684}{1355} = 19.81$

	Yr. of Op.	Tons/yr.	<u>\$/yr.</u>	10% Discount (0% differential)	Present Value
1987	1	15,538	\$ 307,808	.954	\$ 293,649
	2	15,793	312,859	.867	271,249
	3	16,048	317,911	.788	250,514
1990	4	16,303	322,962	.717	231,564
	5	16,558	328,014	.652	213,865
	6	16,813	333,066	.592	197,175
	7	17,068	338,117	.538	181,907
	8	17,323	343,169	.489	167,809
	9	17,578	348,220	.445	154,958
	10	17,833	353,272	.405	143,075
	11	18,088	358,323	.368	131,863
	12	18,343	363,375	.334	121,367
	13	18,598	368,426	.304	112,002
2000	14	18,853	373,478	.276	103,080
	15	19,108	378,529	.251	95,011
	16	19,363	383,581	.228	87,456
	17	19,618	388,632	.208	80,836
	18	19,873	393,684	.189	74,406
	19	20,128	398,763	.172	68,582
	20	20,383	403,787	.156	62,991
	21	20,638	408,839	.142	58,055
	22	20,893	413,890	.129	53,392
	23	21,148	418,942	.117	49,016
	24	21,403	423,993	.107	45,367
2011	25	21,658	429,045	.097	41,617

Total Present Value Transfer Cost

\$3,290,806



f. Annual Ash Disposal Cost

	Yr. of Op.	<u>1982 \$*</u>	<u>1987 \$*</u>	10% Discount (0% differential)	Present Value
1987	1	\$ 13,702	\$ 19,134	.954	\$ 18,254
	2	13,756	19,210	.867	16,655
	3	13,862	19,358	.788	15,254
1990	4	13,916	19,433	.717	13,933
	5	14,022	19,581	.652	12,767
	5 6 7	14,075	19,655	.592	11,636
	7	14,128	19,729	.538	10,614
	8	14,950	20,877	.489	10,209
	8 9	15,003	20,951	.445	9,323
	10	15,110	21,101	.405	8,586
	11	15,163	21,175	.368	7,792
	12	15,216	21,249	.334	7,097
	13	15,269	21,323	.304	6,482
2000	14	15,323	21,398	.276	5,906
	15	15,376	21,472	.251	5,389
	16	15,429	21,546	.228	4,912
	17	15,535	21,694	.208	4,512
	18	15,588	21,768	.189	4,114
	19	15,642	21,843	.172	3,757
	20	15,748	21,991	.156	3,431
	21	15,802	22,067	.142	3,134
	22	15,855	22,141	.129	2,856
	23	15,908	22,215	.117	2,599
	24	16,014	22,363	.107	2,393
2011	25	16,067	22,437	.097	2,176

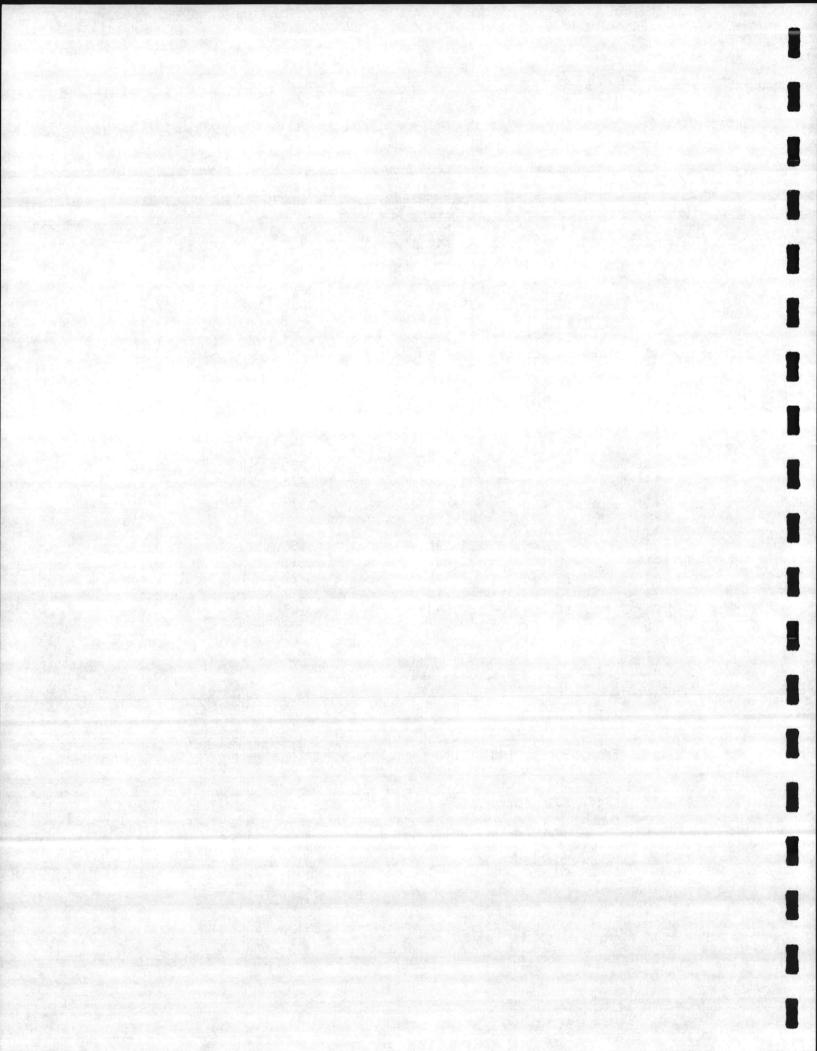
Total Present Value Ash Disposal Cost

\$ 193,781

* Escalation from 1982 to 1987 = $\frac{2684}{1922}$ = 1.3965

Ash - 80 lbs/cf. 30% moisture

Ash Disposal - 5 days per week



3. Benefits -

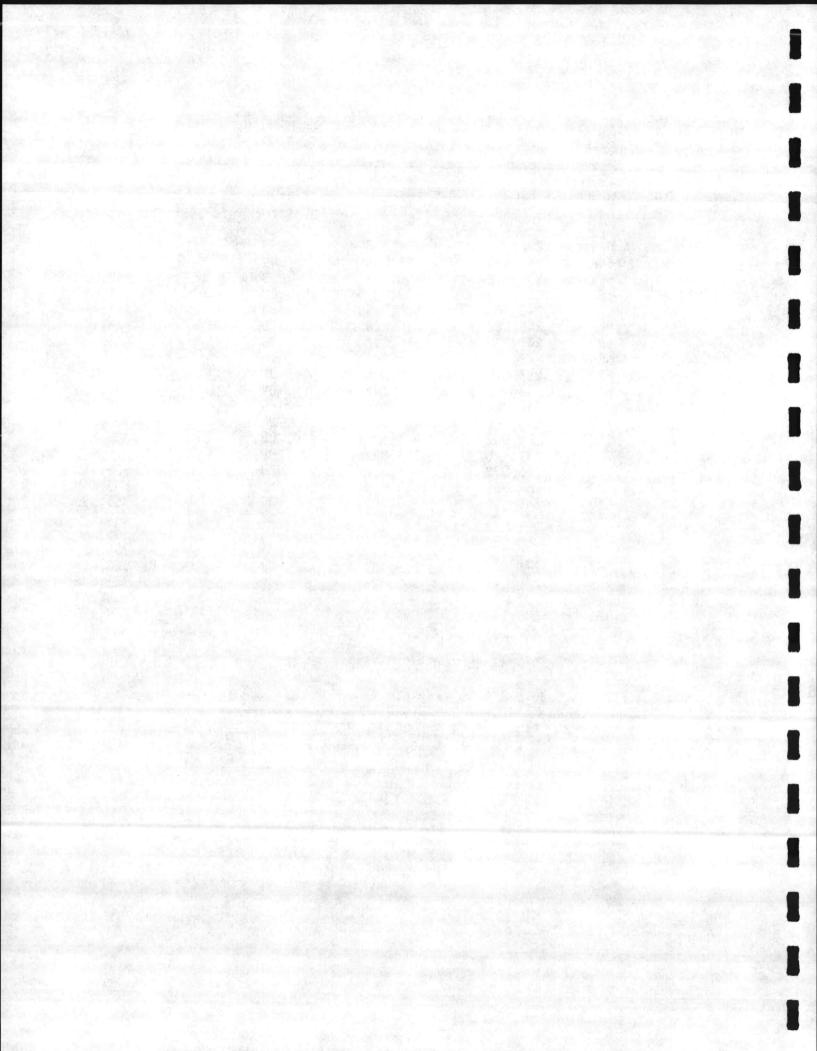
Revenues generated from sale of electricity to CP&L

Year		Kw/hr * merated	Net Revenue Jan. 1982 \$	** Oct. 1987 \$	10% Discount (7% differential)	Present Value
1987	1	640	\$ 232,640	\$ 484,345	.986	\$ 477,564
	2	646	234,821	488,886	.959	468,842
	3	655	238,092	495,697	.933	462,485
1990	4	660	239,910	499,481	.908	453,529
	5	670	243,545	507,049	.883	447,724
	6	674	244,999	510,076	.859	438,155
	7	680	247,180	514,617	.836	430,220
	8	685	248,998	518,401	.813	421,460
	9	690	250,815	522,185	.791	413,048
	10	700	254,450	529,752	.769	407,380
	11	705	256,268	533,536	.748	399,085
	12	710	258,085	537,320	.728	391,169
	13	715	259,902	541,104	.708	383,102
2000	14	720	261,720	544,888	.688	374,883
	15	725	263,538	548,672	.670	367,610
	16	730	265,355	552,456	.651	359,649
	17	740	268,990	560,024	.634	355,055
	18	745	270,808	563,808	.616	347,306
	19	750	272,625	567,592	.600	340,555
	20	760	276,260	575,160	.583	335,318
	21	766	278,441	579,701	.567	328,690
	22	770	279,895	582,728	.552	321,666
	23	775	281,712	586,512	.537	314,957
	24	785	285,348	594,080	.522	310,110
2011	25	790	287,165	597,864	.508	303,715

\$ 9,653,277 Total Present Value Electricity Revenues Benefit

Source: CP&L Schedule CSP-4, Variable Energy Credit and 10-Year Capacity Credit Escalation from Jan. 1982 to Oct. 1987 = Fy82 Fy83 Fy84 Fy85 Fy86 Fy87 1.13 X 1.13 X 1.13 X 1.13 X 1.13 X 1.13 = 2.0819516

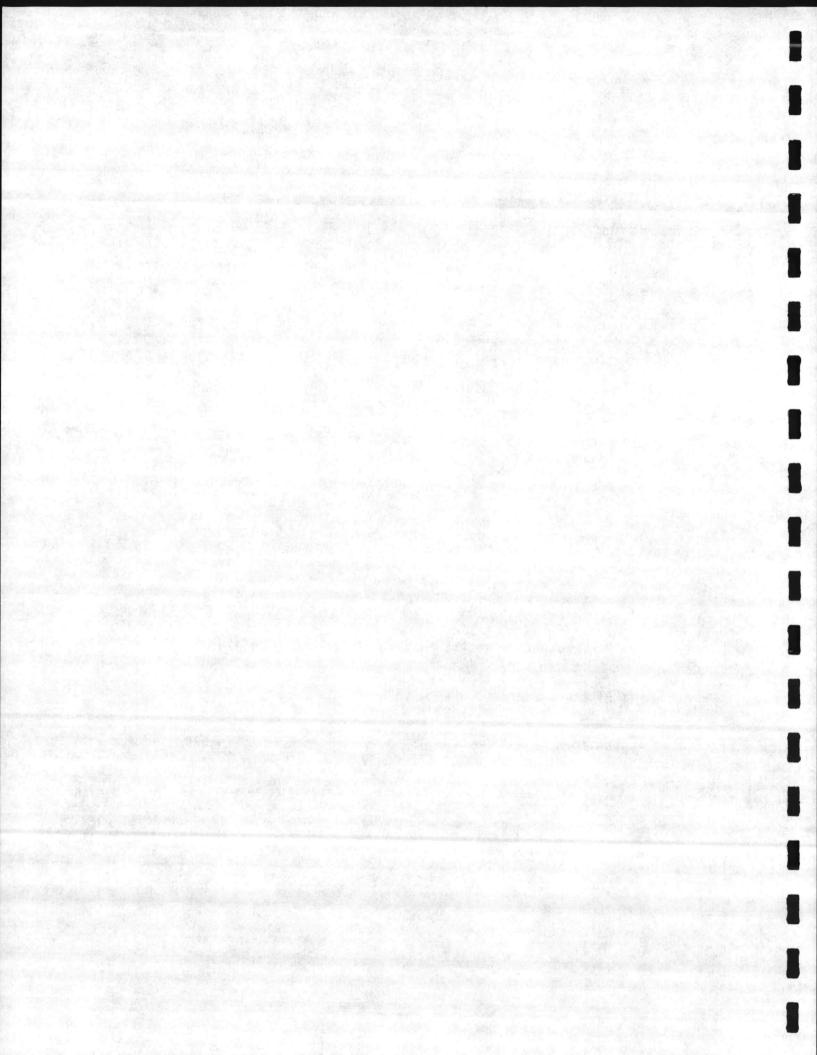
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Summary	Sheet	Alternative	2A -	Total	Present	Val	ue
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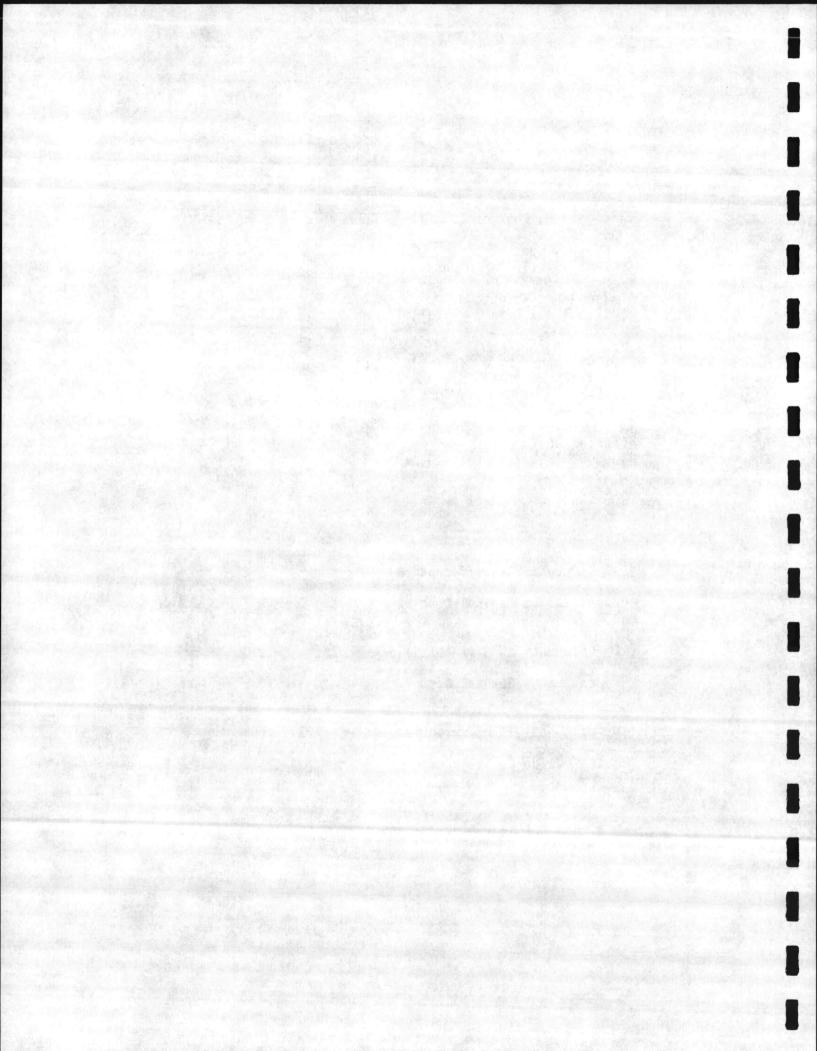
Investment Cost	
Boiler Plant	\$ 28,201,512
Ash Disposal	238,225
Recurring Costs	
Labor	4,404,621
Maintenance	2,424,005
Plant Overhaul	101,506
Incremental Electrical	4,828,920
Trash Transfer	3,290,806
Ash Disposal	193,781
Total Present Value Cost	\$ 43,683,376
Less Present Value Benefits Sale of Electricity	\$_9,653,277
Net Present Value Alternative 2A	\$ 34,030,099
Discount Factor 9.524	
Uniform Annual Cost	\$ 3,573,089

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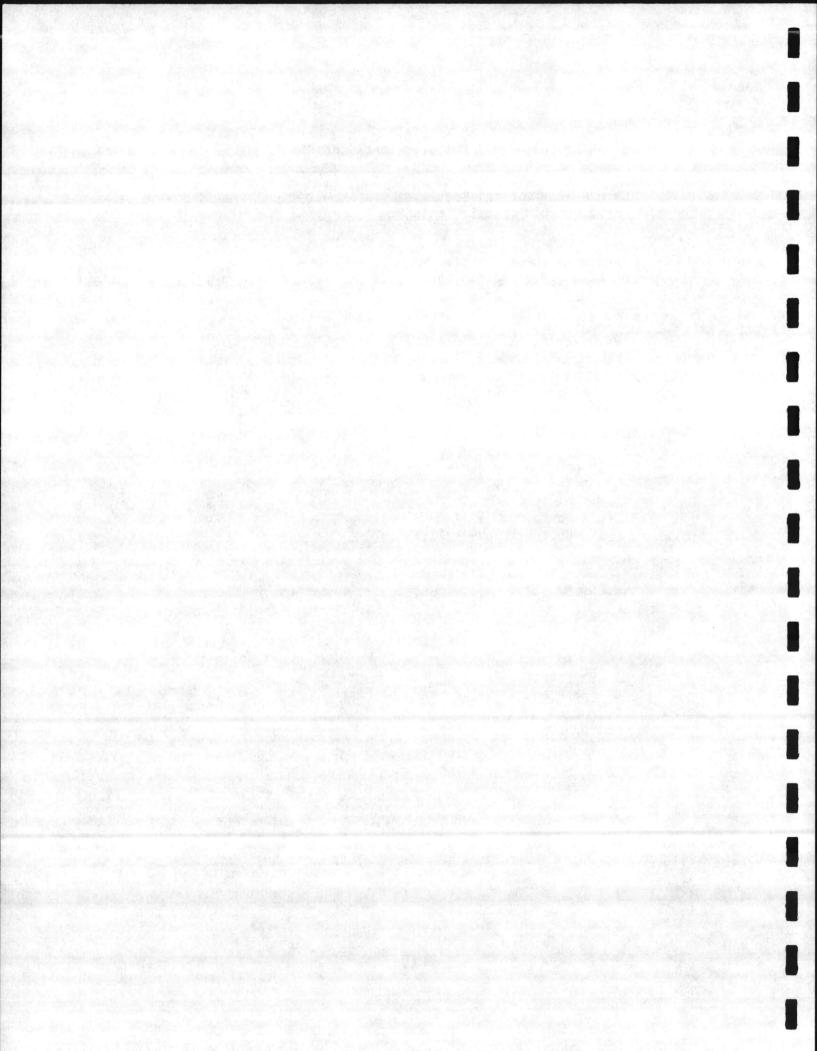


VI-19

<u>ALTERNATIVE B</u> - Incremental Cost of Refuse Landfills at Cherry Camp Lejeune	Point and
1. Investment Costs	
a. Incremental Cost of Landfill - Cherry Point	
Capital Cost \$298,704 (1977) in year 5	
Escalated to Oct. 87 $298,704 \times \frac{2684}{1355} = $591,676$	
10% Discount (2% differential) year 5 .712	
Present Value Capital Cost	\$421,274
Capital Cost \$36,000 (1977) in years 8, 16, 23	
Escalated to Oct. 1987 $36,000 \times \frac{2684}{1355} = $71,309$	
10% Discount (2% differential) year 8 .568	
Present Value Capital Cost	\$ 40,504
10% Discount (2% differential) year 16 .310	
Present Value Capital Cost	\$ 22,106
10% Discount (2% differential) in year 23 .183	
Present Value Capital Cost	\$ 13,050
Total Present Value Capital Costs - Cherry Point	\$496,934



b.	Existing Boiler Plant Replacement/Upgradin	g Cost
	Camp Geiger Capital Cost \$2,000,000 (1982\$) in 1989	
	Escalated to Oct. 1987 $\$2,000,000 \times \frac{2684}{1922} = \$2,792,924$	
	10% Discount (2% differential) year 2	.893
	Present Value Capital Cost	\$2,494,081
	Air Station Capital Cost \$2,000,000 (1982) in 1996	
	Escalated to Oct. 1987 $\$2,000,000 \times \frac{2684}{1922} = \$2,792,924$	
	10% Discount (2% differential) year 10	.488
	Present Value Capital Cost	\$1,362,947
	Total Present Value Replacement Costs	\$3,857,028



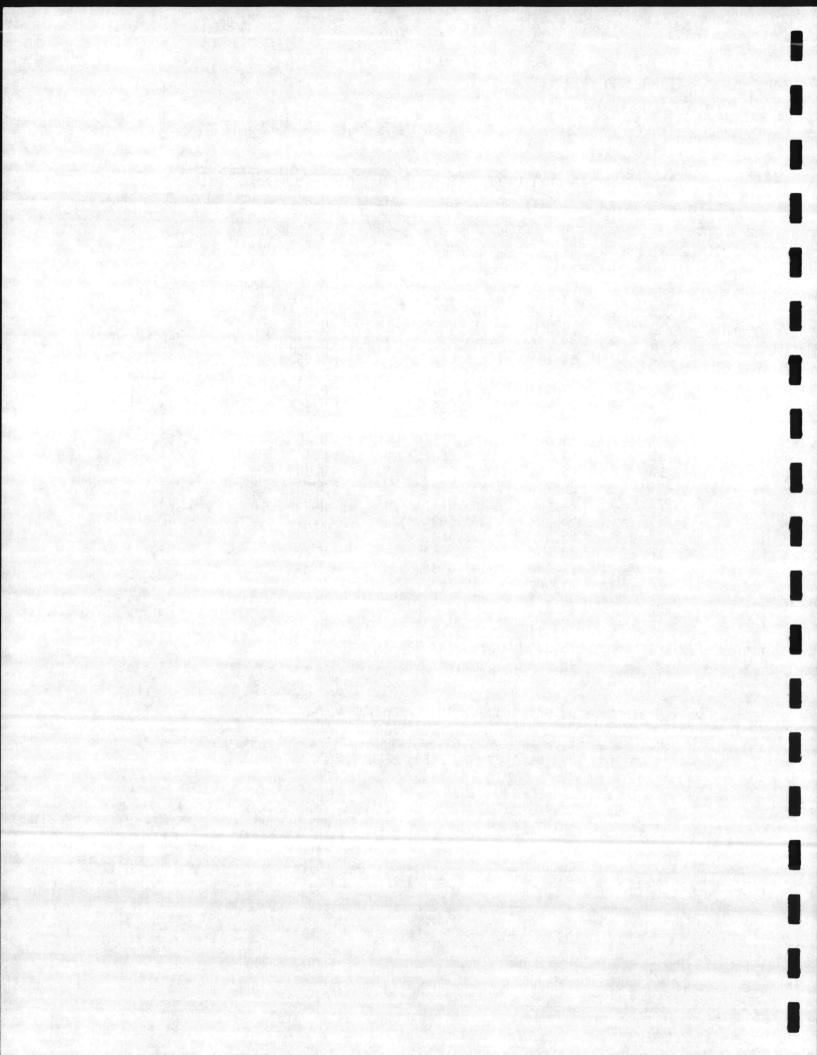
2. Recurring Costs

a. Annual Incremental Landfill Development Cost - Cherry Point

Year Y	r. of Op.	1977\$*	1987\$*	10% Discount (2% differential)	<u>P</u>	resent Value
1987	1	53,312	105,600	0.963	\$	101,693
	2	54,208	107,375	0.893		95,886
	3	55,104	109,150	0.828		90,376
1990	4	56,000	110,925	0.768		85,190
	5	56,896	112,700	0.712		80,242
	6 7	57,792	114,474	0.660		75,553
	7	60,438	119,716	0.612		73,266
	8	61,334	121,490	0.568		69,006
	9	62,230	123,265	0.526		64,837
	10	63,126	125,040	0.488		61,020
	11	64,022	126,815	0.453		57,447
	12	64,918	128,590	0.420		54,008
	13	65,814	130,364	0.389		50,712
2000	14	66,710	132,139	0.361		47,702
	15	67,606	133,914	0.335		44,861
	16	68,502	135,689	0.310		42,064
	17	69,398	137,464	0.288		39,590
	18	70,294	139,238	0.267		37,177
	19	71,190	141,013	0.247		34,830
	20	72,086	142,788	0.229		32,698
	21	72,982	144,563	0.213		30,744
	22	73,878	146,338	0.197		28,829
	23	74,774	148,112	0.183		27,105
	24	75,670	149,887	0.170		25,481
2011	25	76,566	151,662	0.157		23,811

Total Present Value Development Cost - Cherry Point

\$ 1,374,128

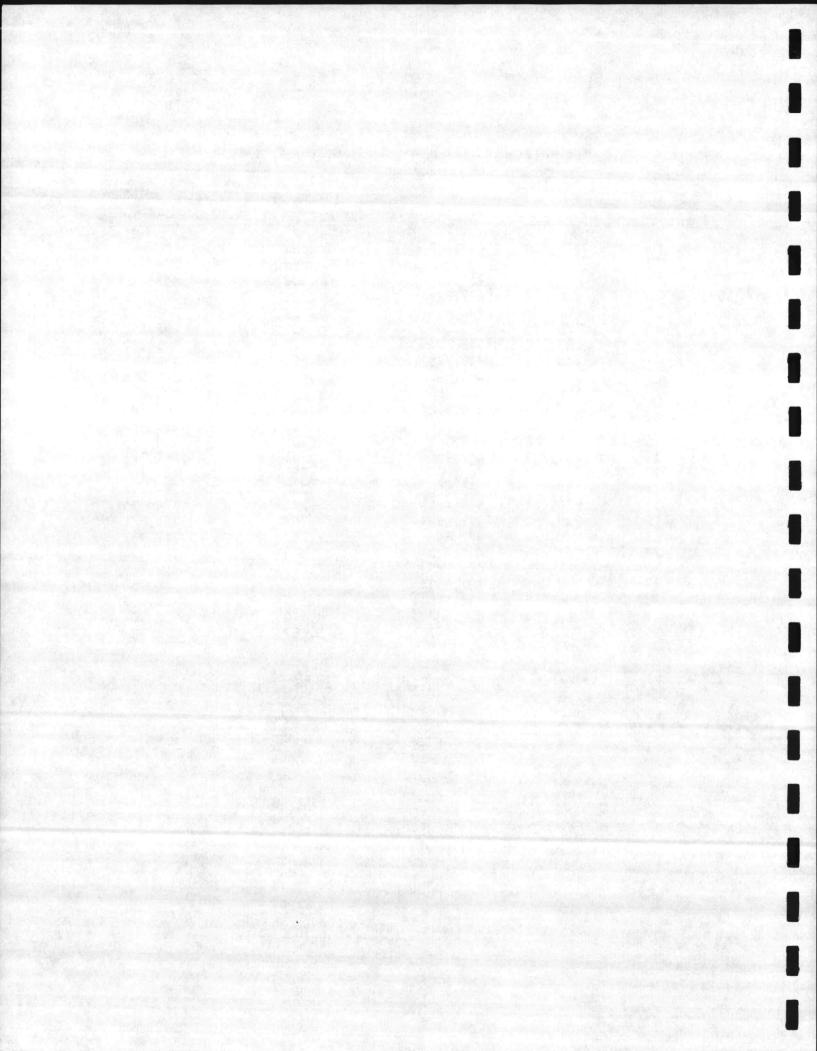


	Yr. of Op.	<u>1977\$*</u>	<u>1987\$*</u>	10% Discount (2% differential)	Pres	ent Value
1987		\$ 215,809	\$ 427,477	.963		11,660
	2	217,609	431,042	.893		84,921
	3	219,157	434,109	.828	3	59,442
1990	4	220,956	437,672	.768	3	36,132
	5	222,505	440,741	.712	3	13,808
	5 6 7	224,304	444,304	.660	2	93,241
	7	223,732	443,171	.612	2	71,221
	8 9	225,532	446,736	.568	2	53,746
	9	227,331	450,300	.526	2	36,858
	10	228,879	453,366	.488	2	21,243
	11	230,679	456,932	.453		06,990
	12	230,107	455,799	.420		91,436
	13	231,906	459,362	.389		78,692
2000	14	233,706	462,928	.361		67,117
	15	233,134	461,795	.335		54,701
	16	234,933	465,358	.310		44,261
	17	236,481	468,424	.288		34,906
	18	238,281	471,990	.267		26,021
	19	240,080	475,553	.247		17,462
	20	241,629	478,622	.229		09,604
	21	243,428	482,185	.213		02,705
	22	242,856	481,052	.197		94,767
	23	244,655	484,616	.183		88,685
	24	246,204	487,684	.170		82,906
2011	25	248,003	491,247	.157		71,126

b. Annual Incremental Landfill Development Cost - Camp Lejeune

Total Present Value Development Costs - Camp Lejeune

\$ 5,053,651

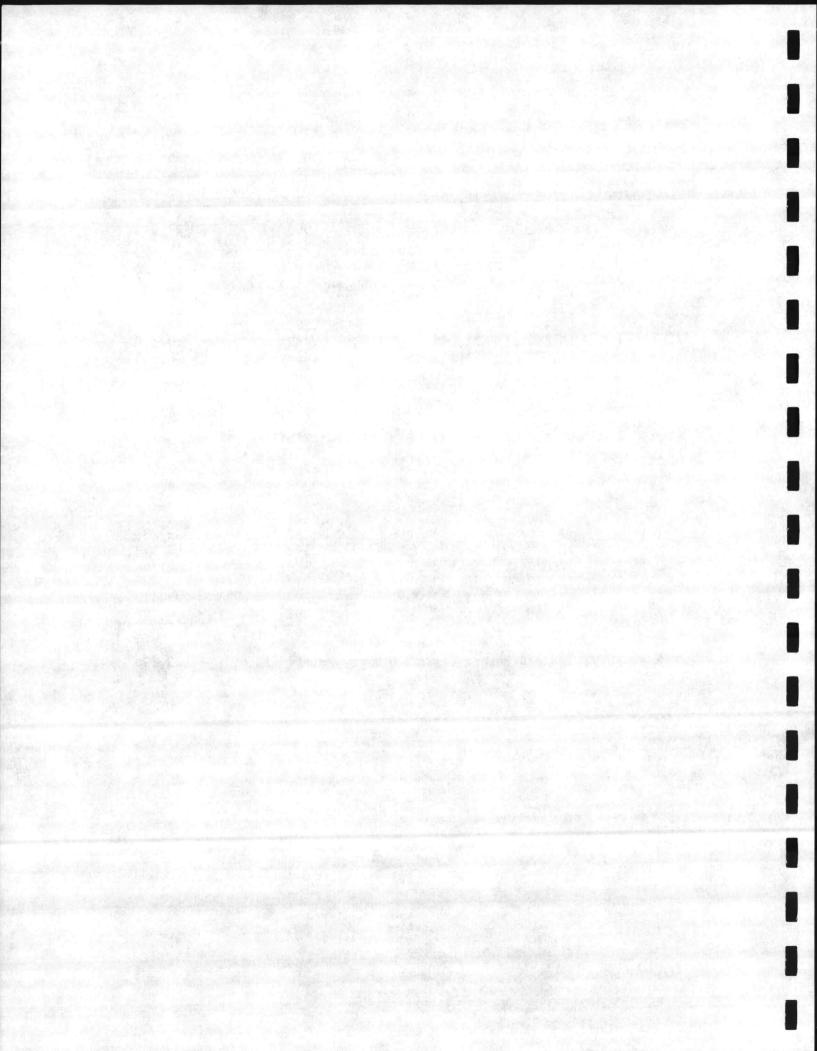


Year	Yr. of Op.	<u>1977\$*</u>	<u>1987\$*</u>	10% Discount (0% differential)	Present Value
1987	1	\$ 9,520	\$ 18,857	.954	\$ 17,990
	2	9,680	19,174	.867	16,624
	2 3	9,840	19,491	.788	15,359
1990	4	10,000	19,808	.717	14,202
	5	10,160	20,125	.652	13,122
	4 5 6 7	10,230	20,442	.592	11.914
		10,480	20,759	.538	11,168
	8 9	10,640	21,076	.489	10,306
	9	10,800	21,393	.445	9,520
	10	10,960	21,710	.405	8,793
	11	11,120	22,027	.368	8,106
	12	11,280	22,343	.334	7,463
	13	11,440	22,660	.304	6,889
2000	14	11,600	22,977	.276	6,342
	15	11,760	23,294	.251	5,847
	16	11,920	23,611	.228	5,383
	17	12,080	23,928	.208	4,977
	18	12,240	24,245	.189	4,583
	19	12,400	24,562	.172	4,225
	20	12,560	24,879	.156	3,881
	21	12,720	25,196	.142	3,579
	22	12,880	25,513	.129	3,292
	23	13,040	25,830	.117	3,022
	24	13,200	26,147	.107	1,412
2011	25	13,360	26,463	.097	1,296

c. Annual Incremental Landfill Maintenance Cost - Cherry Point

Total Present Value Maintenance Costs - Cherry Point

\$ 199,295

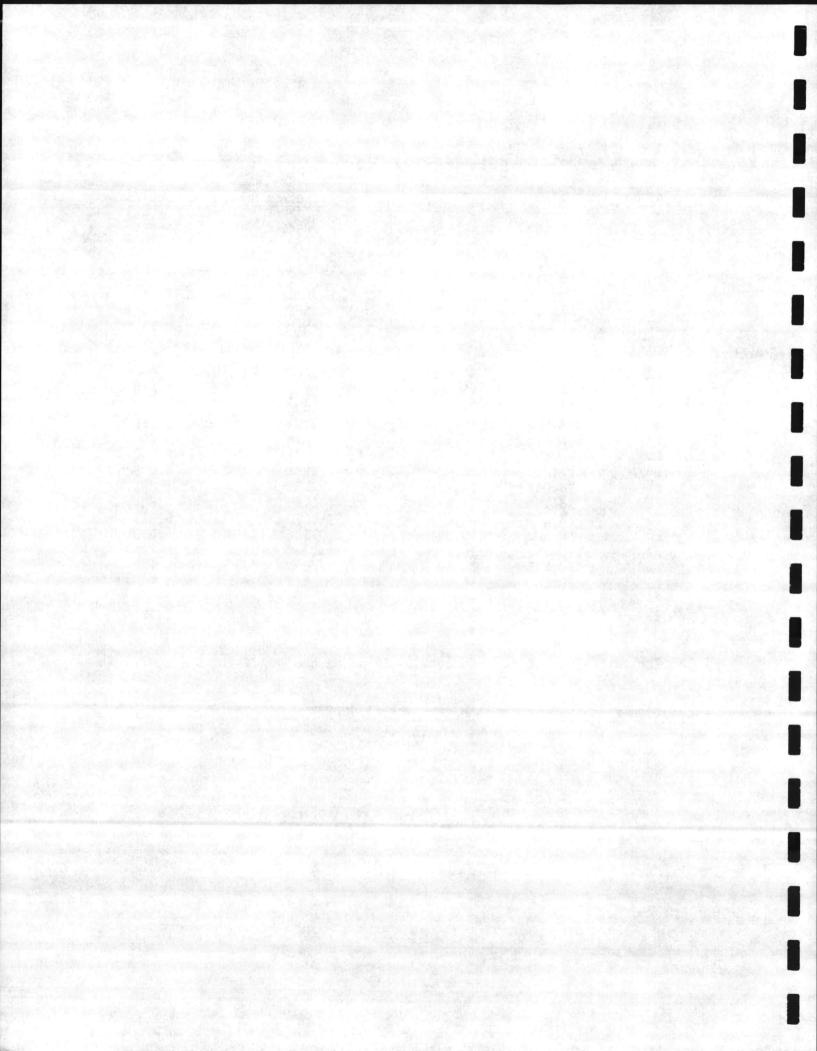


	Yr. of Op.	1977\$*	<u>1987\$*</u>	10% Discount (0% differential)	Present Value
1987	1	\$ 16,460	\$ 32,604	.954	\$ 31,104
	2	16,597	32,876	.867	28,503
	3	16,715	33,109	.788	26,090
1990		16,853	33,383	.717	23,936
	5	16,971	33,616	.652	21,918
	6	17,108	33,888	.592	20,062
	7	17,064	33,801	.538	18,185
	8	17,202	34,074	.489	16,662
	9	17,339	34,345	.445	15,284
	10	17,457	34,579	.405	14,004
	11	17,594	34,850	.368	12,825
	12	17,551	34,765	.334	11,612
	13	17,688	35,037	.304	10,651
2000	14	17,825	35,308	.276	9,745
	15	17,781	35,221	.251	8,840
	16	17,919	35,494	.228	8,093
	17	18,037	35,728	.208	7,431
	18	18,174	35,999	.189	6,804
	19	18,311	36,271	.172	6,239
	20	18,429	36,504	.156	5,695
	21	18,567	36,778	.142	5,222
	22	18,523	36,691	.129	4,733
	23	18,660	36,962	.117	4,325
	24	18,778	37,196	.107	3,980
2011	25	18,915	37,467	.097	3,634

d. Annual Incremental Landfill Maintenance Cost - Camp Lejeune

Total Present Value Maintenance Costs - Camp Lejeune

\$ 325,577



Annual Incremental Cost of #6 Fuel Oil at Camp Geiger and Air Station Plants e.

	av. tons/day trash burned tons/hr trash lbs steam/hr		- 24 hours/day X 5830 lb. stea X 1254 Btu/lb**	a state of the second	= ton = equ = MMB				
	MMBt	u/hr		X \$12.99/MMBtu*	***	= \$/h			
	\$/hr			X 8760 hrs/yr		= \$/y	r		
	\$/yr	· · · ·		X discount fact	or	= pre	esent value		
					Displaced Oil Input			10% Discount	
	Year	tons/day	tons/hr.	lbs steam/hr.	MMBtu/hr.	\$/hr.	\$/yr.	(8% differential)	Present Value
1987	1	128	5.33	31,093	38.99	\$ 506.49	\$ 4,436,884	.991	\$ 4,396,952
	2	129	5.38	31,336	39.30	510.45	4,471,547	.973	4,350,815
	3	131	5.46	31,822	39.90	518.36	4,540,873	.955	4,336,534
1990	4	132	5.50	32,065	40.21	522.32	4,575,537	.938	4,291,853
	5	134	5.58	32,551	40.82	530.24	4,644,863	.921	4,277,919
	6	135	5.62	32,794	41.12	534.19	4,679,526	.904	4,230,291
	7	136	5.67	33,037	41.43	538.15	4,714,189	.888	4,186,200
	8	137	5.71	33,280	41.73	542.11	4,748,852	.871	4,136,250
	9	138	5.75	33,522	42.04	546.06	4,783,516	.856	4,094,689
	10	140	5.83	34,008	42.65	553.98	4,852,842	.840	4,076,387
	11	141	5.88	34,251	42.95	557.93	4,887,505	.825	4,032,192
	12	142	5.92	34,494	43.26	561.89	4,922,168	.810	3,986,956
	13	143	5.96	34,737	43.56	565.85	4,956,831	.795	3,940,681
2000	14	144	6.00	34,980	43.86	569.80	4,991,494	.781	3,898,357
	15	145	6.04	35,223	44.17	573.76	5,026,157	.766	3,850,036
	16	146	6.08	35,466	44.47	577.72	5,060,821	.752	3,805,737
	17	148	6.17	35,952	45.08	585.63	5,130,147	.739	3,791,179
	18	149	6.21	36,194	45.39	589.59	5,164,810	.725	3,744,487
	19	150	6.25	36,438	45.69	593.55	5,199,473	.712	3,702,025
	20	152	6.33	36,923	46.30	601.46	5,268,800	.699	3,682,891
	21	153	6.38	37,166	46.61	605.42	5,303,463	.687	3,643,479
	22	154	6.42	37,409	46.91	609.38	5,338,126	.674	3,597,897
	23	155	6.46	37,652	47.22	613.33	5,372,789	.662	3,557,786
	24	157	6.54	38,138	47.82	621.25	5,442,115	.650	3,537,375
2011	25	158	6.58	38,381	48.13	625.20	5,476,778	.638	3,494,185

Total Present Value Fuel Oil Cost

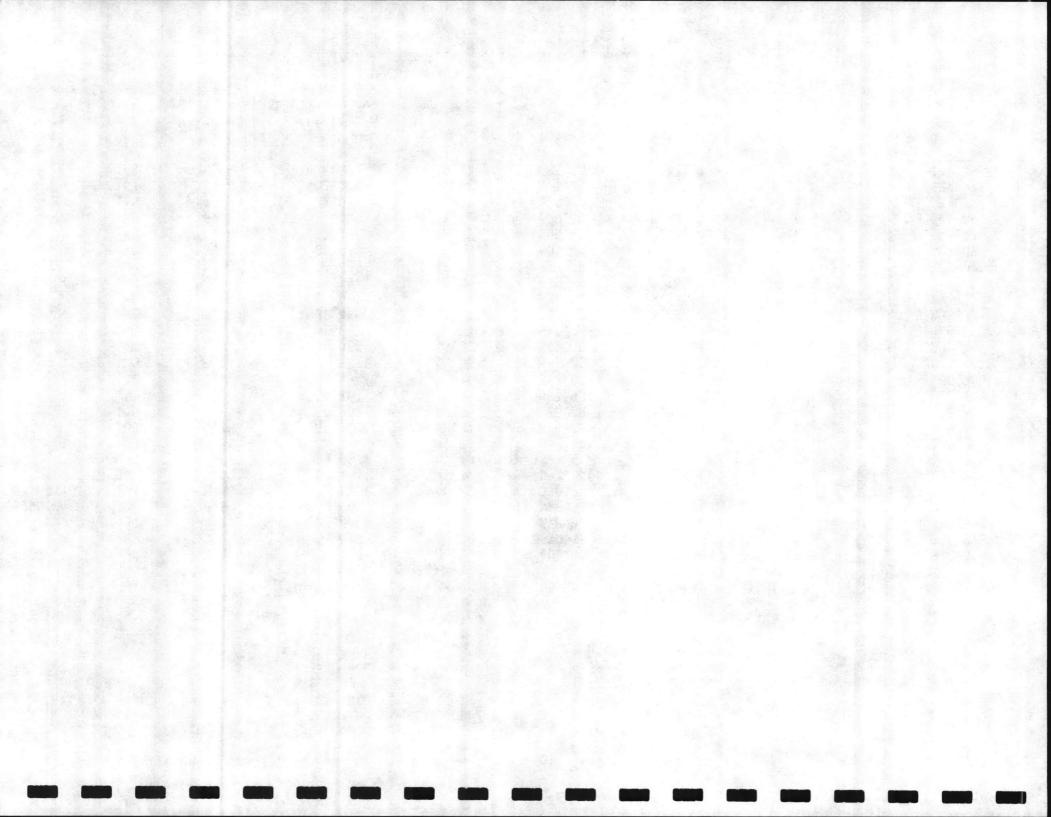
\$ 98,642,153

* Includes blowdown and feedwater heating

** Includes Camp Geiger Plant Efficiency

*** \$5.92 (Jan. 82) escalated to Oct. 87

Fy82 Fy83 Fy84 Fy85 Fy86 Fy87 \$5.92 X 1.14 X 1.14 X 1.14 X 1.14 X 1.14 = \$12.99



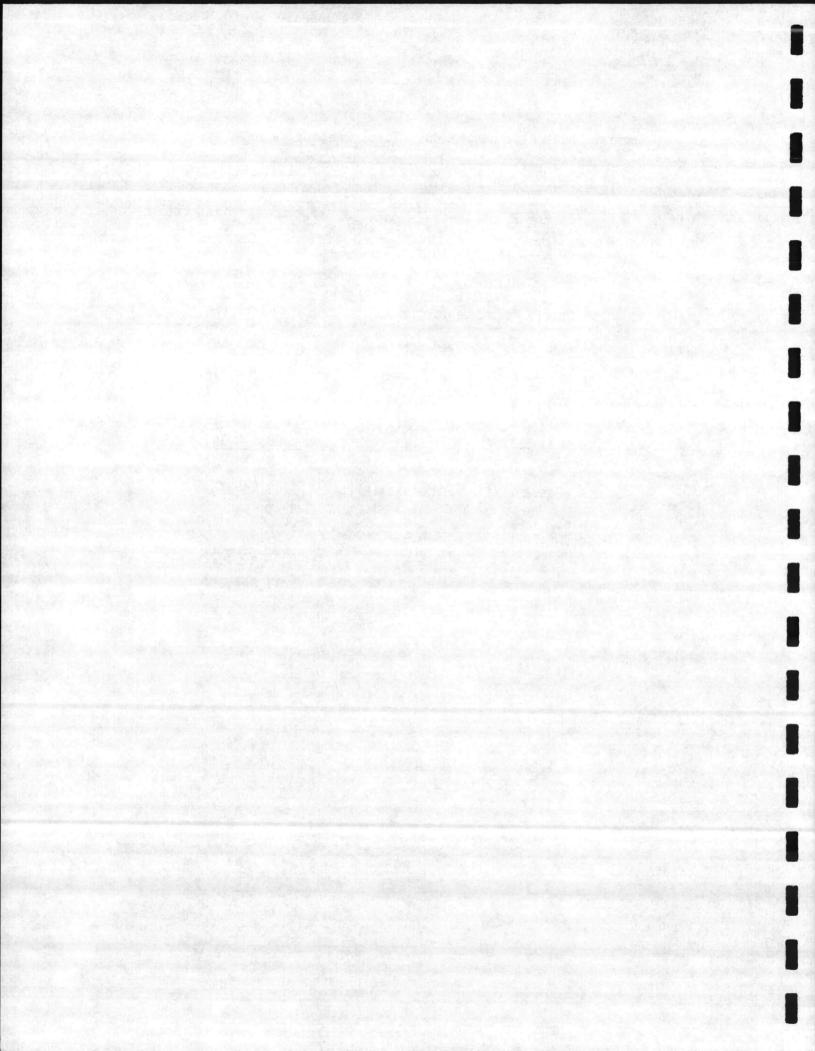
Summary Sheet Alternative 2B - Total Present Value

Investment Costs

Cherry Point Capital Costs	\$	496,934
Boiler Plant Replacement Cost		3,857,028
Recurring Costs		
Cherry Point Development		1,374,128
Camp Lejeune Development		5,053,651
Cherry Point Maintenance		199,295
Camp Lejeune Maintenance		325,577
Fuel Oil	<u>c</u>	8,642,153
Total Present Value Alternative 2B	\$10	9,948,766
Discount Factor 9.524		

Uniform Annual Cost

\$ 11,544,390



VI-27

March 1982

DATE

P NO.

ECONOMIC ANALYSIS OF SHORE FACILITY

-	ACTIVITY	(Name and	Locati	0.01)		1.175
	Refuse	Plant -	Camp	Lejeune,	N.	C
1	PROJECT	TITLE				
	D					

1

Design Analysis (Fy 87) DESCRIPTION OF ALTERNATIVES

Case 2

A. Refuse Plant - Flecricity with Back Pressure Turbine

B. Landfill - Oil-fired Boiler

PROJECT COST PROJECTIONS BY ALTERNATIVES

ALTERNATIVE & _____ Refuse Plant - Electricity w/Back Pressure_Turbing_FE _____ 25_____

DESCRIPTION AND YEAR	COSTS (\$)		DISCOUNT	PRESENT	
	ONE TIME	RECURAINS	FACTOR	VALUE (S)	
IVESTMENT					
PERATIONS		The second			
INTERANCE	San Grander	A State of the sta			
RSCHWEL			· Walker		
BAINAL VALUE	Street Marke	The state of the second	1997、这一部		
10:	and the second		1. 1. 1. 1. 1. 1. 1. 1. 1. 1. 1. 1. 1. 1		
OTAL PRESENT VALUE ALTERNATIV		030,099 -	SCOUNT FACTOR	UNIFORM ANNUAL CO	

Landfill - Oil-fired Boiler

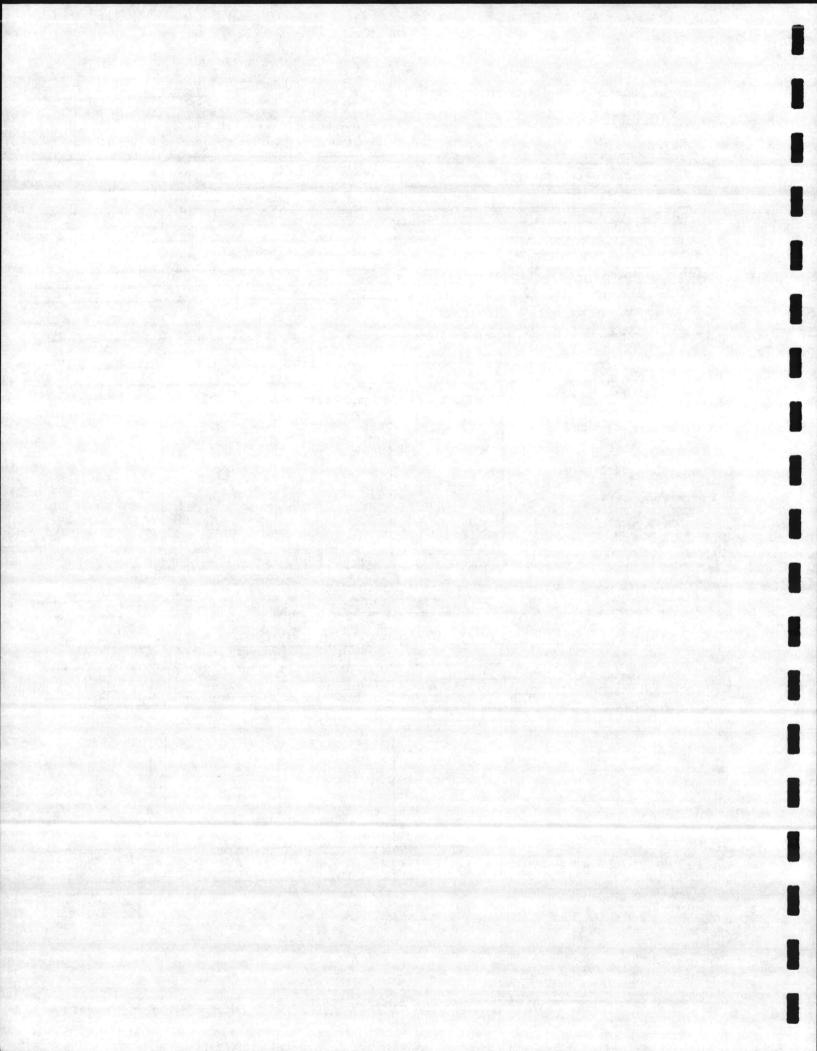
I - Oil-fired Boiler

ECONDHIC 25

TRS.

DESCRIPTION AND YEAR	COSTS	(\$)	DISCOUNT	PRESENT .
	ONE TIME	RECURAING	FACTOR	VALUE (S)
- INVESTMENT				
OPERATIONS	Selfa - Shekara			a second a the second
HAINTENANCE				
PERSONNEL				
TERNINAL VALUE				
OTHER:		「「「「「「「」」」「「「」」」」		
TOTAL PRESENT VALUE ALTERNATIV	El·s 75,9	18,667 ÷ •	SCOUNT FACTOR 9.524 =	UNIFORM ANNUAL COS 7,971,301

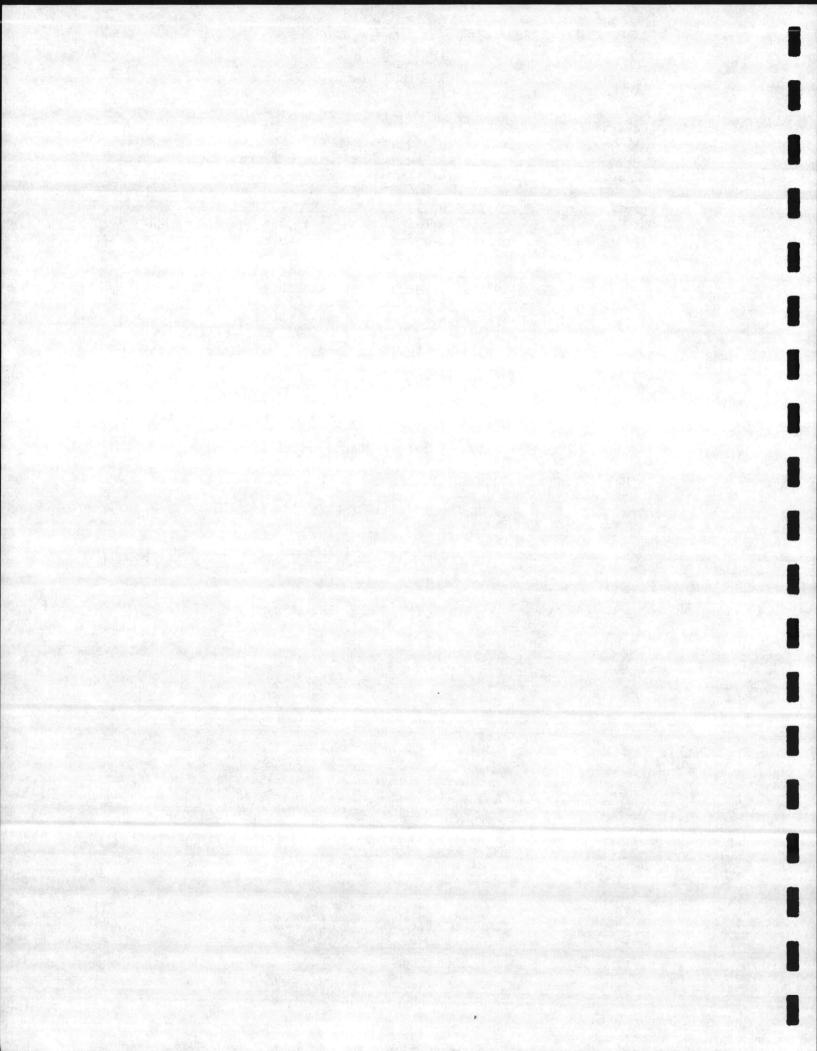
(Attach separate sheet showing derivation of cost entries)



Analysis

	Total Present Value Cost	Uniform Annual Cost		
Case 2A	\$ 34,030,099	\$ 3,573,089		
Case 2B Difference	109,948,766 75,918,667	11,544,390 7,971,301		

The refuse plant is again the least expensive alternative to disposing of burnable trash in landfills and burning oil at Camp Geiger and the Air Station. The total present value cost of the refuse plant is \$75,918,667 less than the landfill and oil alternative. This converts to a \$7,971,301 annual savings (or difference in cost). This is slightly larger than \$7.8 million potential annual savings in Case 1.



TAB PLACEMENT HERE

SECTION VII

DESCRIPTION:

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Section VII 1



VII. CASE 3 - ELECTRICITY WITH CONDENSING TURBINE

Plant Description

Boilers

The boiler configuration would be the same as described in Case 2A.

Turbine

All of the steam generated, 30,200 lb/hr at 130 T/D, would be sent to a turbine. Approximatey 2,750 lb/hr would be extracted at 5 PSIG for feedwater heating and deaerating. The remainder would be sent to a condenser and pumped from there to the deaerator.

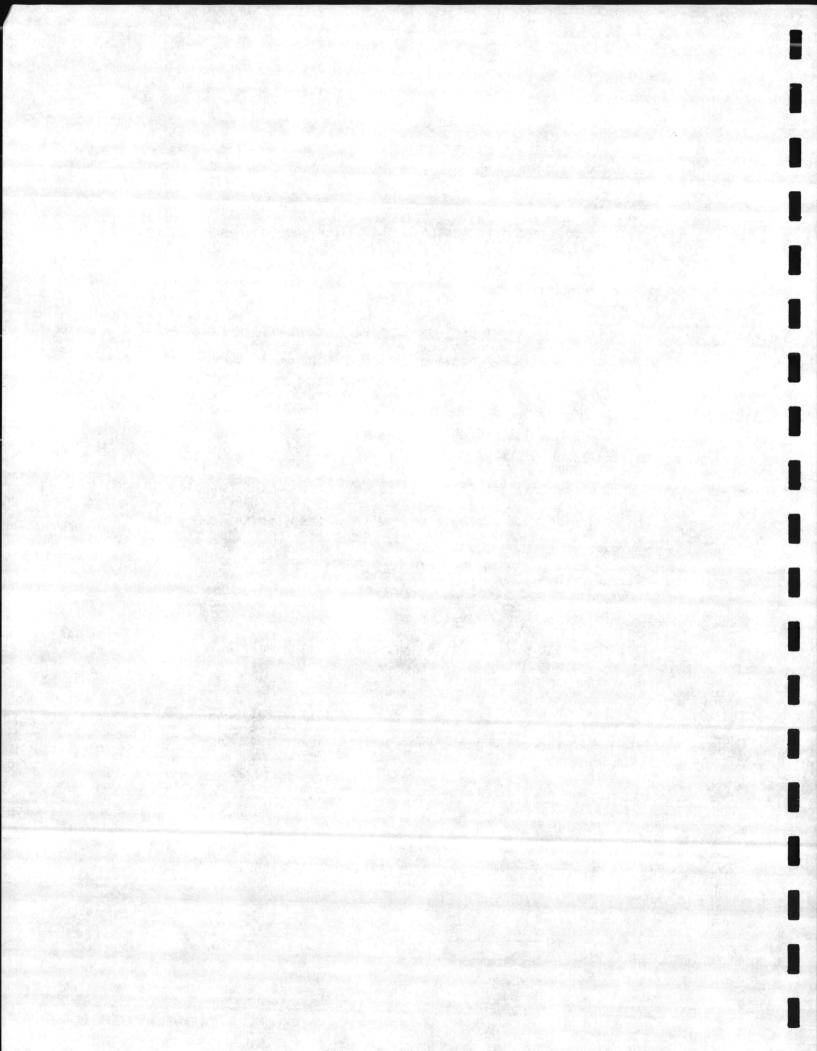
Cooling Tower

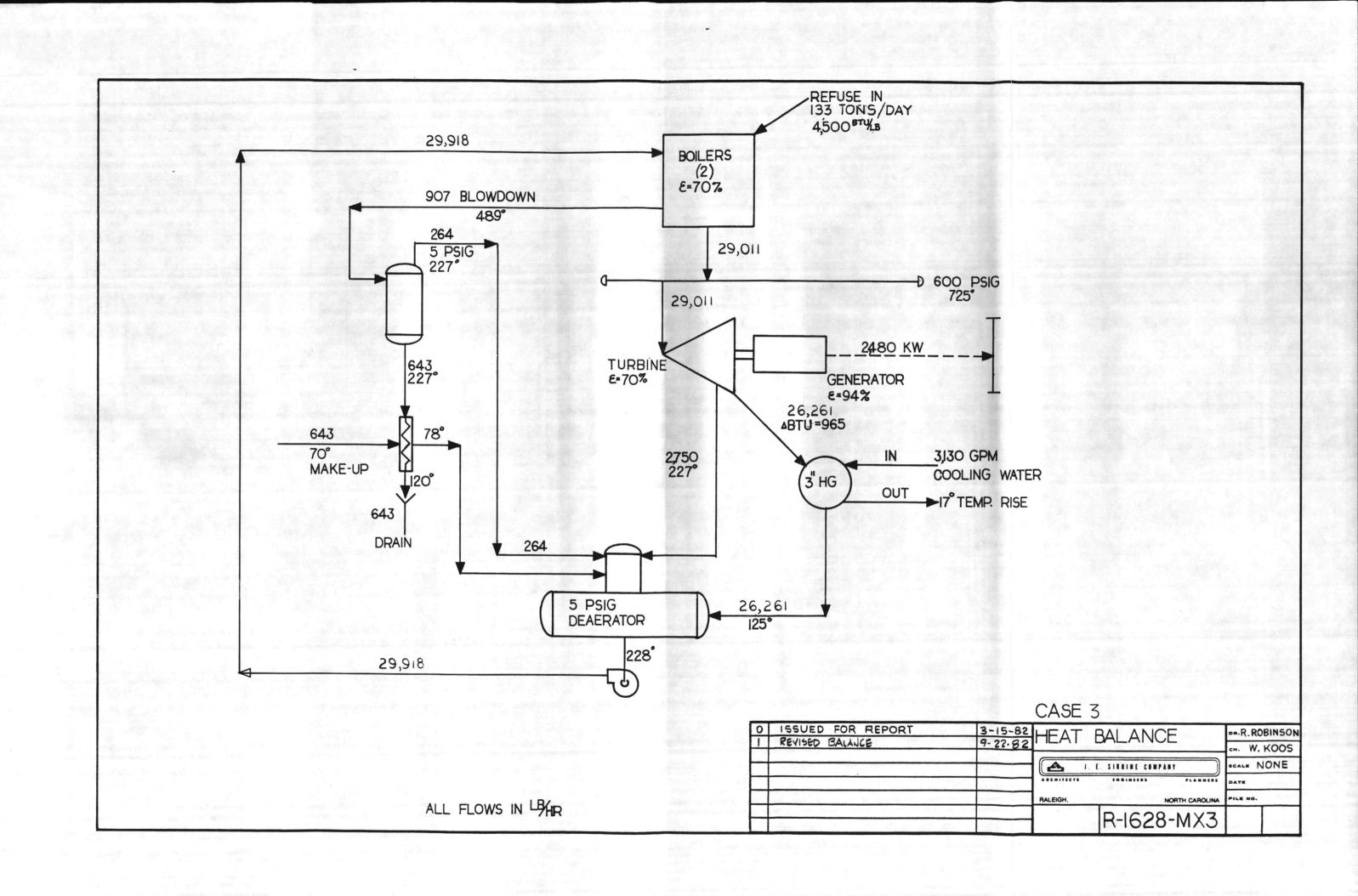
A mechanical draft cooling tower with a design capacity of 3300 GPM would supply a closed loop cooling system for the condenser. A 2-speed fan would be included to supply the cooling draft.

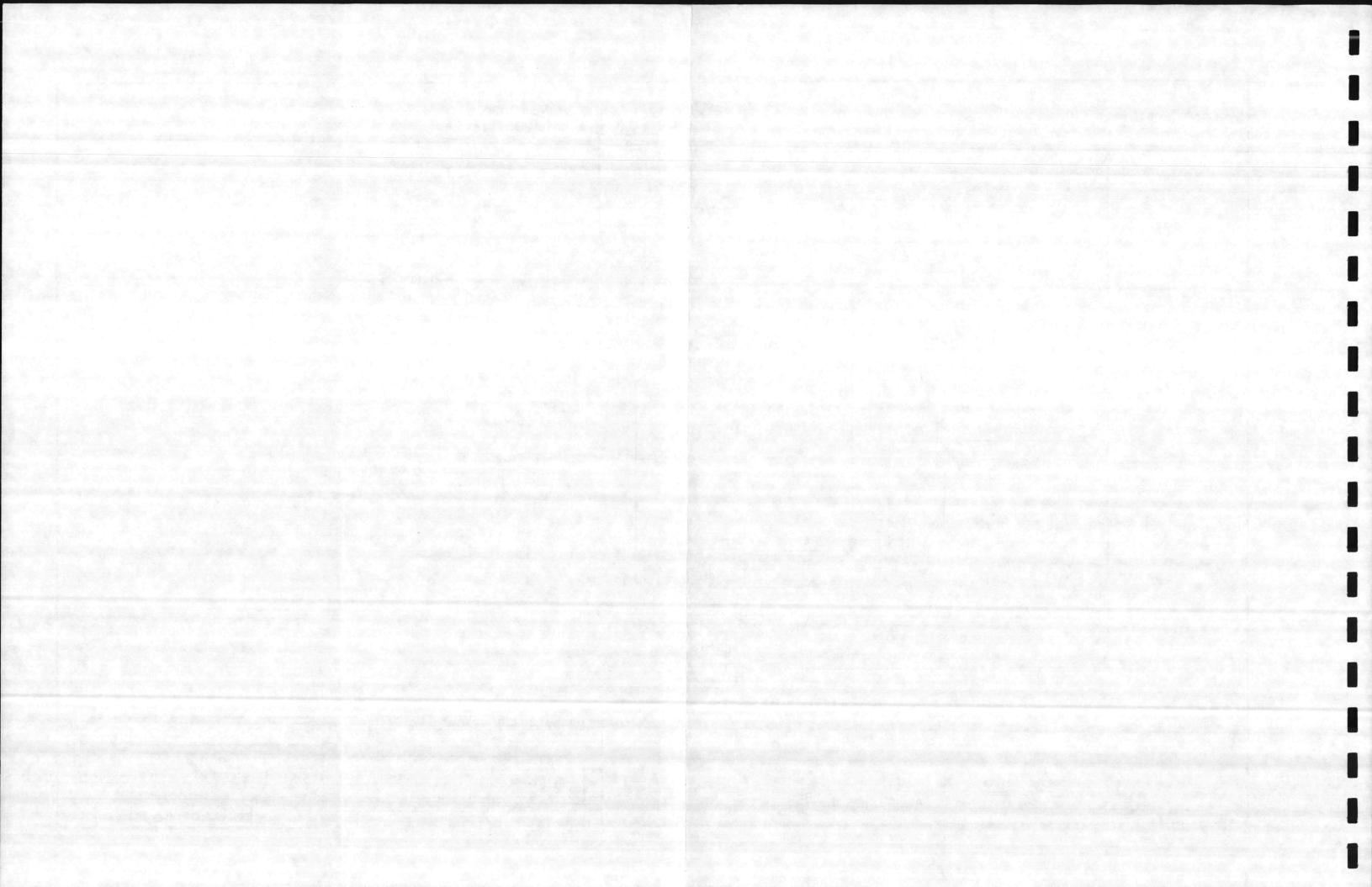
Electrical

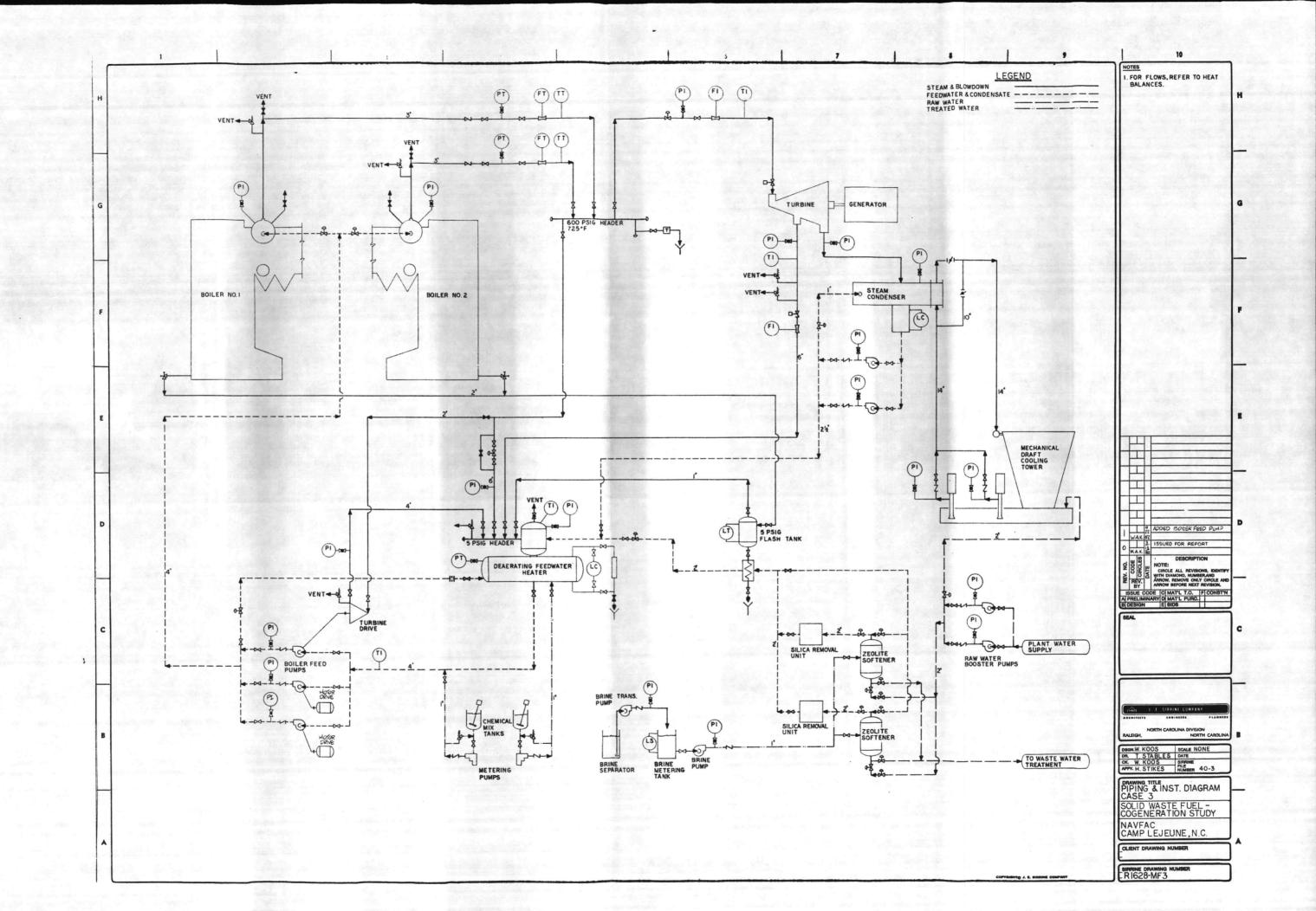
The generator would be sized for a capacity of 3775 KVA and would generate power at 12.47 KV. All other electrical items would be as in Case 2A.

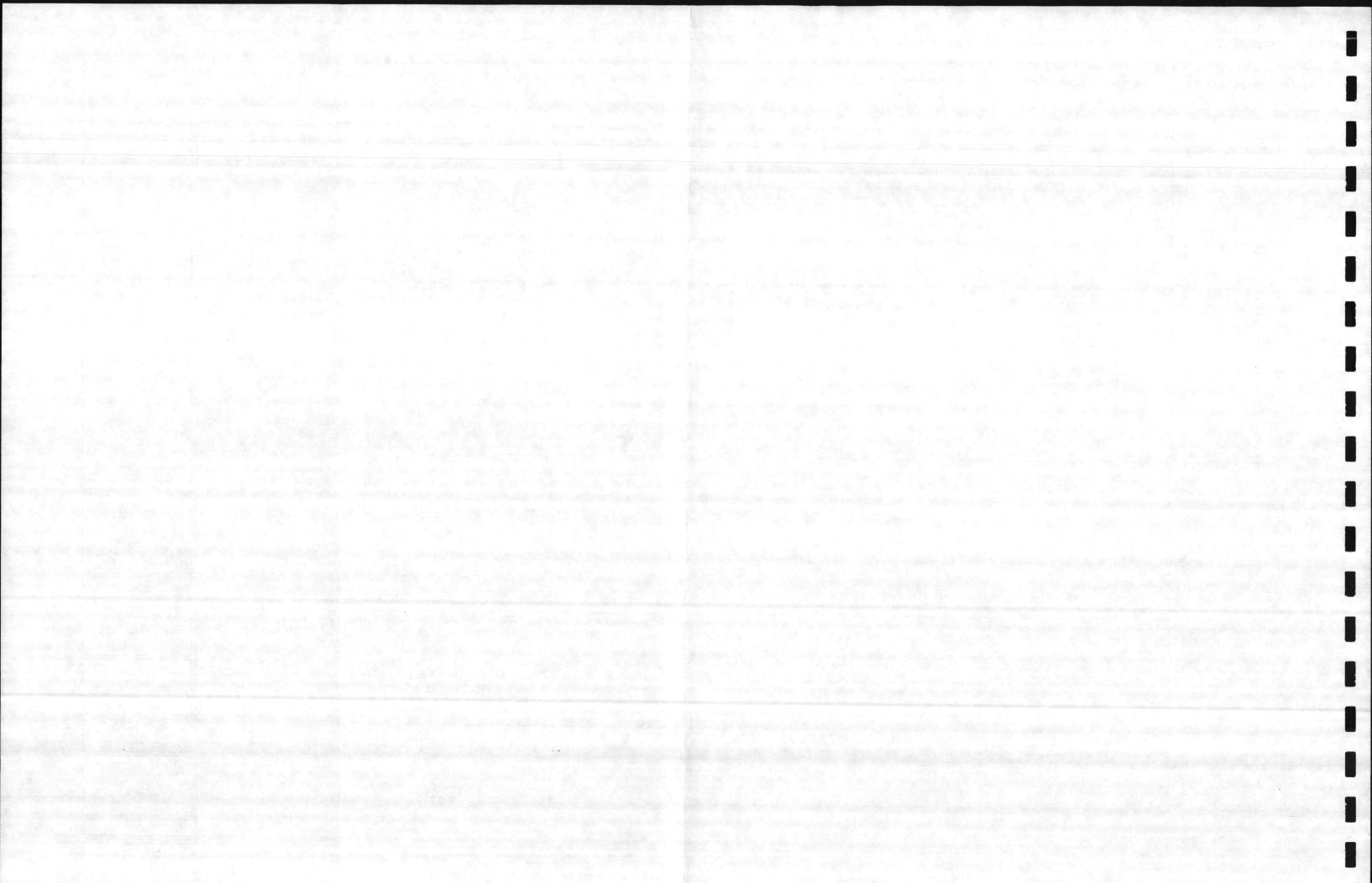
The conceptual heat balance is shown on Drawing MX3. The flow sheet for steam and water systems is on Drawing MF3.









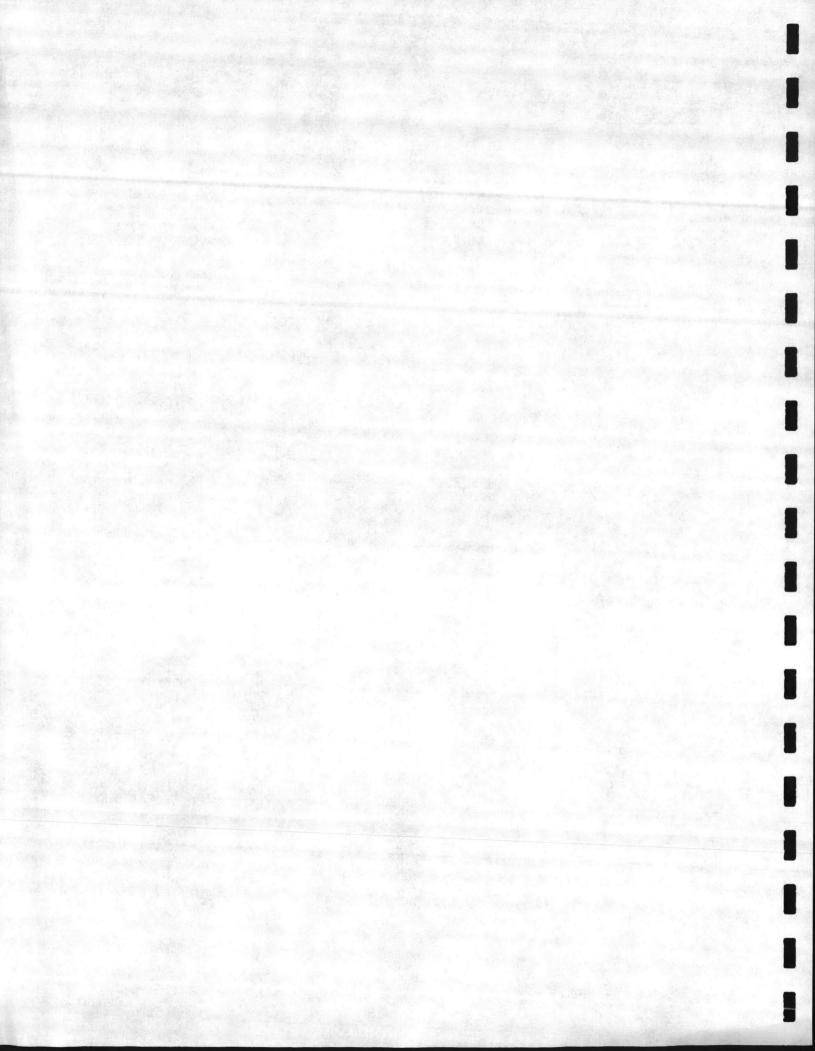


Cost Estimate

DEPARTMENT DIRECT COST SUMMARY

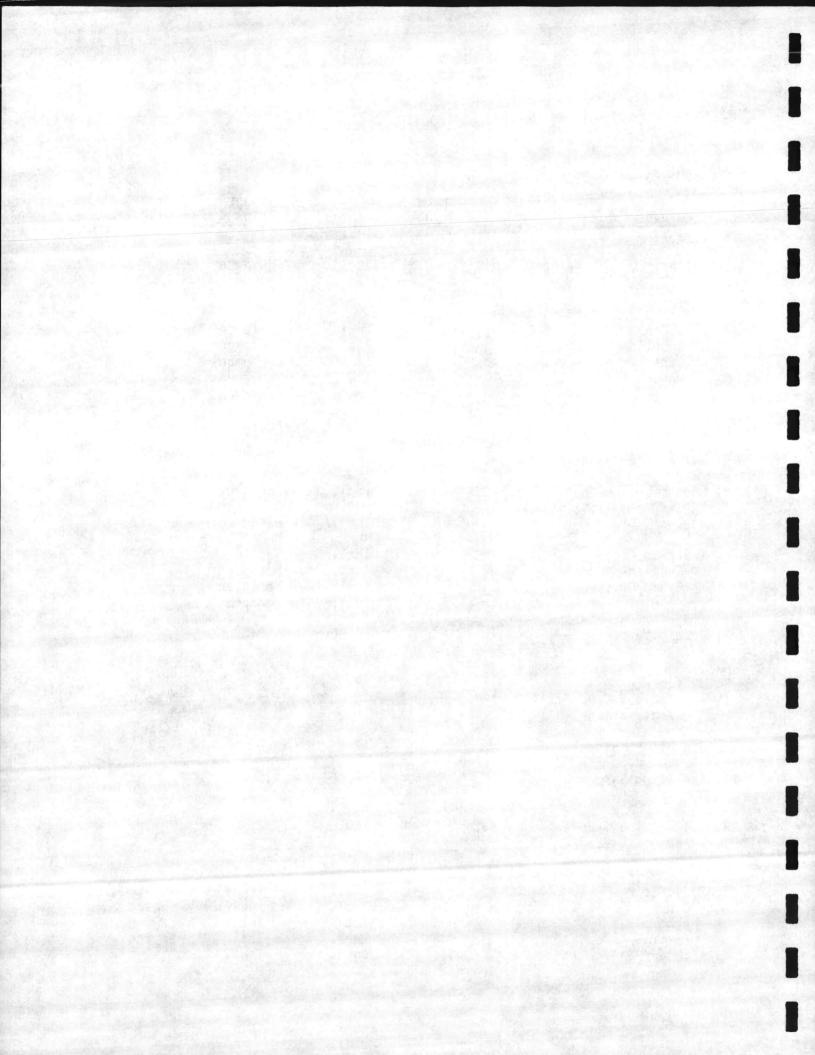
CASE 3 - ELECTRICITY WITH CONDENSING TURBINE

Equipment	\$ 9,362,000	
Equipment Erection	227,500	
Equipment Foundations and Other Cost	302,100	
Buildings & Structures	3,700,000	
Electrical Installation Cost	513,000	
Instrumentation Installation Cost	260,000	
Piping Cost	920,000	
Area Cost	380,000	
SUBTOTAL CONSTRUCTION COST		\$ 15,664,600
SIOH @ 5.5% (Supervision, inspection & overhead)		861,600
Contingency @ 10%		1,652,600
TOTAL CONSTRUCTION COST		\$ 18,178,800



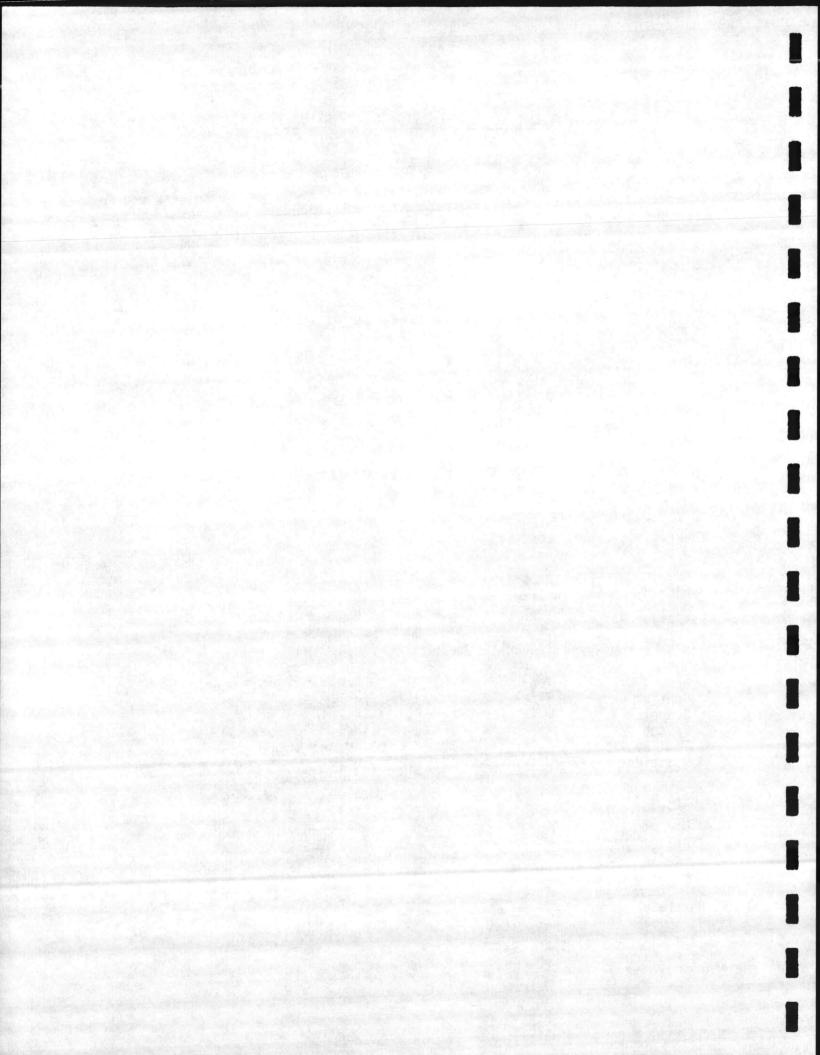
EQUIPMENT LIST

CAS	Item Description	Motor HP-RPM	Equipment S	Equipment Erection \$	Equip. Supports Platforms and Other Costs \$
1.	Boiler, 100 T/D Maximum Input 600 PSIG 725°F Unit No. 1		2,750,000	w/Equipment	w/Bldg. Cost
2.	F.D. Fan Coupling Controls Motor Intake Silencer	50	Incl. Incl. Incl. Incl. Incl.	w/Equipment w/Equipment w/Equipment w/Equipment w/Equipment	
3.	Combustion Controls		Incl.	w/Equipment	
4.	Boiler Breeching		Incl.	w/Equipment	w/Bldg.
5.	Economizer		Incl.	w/Equipment	w/Bldg.
6.	Stoker	10	Incl.	w/Equipment	w/Boiler
7.	I.D. Fan Coupling Fluid Drive Motor	75	Incl. Incl. Incl. Incl.	w/Equipment w/Equipment w/Equipment w/Equipment	
8.	Precipitator No. 1		600,000	w/Equip. Co	ost 20,000
9.	Ductwork - To Precip., Fan, Stack w/Insulation		45,000	D&E	65,000
10.	Expansion Joints		12,000	2,000	N/A
11.	Isolation Damper	5	28,000	2,000	Incl.
12.	Boiler, 100 T/D Maximum Input 600 PSIG 725°F Unit No. 2		2,750,000	w/Equip. Co	ost w/Bldg.
13.	F.D. Fan Coupling Controls Motor Intake Silencer	50	Incl. Incl. Incl. Incl. Incl.	Incl. Incl. Incl. Incl. Incl.	4,000 Incl. Incl. Incl. Incl.



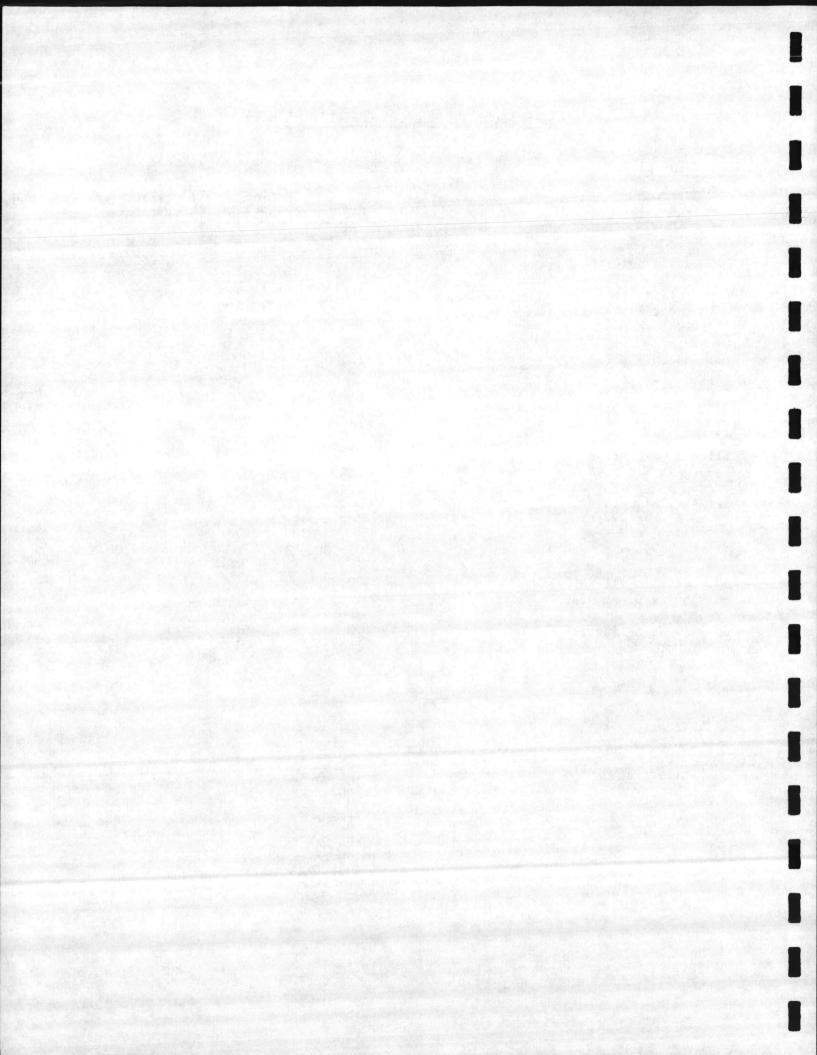
EQUIPMENT LIST

CAS	<u>Item Description</u>	Motor HP-RPM	Equipment \$	Equipment Erection \$	Equip. Supports Platforms and Other Costs \$
14.	Combustion Controls		Incl.	Incl.	
15.	Boiler Breeching		Incl.	Incl.	w/Bldg.
16.	Economizer		Incl.	Incl.	w/Bldg.
17.	Stoker	10	Incl.	Incl.	w/Boiler
18.	I.D. Fan Coupling Fluid Drive Motor	75	Incl. Incl. Incl. Incl.	Incl. Incl. Incl. Incl.	7,000
19.	Precipitator No. 2		600,000	Incl.	20,000
20.	Ductwork - To Precip., Fan, Stack w/Insulation		45,000	D&E	65,000
21.	Expansion Joints		12,000	2,000	N/A
22.	Isolation Damper	5	28,000	2,000	N/A
23.	Ash Handling System	80 (Total)	575,000	Incl.	w/Bldg.
24.	Overhead Crane - 5 Ton Control Cab Grapple Bridge Motor Trolley Motor Hoist Motors (2)	15 10 10 (Ea)	375,000 Incl. Incl. Incl. Incl. Incl.	50,000	w/Bldg.
25.	Spare Crane Control Cab Grapple Bridge Motor Trolley Motor Hoist Motors (2)	15 10 10 (Ea)	375,000 Incl. Incl. Incl. Incl. Incl.	50,000	w/Bldg.
26.	Deaerator		30,000	2,000	1,500
27.	Blow-Off Tank		5,000	1,000	100



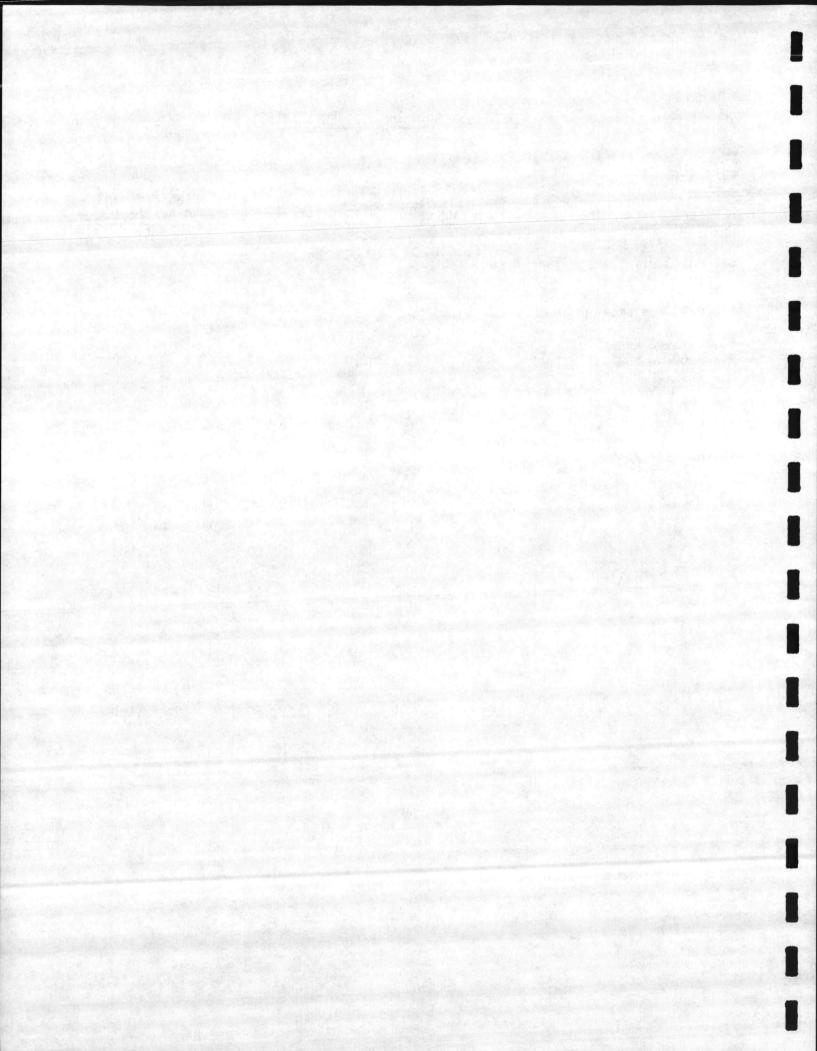
EQUIPMENT LIST

CAS	Item Description	Motor <u>HP-RPM</u>	Equipment \$	Equipment Erection \$	Equip. Supports Platforms and Other Costs \$
28.	Continuous Blowdown System Flash Tank Heat Exchanger Valves		17,000 Incl. Incl. Incl.	2,500 Incl. Incl. Incl.	500
29.	Condensate Tank		15,000	1,000	100
30.	Condensate Transfer Pump Motor	10	3,000 Incl.	500 500	200 200
31.	Air Compressor Air Receiver	25	6,000 Incl.	500	200
32.	Air Compressor Air Receiver	25	6,000 Incl.	500	200
33.	Air Dryer		3,000	200	100
34.	Stack - Dual Wall (2) 150' x 9'-0" Dia.		300,000	Incl.	90,000
35.	Raw Water Booster Pump Motor	20	3,000 Incl.	500 Incl.	100 Incl.
36.	Raw Water Booster Pump Motor	20	3,000 Incl.	500	100
37.	Feedwater Treatment Equipment	30 Total	70,000	8,000	1,000
38.	Boiler Feed Pump Motor	2 @ 75	16,000 Incl.	1,000 Incl.	1,000 Incl.
39.	Boiler Feed Pump Turbine		8,000 12,000	500 Incl.	500 Incl.
40.	Chemical Feed Equipment	2 @ 5	10,000	800	300



EQUIPMENT LIST

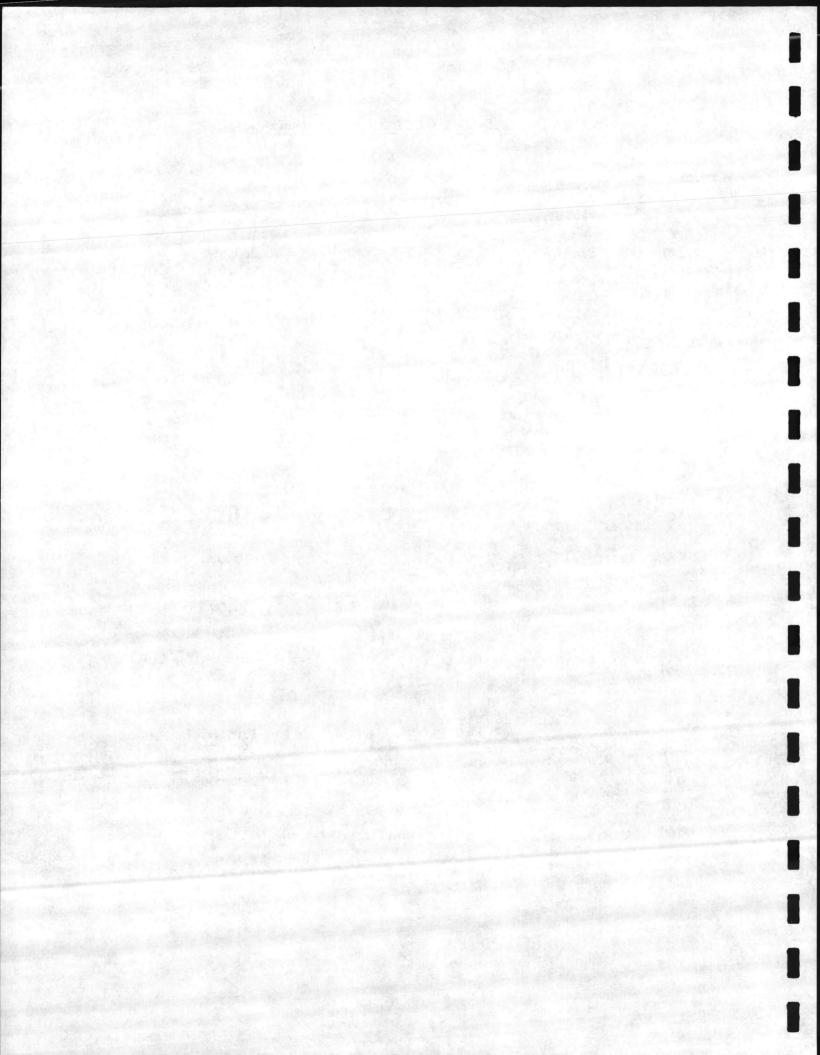
CAS	<u>Item Description</u>	Motor HP-RPM	Equipment \$	Equipment Erection \$	Equip. Supports Platforms and Other Costs \$
41.	No. 2 Oil Storage Tank & Pump 10,000 Gallon	5	25,000	500	500
42.	HVAC Equipment	20	15,000	Incl.	500
43.	Turbine Generator 3700 KW Nominal Output 12,470 Volt Generator 4350 KVA Rating		350,000	80,000	8,000
44.	Condenser		75,000	5,000	1,000
45.	Hotwell Pump Motor	10	5,500 Incl.	500 Incl.	500 Incl.
46.	Hotwell Pump Motor	10	5,500 Incl.	500 Incl.	500 Incl.
47.	Cooling Tower Fan (2) Motor (2)	100 Total	150,000 Incl. Incl.	10,000 Incl. Incl.	1,500 Incl. Incl.
48.	Circulating Water Pump (2) Motor(2)	300 Total	24,000 Incl.	3,000 Incl.	1,500 Incl.
	TOTAL, Equipment	\$	9,362,000	\$227,500	\$ 302,100



CASE 3

49. Buildings and Structures

Structural Steel Excavation and Backfill Refuse Pit and Basement Mat Piling Roof Deck and Roofing Walls and Siding Intermediate Floors Stairs, Doors and Drains Miscellaneous Steel and Grating Support Steel and Miscellaneous	\$ 880,000 445,000 690,000 365,000 86,000 190,000 270,000 89,000 160,000 135,000 390,000
TOTAL, Buildings and Structures	\$ 3,700,000
50. Electrical Building Lighting Electrical Equipment & Wiring TOTAL, Electrical	63,000 450,000 \$ 513,000
51. Instrumentation	\$ 260,000
52. Piping Boiler Plant	920,000
53. Area Area Road Paving	\$ 130,000 250,000
TOTAL, Area	\$ 380,000



CASE 3

DESIGN ANALYSIS COMPUTATIONS

JANUARY 1982

(Present Value = 1987 Dollars)

ALTERNATIVE A - Refuse-Burning Plant

- Investment Cost 1.
 - a. Refuse-Burning Plant Capital Costs (from equipment list)

Construction	\$ 15,664,600
SIOH @ 5.5%	861,600
Contingency @ 10%	1,652,600

Total Unescalated Construction \$ 18,178,800

Total Construction escalated to April 1985 \$ 18,178,800 x <u>2384</u> = \$ 22,548,500 1922

> 10% Discount (2% differential) 1.1198 Present Value Construction Cost

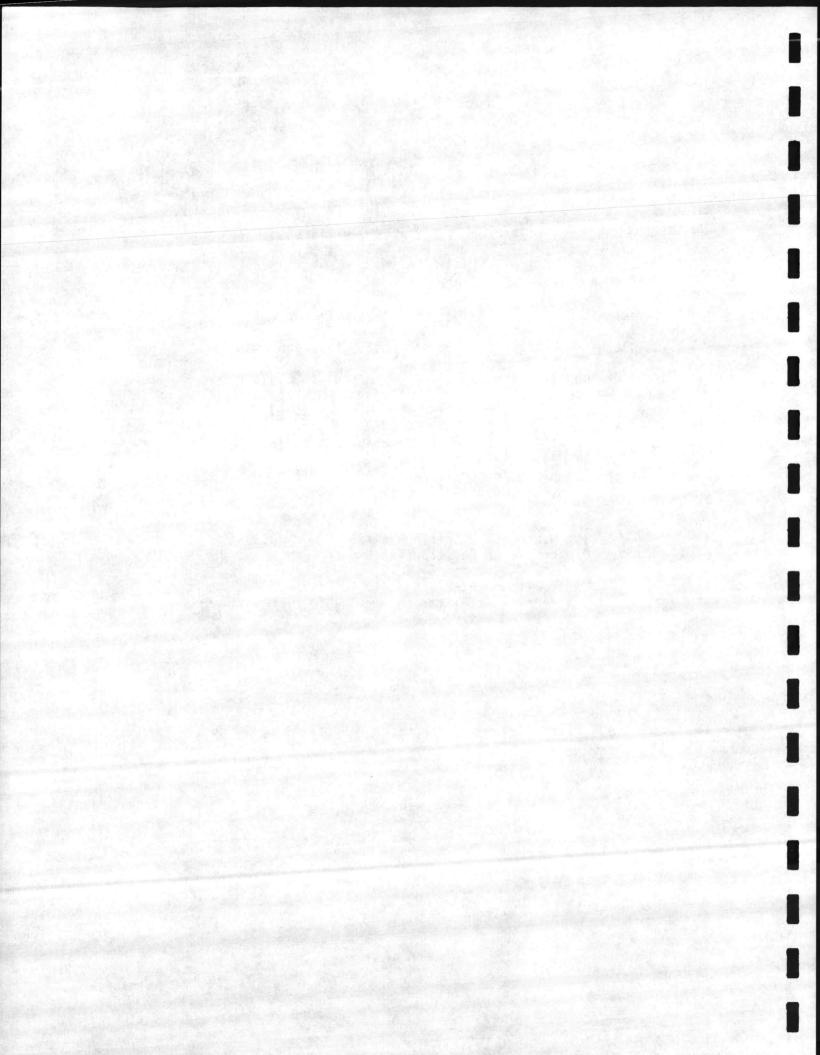
\$ 25,249,810

Engineering @ 6% = \$ 1,090,700 Engineering escalated to April 1984 \$ 1,090,700 x 2253 = \$ 1,278,500 1922

10% Discount (2% differential) Present Value Engineering

1.2071 \$ 1,543,277

Total Present Value Construction & Engineering \$ 26,793,087



b. Capital Costs for Ash Disposal

Investment for truck (\$70,000) and disposal containers (\$26,000) \$96,000 in years 1, 9, 17

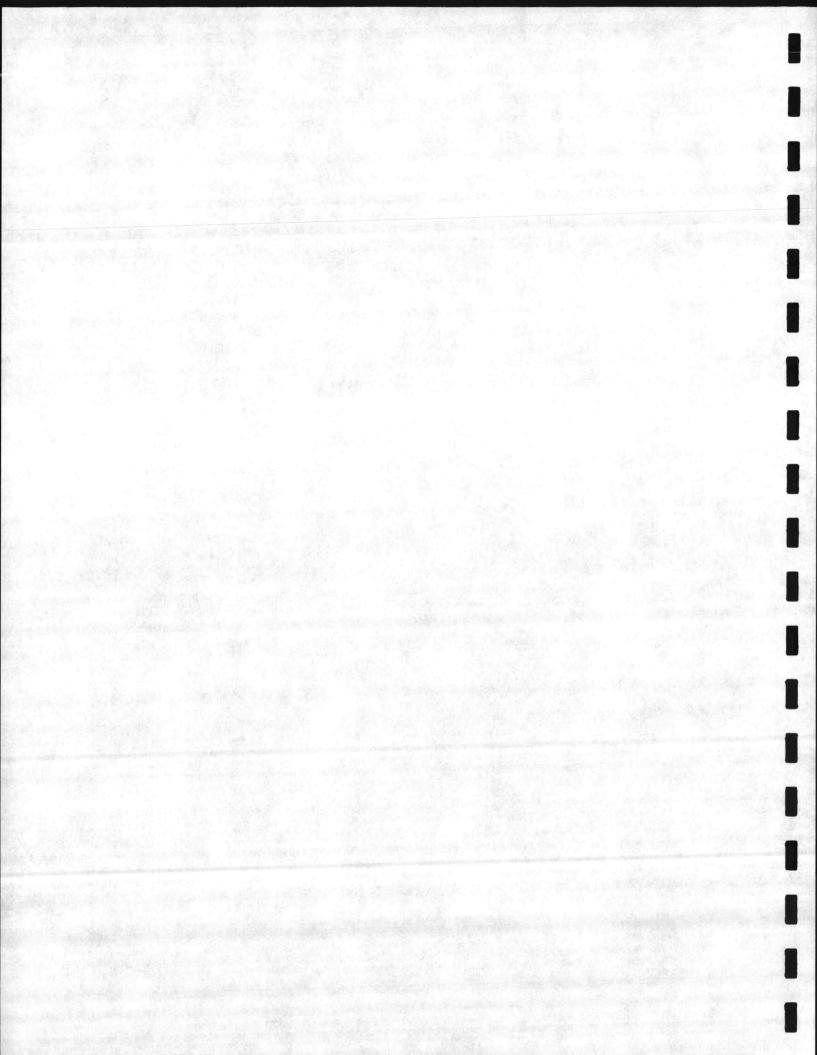
Escalated to Oct. 1987 $\frac{2684}{1922} = $134,060$

10% Discount (2% differential) year 1.963Present Value\$129,100

10% Discount (2% differential) year 9 .526 Present Value \$70,516

10% Discount (2% differential) year 17 .288 Present Value \$ 38,609

Total Present Value Ash Disposal Investment \$238,225



2. Recurring Costs

a. Annual Boiler Plant Labor Costs

4 Crane Operators (WG-8) @ \$9.98/hr. (incl. benefits) 4 Boiler Operators (WG-7) @ \$9.43/hr. (incl. benefits) 4 Boiler Mechanics (WG-10) @ \$11.09/hr. (incl. benefits) 3 Supervisors (WS-7) @ \$12.78/hr. (incl. benefits)

Unescalated Labor Cost

 $(4 \times 9.98 \times 2080) + (4 \times 9.43 \times 2080) + (4 \times 11.09 \times 2080) + (3 \times 12.78 \times 2080) = $333,508$

Labor escalated to Oct. 1987

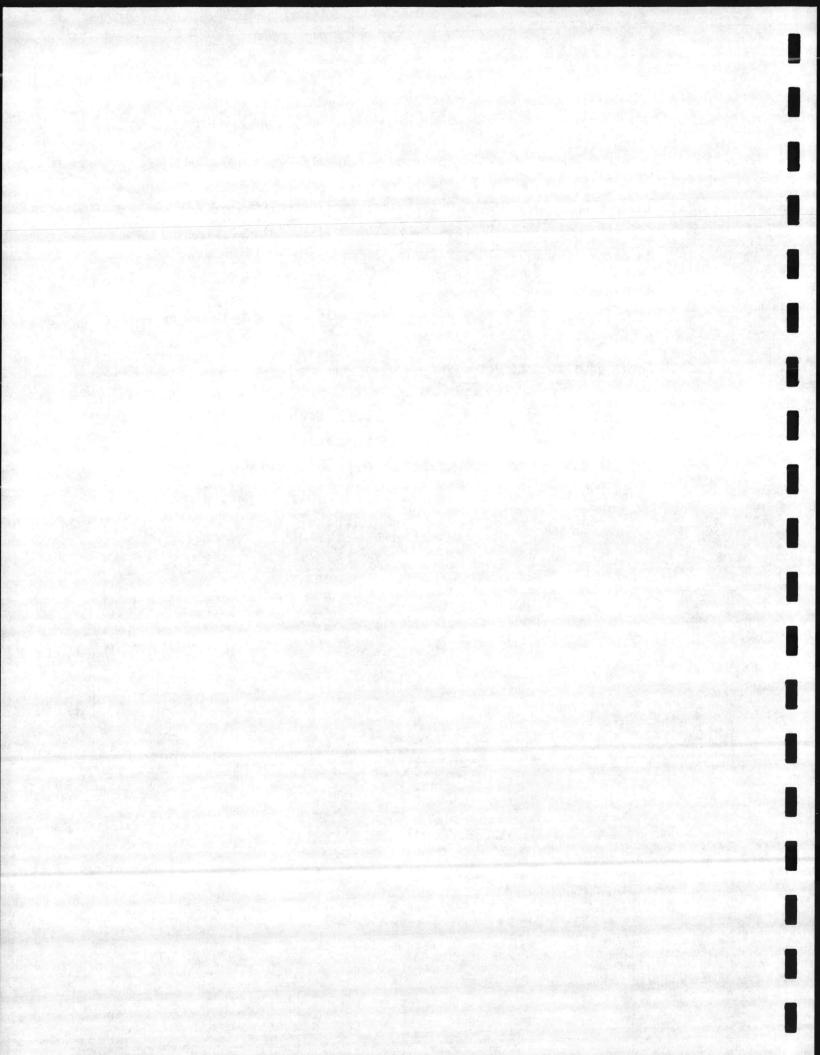
Fy 82 Fy 83 Fy 84 Fy 85 Fy 86 Fy 87 \$333,508 x 1.056 x 1.056 x 1.056 x 1.056 x 1.056 x 1.056 = \$462,476

10% Discount (0% differential)

Present Value Labor Cost

\$4,404,621

9.524



b. Annual Boiler Maintenance Cost

ITEM	INSTALLED COST (\$ X 10 ³)	MAINT. FACTOR	COST <u>(\$ X 10³)</u>
Boilers & Fans	3,250	0.025	81.25
Precipitators	1,200	0.015	18.00
Ducts & Stack	245	0.010	2.45
Ash Handling	575	0.025	14.38
Pumps	68	0.015	1.02
Water Treatment	37	0.020	.74
Building	3,400	0.005	17.00
Internal Piping	740	0.005	3.70
Export Piping	1,376	0.010	13.76
Cranes	850	0.020	17.00
Electrical Instrumentation	538	0.020	10.76
Turbine Generator	200	0.020	4.00
Condenser	. 75	0.010	.75
Cooling Tower	166	0.015	2.49
Total Unesc	alated Maintenance		187.30

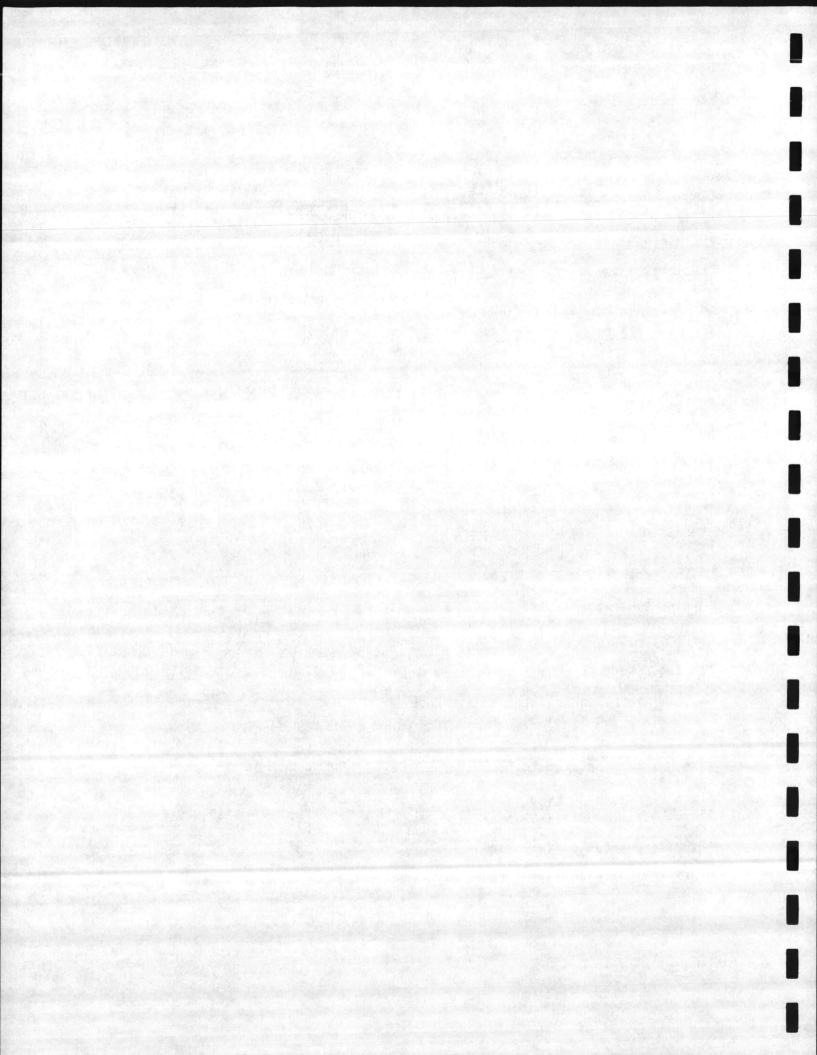
Maintenance escalated to Oct. 1987

 Fy 82
 Fy 83
 Fy 84
 Fy 85
 Fy 86
 Fy 87

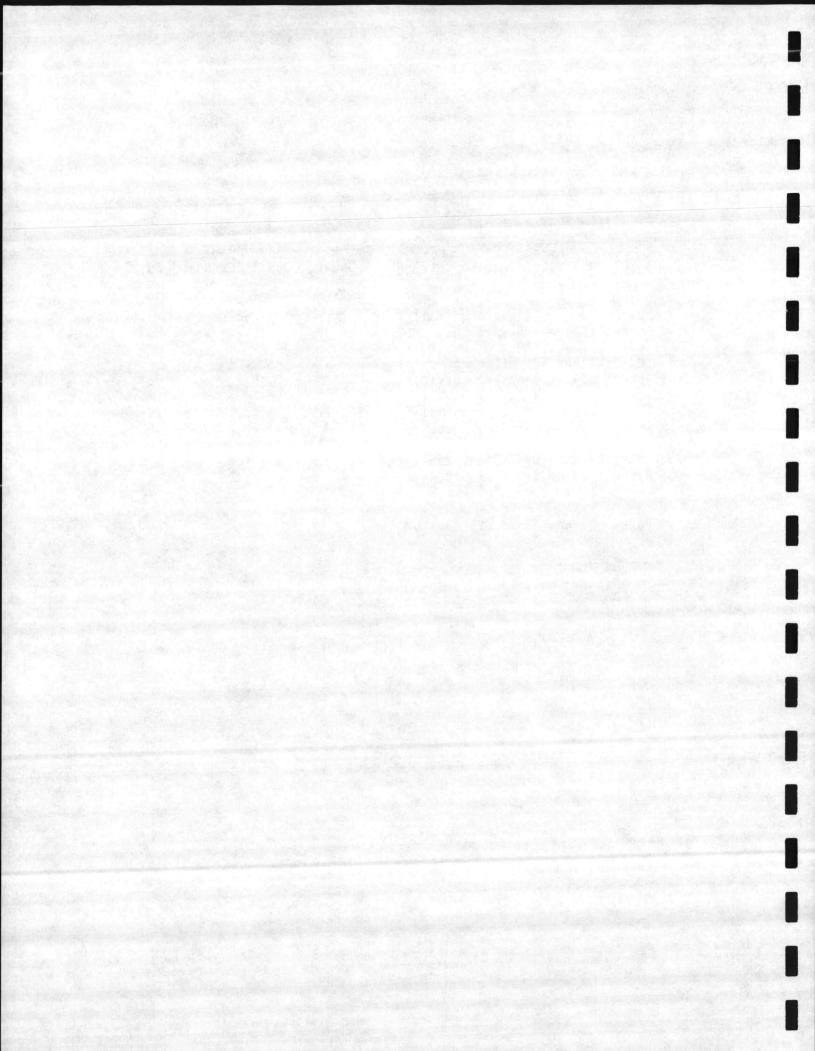
 \$187,300 x 1.056 x 1.056 x 1.056 x 1.056 x 1.056 x 1.056 x 1.056
 \$1.056 x 1.056 x 1.056 = \$259,729

 10% Discount (0% differential)
 9.524

 Present Value Maintenance Costs
 \$2,473,663



c. Plant Overhaul \$ 50,000 every 5 years Escalated to Oct. 1987 Fy 82 Fy 83 Fy 84 Fy 85 Fy 86 Fy 87 \$ 50,000 x 1.056 x 1.056 x 1.056 x 1.056 x 1.056 x 1.056 = \$ 69,335 10% Discount (0% differential) year 5 Present Value Overhaul Cost .652 \$ 45,206 10% Discount (0% differential) year 10 .405 Present Value Overhaul Cost \$ 28,081 10% Discount (0% differential) year 15 .251 Present Value Overhaul Cost \$ 17,403 10% Discount (0% differential) year 20 Present Value Overhaul Cost .156 \$ 10,816 Total Present Value Overhaul Costs \$ 101,506



SERVICE	POWER (KW)	USE FACTOR	EFFECTIVE POWER
Pumping Power*	110	0.8	88
Crane Operation	30	1.0	30
Precipitators	400	0.8	320
Ash Handling	60	0.8	48
Hot Well Pump	75	0.8	6
Cooling Tower	75	0.8	60
Circulating Wat Pumps	er 150	0.8	120
		TOTAL	672 KW

* NOTE: Feedwater pumping is not included since a reduction in existing feedwater pumping will be realized. Adjustment is made for higher pressure feedwater.

Annual Demand Cost Increase 672 KW X \$ 73.598/KW = \$ 49,458/yr.

Annual KWH Increase 672 KW X 7000 hrs/yr. = 4,704,000 KWh/yr.

Annual Dollar Increase per KWH 4,704,000 KWh/hr. X \$.02726/KWh = \$128,231/yr.

Total Annual Increase Electrical Cost \$ 49,458 + \$128,231 = \$ 177,689

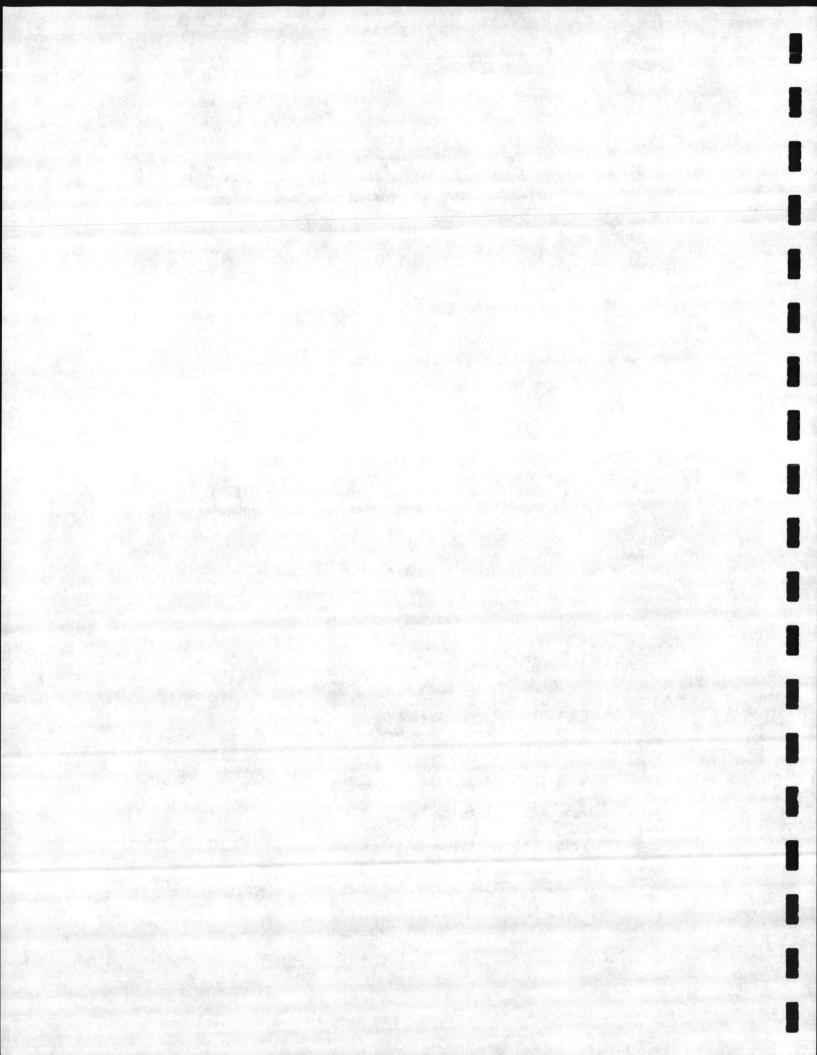
Escalated to Oct. 1987 FY82 FY83 FY84 FY85 FY86 FY87 \$177,689 X 1.13 X 1.13 X 1.13 X 1.13 X 1.13 X 1.13 = \$369,940

10% Discount (7% differential)

18.049

Present Value Incremental Electrical Cost

\$6,677,047



e. Annual Trash Transfer Cost from Cherry Point to Lejeune

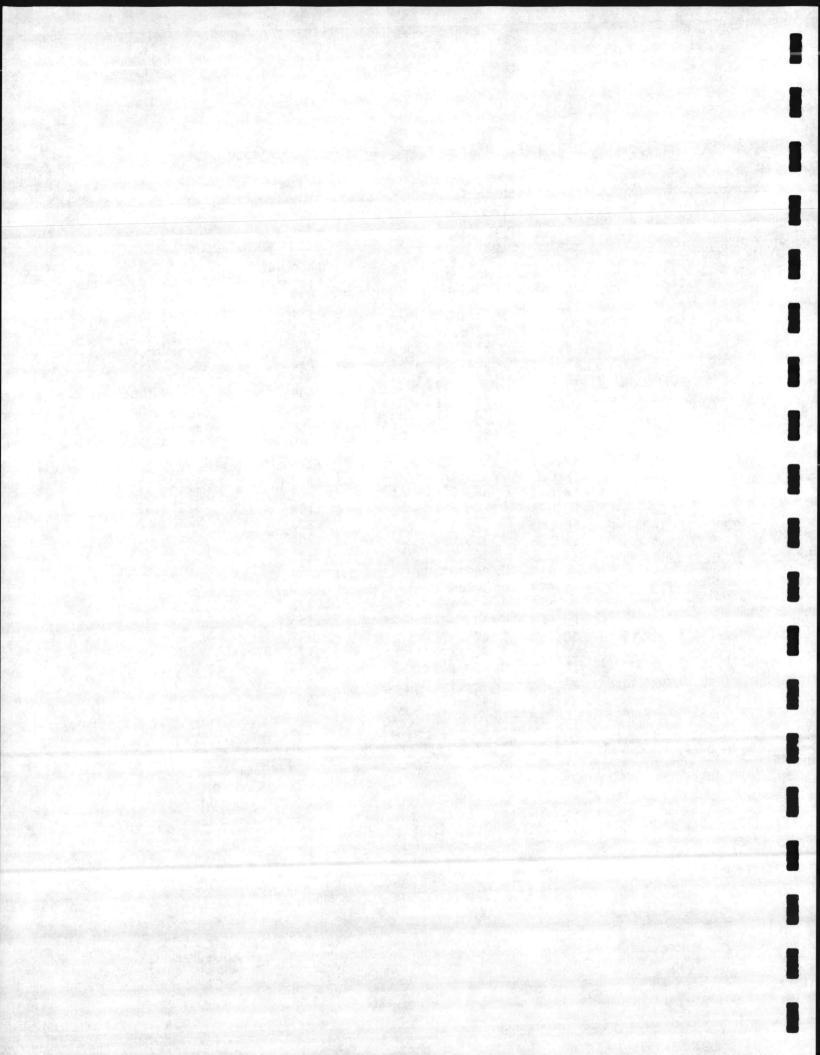
\$10/ton (1977) escalated to Oct. 1987

 $10 \times \frac{2684}{1355} = 19.81$

	Yr. of Op.	Tons/yr.	\$/yr.	10% Discount (0% differential)	Present Value
1987	1	15,538	\$ 307,808	.954	\$ 293,649
		15,793	312,859	.867	271,249
	2 3	16,048	317,911	.788	250,514
1990		16,303	322,962	.717	231,564
1.246	5	16,558	328,014	.652	213,865
	6	16,813	333,066	.592	197,175
	7	17,068	338,117	.538	181,907
		17,323	343,169	.489	167,809
	8 9	17,578	348,220	.445	154,958
	10	17,833	353,272	.405	143,075
	11	18,088	358,323	.368	131,863
	12	18,343	363,375	.334	121,367
	13	18,598	368,426	.304	112,002
2000		18,853	373,478	.276	103,080
	15	19,108	378,529	.251	95,011
	16	19,363	383,581	.228	87,456
	17	19,618	388,632	.208	80,836
	18	19,873	393,684	.189	74,406
	19	20,128	398,763	.172	68,582
	20	20,383	403,787	.156	62,991
	21	20,638	408,839	.142	58,055
	22	20,893	413,890	.129	53,392
	23	21,148	418,942	.117	49,016
	24	21,403	423,993	.107	45,367
2011		21,658	429,045	.097	41,617

Total Present Value Transfer Cost

\$3,290,806



f. Annual Ash Disposal Cost

	Yr. of Op.	1982 \$*	<u>1987 \$*</u>	10% Discount (0% differential)	Present Value
1987	1	\$ 13,702	\$ 19,134	.954	\$ 18,254
	2	13,756	19,210	.867	16,655
	2 3	13,862	19,358	.788	15,254
1990	4	13,916	19,433	.717	13,933
	4 5 6 7	14,022	19,581	.652	12,767
	6	14,075	19,655	.592	11,636
	7	14,128	19,729	.538	10,614
	8	14,950	20,877	.489	10,209
	9	15,003	20,951	.445	9,323
	10	15,110	21,101	.405	8,586
	11	15,163	21,175	.368	7,792
	12	15,216	21,249	.334	7,097
	13	15,269	21,323	.304	6,482
2000	14	15,323	21,398	.276	5,906
	15	15,376	21,472	.251	5,389
	16	15,429	21,546	.228	4,912
	17	15,535	21,694	.208	4,512
	18	15,588	21,768	.189	4,114
	19	15,642	21,843	.172	3,757
	20	15,748	21,991	.156	3,431
	21	15,802	22,067	.142	3,134
	22	15,855	22,141	.129	2,856
	23	15,908	22,215	.117	2,599
	24	16,014	22,363	.107	2,393
2011	25	16,067	22,437	.097	2,176

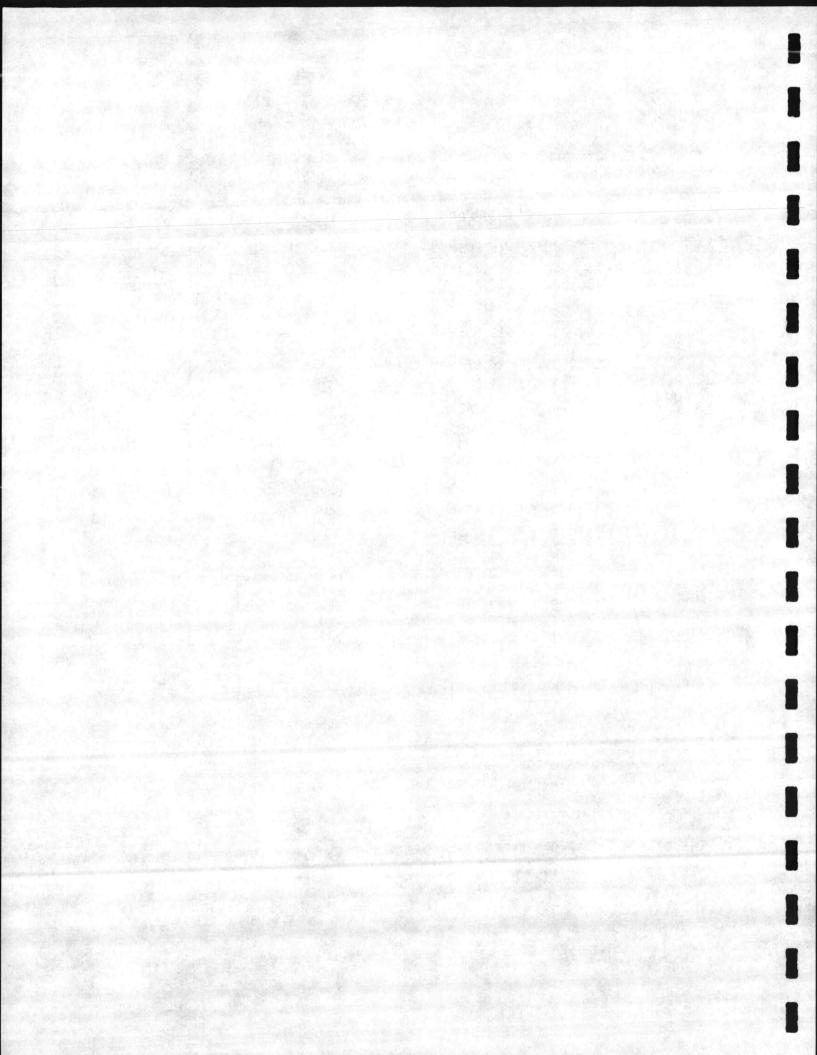
Total Present Value Ash Disposal Cost

\$ 193,781

* Escalation from 1982 to 1987 = $\frac{2684}{1922}$ = 1.3965

Ash - 80 lbs/cf. 30% moisture

Ash Disposal - 5 days per week



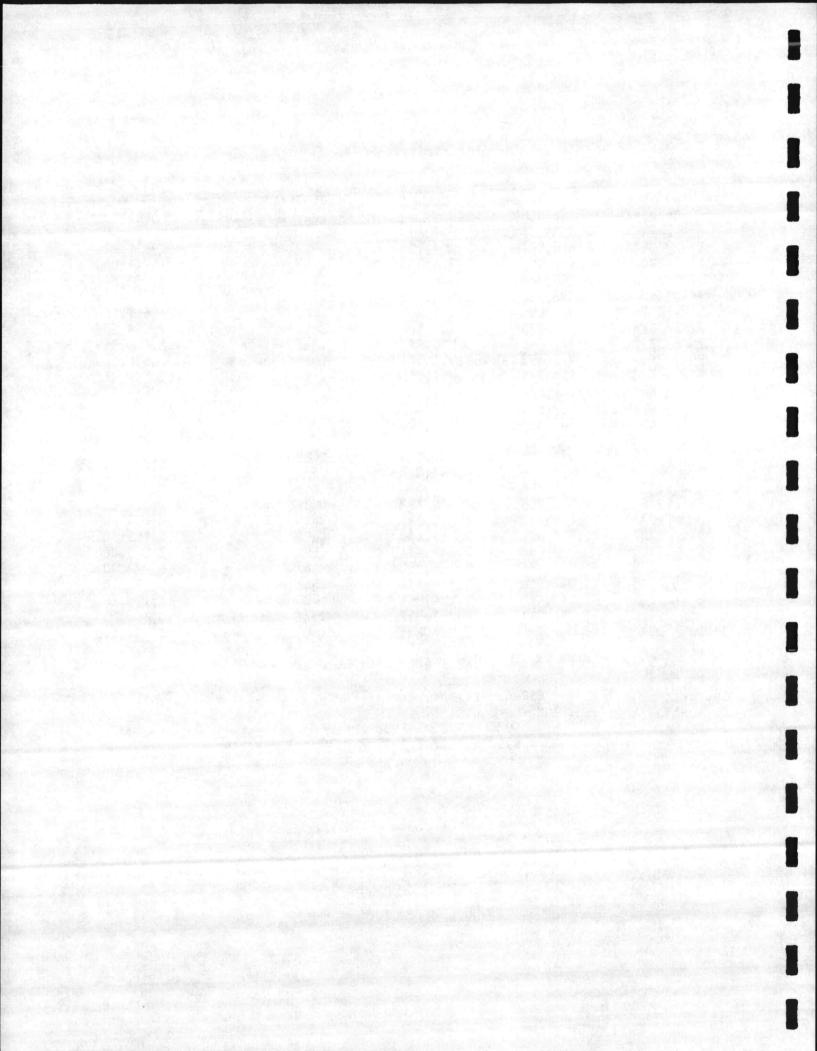
Benefits -3.

Revenues generated from sale of electricity to CP&L

Y	ear	Av. Kw/hr Generated	* Net Revenue Jan1982 \$	** Oct. 1987 \$	10% Discount (7% differential)	Present Value
		ucheruteu			(7% differencial)	ricsent value
1987	1	2384	\$ 866,584 \$	1,804,186	.986	\$ 1,778,927
	2	2403	873,490	1,818,565	.959	1,744,004
	3	2440	886,940	1,846,566	.933	1,722,846
1990	4	2458	893,483	1,860,188	.908	1,689,051
	5	2496	907,296	1,888,946	.883	1,667,940
	6	2514	913,839	1,902,568	.859	1,634,306
	7	2533	920,746	1,916,948	.836	1,602,568
	8	2552	927,652	1,931,326	.813	1,570,168
	9	2570	934,195	1,944,949	.791	1,538,454
	10	2607	947,644	1,972,950	.769	1,517,198
	11	2626	954,551	1,987,329	.748	1,486,522
	12	2645	961,458	2,001,708	.728	1,457,243
	13	2663	968,000	2,015,330	.708	1,426,854
2000	14	2682	974,907	2,029,709	.688	1,396,440
	15	2701	981,814	2,044,088	.670	1,369,539
	16	2719	988,356	2,047,710	.651	1,339,569
	17	2756	1,001,806	2,085,712	.634	1,322,341
	18	2775	1,008,712	2,100,091	.616	1,293,656
	19	2794	1,015,619	2,114,470	.600	1,268,682
	20	2831	1,029,068	2,142,471	.583	1,249,060
	21	2850	1,035,975	2,156,850	.567	1,222,934
	22	2868	1,042,518	2,170,472	.552	1,198,100
	23	2887	1,049,424	2,184,851	.537	1,173,265
	24	2924	1,062,874	2,212,852	.522	1,155,109
2011	25	2943	1,069,780	2,227,231	.508	1,131,433

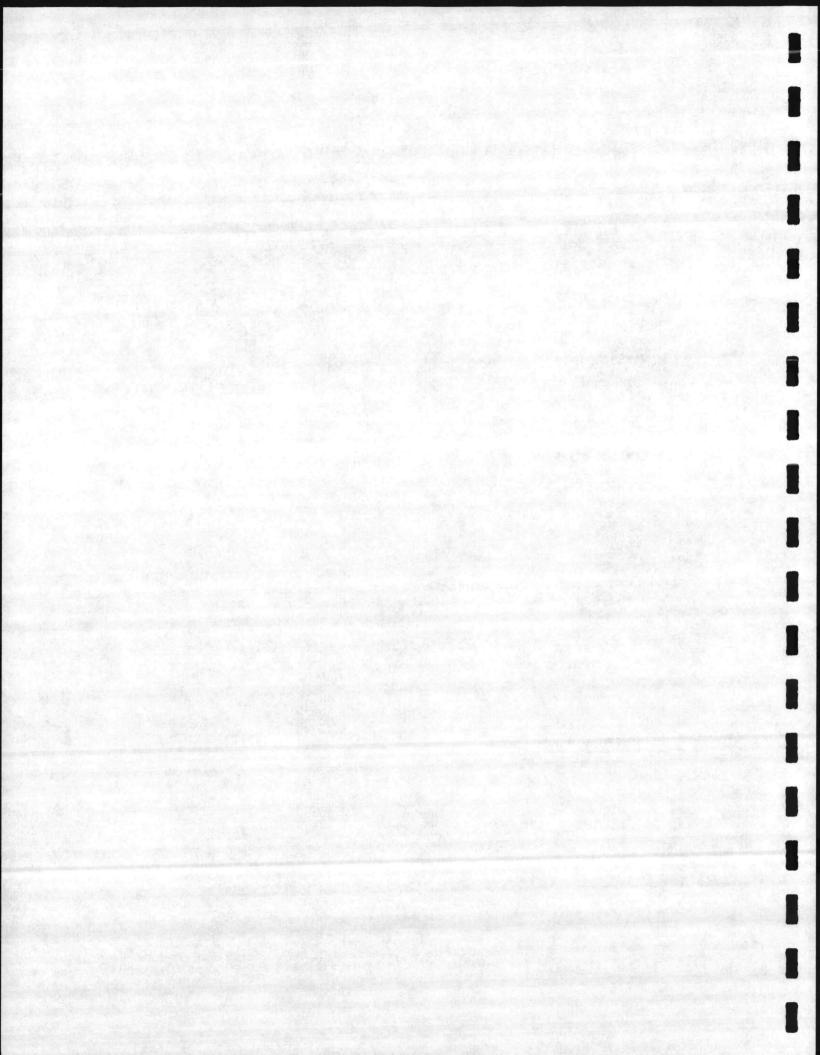
Total Present Value Electricity Revenues Benefit \$ 35,956,209

* Source: CP&L Schedule CSP-4, Variable Annual Energy Credit, 10-Year Capacity Credit ** Escalation from Jan. 1982 to Oct. 1987 = Fy82Fy83Fy84Fy85Fy86Fy871.13X1.13X1.13X1.13X1.13

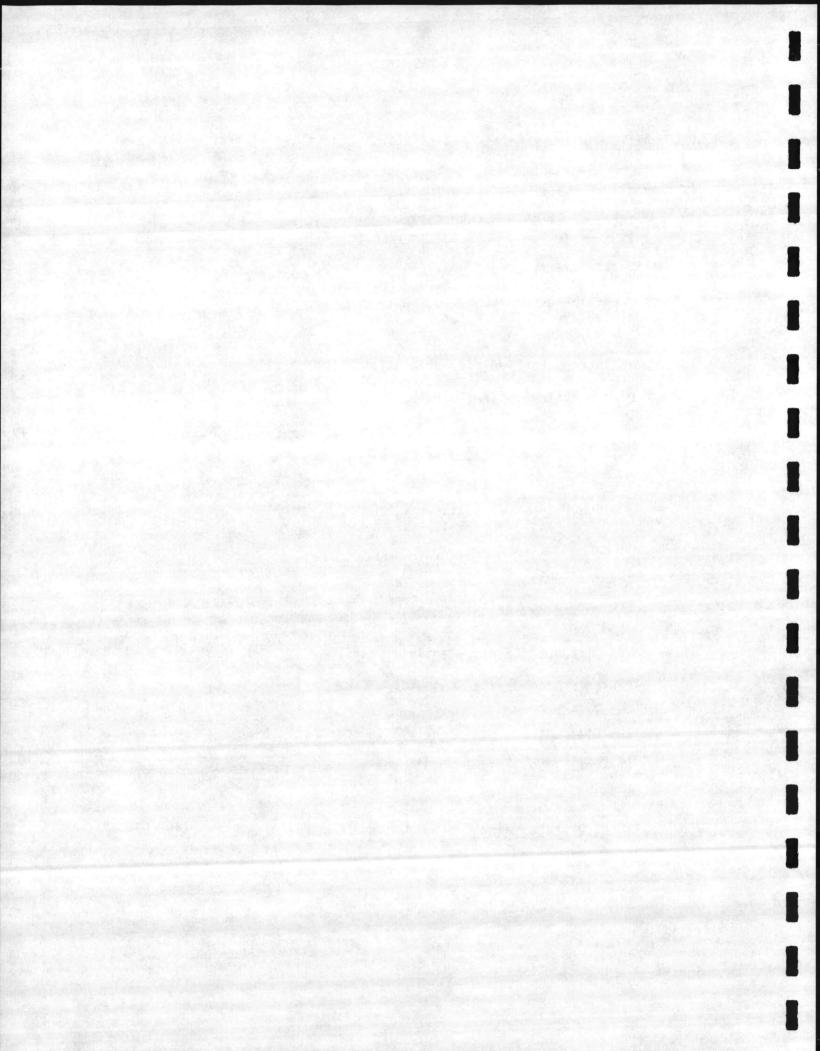


Summary Sheet Alternative 3A - Total Present Value

Investment Cost	
Boiler Plant	\$ 26,793,087
Ash Disposal	238,225
Recurring Costs	
Labor	4,404,621
Maintenance	2,473,663
Plant Overhaul	101,506
Incremental Electrical	6,677,047
Trash Transfer	3,290,806
Ash Disposal	193,781
Total Present Value Cost	\$ 44,172,736
Less Present Value Benefits Sale of Electricity	\$ 35,956,209
Net Present Value Alternative 3A	\$ 8,216,527
Discount Factor 9.524	
Uniform Annual Cost	\$ 862,718



ALT	ERNA	TIVE B - Incremental Cost of Refuse Landfill Camp Lejeune	s at Cherry	Point and			
1.	Investment Costs						
	a.	Incremental Cost of Landfill - Cherry Point					
		Capital Cost \$298,704 (1977) in year 5					
		Escalated to Oct. 87 $298,704 \times \frac{2684}{1355} = $591,676$					
		10% Discount (2% differential) year 5	.712				
		Present Value Capital Cost		\$421,274			
		Capital Cost \$36,000 (1977) in years 8, 16, 23					
		Escalated to Oct. 1987 \$36,000 X <u>2684</u> = \$71,309 1355					
		10% Discount (2% differential) year 8	.568				
		Present Value Capital Cost		\$ 40,504			
		10% Discount (2% differential) year 16	.310				
		Present Value Capital Cost		\$ 22,106			
		10% Discount (2% differential) in year 23	.183				
		Present Value Capital Cost		\$ 13,050			
		Total Present Value Capital Costs - Cherry	Point	\$496,934			



2. Recurring Costs

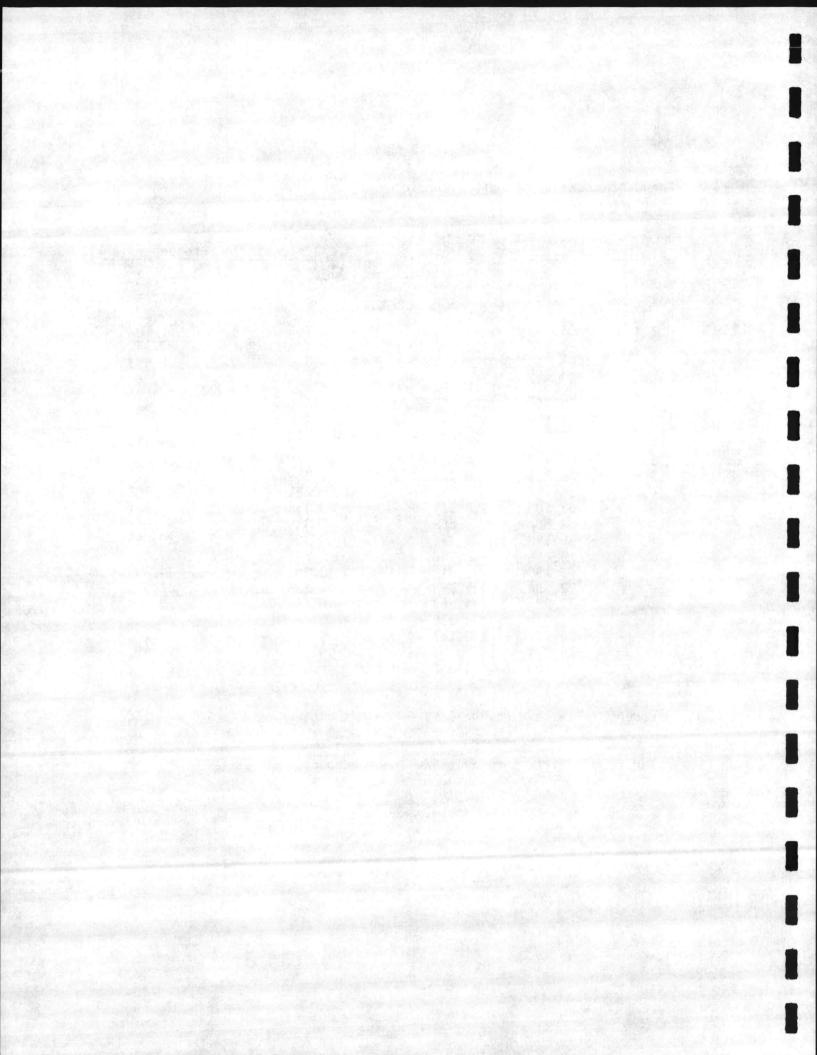
a. Annual Incremental Landfill Development Cost - Cherry Point

<u>Year Y</u>	r. of Op.	<u>1977\$*</u>	1987\$*	10% Discount (2% differential)	P	resent Value
1987	1	53,312	105,600	0.963	\$	101,693
	2 3	54,208	107,375	0.893		95,886
	3	55,104	109,150	0.828		90,376
1990	4	56,000	110,925	0.768		85,190
	5 6	56,896	112,700	0.712		80,242
	6	57,792	114,474	0.660		75,553
	7	60,438	119,716	0.612		73,266
	8 9	61,334	121,490	0.568		69,006
	9	62,230	123,265	0.526		64,837
	10	63,126	125,040	0.488		61,020
	11	64,022	126,815	0.453		57,447
	12	64,918	128,590	0.420		54,008
	13	65,814	130,364	0.389		50,712
2000	14	66,710	132,139	0.361		47,702
	15	67,606	133,914	0.335		44,861
	16	68,502	135,689	0.310		42,064
	17	69,398	137,464	0.288		39,590
	18	70,294	139,238	0.267		37,177
	19	71,190	141,013	0.247		34,830
	20	72,086	142,788	0.229		32,698
	21	72,982	144,563	0.213		30,744
	22	73,878	146,338	0.197		28,829
	23	74,774	148,112	0.183		27,105
	24	75,670	149,887	0.170		25,481
2011	25	76,566	151,662	0.157		23,811

Total Present Value Development Cost - Cherry Point

\$ 1,374,128

* Escalation from 1977 to 1987 = $\frac{2684}{1355}$ = 1.9808



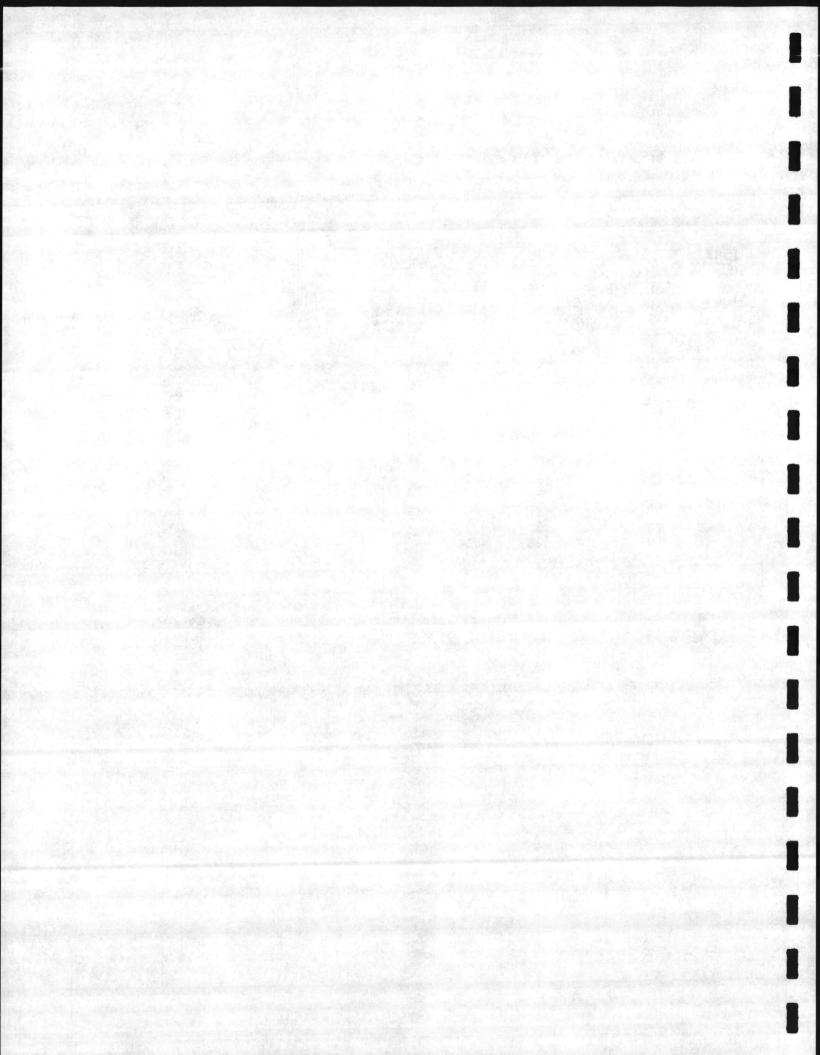
	Yr. of Op.	1977\$*	1987\$*	10% Discount (2% differential)	Present Value
1987	1	\$ 215,809	\$ 427,477	.963	\$ 411,660
1907	2	217,609	431,042	.893	384,921
	3	219,157	434,109	.828	359,442
1990	3 4	220,956	437,672	.768	336,132
	5	222,505	440,741	.712	313,808
	5 6	224,304	444,304	.660	293,241
	7	223,732	443,171	.612	271,221
	8	225,532	446,736	.568	253,746
	9	227,331	450,300	.526	236,858
	10	228,879	453,366	.488	221,243
	11	230,679	456,932	.453	206,990
	12	230,107	455,799	.420	191,436
	13	231,906	459,362	.389	178,692
2000	14	233,706	462,928	.361	167,117
	15	233,134	461,795	.335	154,701
	16	234,933	465,358	.310	144,261
	17	236,481	468,424	.288	134,906
	18	238,281	471,990	.267	126,021
	19	240,080	475,553	.247	117,462
	20	241,629	478,622	.229	109,604
	21	243,428	482,185	.213	102,705
	22	242,856	481,052	.197	94,767
	23	244,655	484,616	.183	88,685
	24	246,204	487,684	.170	82,906
2011	. 25	248,003	491,247	.157	71,126

b. Annual Incremental Landfill Development Cost - Camp Lejeune

Total Present Value Development Costs - Camp Lejeune

\$ 5,053,651

* Escalation from 1977 to 1987 = $\frac{2684}{1355}$ = 1.9808



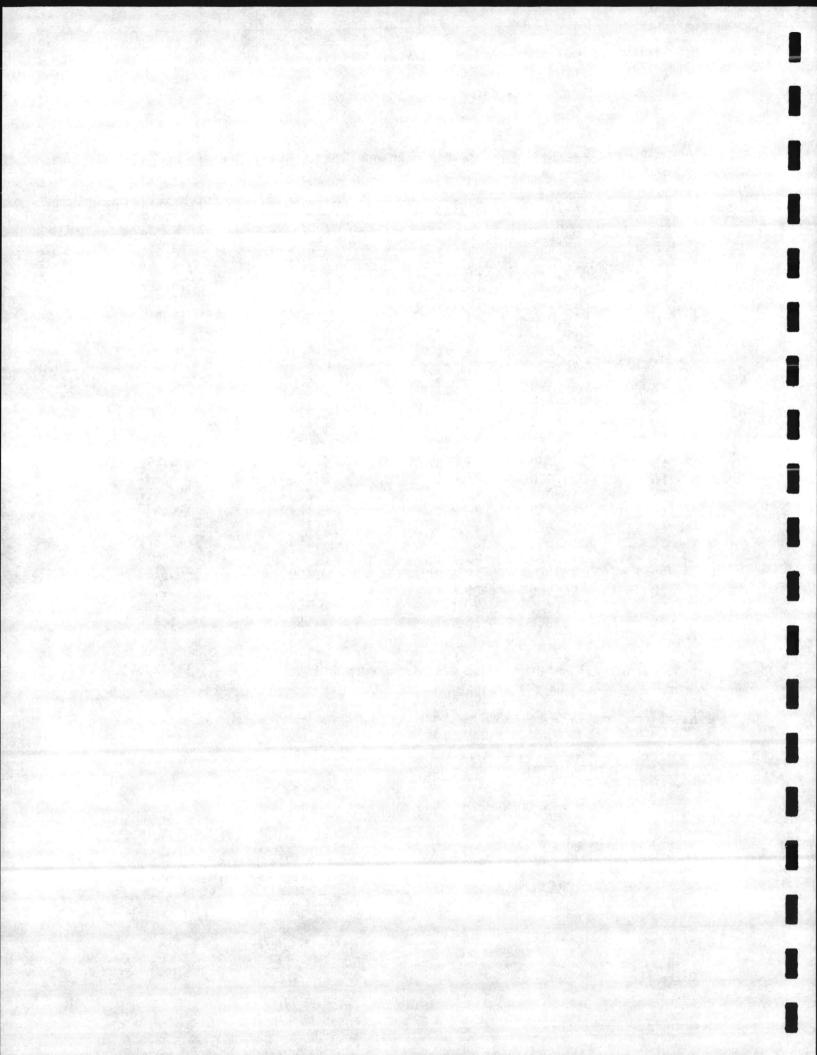
Year	Yr. of Op.	1977\$*	1987\$*	10% Discount (0% differential)	Present Value
1987	1	\$ 9,520	\$ 18,857	0.954	\$ 17,990
		9,680	19,174	0.867	16,624
	2 3	9,840	19,491	0.788	15,359
1990	4	10,000	19,808	0.717	14,202
		10,160	20,125	0.652	13,122
	5 6 7	10,230	20,442	0.592	11.914
		10,480	20,759	0.538	11,168
	8 9	10,640	21,076	0.489	10,306
	9	10,800	21,393	0.445	9,520
	10	10,960	21,710	0.405	8,793
	11	11,120	22,027	0.368	8,106
	12	11,280	22,343	0.334	7,463
	13	11,440	22,660	0.304	6,889
2000	14	11,600	22,977	0.276	6,342
	15	11,760	23,294	0.251	5,847
	16	11,920	23,611	0.228	5,383
	17	12,080	23,928	0.208	4,977
	18	12,240	24,245	0.189	4,583
	19	12,400	24,562	0.172	4,225
	20	12,560	24,879	0.156	3,881
	21	12,720	25,196	0.142	3,579
	22	12,880	25,513	0.129	3,292
	23	13,040	25,830	0.117	3,022
	24	13,200	26,147	0.107	1,412
2011	. 25	13,360	26,463	0.097	1,296

c. Annual Incremental Landfill Maintenance Cost - Cherry Point

Total Present Value Maintenance Costs - Cherry Point

\$ 199,295

* Escalation from 1977 to 1987 = $\frac{2684}{1355}$ = 1.9808



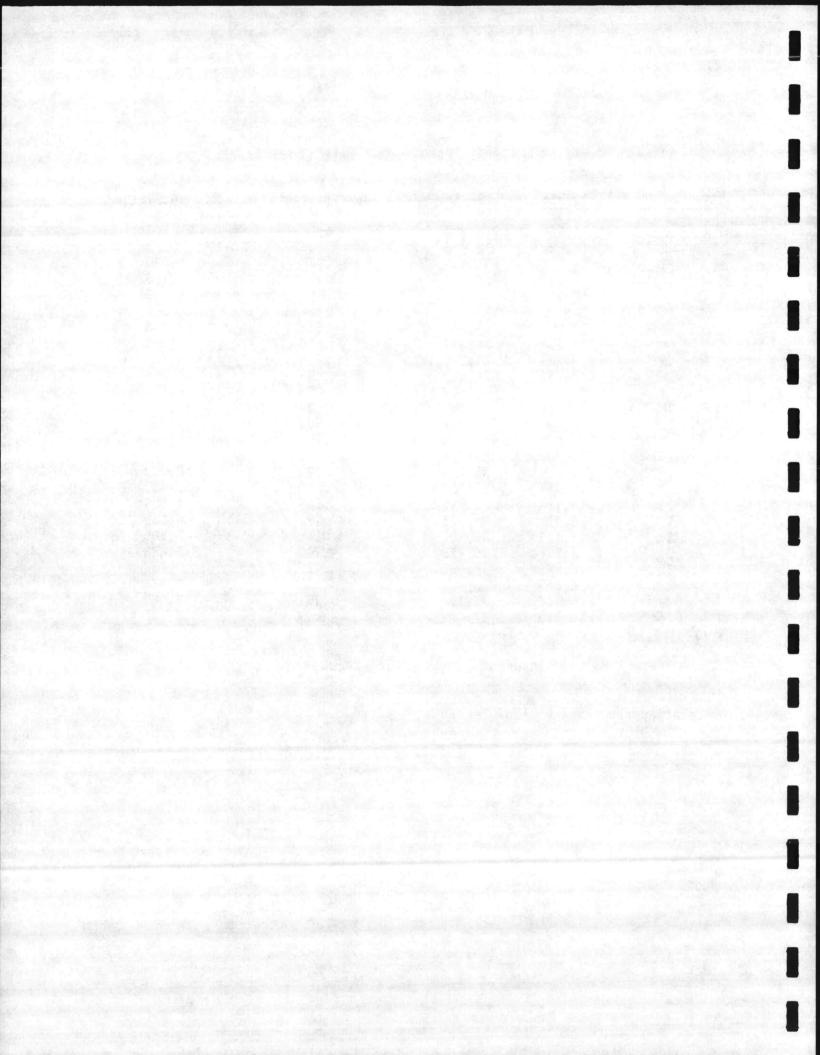
	Yr. of Op.	<u>1977\$*</u>	<u>1987\$*</u>	10% Discount (0% differential)	Present Value
1987	1	\$ 16,460	\$ 32,604	.954	\$ 31,104
	2	16,597	32,876	.867	28,503
	3	16,715	33,109	.788	26,090
1990	4	16,853	33,383	.717	23,936
	5	16,971	33,616	.652	21,918
	6	17,108	33,888	.592	20,062
	7	17,064	33,801	.538	18,185
	8	17,202	34,074	.489	16,662
	9	17,339	34,345	.445	15,284
	10	17,457	34,579	.405	14,004
	11	17,594	34,850	.368	12,825
	12	17,551	34,765	.334	11,612
	13	17,688	35,037	.304	10,651
2000	14	17,825	35,308	.276	9,745
	15	17,781	35,221	.251	8,840
	16	17,919	35,494	.228	8,093
	17	18,037	35,728	.208	7,431
	18	18,174	35,999	.189	6,804
	19	18,311	36,271	.172	6,239
	20	18,429	36,504	.156	5,695
	21	18,567	36,778	.142	5,222
	22	18,523	36,691	.129	4,733
	23	18,660	36,962	.117	4,325
	24	18,778	37,196	.107	3,980
2011	25	18,915	37,467	.097	3,634

d. Annual Incremental Landfill Maintenance Cost - Camp Lejeune

Total Present Value Maintenance Costs - Camp Lejeune

\$ 325,577

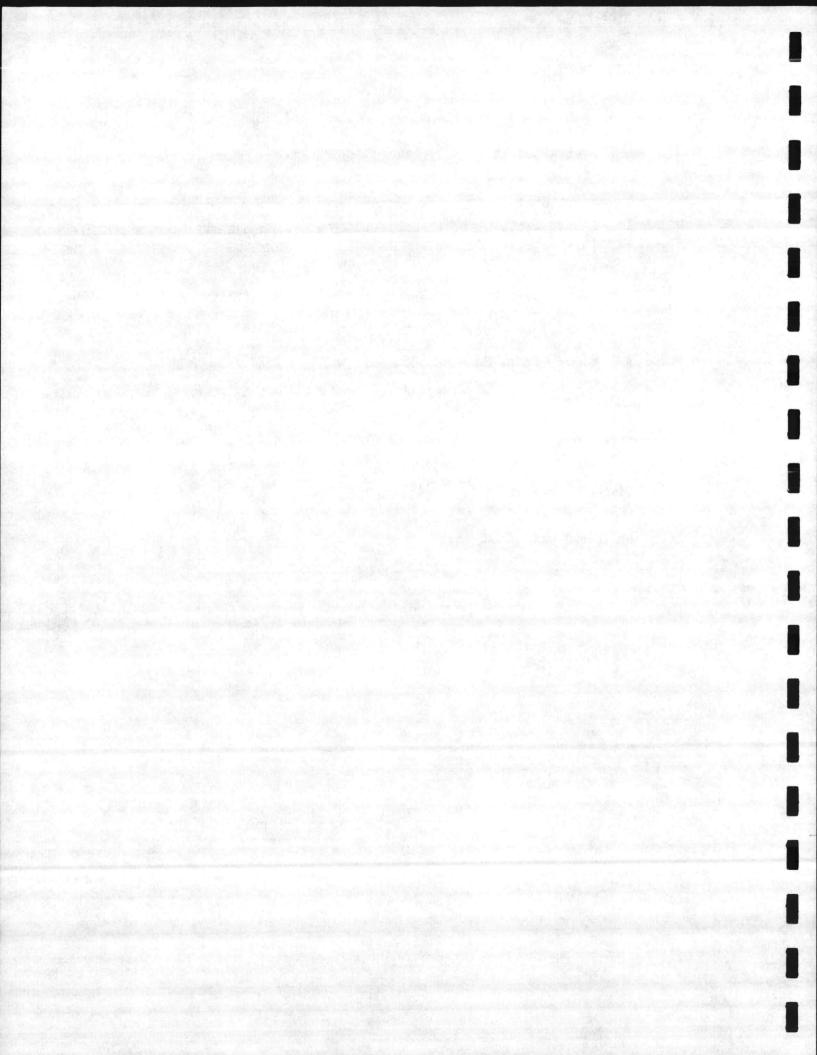
* Escalation from 1977 to 1987 = $\frac{2684}{1355}$ = 1.9808



Summary Sheet	Alternative	3B	-	Total	Present	Valu	e
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Investment Costs

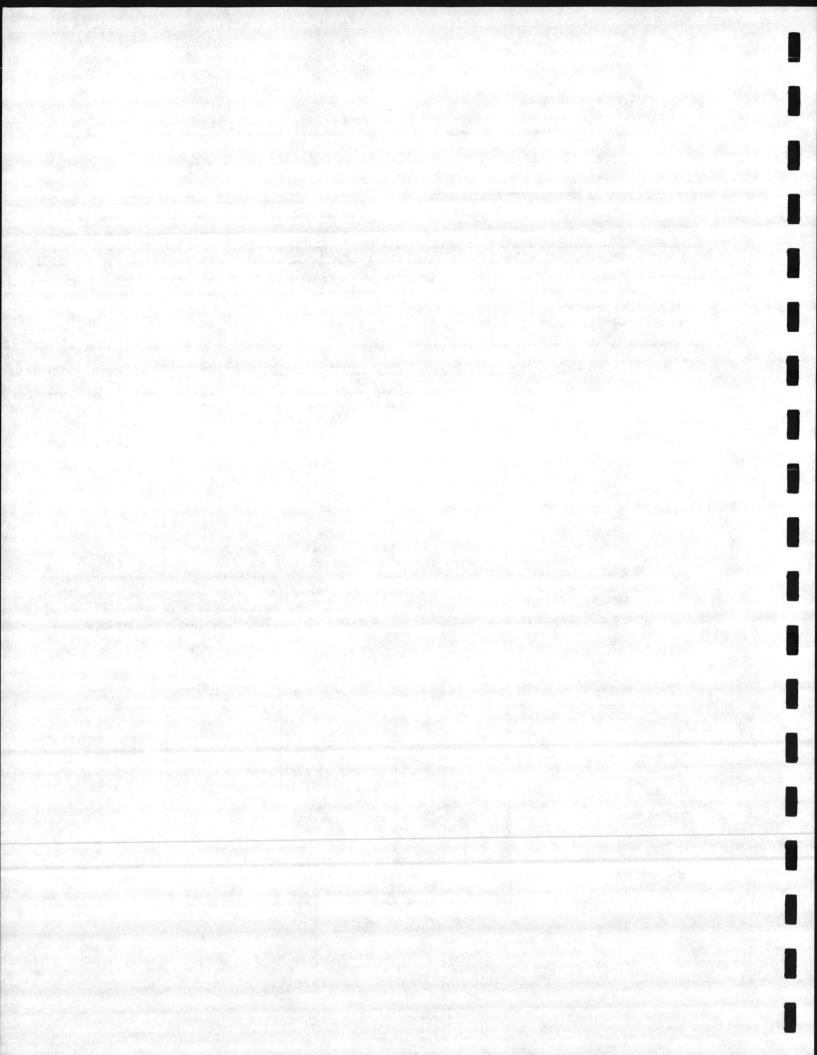
Cherry Point Capital Costs	\$ 496,934
Recurring Costs	
Cherry Point Development	1,374,128
Camp Lejeune Development	5,053,651
Cherry Point Maintenance	199,295
Camp Lejeune Maintenance	325,577
Total Present Value Alternative 3B	\$ 7,449,585
Discount Factor 9.524	
Uniform Annual Cost	\$ 782,191



VII-24

DNOMIC ANALYSIS OF SHORE FACI			DATE	March 1982
Refuse Plant, Camp Lej	eune. N. C.	tedar - ser - so dilles	and the second second	Arren and a subset of
PROJECT TITLE			P	NQ.
Design Analysis (Fy 87)		A Constant of the	
Case 3				and the state of the
Lase 3	A PARTY AND A PART		Contraction of the second	
A. Refuse Plant - Ele	ctricity with Co	indensing Turb	Dine	
B. Landfill			the second s	
PROJECT COST PROJECTIONS BY	ALTERNATIVES			a Alter Longerst
ALTERNATIVE & Refuse Plan	t - Electricity	w/Condensing	Turbine LIFE	міс 25 те
DESCRIPTION AND YEAR	COSTS ONE TIME	(S) RECURRING	DISCOUNT FACTOR	PRESENT VALUE (S)
INVESTMENT				
OPERATIONS				
HAINTENANCE			A strange the second	
PER SORNEL				the there a
TERMINAL VALUE	· · ··································			
OTHER:				
TOTAL PRESENT VALUE ALTERNAT	1 8.2	16,527 ÷	SCOUNT FACTOR 9.524 =	UNIFORM ANNUAL CO 862,718
			<u> </u>	
ALTERNATIVE 3 Lanc	ifill		ECOXON	IIC 25 TRS.
	1 1 COST3		LIFE	1/3.
DESCRIPTION AND YEAR				PRESENT VALUE (S)
DESCRIPTION AND YEAR	COSTS	(\$)	DISCOUNT	PRESENT
DESCRIPTION AND YEAR	COSTS	(\$)	DISCOUNT	PRESENT
DESCRIPTION AND YEAR INVESTMENT OPERATIONS	COSTS	(\$)	DISCOUNT	PRESENT
DESCRIPTION AND YEAR INVESTMENT OPERATIONS MAINTENANCE	COSTS	(\$)	DISCOUNT	PRESENT
	COSTS	(\$)	DISCOUNT	PRESENT
DESCRIPTION AND YEAR INVESTMENT OPERATIONS MAINTENANCE PERSONNEL TERMINAL YALUE	COSTS	(\$)	DISCOUNT	PRESENT
DESCRIPTION AND YEAR INVESTMENT OPERATIONS MAINTENANCS PERSONNEL	COSTS ONE TIME	(S) RECURAING	DISCOUNT	PRESENT

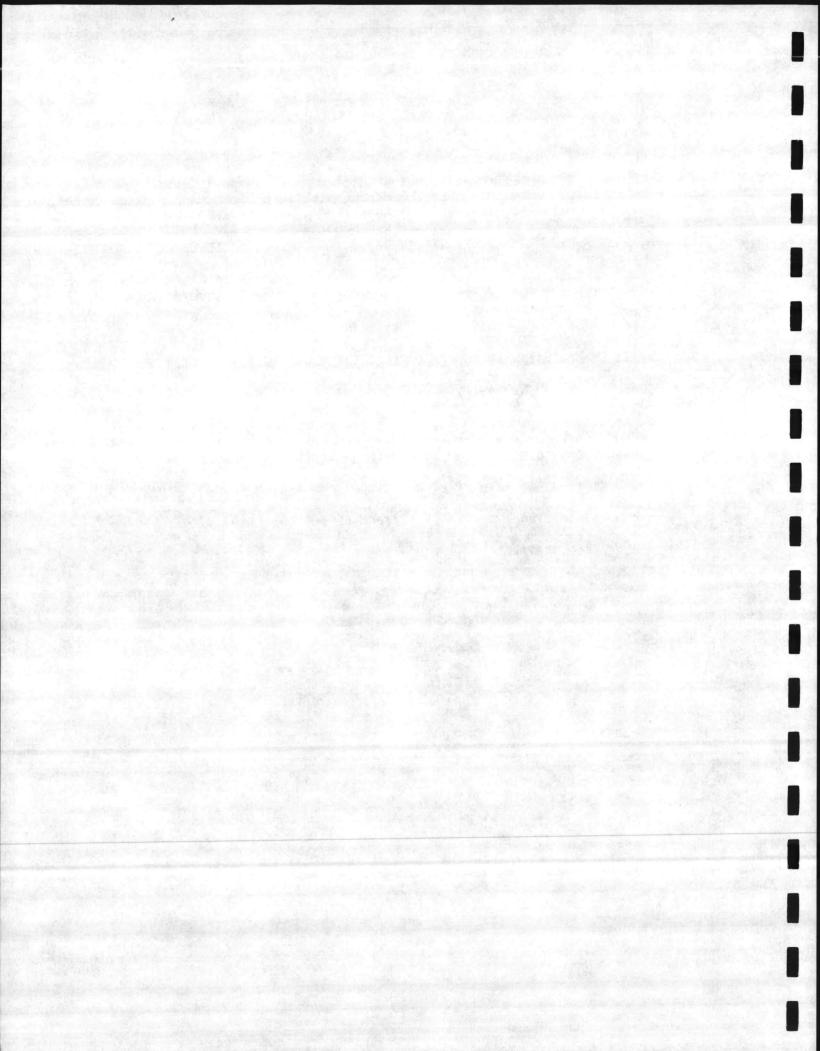
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Analysis

	Total Present Value Cost	Uniform Annual Cost		
Case 3A	\$ 8,216,527	\$ 862,718		
Case 3B	7,449,585	782,191		
Difference	766,942	80,527		

This is the only one of three cases where the least expensive alternative is to continue with existing operations rather than build the refuse plant. The present value cost difference is \$766,942 or \$80,527 per year. The major reason for this difference is that no oil-generated steam is replaced by the refuse plant. The steam in this case is used solely to generate electricity and the revenues from the sale of electricity are not high enough to pay back the additional capital costs and offset the price of oil used to generate steam.



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SECTION VIII

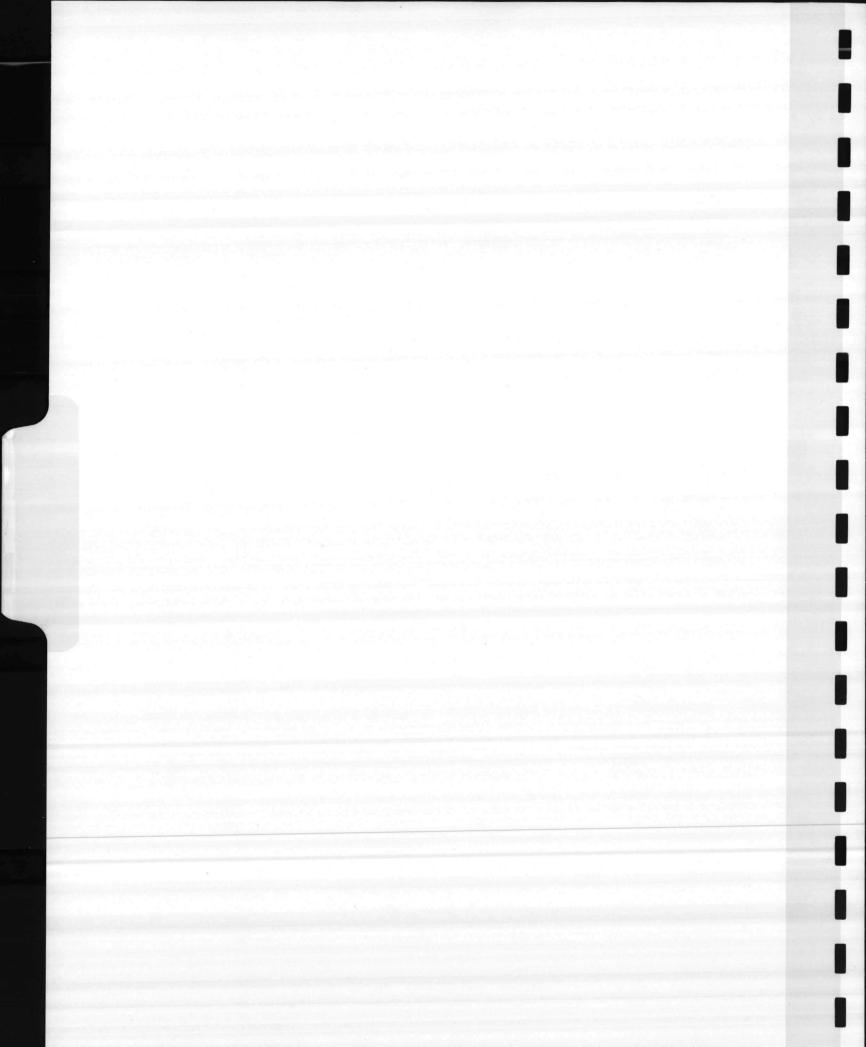
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Section VIII



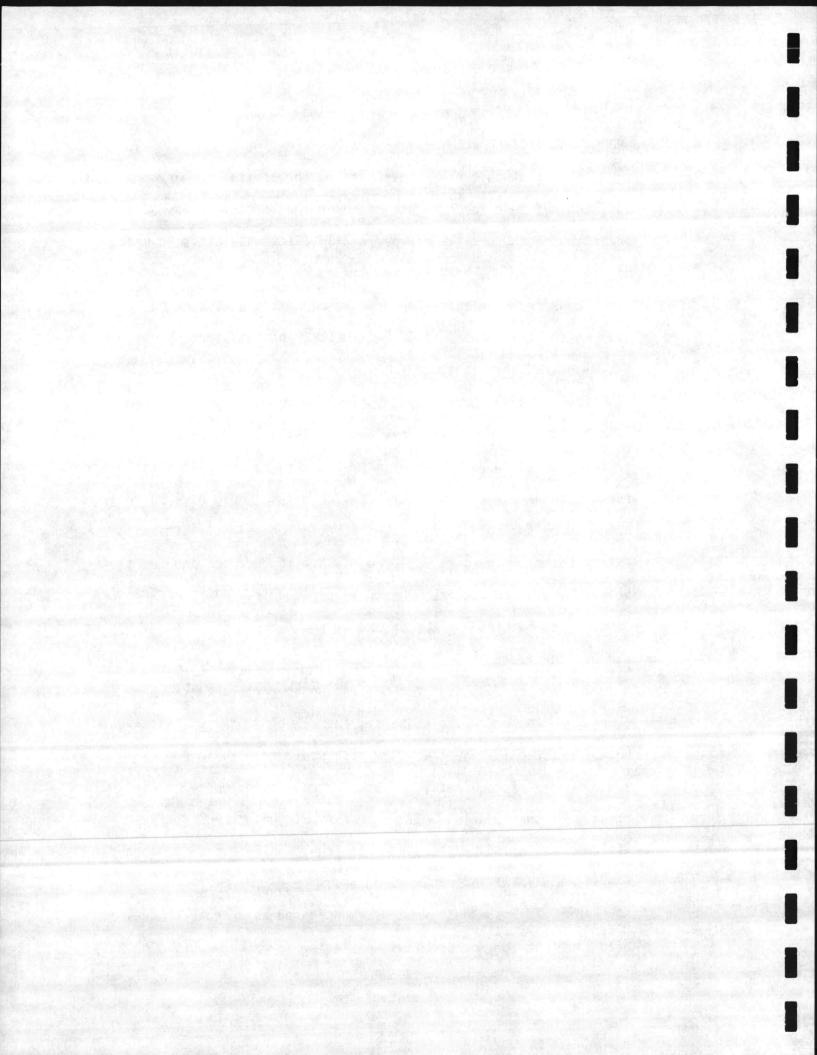
VIII. WOOD-FIRED BOILER PLANT

Phase I of this study investigated the possibility of combining wood and refuse to produce steam and/or electricity. Phase I also investigated the details of wood availability and cost, including manpower, chipping, handling and transportation. However, after close consideration there appeared to be little advantage for the Navy in combining the fuels. Equipment compatibility problems are the major reason.

The equipment compatibility problems in combining wood and refuse arise in the boiler feed and burning systems. A boiler designed to use wood as the primary fuel and refuse as the secondary fuel would have a traveling grate. The refuse would have to be prepared by shreading, magnetic separation and air classification. This treated solid waste would be mixed with the wood and fed to the boiler by a screw feeder. Due to high electrical cost, and frequent maintenance required by the shredding equipment, this type of system was not considered for this project.

The boilers proposed for the refuse energy plant are mass burning incinerator-type stokers. The mix of wood and refuse would be very critical. The crane operator would have to insure an adequate mix of wood/refuse. Too much wood fired on the grate would create hot spots, which would increase maintenance and decrease the system availability. Also, the wood fuel would have to be hogged to a maximum size of less than 4 inches.

Another reason that wood was considered as a separate fuel is because of the policy problems that arise in procurement. The Navy

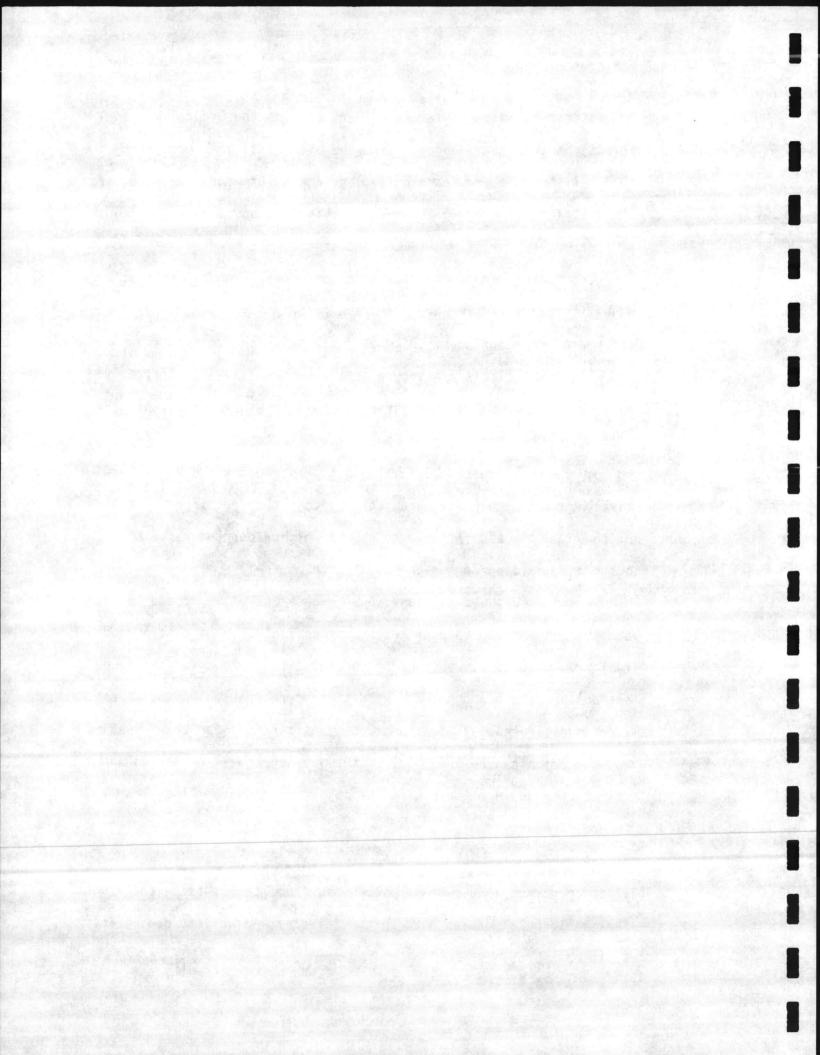


requested that only federal land (Marine bases and Croatan National Forest) be considered to determine the availability of wood for fuel. Although there was a sufficient amount of wood available (see Phase I, Interim Report) the cost of this fuel could be high because of restrictive forest management practices.

The forest management practices on federal land are so that wildlife and recreation are given a high priority. Logging residues which are the major source of wood fuel, are often used in windrows for wildlife habitats. Also, selective thinnings are preferred over clear cuts. If wood is harvested for fuel, the number of tons harvested per hour must be high, because the cost per ton must be low to compete with other fuels. If small, wastewood trees are selectively thinned, this high productivity cannot be obtained. The price of wood would increase to pay for higher per ton harvesting costs and would no longer be competitive as fuel.

If wood fuel was purchased on the open market, it could be obtained at a reasonable price. Most contract loggers obtain wood fuel from private timber owners who manage their land for the highest dollar return and not for wildlife and recreation. Since these lands are clearcut, a high number of tons per hour can be harvested, and the price can be low. But if the Navy purchases on the open market they would be defeating the objective of using trees from federal property.

Another policy problem in procurement could arise in Naval interdepartmental accounting procedures. How the costs of the wood fuel would be allocated between the forestry and utility departments could be a problem.



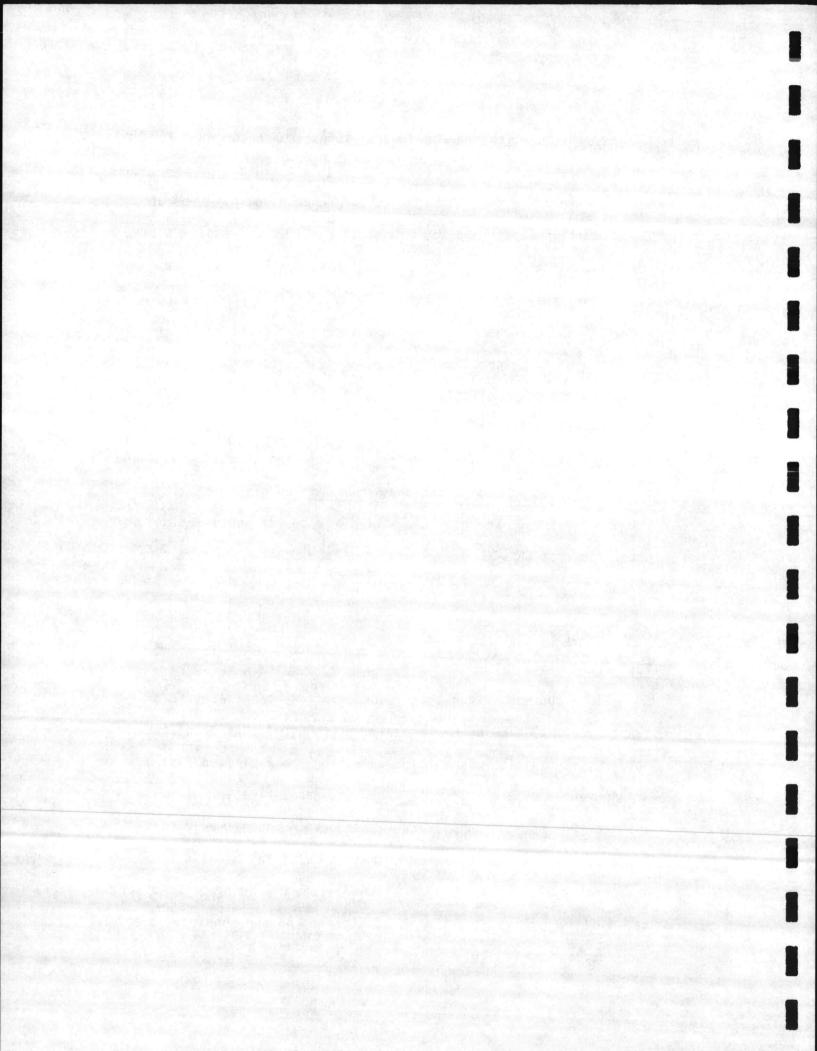
For instance, the reason federal forests were targeted for wood fuel use was so that a stumpage fee could be avoided. However, the base foresters use the stumpage fee for revenues to pay much of their operating costs and would hope to continue to receive those revenues. If the Utilities Department must add the cost of stumpage to the fuel they buy from federal lands, then fuel from the open market might be a better buy because production costs are lower.

None of these problems is impossible to overcome. However, to determine the most reliable and cost-effective installation for this study it was elected to handle the fuels in separate systems. Since disposing of the refuse is a major consideration of this study, and its cost is considerably less than wood, it was given priority as the primary fuel. Therefore, a wood-fired boiler installation, for the purpose of this study, was treated as a "battery limit" type concept.

Plant Description

Fuel Feed

Since the wood fired boiler installation was treated as a "battery limit" type concept, equipment required outside of the boiler system limits was not included. On the fuel feed system, nothing ahead of the boiler feed hoppers was estimated. It was assumed that no wood chips larger than 3 to 4 inches would be fed to the hoppers. It should be noted that the material handling equipment could become a major expense item, depending on what form the wood is received in, how it is stored, and the sophistication of the feed system design.



VIII-4

Boiler

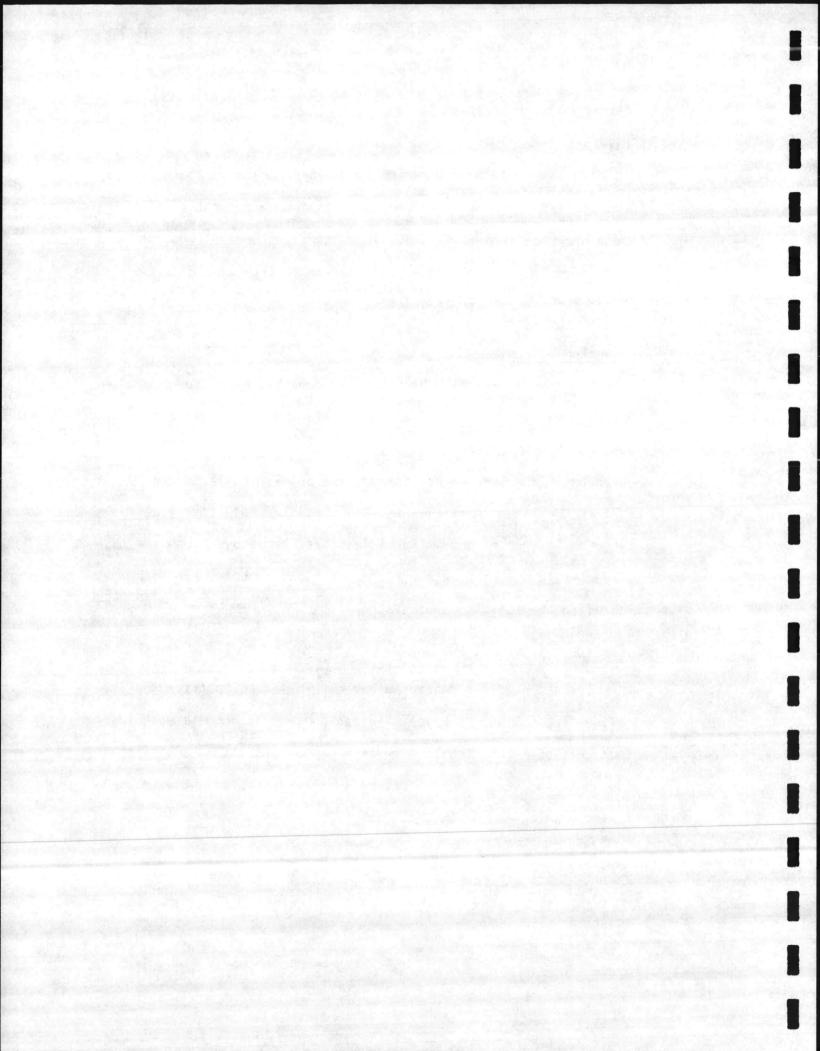
Two boilers, each rated at 30,000 lb/hr maximum output, would be installed for burning wood having a moisture content of 45-55% and a heating value of 4500 Btu/lb as fired. The fuel would be fed by a pneumatic spreader to a stationary grate stoker. The power plant concept would be identical to that shown on Drawing MF1.

Pollution Control

It is expected that the particulate matter pollution limit would be met through use of a mechanical-type dust collector on each boiler. A primary and secondary collector would be installed upstream of the induced draft fan. The primary collector would collect the larger particles and the secondary collecter would capture the smaller ones. Particles that are removed from the gas stream would drop out into a hopper, through a rotary air lock valve, to the ash discharge system.

Ash Handling

The ash handling concept would be similar to that for the refuse fired plant. However, the ash content of wood is much lower than that of refuse fuel. A maximum range of 3 -5% is anticipated. The equipment sizing would be smaller than depicted in the refuse firing plant.



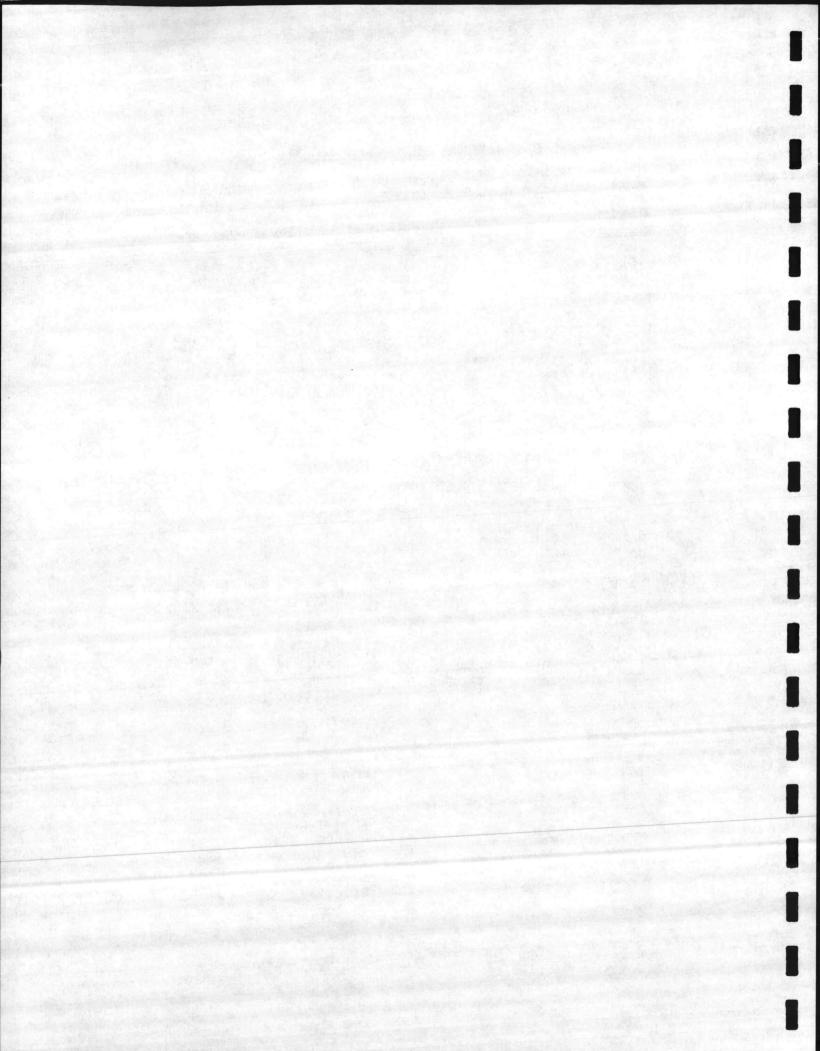
Cost Estimate

DEPARTMENT DIRECT COST SUMMARY

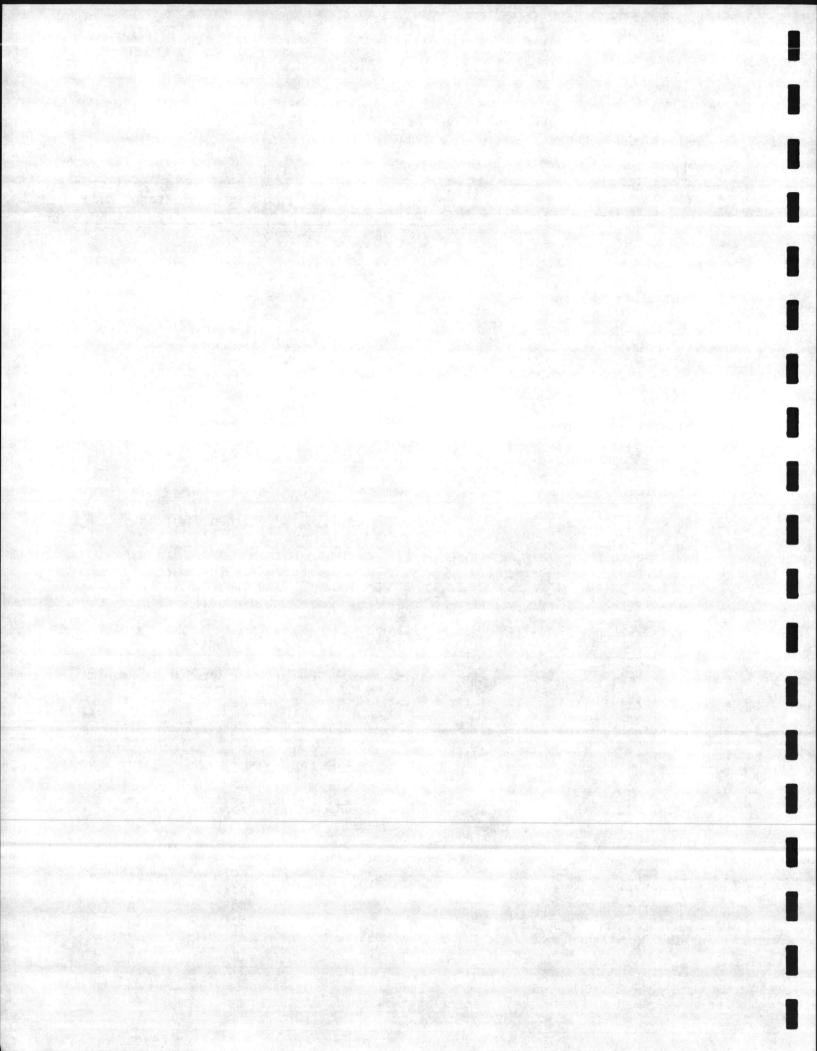
WOOD FIRING

Equipment	\$	2,603,500	
Equipment Erection		62,500	
Equipment Foundations and Other Cost		213,100	
Buidings & Structures		920,000	
Electrical Installation Cost		240,000	
Instrumentation Installation Cost		200,000	
Piping Cost		740,000	
Area Cost	_	130,000	
SUBTOTAL CONSTRUCTION COST			\$ 5,109,100
SIOH @ 5.5% (Supervision, inspection & overhead)			281,000
Contingency @ 10%			539,000
TOTAL CONSTRUCTION COST			\$ 5,929,100

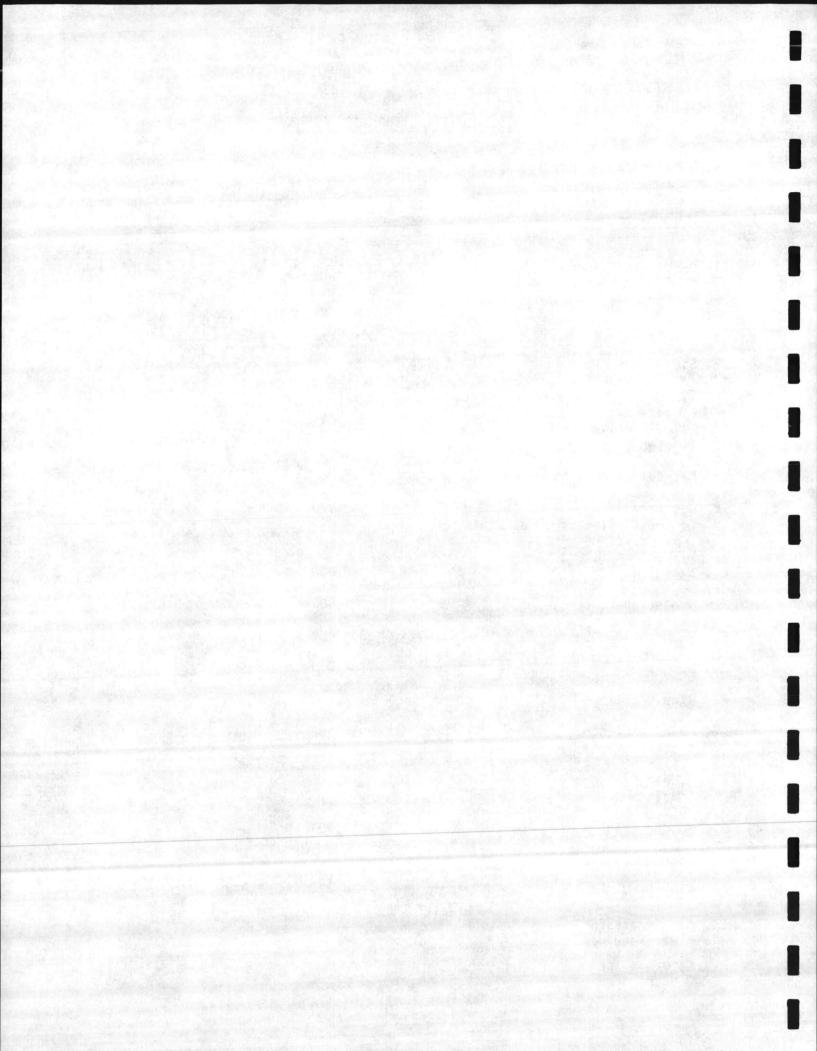
This estimate does not include equipment for fuel preparation and handling or any site specific cost items. NOTE:



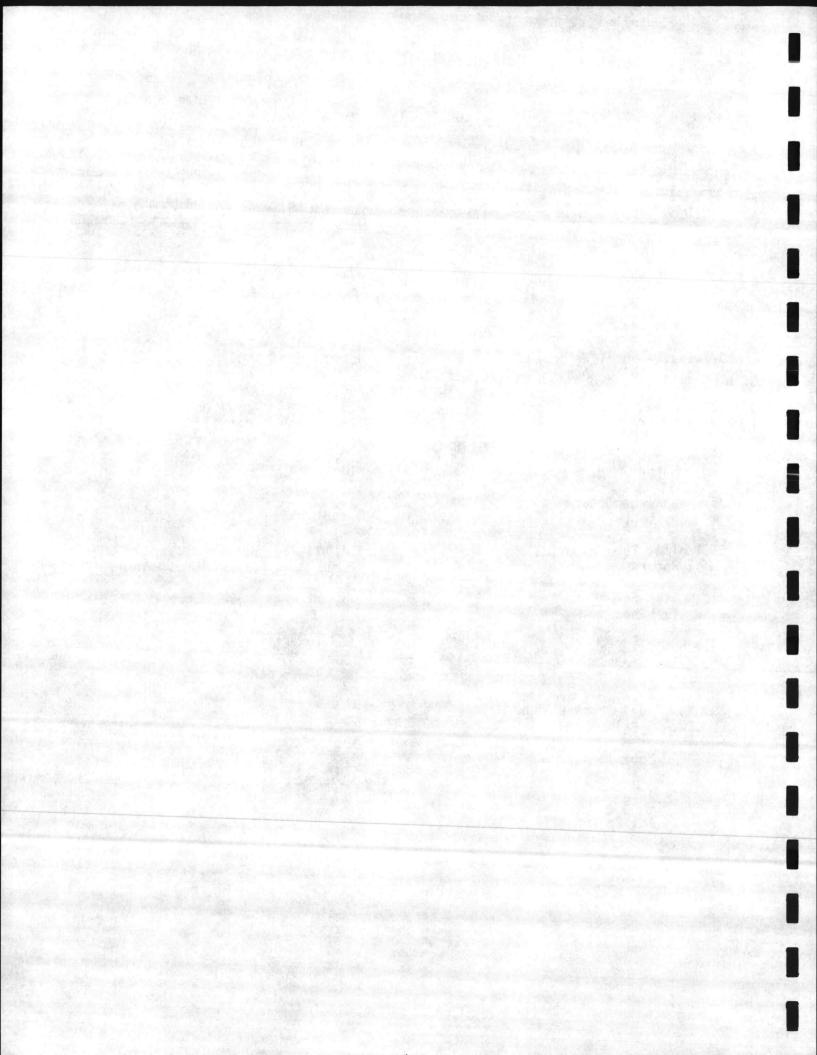
	IPMENT LIST D PLANT Item Description	Motor HP-RPM	Equipment \$	Equipment Erection \$	Equip. Supports Platforms and Other Costs \$
1.	Boiler, 30,000 Lb/Hr Capacity 250 psig Design Pressure Unit No. 1		750,000	w/Equipment	w/Bldg. Cost
2.	F.D. Fan Coupling Controls Motor Intake Silencer	50	Incl. Incl. Incl. Incl. Incl.	w/Equipment w/Equipment w/Equipment w/Equipment w/Equipment	
3.	Combustion Controls		Incl.	w/Equipment	
4.	Boiler Breeching		Incl.	w/Equipment	w/Bldg.
5.	Economizer		Incl.	w/Equipment	w/Bldg.
6.	Stoker		Incl.	w/Equipment	w/Boiler
7.	I.D. Fan Coupling Fluid Drive Motor	75	Incl. Incl. Incl. Incl.	w/Equipment w/Equipment w/Equipment w/Equipment	
8.	Mechanical Dust Collector		75,000	20,000	7,000
9.	Ductwork - To Dust Collector, Fan, Stack w/Insulation		35,000	D&E	40,000
10.	Expansion Joints		12,000	2,000	N/A
11.	Isolation Damper	5	28,000	2,000	Incl.
12.	Boiler, 30,000 Lb/Hr Capacity 250 psig Design Pressure Unit No. 2		750,000	w/Equip. Co	ost w/Bldg.
13.	F.D. Fan Coupling Controls Motor Intake Silencer	50	Incl. Incl. Incl. Incl. Incl.	Incl. Incl. Incl. Incl. Incl.	4,000 Incl. Incl. Incl. Incl.



	IPMENT_LIST D_PLANT Item Description	Motor HP-RPM	Equipment	Equipment Erection	Equip. Supports Platforms and Other Costs
		<u>HF-KFH</u>	\$	\$	\$
14.	Combustion Controls		Incl.	Incl.	
15.	Boiler Breeching		Incl.	Incl.	w/Bldg.
16.	Economizer		Incl.	Incl.	w/Bldg.
17.	Stoker		Incl.	Incl.	w/Boiler
18.	I.D. Fan Coupling Fluid Drive Motor	75	Incl. Incl. Incl. Incl.	Incl. Incl. Incl. Incl.	7,000
19.	Mechanical Dust Collector		75,000	20,000	7,000
20.	Ductwork - To Dust Collector, Fan, Stack w/Insulation		35,000	D&E	40,000
21.	Expansion Joints		12,000	2,000	N/A
22.	Isolation Damper	5	28,000	2,000	N/A
23.	Ash Handling System	50 (Total)	300,000	Incl.	w/Bldg.
24.	Deaerator		30,000	2,000	1,500
25.	Blow-Off Tank		5,000	1,000	100
26.	Continuous Blowdown		16,500	2,500	500
	System Flash Tank Heat Exchanger Valves		Incl. Incl. Incl.	Incl. Incl. Incl.	
27.	Condensate Tank		15,000	1,000	100
28.	Condensate Transfer Pump Motor	10	3,000 Incl.	500 500	200 200
29.	Air Compressor Air Receiver	25	6,000 Incl.	500	200

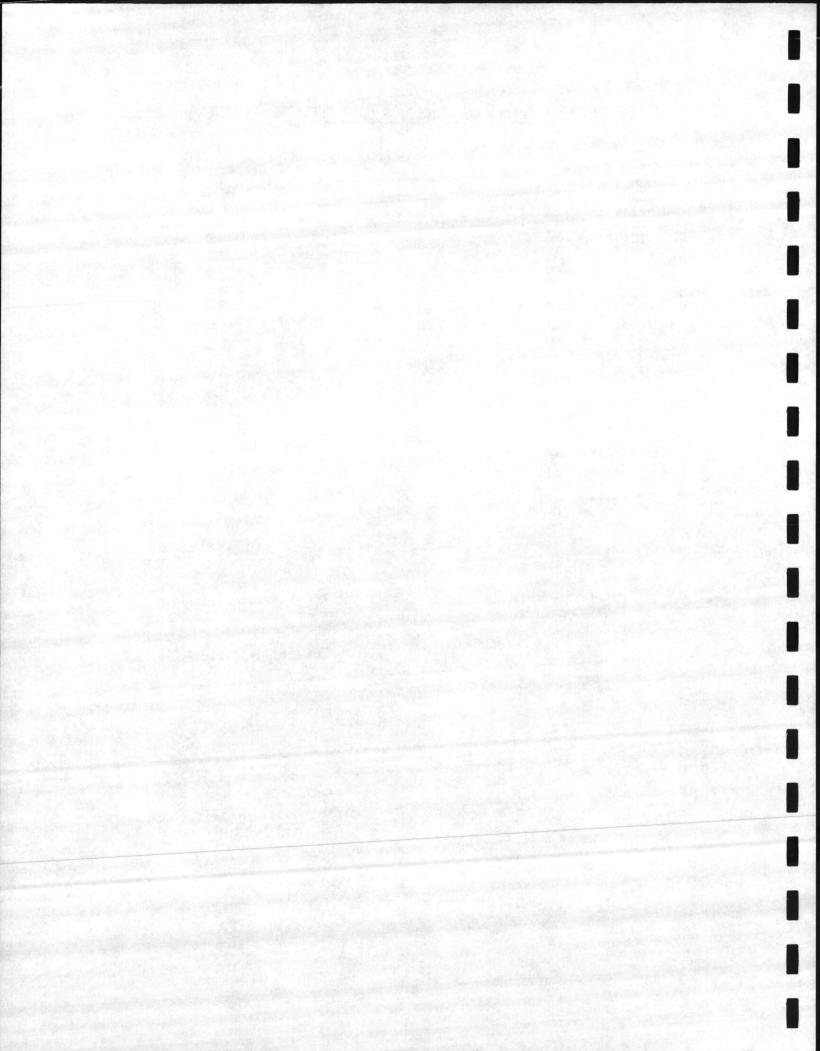


	IPMENT_LIST D_PLANT	Motor		Equipment	Equip. Supports Platforms and
	Item Description	HP-RPM	Equipment \$		Other Costs
30.	Air Compressor Air Receiver	25	6,000 Incl.	500	200
31.	Air Dryer		3,000	200	100
32.	Stack - Dual Wall (2) 150' x 9'-0" Dia.		310,000	Incl.	40,000
33.	Raw Water Booster Pump Motor	20	3,000 Incl.	500 Incl.	100 Incl.
34.	Raw Water Booster Pump Motor	20	3,000 Incl.	500	100
35.	Feedwater Treatment Equipment	30 Total	35,000	2,000	1,000
36.	Boiler Feed Pump (2) Motor	2 @ 50	10,000 Incl.	1,000 Incl.	1,000 Incl.
37.	Boiler Feed Pump Turbine		5,000 8,000	500 Incl.	500 Incl.
38.	Chemical Feed Equipment	2 @ 5	5,000	800	300
39.	No. 2 Oil Storage Tank 10,000 Gallon		25,000	500	500
40.	HVAC Equipment	20	15,000	Incl.	500
	TOTAL, Equipment	\$	2,603,500	\$ 62,500	\$ 213,100



WOOD PLANT

41.	Buildings and Structures		
	Structural Steel Mat Piping Roof Deck and Roofing Walls and Siding Intermediate Floors Stairs, Doors and Drains Miscellaneous Steel and Grating Support Steel and Miscellaneous	300,000 150,000 50,000 90,000 100,000 30,000 50,000 50,000 100,000	
	TOTAL, Buildings and Structures	\$ 920,000	
42.	Electrical Building Lighting Electrical Equipment & Wiring	\$ 40,000 200,000	
	TOTAL, Electrical	\$ 240,000	
43.	Instrumentation	\$ 200,000	
44.	Piping Boiler Plant	\$ 740,000	
45.	Area	\$ 130,000	



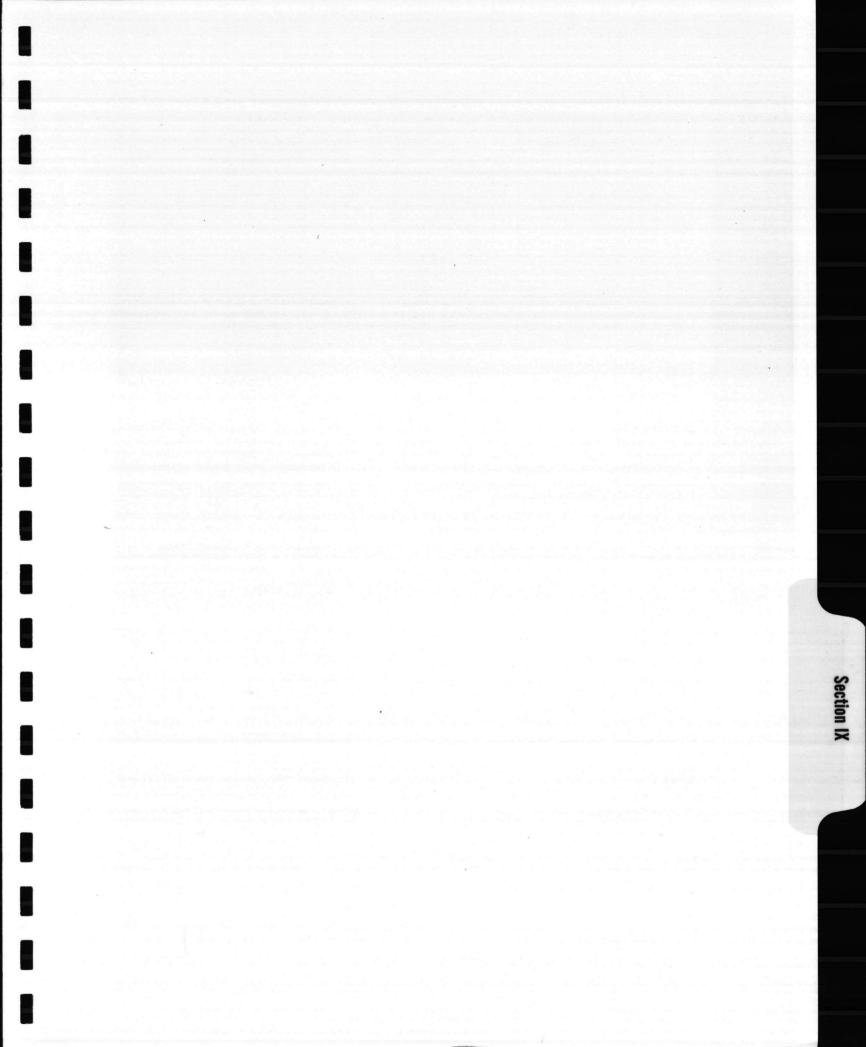
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IX. CONCLUSIONS AND RECOMMENDATIONS

Case Comparisons

Table 6 summarizes the capital costs, present values, and uniform annual costs of the three refuse plant case options. The table also points out the total and annual savings that could be realized if the refuse plant in that case is constructed.

In absolute numbers, the most savings, \$75.9 million, can be realized if refuse is burned to generate steam and electricity (Case 2A). However, the savings that can be realized if only steam is generated (Case 1A) are only slightly less, \$74.2 million. There is a net cost and no savings to be realized if only electricity is generated (Case 3A).

The difference in savings between generating just steam or steam and electricity is only \$1.7 million total project present value or \$176,000 per year. This difference is only about 2% of the savings in either case. The other tangible factor that can be compared is the construction cost. The construction cost of the steam only case is \$15.5 million and of the steam and electricity case is \$19.1 million, a difference of \$3.6 million. However, this difference is offset by the additional electricity revenue benefits in Case 2A. Considering the level of both the construction and operating cost estimates, these two cases are virtually equal.

Sensitivities to Critical Costs

<u>Price of oil</u> - At \$5.92 per MMBtu, this price equates to approximately \$.88 per gallon of No. 6 fuel oil. In recent months the price of oil has been dropping. Since this is the major factor in determining the amount of the savings for the refuse plant, the

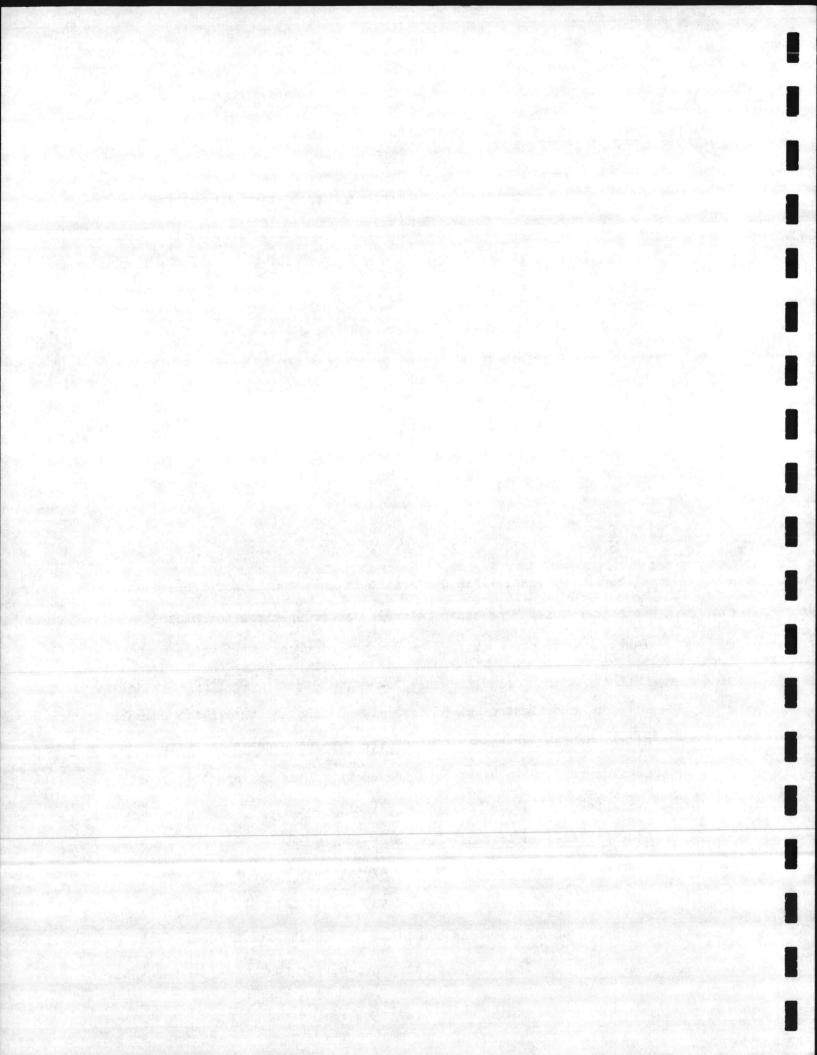
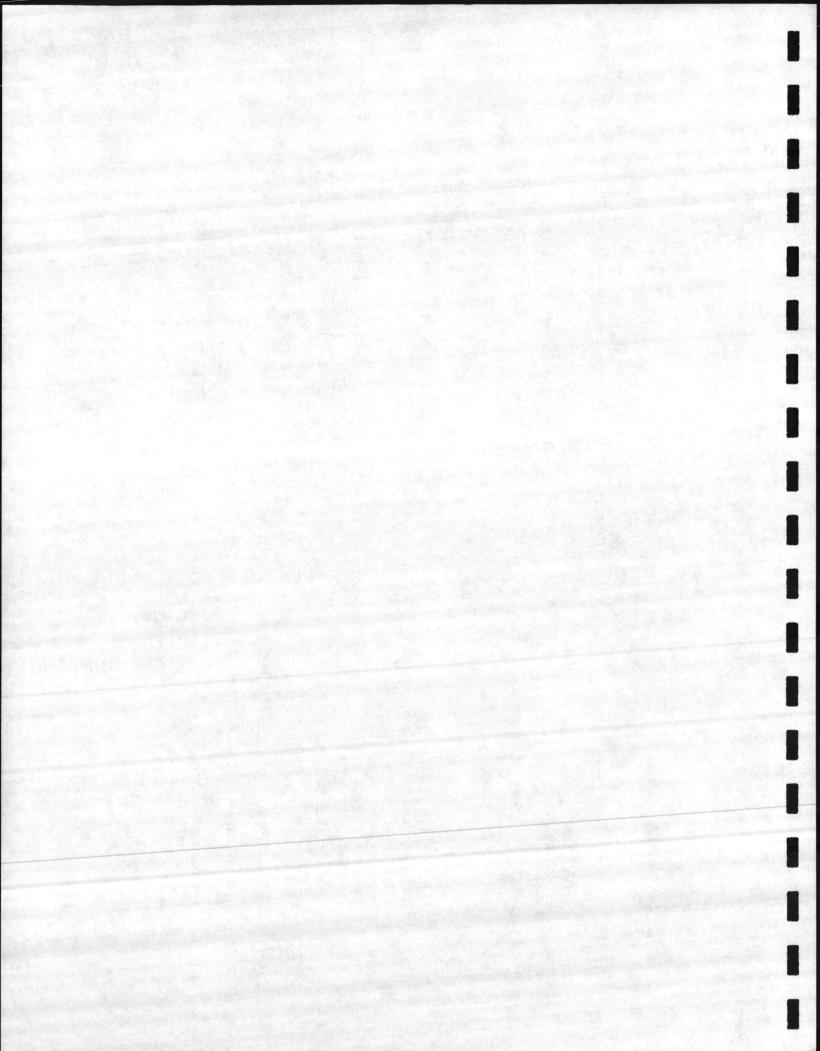


TABLE 6 COST SUMMARY DESIGN ANALYSIS (FY87)

	Construction Costs (1982 \$)	Total Project Cost Present Value	Total Refuse Plant Savings	Uniform Annual Cost	Annual Refuse Plant Savings
Case 1A - Refuse-fired p producing stea only		37,728,374	74,241,165	3,961,400	7,795,166
Case 1B - Incremental co landfill for r and oil for st	refuse	111,969,539		11,756,566	
Case 2A - Refuse-fired p producing stea electricity wi	am and ith a	34,030,099	75,918,667	3,573,089	7,971,301
backpressure t Case 2B - Incremental co landfill for r and oil for st	ost of refuse	109,948,766		11,544,390	
Case 3A - Refuse-fired p producing elec with a condens turbine	tricity	8,216,527		862,718	
Case 3B - Incremental co of a landfill	ost of	7,449,585	<766,942>	782,191	<80,527>

IX-2

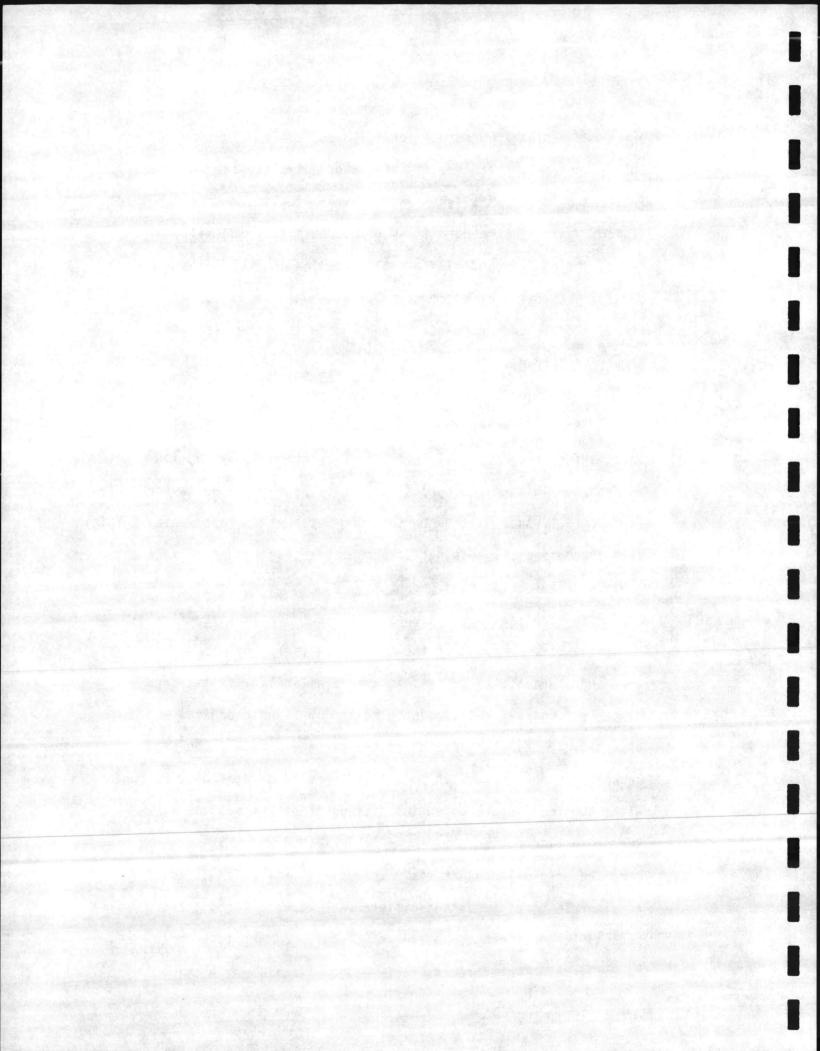


price was set at \$.50 per gallon (\$3.38/MMBtu) and incorporated in the design analysis to see its effect on total project feasibility. This change would still enable the Navy to realize a total project savings over existing conditions of approximately \$34 million, or an annual savings of approximately \$3.5 million in both Cases 1 and 2. Because both cases displace such large amounts of oil generated steam, a decreased price of oil does not affect one case significantly more than another.

<u>Construction costs</u> - This is the largest single cost within each Case option. To determine if a substantial increase in this cost would affect project feasibility, it was increased by 20% for Cases 1A and 2A. This would decrease the total present value savings only approximately \$4.5 million or \$500,000 per year for both Cases. This cost increase still does not affect either case enough to make the savings differential significant.

<u>Plant availability</u> - The assumed plant availability for this report is 80%. Because of the double system (2 boilers, 2 precipitators and spare crane) it is felt this availability is attainable. Of the 20% outage, 15% is scheduled and 5% is unscheduled. Because of the 3-day storage capacity at the garbage pit, and the extra capacity of the boiler, up to 10% unscheduled outage could be handled without effecting the potential savings of either system. Recommendation

The original project cost assumptions reflect a \$1.7 million total present value savings differential between Cases 1 and 2. Cost sensitivities affect the differential only to make it even less significant. Therefore, strictly economics will not provide the

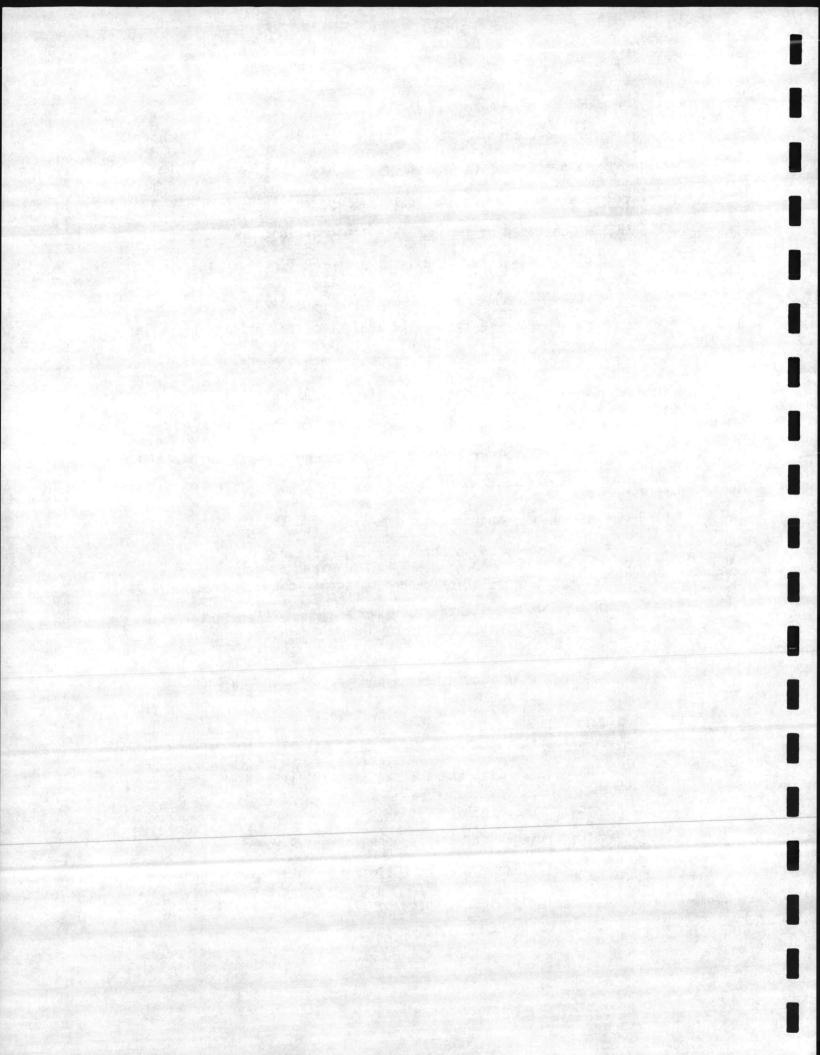


basis for a decision. Because, these tangible economic factors do not prove one case over the other, the Navy must consider the intangible and other policy factors. The following are some of the points which could be important to the decision:

- Boiler tube corrosion is an unproven factor in the cogeneration option. Even though additional maintenance costs have been calculated, the subject of reliability of boiler tubes under the higher pressures and temperatures is controversial among boiler technology experts.
- CP&L is urging all customers with industrial-type boiler projects to seriously consider the possibility of cogeneration. Because of this urgency, they are willing to negotiate the prices and terms of the avoided cost rate schedule. A more favorable position might be obtained.

Several factors which cannot be shown in the economic analysis but which would have a positive influence on either installation are:

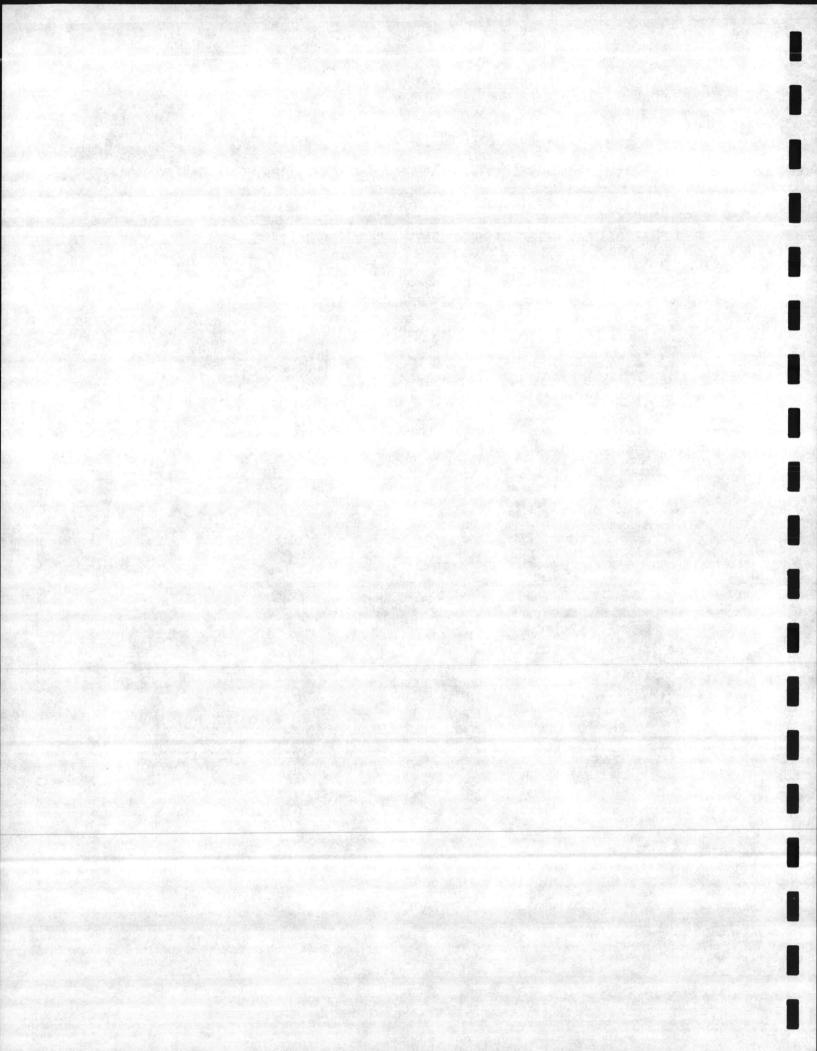
- Either plant would have excess refuse-burning capacity available and a market for excess steam output in the winter.
 During this period a mutually beneficial agreement could be negotiated with the surrounding civilian community for additional trash to burn.
- The project estimate is a conservative one and no value engineering or systems optimization has been attempted.
 Detailed design may produce a lower total installed cost.



- Cherry Point's landfill situation may be approaching a capacity crisis. The refuse energy plant would relieve the potential problem.

A factor which would have a negative influence on either case

- is:
- Any successful steam and condensate conservation program would diminish the benefits derived.



become effective on the date indicated.

Carolina Power & Light Company (North Carolina Only)

COGENERATION AND STALL POWER PRODUCER

SCREDULE CSP-

AVAILABILIT

This Schedule is available for electrical energy and capacity supplied by Seller to Company if Seller is a Qualifying Facility as defined by the Federal Energy Regulatory Commission's (FERC) Order No. 70 under Docket No. EX79-54.

This Schedule is not available for electric service supplied by Company to Seller or for Seller who has negotiated rate credits or conditions which are different from those below. If Seller requires supplemental, standby, or interruptible services, Seller shall enter into a separate service agreement with Company in accordance with Company's applicable electric rates, riders, and Service Regulations on file with and authorized by the state regulatory agency having jurisdiction.

APPLICABILITY

This Schedule is applicable to all electric energy and capacity supplied by Seller to Company at one point of delivery through Company's metering facilities.

CONTRACT CAPACITY

The Contract Capacity shall be the normal maximum dependable capacity of the qualifying facility.

MONTHLY RATE

Pavment

For Qualifying Tacilities classified as New Capacity in accordance with FIEC Order No. 69 under Dockat No. RM79-55, Company will pay Seller a monthly credit equal to the sum of the Energy and Capacity Credits reduced by both the Seller Charge and any applicable Interconnection Cost. For Qualifying Facilities classified as other than New Capacity in accordance with the above FEEC Regulations. Company will pay Seller a monthly credit equal to the Energy Credit reduced by both the Seller Charge and any applicable Interconnection Cost.

Inerty Credit

Company shall pay Seller an Energy Credit for all energy delivered to Company's System as registered or computed from Company's metering facilities. This Energy Credit will be in accordance with the length of rate term for energy sales so established in the Furchase Agreement. The Energy Credit shall be:

	· Variable	Fixed Long-Term Rates		
	Rate	5 .	10 vr.	15 .
On-?eak kin (c/kin)	4.51*	4.93	5.98	7.68
Off-Peak kith (c/kith)	2.92*	3.08	3.62	4.49

#Will be adjusted for Approved Tuel Charges.

Capacity Credit

Company shall pay Seller a Capacity Credit based on the on-peak kith supplied by Seller.

	Fixed Long-Term Rates		
	5 77.	10 .	15 .
On-Peak kith (c/kith)-Summer	2.15	2.15	3.63**
On-Peak kith (c/kith)-Non-summer	1.86	1.86	3.14##

**Applies to Purchase Agreements of 15 years or longer.

Summer months are defined as the calendar months of June through September. Non-summer months are defined as all other months.

Seller Charge

Seller shall pay to Company a Seller Charge outlined below in accordance with the Contract Capacity:

	c	ontract Capacit	7
	0 to	101 20	1000 kW
	100 kW .	999 ku	and above
Monthly Seller Charge	\$5	\$65	\$193

